**Electronic Supplementary Information** 

# One-pot cascade transformation of xylose into γ-valerolactone (GVL) over bifunctional Brønsted-Lewis Zr-Al-Beta zeolite

# 1-Synthesis of materials

Commercial Al-Beta zeolite (2 wt% Al) was purchased from Zeolyst international. Partial dealumination was carried out by treatment in  $HNO_3$  solution in the concentration range 0.1-10 M (room temperature, 1h, 20 mL·g<sup>-1</sup>). Total dealumination was accomplished using more severe conditions (100 °C, 20 h, 20 mL·g<sup>-1</sup>). After filtration and washing with deionized water, the resulting materials were dried overnight (110 °C) before proceeding to Zr incorporation.

Zirconium incorporation was accomplished by impregnation in water suspending the pre-treated Al-Beta zeolite in deionized water followed by the addition of the appropriate amount of zirconium(IV) oxychloride octahydrate (Sigma Aldrich, 99 % w/w). The resultant slurry was heated at 110 °C to distil the water off, dried overnight and calcined in air at 200 °C for 6 h (3 °C·min<sup>-1</sup> heating ramp) and then at 550 °C for another 6 h at the same heating rate.

Four Zr-Al-Beta zeolites were synthesised and named Zr-Al-Beta (x), x denoting their Zr wt. content. The Al free material was denoted Zr-Beta (x).

# 2-Characterization of materials

Zirconium and aluminium content was determined by Inductively Coupled Plasma-Optical Emission Spectroscopy (ICP-OES) with a Varian Vista AX apparatus. Textural properties of the catalyst were evaluated through nitrogen adsorption-desorption isotherms recorded at 77 K, using a Micromeritics Tristar 3000 system. Surface area values were calculated from isotherm data using the B.E.T. method and total pore volume was taken at  $P/P_0 = 0.975$  single points. X-ray powder diffraction (XRD) patterns were collected in a Philips X-pert diffractometer using the Cu K $\alpha$  line in the 2 $\theta$  angle range from 5° to 60° (step size of 0.04°). Structural characterization was completed by transmission electron microscopy (TEM) on a Philips Tecnai-20 electronic microscope operating at 200 kV. Scanning electron microscopy (SEM) images and elemental mapping for Zr, Al and Si were obtained on a Philips XL30 ESEM electronic microscope operating at 3.5 kV.

Acidity was measured by temperature programmed desorption of NH<sub>3</sub> in a Micromeritics 2910 (TPD/TPR) equipment fitted with a TCD detector. Fourier Transform Infra-red (FTIR) spectra were collected in a Varian Excalibur Series 3100 apparatus (400-4000 cm<sup>-1</sup>, 4 cm<sup>-1</sup>, resolution, 64 scans). For the ex-situ pyridine adsorption, samples were exposed to pyridine vapour overnight. Diffuse Reflectance Infra-red Fourier Transform (DRIFT) spectra were recorded using a Nicolet Avatar 370 MCT equipment.

X-ray Photoelectron Spectroscopy (XPS) measurements were obtained using a Specs Phoibos 150 9MCD photoelectron spectrometer.

## **3-Catalytic tests**

Catalytic runs were performed under the following reaction conditions: catalyst 0.01  $g \cdot mL^{-1}$ , substrate: 2-propanol (Scharlab 98 % w/w) molar ratio 1:50, substrate loading: 4 g xylose (Sigma Aldrich), 2.5 g furfural (Sigma Aldrich 99% w/w). Decane (Acros organics >99 % w/w) was used as internal standard (0.01  $g \cdot mL^{-1}$ ).

The experiments were carried out in a stainless steel stirred autoclave (200 mL) with temperature control and pressure gauge. The reactants and catalyst, together with the internal standard, were placed within the reaction vessel to a total volume of 100 mL. After sealing the reactor, stirring was fixed at 1000 rpm and a heating rate was established to reach the desired temperature within 1 h. This point is taken as the beginning of the reaction, ignoring the time needed for heating up. Samples were taken periodically and the solution filtered into a vial.

Samples were analysed by GC-FID (Varian 3900) using a capillary column (Agilent CP-WAX 52 CB, 30 m-long, 0.25 mm-i.d., 0.25  $\mu$ m thickness). Conversion of xylose was evaluated by HPLC analysis with a refractive index detector (Varian 356-LC), using a Hi-PLEX H+ column (300 mm-long, 7.7 mm-i.d., 8  $\mu$ m particle size). Conversion was calculated as (mol substrate converted/mol initial substrate)x100 and products yield as (mol produced/mol initial substrate)x100.

#### 4-Tables

	Composition <sup>a</sup>					Surface	Total pore	Acid site
Catalyst	% Al	% Zr	Si/Al	Si/Zr	Al/Zr	area <sup>5</sup> (m²g⁻¹)	volume <sup>c</sup> (cm <sup>3</sup> g <sup>-1</sup> )	) (mmol H <sup>+</sup> g <sup>-1</sup> )
Al-Beta	2.0	0.0	22	~	-	623	0.36	0.413
Zr-Al-Beta (2.8)	1.2	2.8	35	51	1.46	571	0.24	0.351
Zr-Al-Beta (3.7)	1.0	3.7	43	38	0.88	571	0.25	0.306
Zr-Al-Beta (4.0)	0.7	4.0	62	35	0.57	560	0.26	0.233
Zr-Al-Beta (5.7)	0.4	5.7	111	24	0.22	539	0.24	0.215
Zr- Beta (6.4)	0.02	6.4	∞	22	0.00	638	0.28	0.083

Table S1. Al and Zr content, textural properties and acidity of the parent Al-Beta and modified Zr-Al-Beta zeolites.

<sup>a</sup> % Al, % Zr (w/w); Si/Al, Si/Zr, Al/Zr (atomic ratio) measured by ICP-OES. <sup>b</sup> Surface area calculated by the B.E.T. method. <sup>c</sup> Total pore volume recorded at  $P/P_0 = 0.975$ . <sup>d</sup> Acid site loading analysed by NH<sub>3</sub>-TPD.

Catalust	Brønsted/	Acid site loading (mmol H⁺g⁻¹)		
Catalyst	sites ratio	Brønsted	Lewis	
Al-Beta	0.56	0.149	0.264	
Zr-Al-Beta (2.8)	0.52	0.120	0.231	
Zr-Al-Beta (3.7)	0.39	0.087	0.220	
Zr-Al-Beta (4.0)	0.31	0.055	0.178	
Zr-Al-Beta (5.7)	0.17	0.031	0.185	
Zr- Beta (6.4)	0.04	0.003	0.080	

 Table S2. Brønsted to Lewis acid sites ratio determined by FTIR using pyridine as molecular probe and total Brønsted and Lewis acid site loading.

**5-Figures** 



**Figure S1.** Catalytic performance of Al-Beta in the conversion of a) xylose and b) furfural. Reaction conditions: 170 °C, substrate:2-propanol molar ratio 1:50, catalyst 0.1 g·mL<sup>-1</sup>.



**Figure S2.** XRD patterns of (a) Al-Beta, (b) Zr-Al-Beta (2.8), (c) Zr-Al-Beta (3.7), (d) Zr-Al-Beta (4.0), (e) Zr-Al-Beta (5.7), (f) Zr-Beta (6.4) zeolites and (g) tetragonal ZrO<sub>2</sub> (different scale) for comparative purposes.



Figure S3.  $N_2$  adsorption-desorption isotherms of Beta zeolites.



Figure S4. NH<sub>3</sub>-TPD profiles of Beta zeolites.



Figure S5. FTIR spectra of Zr containing Beta zeolites and their corresponding dealuminated zeolites.



Figure S6. XPS spectra of Zr-Al-Beta zeolites.



Figure S7. TEM of (a) parent Al-Beta and (b) Zr-Al-Beta (5.7) zeolites.



Figure S8. SEM and mapping of Si, Al and Zr for Zr-Al-Beta (5.7) zeolite.



Figure S9. DRIFT signal of adsorbed pyridine on (a) Al-Beta, (b) Zr-Al-Beta (2.8), (c) Zr-Al-Beta (3.7), (d) Zr-Al-Beta (4.0), (e) Zr-Al-Beta (5.7), (f) Zr-Beta (6.4) zeolites.



**Figure S10.** Catalytic performance of Zr-Al-Beta zeolites in the conversion of furfural. a) FAL conversion; b)FOL+FE; c) IL; d) LA; e) LACT and f) GVL yield. Reaction conditions: 170 °C, furfural:2-propanol molar ratio 1:50, catalyst 0.1 g·mL<sup>-1</sup>.



**Figure S11.** Catalytic performance of Zr-Al-Beta (5.7) zeolite in the conversion of xylose at different temperatures: a) 150 °C; b) 170 °C; c) 190 °C. Reaction conditions: xylose:2-propanol molar ratio 1:50, catalyst 0.1 g·mL<sup>-1</sup>.



**Figure S12.** Comparison of GVL yield obtained for xylose conversion in presence of: Zr-Al-Beta (5.7) and a mixture of Al-Beta and Zr-Beta (6.4). The amount of each catalyst in the mixture was calculated to match the Al and Zr content of the bifunctional catalyst Zr-Al-Beta (5.7). Reaction conditions: 190 °C, xylose:2-propanol molar ratio 1:50, total amount of the single catalyst or the mixture  $0.1 \text{ g} \cdot \text{mL}^{-1}$ .



**Figure S13.** Reusability of Zr-Al-Beta (5.7) zeolite in the conversion of xylose. The catalyst was re-calcined after run 1 at 550 °C in air for 5 h. Reaction conditions: 190 °C, xylose:2-propanol molar ratio 1:50, catalyst 0.1 g·mL<sup>-1</sup>.

### **6-Schemes**



**Scheme S1**. Proposed reaction network for the cascade conversion of xylose into GVL considering side reactions. Products: X ETHERS. xylose ethers; FAL, furfural; FOL, furfuryl alcohol; FE, isopropyl furfuryl ether; IL, isopropyl levulinate; LA, levulinic acid;  $\alpha/\beta$ -LACT,  $\alpha/\beta$ -angelica lactone; IHP, isopropyl 4-hydroxypentanoate; HPA, 4-hydroxypentanoic acid; GVL,  $\gamma$ -valerolactone.