

A steric pore-flow model to predict the transport of small and uncharged solutes through a reverse osmosis membrane

Haruka Takeuchi ^a, Hiroaki Tanaka ^a, Long D. Nghiem ^b, Takahiro Fujioka ^{c,*}

^a Research Center for Environmental Quality Management,

Kyoto University, Shiga 520-0811, Japan

^b Strategic Water Infrastructure Laboratory, School of Civil Mining and Environmental

Engineering, The University of Wollongong, NSW 2522, Australia

^c Water and Environmental Engineering, Graduate School of Engineering, Nagasaki

University, 1-14 Bunkyo-machi, Nagasaki 852-8521, Japan

SUPPLEMENTARY INFORMATION

* Corresponding author: Takahiro Fujioka, Email: tfujioka@nagasaki-u.ac.jp, Ph +81 095 819 26

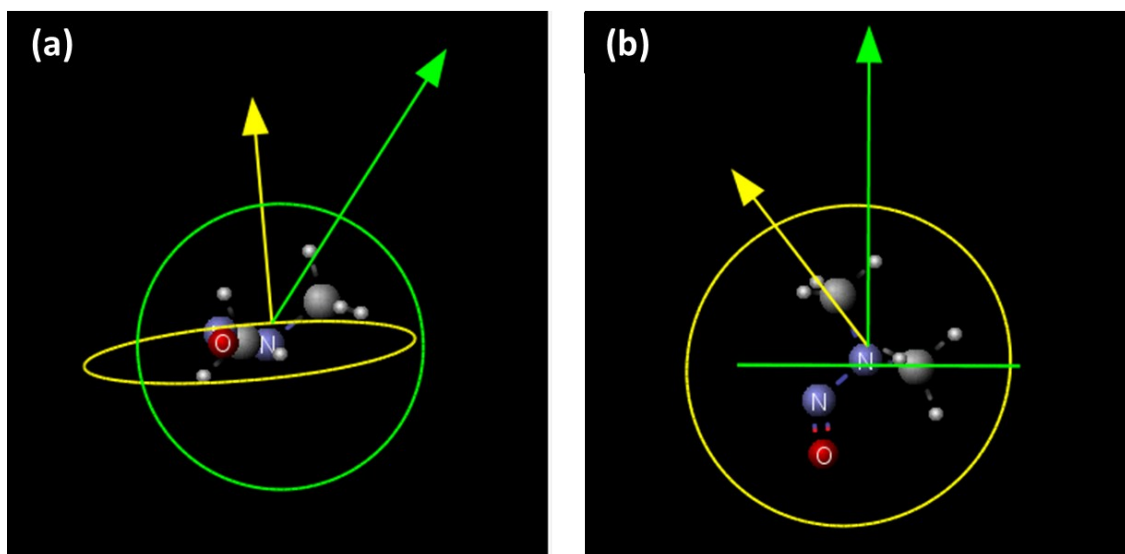


Fig. S1. (a) Minimally projected graphic of NDMA (green circle) and (b) the side view. These figures were illustrated with a software Marvin Sketch (ChemAxon, Budapest, Hungary). Molecular radius (r_c) is defined as a radius of the minimally projected graphic.

Table. S2. Experimentally obtained observed and real rejections.

Compound	Diffusion coefficient at 20 °C [nm ² /s]	Mass transfer coefficient at 20 °C [m/s]	2.6 L/m ² h		5 L/m ² h		10 L/m ² h		20 L/m ² h	
			<i>R_{obs}</i>	<i>R_{real}</i>	<i>R_{obs}</i>	<i>R_{real}</i>	<i>R_{obs}</i>	<i>R_{real}</i>	<i>R_{obs}</i>	<i>R_{real}</i>
			[%]	[%]	[%]	[%]	[%]	[%]	[%]	[%]
NDMA	8.88×10 ⁸	1.16×10 ⁻⁴	14	14	31	31	35	36	54	56
NMEA	7.84×10 ⁸	1.07×10 ⁻⁴	45	45	66	66	76	77	83	84
NPYR	6.96×10 ⁸	9.96×10 ⁻⁵	64	64	81	81	86	87	88	89
NDEA	7.17×10 ⁸	1.02×10 ⁻⁴	85	86	91	91	93	93	96	96
NPIP	6.18×10 ⁸	9.25×10 ⁻⁵	95	95	96	96	98	98	98	99
NMOR	6.53×10 ⁸	9.75×10 ⁻⁵	89	90	93	93	96	96	98	98
NDPA	6.43×10 ⁸	9.48×10 ⁻⁵	96	96	97	97	98	98	99	99
NDBA	6.19×10 ⁸	9.25×10 ⁻⁵	99	99	99	99	99	99	99	99
1,1,2-trichloroethane	6.86×10 ⁸	1.06×10 ⁻⁴	80	80	89	89	86	87	84	85
1,2-Dichloropropane	7.72×10 ⁸	1.06×10 ⁻⁴	91	91	94	94	92	92	89	90
Bromodichloromethane	8.27×10 ⁸	1.11×10 ⁻⁴	75	75	82	83	76	77	67	69
Bromoform	7.64×10 ⁸	1.06×10 ⁻⁴	84	84	93	93	92	92	91	91
Chloroform	8.63×10 ⁸	1.14×10 ⁻⁴	57	57	68	68	61	62	53	54
Dibromochloromethane	9.22×10 ⁸	1.09×10 ⁻⁴	80	80	89	89	86	87	82	83
Dichloroacetonitrile	8.27×10 ⁸	1.10×10 ⁻⁴	52	53	72	74	74	77	78	84

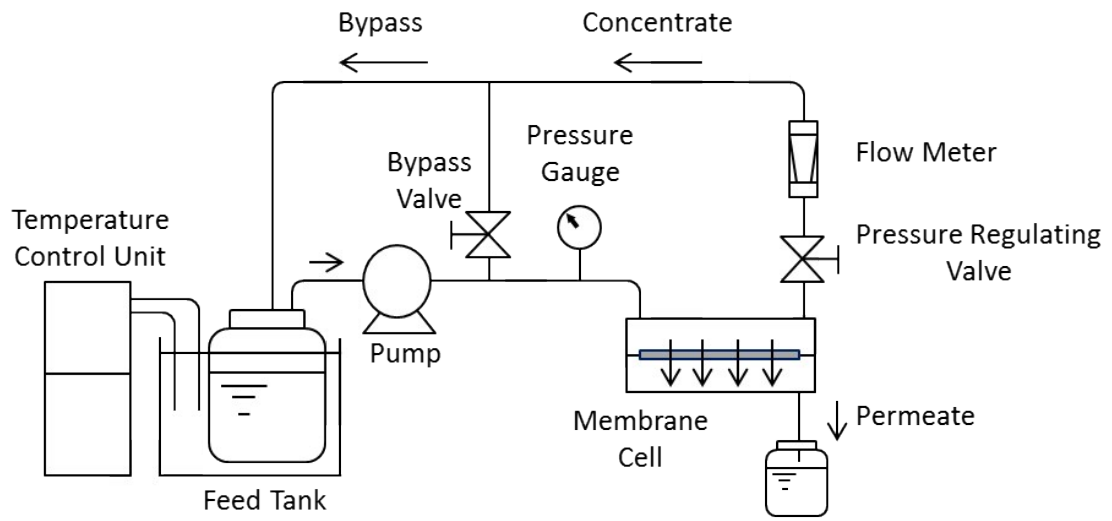


Fig. S3. Schematic diagram of the bench-scale cross-flow filtration system.

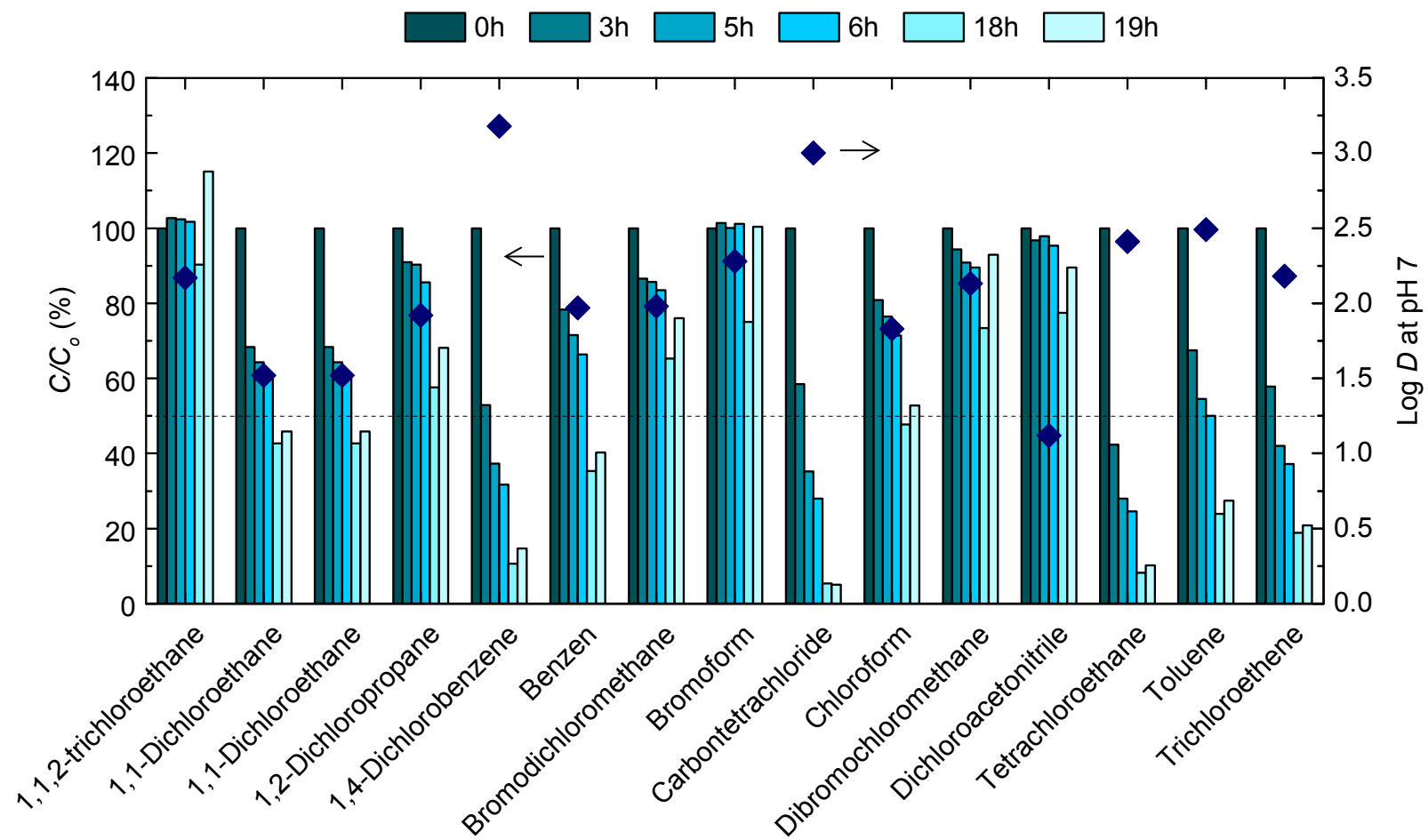


Fig. S4. Normalized VOC concentrations in the RO feed during 19 h of membrane system operation.

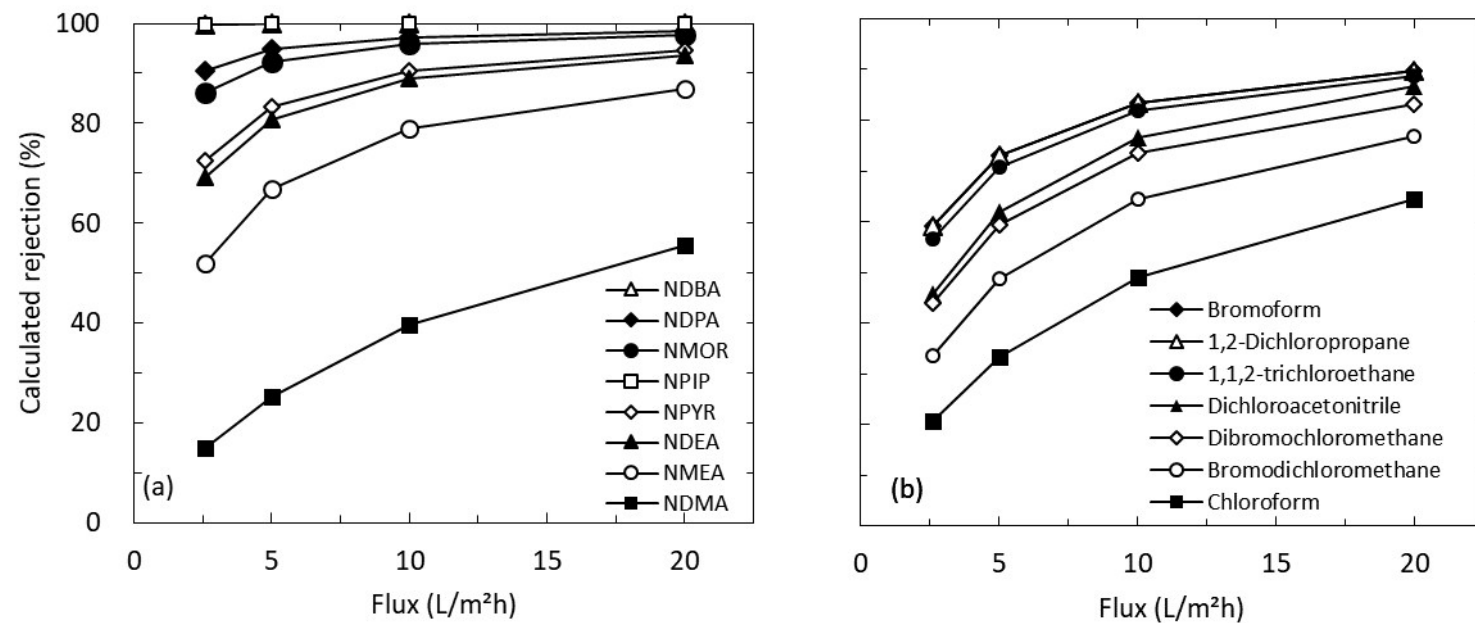


Fig. S5. Calculated rejection of (a) *N*-nitrosamines and (b) VOCs by the ESPA2 membrane as a function of permeate flux (feed solution temperature = 20 °C and permeate flux = 2.6–30 L/m²h). The rejections were predicted by incorporating the estimated free-volume hole-radius (0.348 nm).

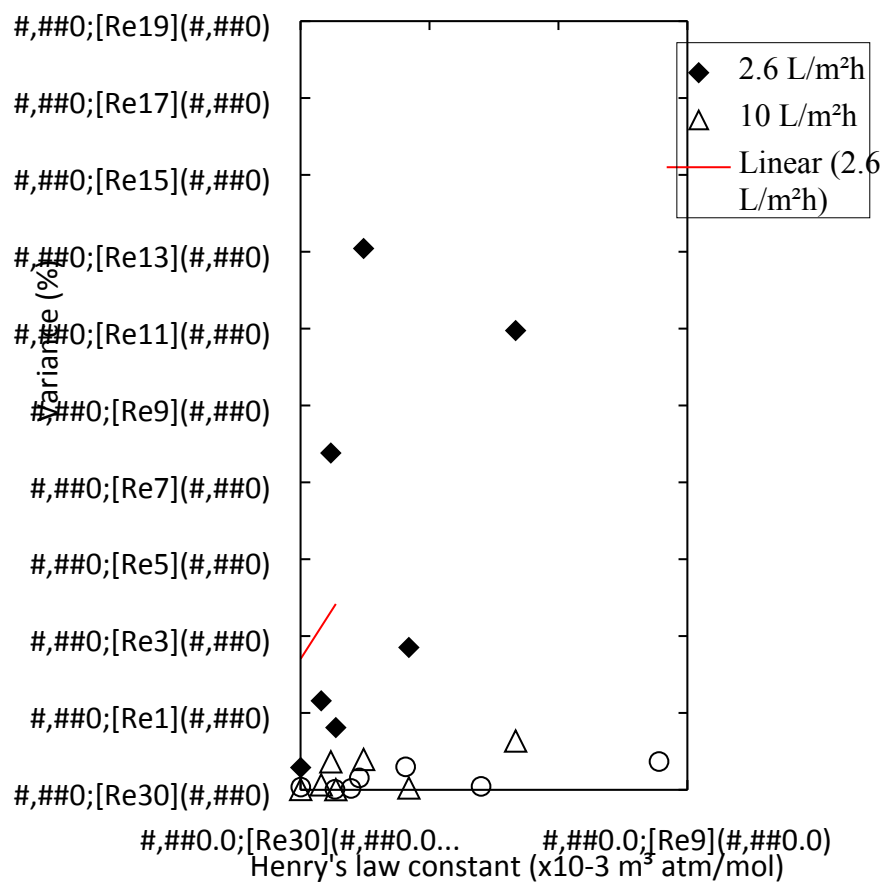


Fig. S6. Variance between calculated and experimentally obtained rejections of seven VOCs under the permeate flux of 2.6–20 L/m²h as a function of their Henry's law constant. The solid line represents the linear regression line for data obtained under 2.6 L/m²h.