

## **Entropy–Stabilized Metal Oxide Solid Solutions as CO Oxidation Catalysts with High–Temperature Stability**

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## **Experimental**

### **Materials and Chemicals**

$\text{H}_2\text{PtCl}_6 \cdot x\text{H}_2\text{O}$  (99.9%, ALDRICH, USA),  $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$  (AR, ACROS, USA),  $\text{ZnCl}_2$  (98%+, Alfa Aesar, USA),  $\text{CoCl}_2$  (97.0%, ACROS, USA),  $\text{CuCl}_2$  (AR, ACROS, USA) and  $\text{Ni}(\text{OOCCH}_3)_2 \cdot 4\text{H}_2\text{O}$  (99.0%, ACROS, USA) were purchased as received. Ammonium hydroxide ( $\text{NH}_3 \cdot \text{H}_2\text{O}$ , 28.0~30.0%) was brought from Avantor Performance Materials (USA) and cetyltrimethyl ammonium bromide (CTAB, AR) was purchased from MP Biomedicals, LLC (France).

### **Synthesis of entropy-stabilized metal oxide solid solutions**

#### **NiMgCuZnCoOx (mix)**

$\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$ ,  $\text{ZnCl}_2$ ,  $\text{CoCl}_2$ ,  $\text{CuCl}_2$  and  $\text{Ni}(\text{OOCCH}_3)_2 \cdot 4\text{H}_2\text{O}$  are massed and physical mixed just using agate mortar. To ensure adequate mixing, all batches are milled for at least 2 h. Mixed powders are then calcinated in air under 800, 900 and 1000 °C for 4 h (5 °C/min) to obtain desired crystallineoxide phase.

#### **NiMgCuZnCoOx (co-precipitation)**

Equal molar ratio (0.02 M) of  $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$ ,  $\text{ZnCl}_2$ ,  $\text{CoCl}_2$ ,  $\text{CuCl}_2$  and  $\text{Ni}(\text{OOCCH}_3)_2$  are dissolved in 30 ml water followed by adding the 0.47 g CTAB. After stirring for 12 h at 60 °C, 2.5 ml  $\text{NH}_3 \cdot \text{H}_2\text{O}$  was added and continues stirring for 12 h at 60 °C. After filtering, the precipitate was dried at 120 °C for 4 h and finally calcined at 900 °C for 4 h (5 °C/min)

to obtain desired crystallineoxide phase.

### **PtNiMgCuZnCoOx (co-deposition)**

Equal molar ratio (0.02 M) of  $\text{MgCl}_2 \cdot 6\text{H}_2\text{O}$ ,  $\text{ZnCl}_2$ ,  $\text{CoCl}_2$ ,  $\text{CuCl}_2$  and  $\text{Ni}(\text{OOCCH}_3)_2$  are dissolved in 30 ml water followed by adding the 0.47 g CTAB. After stirring for 12 h at 60 °C, precalculated amount of  $\text{H}_2\text{PtCl}_6$  (0.3, 0.6 and 1.0 wt%) in  $\text{H}_2\text{O}$  was added and then stirred constantly for 12 h. 2.5 ml  $\text{NH}_3 \cdot \text{H}_2\text{O}$  was added and continues stirring for 12 h at 60 °C. After filtering, the precipitate was dried at 120 °C for 4 h and finally calcined at 900 °C for 4 h (5 °C/min) to obtain desired crystallineoxide phase.

The reduced 0.3wt%PtNiMgCuZnCoOx were measured under 300 °C for 2 h using a mixture of 4%  $\text{H}_2$  in 96%  $\text{N}_2$ .

### **Characterization of the catalyts**

The powder X-ray diffraction (XRD) data were recorded with a PANalytical Empyrean diffractometer, operated at 45 kV and 40 mA (scanning step: 0.02 ° per step). The diffraction patterns were recorded in the range of 10-80°. The nanoparticle size (d<sub>Ba</sub>, nm) was estimated according to Scherrer equation:  $S4 \text{ dBa} = K \cdot \lambda / (\beta \cdot \cos\theta)$  ( $K = 0.9$ ,  $\lambda = 0.1540598 \text{ nm}$ ).

The nitrogen adsorption and desorption isotherms were measured at 77 K under a Gemini VII surface area analyzer. Samples were degassed for 12 h under  $\text{N}_2$  at 100 °C prior to the measurement.

High resolution transmission electron microscopy (HRTEM) and high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) were conducted on

an aberration-corrected FEI Titan S 80-300 TEM/STEM operated at 300 kV and a large active area (60mm<sup>2</sup>) EDAX silicon drift detector (SDD) for high-collection-efficiency energy dispersive x-ray spectroscopy (EDS).

X-ray photoelectron spectroscopy (XPS) experiments were performed with a PHI 3056 spectrometer equipped with an Al anode source operated at 15 KV and an applied power of 350 W and a pass energy of 93.5 eV.

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Temperature-programmed reduction of H<sub>2</sub> (H<sub>2</sub>-TPR) experiments were conducted on a PX200 apparatus with a TCD. 50 mg of sample was pretreated at 450 °C (10 °C/min) in He for 1 h and then cooled to room temperature. Then the sample was directly heated from 60 °C to 700 °C at a rate of 10 °C/min in a flow of 5 vol % H<sub>2</sub>/N<sub>2</sub> (40 mL/min). The hydrogen consumption was quantitatively evaluated by the TCD signal.

### **Catalytic CO oxidation**

Catalytic CO oxidation was carried out in a fixed-bed reactor (straight quartz tube) at atmospheric pressure <sup>1</sup>. For the measurement of CO light-off curves showing CO conversion as a function of reaction temperature, a 20 mg catalyst supported by quartz wool was loaded in the reactor. The feed gas of 1 % CO balanced with dry air (< 4 ppm water) passed though the catalyst bed at a flow rate of 10 ml/min corresponding to gas hourly space velocity (GHSV) of 30,000 mL (h g<sub>cat</sub>)<sup>-1</sup>. The concentrations of CO and CO<sub>2</sub> in the

reactor effluent were analyzed by a Buck Scientific 910 gas chromatograph equipped with a dual molecular sieve/porous polymer column (Alltech CTR1) and a thermal conductivity detector. We controlled the reaction temperature through changing its discharge and maintained at each temperature point for 5 min to detect each experiment for two times.

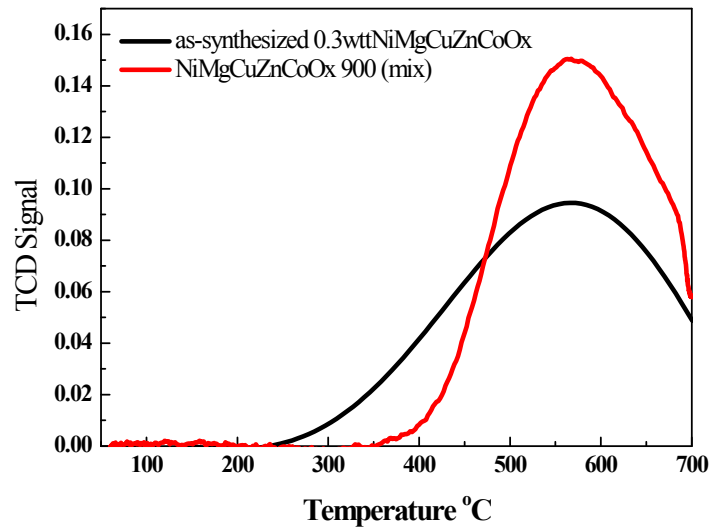
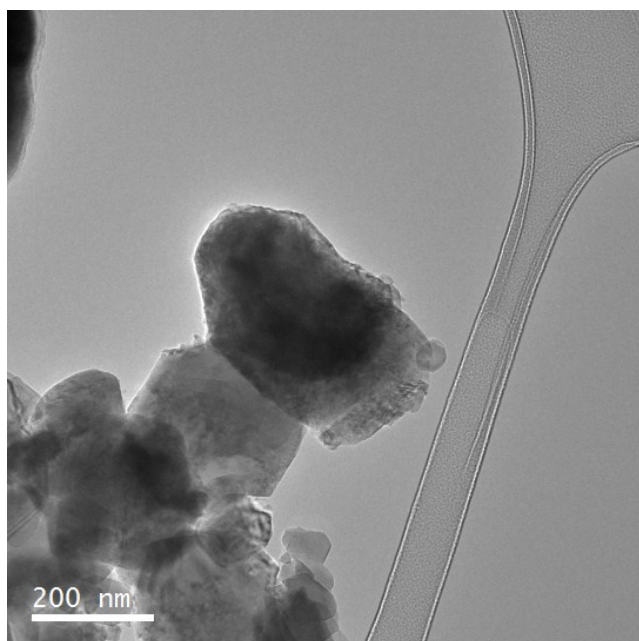
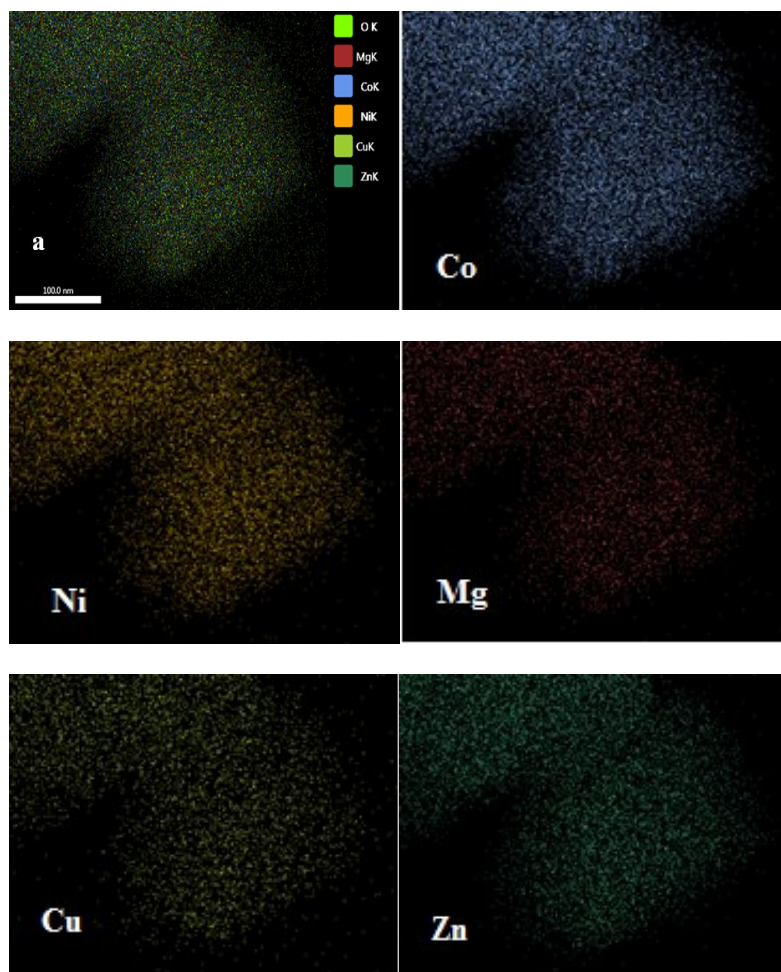


Figure S1. TPR result of NiMgCuZnCoO<sub>x</sub> 900 and as-synthesized 0.3wt%PtNiMgCuZnCoO<sub>x</sub>.

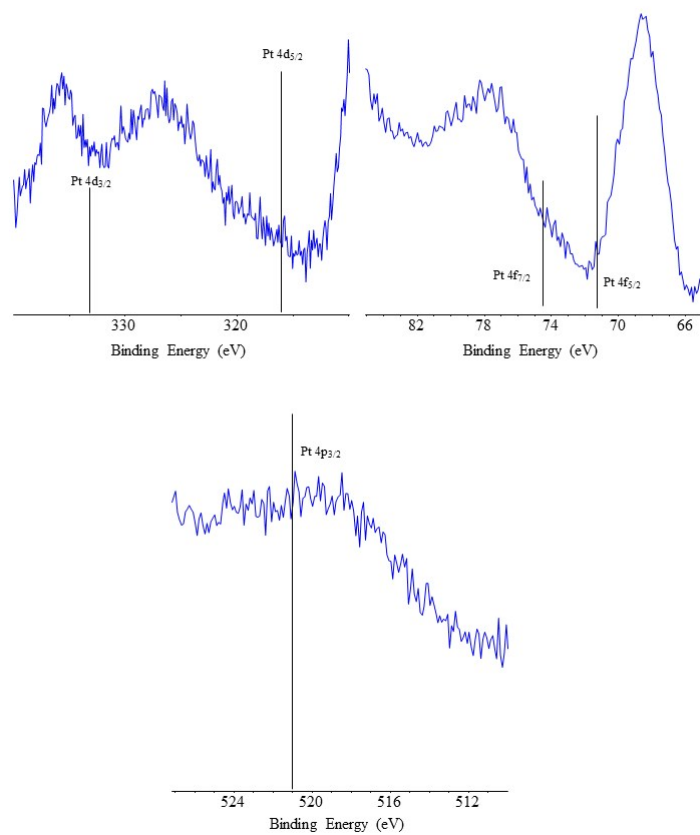


**Figure S2.** HRTEM images of reduced 0.3wt%PtNiMgCuZnCoO<sub>x</sub>.

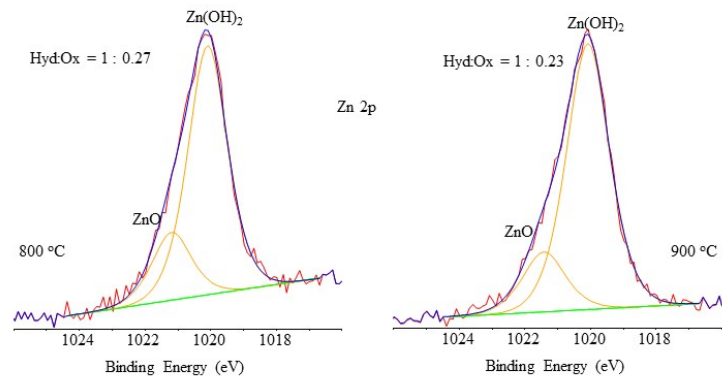
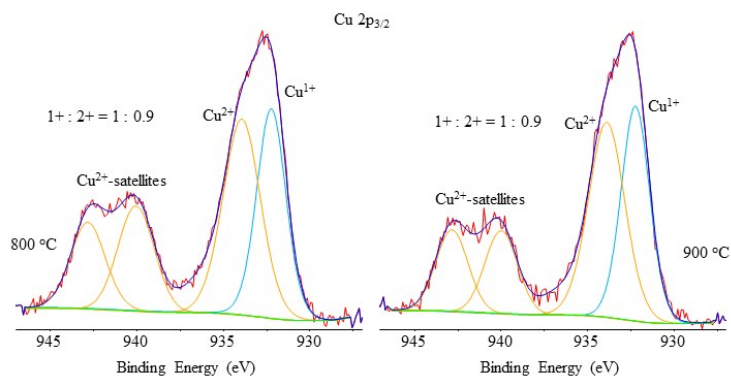
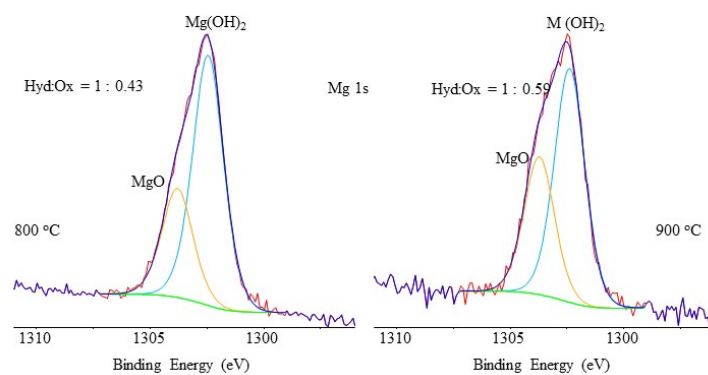
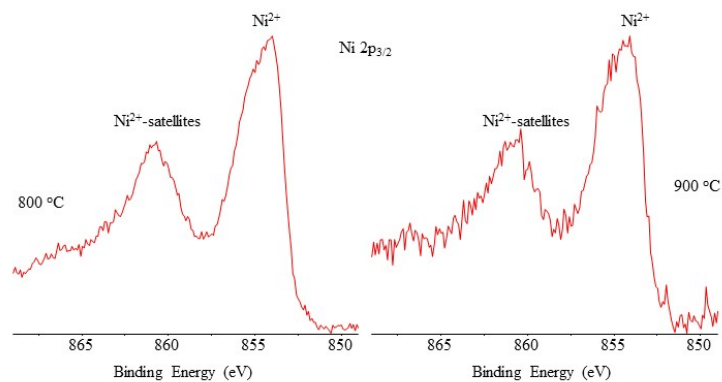


**Figure S3.** TEM-EDS analysis of reduced  $0.3\text{wt}\%\text{PtNiMgCuZnCoO}_x$ .





**Figure S4.** XPS results of Pt in reduced 0.3wt%PtNiMgCuZnCoO<sub>x</sub>.



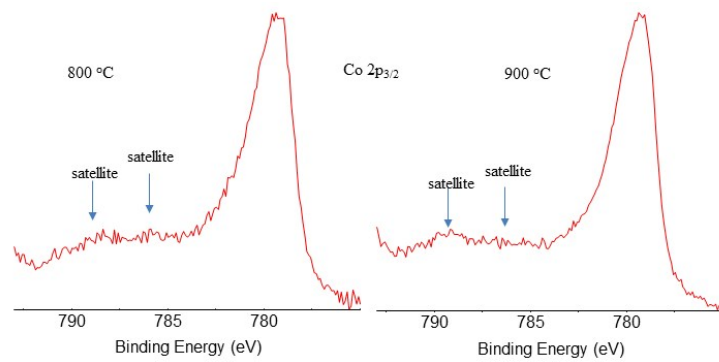
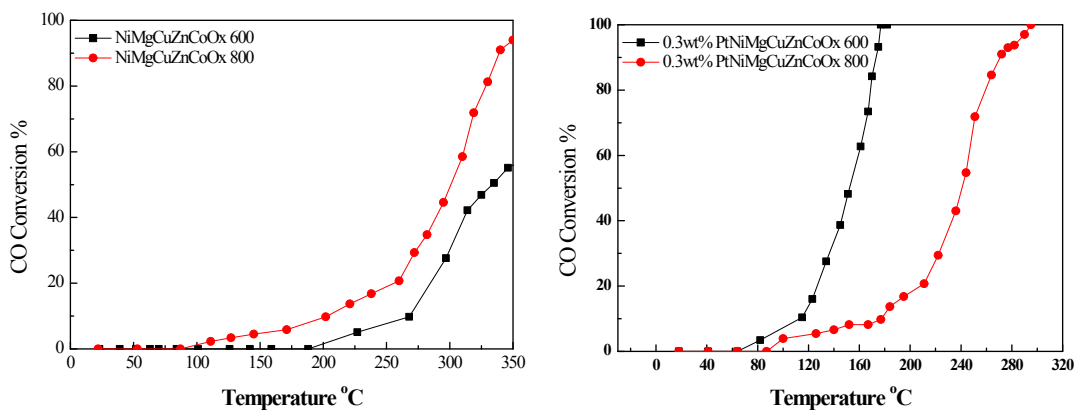
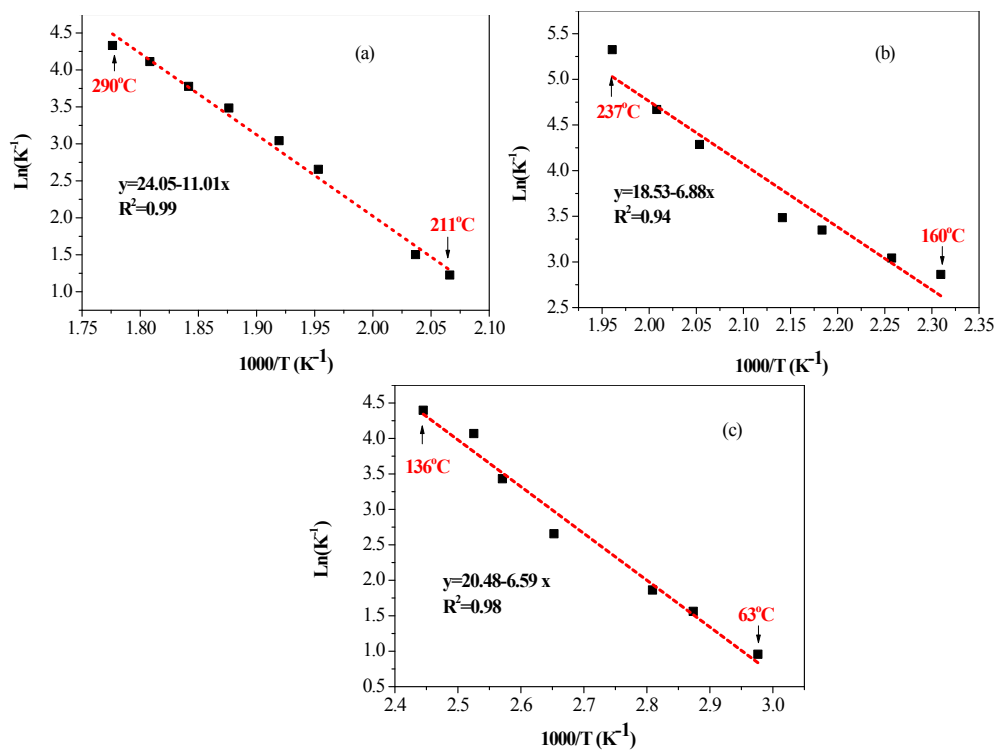


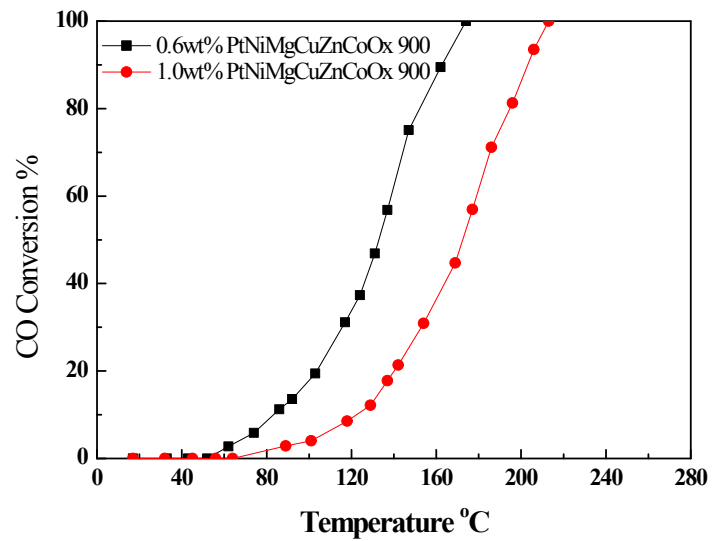
Figure S5. XPS results of Ni, Mg Cu, Zn and Co in NiMgCuZnCoO<sub>x</sub> treated at 800 °C and 900 °C.



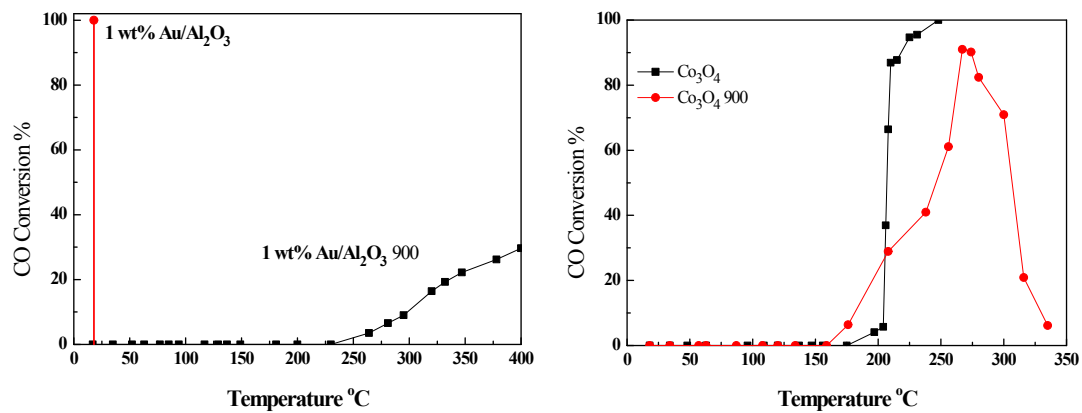
**Figure S6.** CO oxidation over NiMgCuZnCoO<sub>x</sub> and reduced 0.3wt%PtNiMgCuZnCoO<sub>x</sub> calcined at 600 and 800 °C.



**Figure S7.** The variation of  $\ln k$  with the  $1/T$  for (a) NiMgCuZnCoO<sub>x</sub> 900; (b) as-synthesized 0.3wt%PtNiMgCuZnCoO<sub>x</sub> and (c) reduced 0.3wt%PtNiMgCuZnCoO<sub>x</sub>. The relations between  $\ln k$  and  $1/T$  were all found to be in linearly.



**Figure S8.** CO oxidation over reduced PtNiMgCuZnCoO<sub>x</sub> 900 with different Pt loading.



**Figure S9.** CO oxidation over 1wt%Au/Al<sub>2</sub>O<sub>3</sub> and Co<sub>3</sub>O<sub>4</sub> (as-received and calculated at 900 °C).

**Table S1.** Calculated pre-exponential factor ( $A$ ) and apparent activation energy ( $E_a$ ) for NiMgCuZnCoO<sub>x</sub> 900, as-synthesized 0.3wt%PtNiMgCuZnCoO<sub>x</sub> and reduced 0.3wt%PtNiMgCuZnCoO<sub>x</sub>.

Catalyst	$A$ (min <sup>-1</sup> )	$E_a$ (KJ·mol <sup>-1</sup> )
NiMgCuZnCoO <sub>x</sub> 900	$2.78 \times 10^{10}$	$91.5 \pm 3.57$
as-synthesized 0.3wt%PtNiMgCuZnCoO <sub>x</sub>	$1.12 \times 10^8$	$57.2 \pm 6.07$
reduced 0.3wt%PtNiMgCuZnCoO <sub>x</sub>	$7.53 \times 10^8$	$54.8 \pm 3.41$



References:

1. C. Tian, X. Zhu, C. W. Abney, X. Liu, G. S. Foo, Z. Wu, M. Li, H. M. Meyer, S. Brown, S. M. Mahurin, S. Wu, S. Z. Yang, J. Liu and S. Dai, *ACS Catal.*, 2017, 7, 3388–3393.