

Electronic Supplementary Information

**Covalent triazine framework-decorated phenyl-functionalized SBA-15:
Synthesis and application as a novel nanoporous adsorbent**

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Table S1. The list of adsorption equilibrium, kinetics, and thermodynamic equations.

Adsorption equilibrium equations	$\% \text{Removal} = 100 \cdot (C_0 - C_e)/C_0$ (1)	$Q_e = (C_0 - C_e) \cdot V/W$ (2)
	$K_d = Q_e/C_e$ (3)	$R_L = 1/(1 + (K_L \cdot C_e))$ (4)
	Thermodynamic	
	$\Delta G^\circ = -R \cdot T(\ln K_d)$ (5)	$\ln K_d = (-\Delta H^\circ/R \cdot T) + (-\Delta S^\circ/R)$ (6)
	Isotherms	
	Non-linear	Linear
Langmuir	$Q_e = (Q_m \cdot K_L \cdot C_e)/(1 + K_L \cdot C_e)$ (7)	$C_e/Q_e = (1/K_L \cdot Q_m) + (C_e/Q_m)$ (8)
Freundlich	$Q_e = K_F \cdot C_e^{1/n_F}$ (9)	$\log Q_e = \log K_F + (1/n_F) \log C_e$ (10)
Temkin	$Q_e = (R \cdot T/b_T) \ln(K_T \cdot C_e)$ (11)	$Q_e = (R \cdot T/b_T) \ln K_T + (R \cdot T/b_T) \ln C_e$ (12)
Dubinin-Radushkevich (D-R)	$Q_e = Q_m^{DR} \cdot \exp(-K_{DR} \cdot \varepsilon^2)$ (13)	$\ln Q_e = \ln Q_m^{DR} - K_{DR} \cdot \varepsilon^2$ (14)
Redlich-Peterson (R-P)	$Q_e = (K_{RP} \cdot C_e)/(1 + \alpha_{RP} \cdot C_e^g)$ where $g \leq 1$ (15)	-
Sips	$Q_e = (Q_{max}^S \cdot K_S \cdot C_e^{1/n_S})/(1 + K_S \cdot C_e^{1/n_S})$ (16)	-
Koble-Corrigan (K-C)	$Q_e = (A \cdot C_e^\beta)/(1 + B \cdot C_e^\beta)$ (17)	-
	Kinetics	
	Non-linear	Linear
Pseudo-First order (PFO)	$Q_t = Q_e \cdot (1 - \exp(-k_1 \cdot t))$ (18)	$\log(Q_e - Q_t) = \log Q_e - (k_1 \cdot t/2.303)$ (19)
Pseudo-Second order (PSO)	$Q_t = (k_2 \cdot Q_{e,calc}^2 \cdot t)/(1 + k_2 \cdot Q_{e,calc} \cdot t)$ (20)	$(t/Q_t) = (1/k_2 \cdot Q_e^2) + (t/Q_e)$ (21)
Elovich	$Q_t = (1/\beta) \ln h \cdot \beta + (1/\beta) \ln t$ (22)	$Q_t = (1/\beta) \ln h \cdot \beta + (1/\beta) \ln t$ (23)
Intra-particle diffusion (IPD)	$Q_t = k_{IPD} \cdot t^{0.5} + C$ (24)	$Q_t = k_{IPD} \cdot t^{0.5} + C$ (25)
Nomenclature:		
<p>C_0 (mg·L⁻¹): Adsorbate initial concentration; C_e (mg·L⁻¹): Equilibrium concentration; Q_e (mg·g⁻¹): Amount of adsorbate in the adsorbent at equilibrium (adsorption capacity); Q_t (mg·g⁻¹): Amount of adsorbate in the adsorbent at any time t; $Q_{e,calc}$ (mg·g⁻¹): calculated amount of adsorbate in equilibrium; Q_m (mg·g⁻¹): Maximum monolayer coverage capacities; Q_m^{DR} (mg·g⁻¹): D-R maximum adsorption capacity; R_L: Separation factor; Calculated adsorption capacity; K_d (L·g⁻¹): distribution coefficient; K_L (L·mg⁻¹): Langmuir isotherm constant; K_{DR} (mol²·kJ⁻²): Dubinin–Radushkevich isotherm constant; K_F (mg·g⁻¹): Freundlich constant related to the rate of adsorption; K_{RP} (L·g⁻¹): Redlich–Peterson isotherm constant; K_{max}^S (L·mg⁻¹): Sips isotherm model constant; K_T (L·g⁻¹): Temkin isotherm equilibrium binding constant; k_1 (min⁻¹): Rate constant of the pseudo-first-order kinetic model; k_2 (g·mg⁻¹·min⁻¹): Rate constant of the pseudo-first-order kinetic model; k_{IPD} (mg·g⁻¹·min⁻¹): ; α_{RP} (mg⁻¹): Redlich–Peterson isotherm constant; b_T (kJ·mol⁻¹): Temkin isotherm constant related to the heat of sorption; n_F: adsorption intensity; n_S: Sips isotherm model exponent; Q: Adsorption intensity; Q: Dubinin–Radushkevich isotherm constant (Q (Polanyi potential) is equal to $RT \ln(1 + 1/C_e)$); A (Lⁿ·mg¹⁻ⁿ·g⁻¹): Koble–Corrigan isotherm constant; B ((L·mg⁻¹)ⁿ): Koble–Corrigan isotherm constant (L·mg⁻¹)ⁿ; R (8.314 J·K⁻¹·mol⁻¹): Universal gas constant ; V (L): Volume of the aqueous phase; W (g): Dry weight of the adsorbent; T (K): Temperature; ΔG° (kJ·mol⁻¹): Standard Gibbs free energy change; ΔH° (kJ·mol⁻¹): Standard enthalpy change; ΔS° (J·K⁻¹·mol⁻¹): Standard entropy change.</p>		

Table S2. Comparison of the adsorption isotherms, kinetics, and thermodynamic constants.

Thermodynamic						
$\Delta G^\circ / (\text{kJ} \cdot \text{mol}^{-1})$			$\Delta H^\circ / (\text{kJ} \cdot \text{mol}^{-1})$	$\Delta S^\circ / (\text{J} \cdot \text{K} \cdot \text{mol}^{-1})$		
293 K	313 K	333 K				
-10.670	-5.2550	-1.8150	-75.8570	-223.4637		

Isotherm				Kinetic				
Langmuir	R^2	$Q_m / \text{mg} \cdot \text{g}^{-1}$	$K_L / \text{L} \cdot \text{mg}^{-1}$	PFO	R^2	k_1 / min^{-1}		
	Nonlinear	0.9688	569.049	0.0307	Nonlinear	0.8855	1.9321	
	Linear	0.9910	555.555	0.0508	Linear	0.9932	0.0836	
Freundlich	R^2	$K_F / \text{mg} \cdot \text{g}^{-1}$	n_F	PSO	R^2	$Q_{e,\text{calc}} / \text{mg} \cdot \text{g}^{-1}$	$k_2 / \text{g} \cdot \text{mg}^{-1} \cdot \text{min}^{-1}$	
	Nonlinear	0.8851	38.897	1.000	Non-linear	0.8122	296.794	0.0511
	Linear	0.9012	56.754	2.236	Linear	0.9999	294.118	0.0385
Temkin	R^2	$K_T / \text{L} \cdot \text{g}^{-1}$	$b_T / \text{kJ} \cdot \text{mol}^{-1}$	Elovich	R^2	β	h	
	Nonlinear	0.9373	1.9172	32.5338	Nonlinear	0.7401	0.3448	2.6×10^{43}
	Linear	0.9321		31.7312	Linear	0.9790	0.5415	2.6×10^{68}
D-R	R^2	$Q_m^{\text{DR}} / \text{mg} \cdot \text{g}^{-1}$	ϵ	IPD	R^2	$K_{\text{IPD}} / \text{L} \cdot \text{g}^{-1}$	C	
	Nonlinear	0.8179	449.0837	1	Non-linear	0.9505	0.9563	290.45
	Linear	0.7779			Linear 1 (y_1)	0.9956	1.3082	289.49
R-P	R^2	$K_{\text{RP}} / \text{L} \cdot \text{g}^{-1}$	$\alpha_{\text{RP}} / \text{mg}^{-1}$	g	Linear 2 (y_2)	0.9486	0.2121	295.37
	Nonlinear	0.9798	94.884	0.8006	0.7237			
Sips	R^2	$Q_m^{\text{S}} / \text{mg} \cdot \text{g}^{-1}$	$K_S / \text{L} \cdot \text{mg}^{-1}$	n_S				
	Nonlinear	0.9625	569.473	7.407	2.415			
K-C	R^2	A	B	β				
	Nonlinear	0.9623	17.830	0.0312	1			

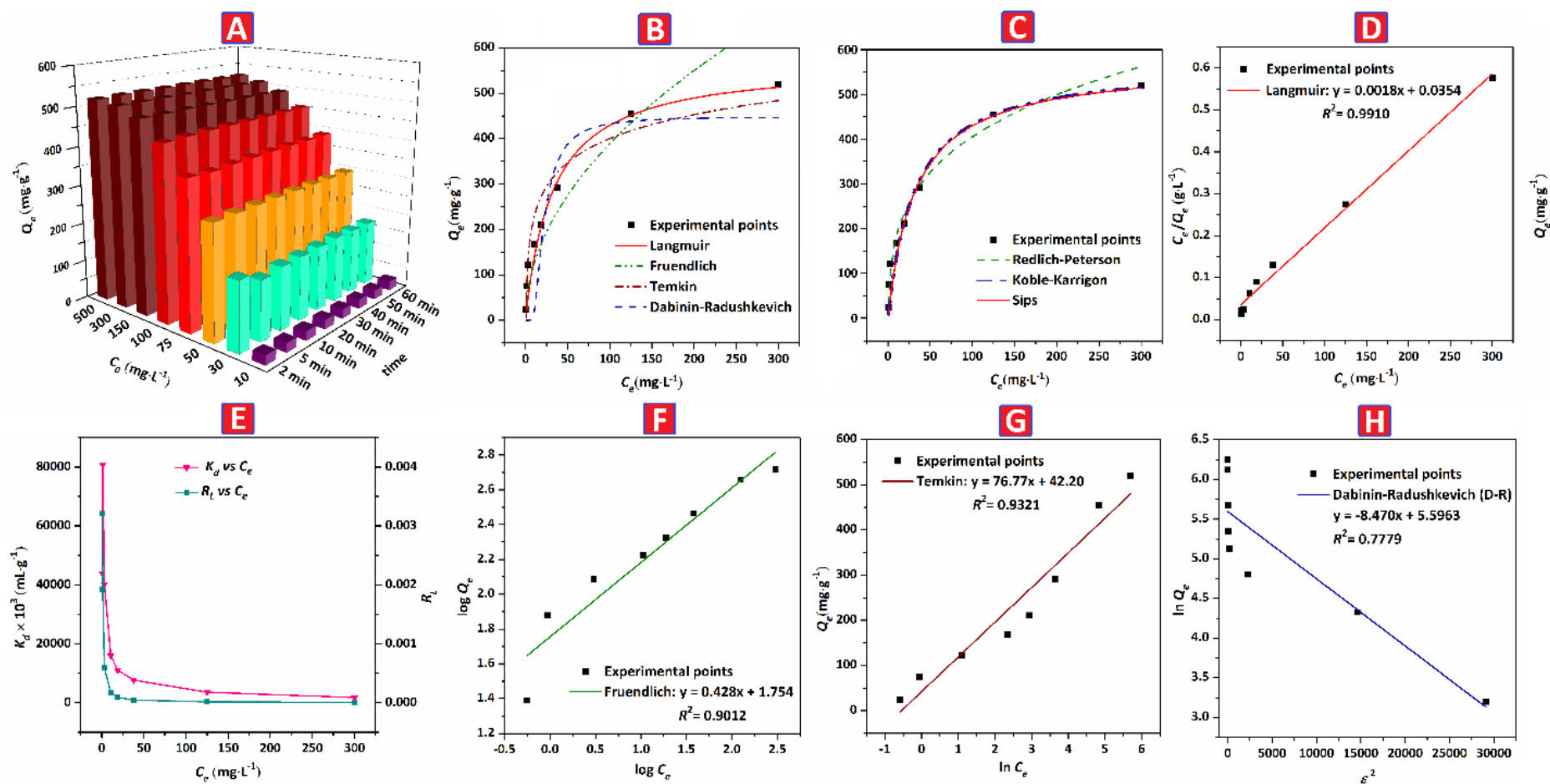


Figure S1. (A) Time-concentration profile for the MB adsorption onto the RS-3. (B) The Langmuir, Freundlich, Temkin, D-R and (C) R-P, K-C and Sips isotherms plots in the non-linear regression analysis. (D) The Langmuir, (F) Freundlich, (G) Temkin, and (H) D-R isotherms plots in the linear regression analysis. (E) the values of R_L and K_d .

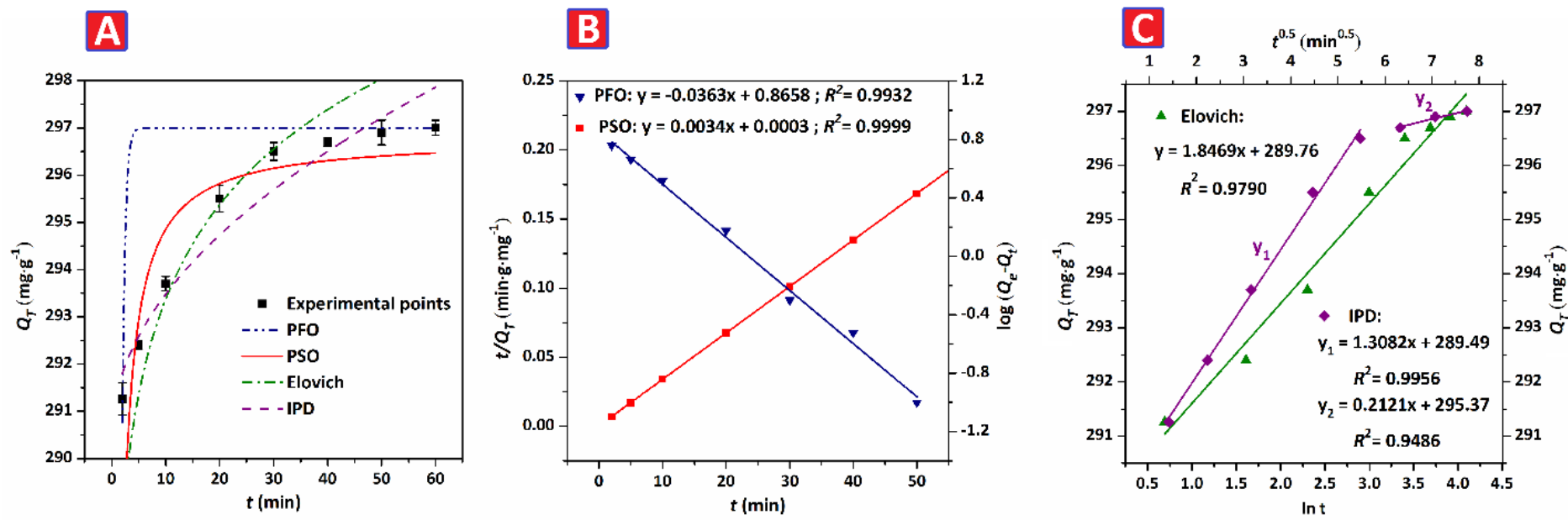


Figure S2. (A) The PFO, PSO, Elovich, and IPD kinetics plots in the non-linear regression analysis. (B) The PFO, PSO, (C) Elovich, and IPD kinetics plots in the linear regression analysis.