

Supplementary Information:

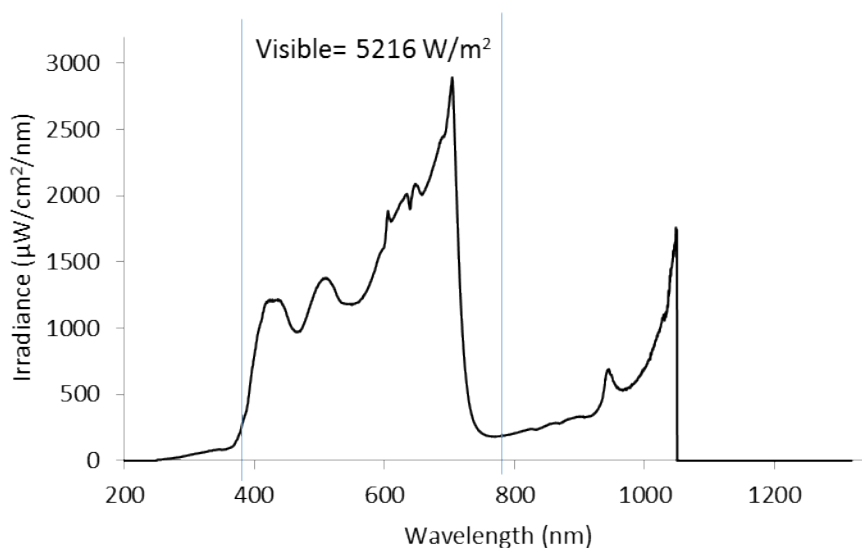


Figure S1. Spectral distribution of the light source used for plasmon enhanced reduction of CO₂ through reverse water gas shift reaction

Table S1. Criteria for showing absence of mass and heat transfer limitations in plasmon-enhanced RWGS reaction over Au/TiO₂ (DP) catalyst

	Criterion	Computed value	Controlling Regime	Ref.
Interphase heat	$\frac{ \Delta H r_p''' r_p^2}{h T_b} < 0.15 \frac{RT_b}{E}$	1.5×10^{-8}	$> 1.3 \times 10^{-2}$	Ref ¹
Interparticle heat	$\frac{ \Delta H r_p''' r_p^2}{k_e T_w} < 0.4 \frac{RT_w/E}{\left[1 + 8\left(\frac{r_p}{R_o}\right) Bi_w\right]}$	1.3×10^{-8}	$> 3.0 \times 10^{-2}$	Ref ¹
Intraparticle heat	$\frac{ \Delta H r_p''' r_p^2}{h T_s} < \frac{0.75 RT_s}{E}$	1.3×10^{-8}	$> 6.3 \times 10^{-2}$	Ref ²
Intraparticle mass	$\frac{r_p''' r_p^2}{C_s D_e} < 0.3$	5.2×10^{-6}	$> 3.0 \times 10^{-1}$	Ref ³
Interphase mass	$\frac{r_p''' r_p^2}{C_s k_c} < \frac{0.15}{n}$	3.4×10^{-10}	$> 3.0 \times 10^{-1}$	Ref ⁴

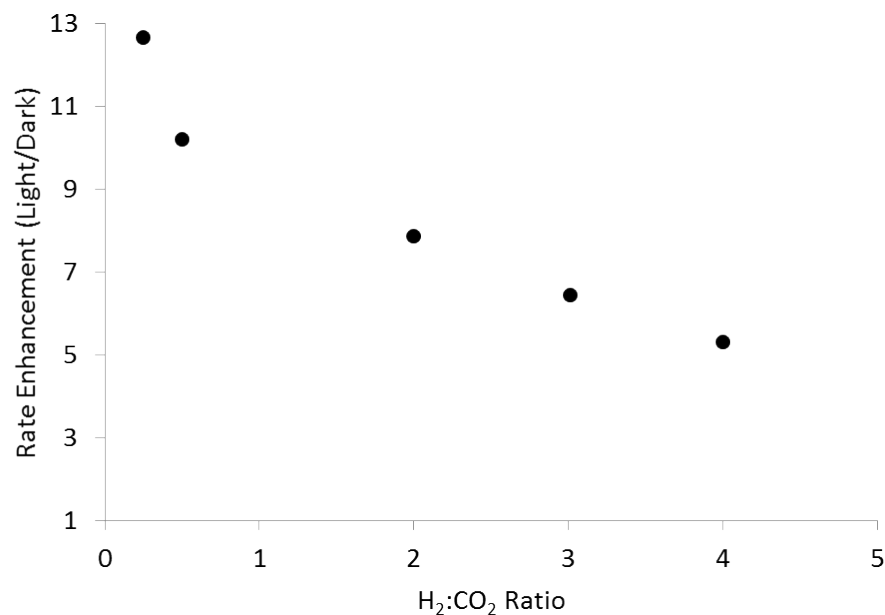


Figure S2. Dependence of rate enhancement (ratio of light to dark reaction rates) on H₂:CO₂ ratio in plasmon enhanced reverse water gas shift reaction over Au/TiO₂ catalyst. Experimental conditions: P= 103 psia, T=200 °C, Total gas flow rate= 15 sccm, catalyst amount= 7.9 mg.

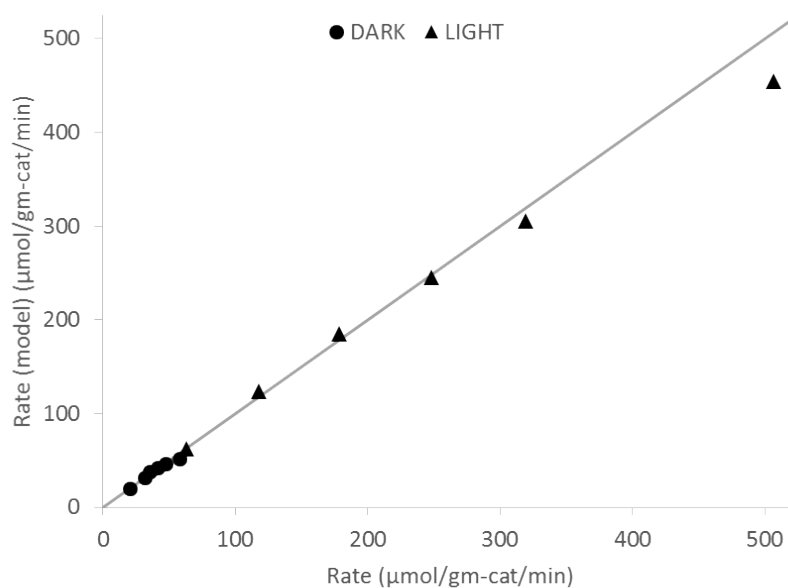


Figure S3. Model results against the experimental values for fitting the experimental data of rate dependence of RWGS reaction on CO₂ partial pressure with Equation 9

Nomenclature

ΔH : Heat of reaction

Bi_w : Biot number at the wall

C_s : Concentration of reactant at the external surface of the catalyst particle

D_e : Effective diffusivity

E : Activation energy of the reaction

h : Heat transfer coefficient

K_c : Mass-transfer coefficient between the catalyst and bulk phases

n : Reaction order

r''' : Reaction rate per catalyst volume

R : Universal gas constant

R_o : Outer radius of reactor

r_p : Catalyst particle radius

T_b : Temperature of bulk phase

T_s : Catalyst surface temperature

T_w : Reactor wall temperature

References:

1. D. E. Mears, *J. Catal.*, 1971, 20, 127-131.
2. J. B. Anderson, *Aiche J.*, 1962, 18, 147-148.
3. P. B. Weisz and C. D. Prater, in *Advances in Catalysis*, eds. V. I. K. W.G. Frankenburg and E. K. Rideal, Academic Press, 1954, vol. Volume 6, pp. 143-196.
4. D. E. Mears, *Industrial & Engineering Chemistry Process Design and Development*, 1971, 10, 541-547.