

Electronic Supplementary Information (ESI)

Fabrication of Active Cu-Zn Nanoalloys on H-ZSM5 Zeolite for Enhanced Dimethyl Ether Synthesis via Syngas

Jian Sun ^a, Guohui Yang ^a, Qingxiang Ma ^a, Issei Ooki ^a, Akira Taguchi ^b, Takayuki Abe ^b, Qing Xie ^c, Yoshiharu Yoneyama ^a, and Noritatsu Tsubaki ^{a,d*}

^a Department of Applied Chemistry, School of Engineering, University of Toyama, Gofuku 3190, Toyama 930-8555, Japan

^b Hydrogen Isotope Research Center, University of Toyama, Gofuku 3190, Toyama 930-8555, Japan

^c Key Laboratory of Industrial Ecology and Environmental Engineering (MOE), School of Environmental Science and Technology, Dalian University of Technology, Dalian 116024, P. R. China

^d Japan Science and Technology Agency (JST), ACT-C, 4-1-8 Honcho, Kawaguchi, Saitama 332-0012, Japan

1. Details of experimental section

In situ diffuse reflectance infrared Fourier transform spectra (DRIFTS) were conducted on Nicolet Nexus 470 FTIR spectrometer with a diffuse reflectance attachment and MCT detector. ZnSe window was used for the *in situ* infrared cell. The absorbance spectra were collected for 32 scans with a resolution of 2 cm⁻¹. Prior to CO adsorption, catalyst of about 0.015 g was heated to the corresponding reduction temperature with a He flow (99.99%) of 30 mL·min⁻¹. After sweeping for 1h, a pure H₂ flow (99.99%) of 30 mL·min⁻¹ was introduced instead of He to reduce the catalyst for 1h. Subsequently, a pure He was flowed into the cell for 4 h to remove H₂ residual in cell and adsorbed on the catalyst, followed by cooling down the temperature to 50°C. After keeping for 0.5 h, the background spectra under this condition were recorded. Then, pure CO flow (99.99%) of 30 mL·min⁻¹ was introduced into the IR cell for 0.5 h at 50°C. After adsorption, He flow of 50 mL·min⁻¹ was employed to sweep for 2 h,

followed by obtaining desorption spectra of CO desorption.

H₂ temperature-programmed reduction (H₂-TPR) for the reduced catalysts and N₂O-pulse experiment were performed with an in situ reduction procedure at corresponding temperature prior to the common tests. Samples used in this experiment were CZ-S and CZ-I. H₂-TPR was performed by using Catalyst Analyzer BELCAT-B-TT (Nippon Bel Co.) The catalyst was heated to 150°C for 1 h in an Ar flow prior to the following test. Samples needing in situ reduction continued to be heated to corresponding temperature, followed by cooling down to 50°C in a Ar flow. Then, TCD signals were recorded at 5% H₂ (Ar balance) flow with a heating rate of 10°C·min⁻¹.

NH₃-TPD was performed using the same equipment as in H₂-TPR. Samples were pretreated at 150°C in a He flow followed by cooling down to 80°C. A flow of 5% NH₃ (He balance) was introduced at a rate of 30 mL·min⁻¹ for 0.5 h. Then, sweeping by He until a constant TCD signal was conducted. Desorption curves of NH₃ were recorded with a heating rate of 10°C·min⁻¹.

2. Acidic sites distribution of prepared catalysts and H-ZSM5

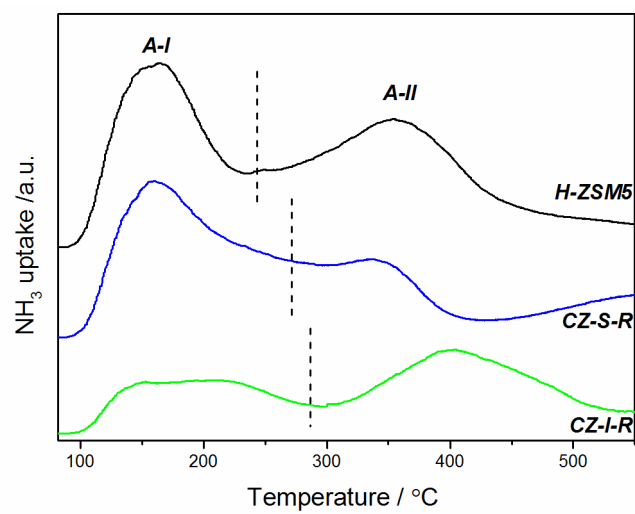


Figure S1 NH₃-TPD curves of prepared catalysts and H-ZSM5 zeolite.