

## Electronic Supplementary Information (ESI)

# Ionic liquid@MIL-101 prepared via the ship-in-bottle technique: Remarkable adsorbents for removal of benzothiophene from liquid fuel

Nazmul Abedin Khan, Zubair Hasan,<sup>1</sup> and Sung Hwa Jung\*

Department of Chemistry and Green-Nano Materials Research Center, Kyungpook National University, Daegu 702-701, Republic of Korea, [sung@knu.ac.kr](mailto:sung@knu.ac.kr)

<sup>1</sup>Present address: Department of Environment and Energy, Sejong University, Republic of Korea.

## Experimental:

**Materials:** Terephthalic acid (TPA,  $C_6H_4-1,4-(CO_2H)_2$ , 98%), chromium chloride ( $CrCl_3 \cdot 6H_2O$ , 96%), *n*-octane ( $C_8H_{18}$ , 99%), benzothiophene (BT,  $C_8H_6S$ , 98%), diallyldimethylammonium chloride ( $C_8H_{16}ClN$ , 97%), 1,4-butane sultone ( $C_4H_8O_3S$ , 98%), cysteamine ( $C_2H_7NS$ ,  $\geq 98.0\%$ ) were purchased from Sigma Aldrich. 4,4'-Azobis(4-cyanovaleric acid) (AVCA,  $C_{12}H_{16}N_4O_4$ , 98%) was obtained from Alfa Aesar. Methanol ( $CH_4O$ , 99.5%), ethanol ( $C_2H_5O$ , 78%), toluene ( $C_7H_8$ ) and dichloromethane ( $CH_2Cl_2$ , 99.5%) were purchased from OCI company Ltd. Triethylenediamine ( $C_6H_{12}N_2$ ,  $>98\%$ ) was obtained from Tokyo Chemicals Ltd. All chemicals were used without further purification.

**Synthesis of MIL-101:** MIL-101 was synthesized from  $CrCl_3 \cdot 6H_2O$ , TPA and deionized water similar to a reported method.<sup>1</sup> The reactants composition was 1.0  $CrCl_3 \cdot 6H_2O$  : 1.0 TPA : 300  $H_2O$ . The precursor of 30 g was loaded in a Teflon-lined autoclave and put in a preheated electric oven at 210 °C for 8 h. After the reaction, the autoclave was cooled to room temperature and solid green-colored products were recovered by filtration. After synthesis, the MOF was purified in three steps. In the first step, 1.0 g MIL-101 was added to 300 mL water and stirred magnetically for 5 h at 70 °C. Then the MOF was filtered and dried overnight in a drying oven. In the second step, the dried MOF was added to 250 mL ethanol; stirred magnetically at 60 °C for 3 h and then filtered. In the third step, the dried MOF from the second step was added to 150 mL 30 mM  $NH_4F$  solution and stirred for 10 h at 60 °C. After that, it was filtered and washed at least five times with hot water and then dried in a drying oven again. Finally, the purified MIL-101 was dehydrated at 150 °C overnight and stored in a desiccator.

**Synthesis of IL/MIL-101-imp:** The acidic chloroaluminate IL was prepared by mixing of 1-butyl-3-methylimidazolium chloride (10 mmol) and AlCl<sub>3</sub> (10 mmol) in a vial to follow the previous report.<sup>1</sup> The vial was sealed and a colorless thick liquid was observed by stirring the mixture for 24 h at 70 °C. IL supported MIL-101 adsorbents were prepared by impregnating IL (33 wt.%) to MIL-101 using dichloromethane as solvent. For example, an exact amount of IL was taken into a vial containing 5 mL of dichloromethane. Dehydrated MIL-101 (0.2 g) was added to that solution and stirred magnetically for 10 min at room temperature. The solvent was evaporated by using a rotary evaporator and the solid was dried overnight in a vacuum oven at 100 °C. Finally, the adsorbent was designated as IL/MIL-101-imp. The handling of IL and IL/MIL-101-imp adsorbents prior to adsorption experiments was carried out under inert conditions in a glove box.

**Synthesis of IL/MIL-101-cov:** The synthesis of covalently bound IL/MIL-101 was carried out according to the reported method with a small modification.<sup>2</sup> In brief, 0.5 g of MIL-101 (dehydrated at under vacuum 150 °C for 12 h), 40 mL of anhydrous toluene, and 2.5 mmol of triethylenediamine were taken in an 100 mL round bottom flask and the mixture was refluxed at 80 °C for 12 h with continuous magnetic stirring. The solids were separated by filtration, washed thoroughly to remove excess triethylene diamine, and again dispersed in 40 mL of anhydrous toluene in a 100 mL round bottom flask. 2.5 mmol of 1,4-butane sultone was added and the solution was refluxed at 80 °C for 12 h with continuous magnetic stirring. The solids were filtered and dried under vacuum at 120 for 4 h. In the final step, the dried solids were suspended in 30mL of ethanol, equivalent of concentrated H<sub>2</sub>SO<sub>4</sub> (98%) was added drop by drop at 50 °C for 24 h. Finally, the catalyst was separated by filtration and dried under vacuum at 60 °C for 12h.

**Synthesis of IL/MIL-101-click:** The IL-fuctionalized MIL-101 was synthesized using the concept of click chemistry reported by Shaplov et al. with small modification.<sup>3</sup> In brief, 0.5 g of MIL-101 (dehydrated at under vacuum 150 °C for 12 h), 30 mL of anhydrous toluene, and 1.0 mmol of cysteamine were taken in an 100 mL round bottom flask and the mixture was refluxed at 110 °C for 12 h with continuous magnetic stirring. The solids were separated by filtration and termed as MIL-101-SH. 0.4 g MIL-101-SH, 6 mL H<sub>2</sub>O, 0.01 g AVCA (initiator) and 0.5 g diallyldimethylammonium chloride was taken in around bottom flask and the solution was stirred magnetically for 4 h at 70 °C. The solids were collected after vacuum drying at 70 °C. The obtained solids (0.5 g) were dispersed in 5 mL dichloromethane and 0.005 g AlCl<sub>3</sub> was added. The mixture was stirred magnetically for 10 min at room temperature. The solvent was evaporated by using a rotary evaporator and the solid was dried overnight in a vacuum oven at 100 °C.

**Adsorption experiments:** All the adsorption capacities (mg/g) were calculated from the difference between final and initial concentrations of an adsorbate by using following equation:

$$q_t = \frac{(C_i - C_f)V}{m}$$

Where,

$q_t$  = adsorbed amount in time t (mg/g)

$C_i$  = initial concentration of the adsorbate (mg/ml)

$C_f$  = final concentration after adsorption (mg/ml)

$V$  = volume of the solution subjected to a single adsorption (ml)

$m$  = mass of the adsorbent taken during a single adsorption (g)

**Calculation of maximum adsorption capacity ( $Q_0$ ):** The maximum adsorption capacity ( $Q_0$ ) was calculated using the Langmuir adsorption isotherm. The adsorption isotherms for different adsorbents were plotted according to the Langmuir equation<sup>4,5</sup>

$$\frac{C_e}{q_e} = \frac{C_e}{Q_0} + \frac{1}{Q_0 b}$$

Where,

$C_e$ : the equilibrium concentration of the adsorbate (mg/L)

$q_e$ : the amount adsorbed at equilibrium (mg/g)

$Q_0$ : the Langmuir constant (maximum adsorption capacity, mg/g)

$b$ : the Langmuir constant (L/mg)

Therefore, the maximum adsorption capacity,  $Q_0$ , could be obtained from the reciprocal of the slope of a plot of  $C_e/q_e$  against  $C_e$ .

**Separation factor:** The separation factor ( $R_L$ ) was calculated using the following equation that describes the adsorption process:<sup>6-8</sup>

$$R_L = \frac{1}{1 + bC_0}$$

Where,

$R_L$ : separation factor

$b$ : the Langmuir constant (L/mg)

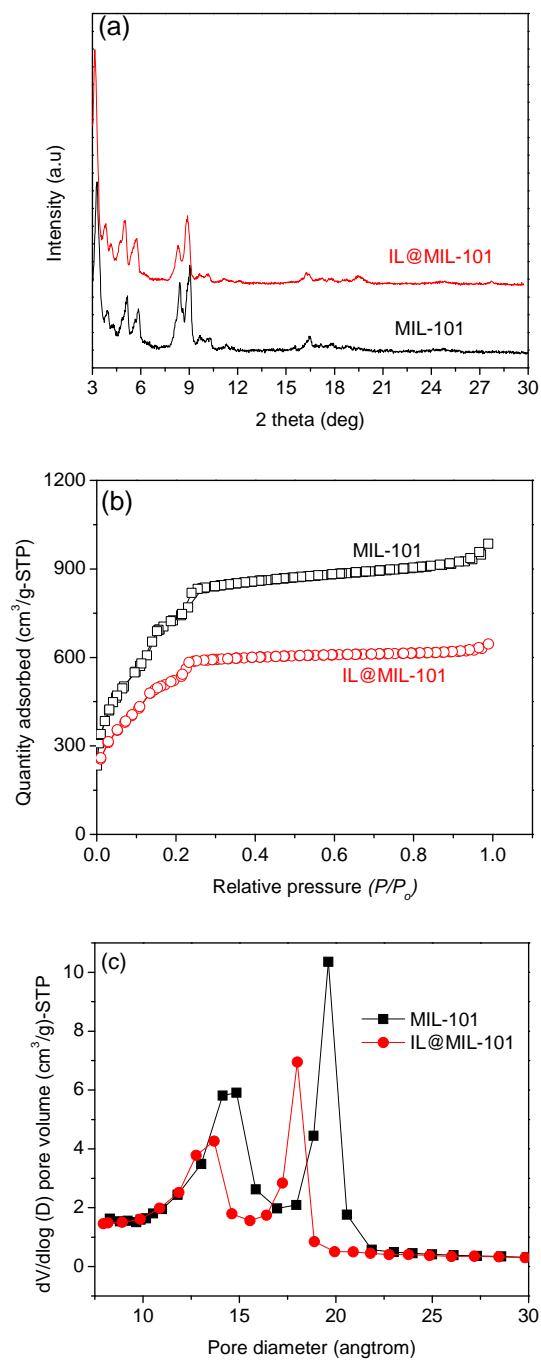
$C_0$ : initial concentration of adsorbate (mg/L)

**Adsorbent regeneration:** The used adsorbents were reactivated for further utilization following the two consecutive procedure. Firstly, the used adsorbent was soaked into n-octane solvent and allowed to stir 12 h at room temperature. While, the solvent was exchanged three times with fresh n-octane to wash out the adsorbed BT from the adsorbent. In next step,

the solid adsorbent was filtered and dried at 100 °C for 12 h. Then the dried adsorbent was heated at 230 °C under vacuum to evaporate the remaining adsorbed materials.

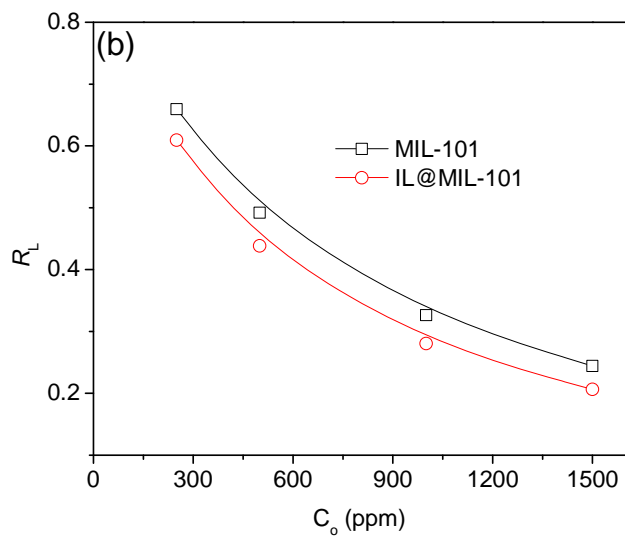
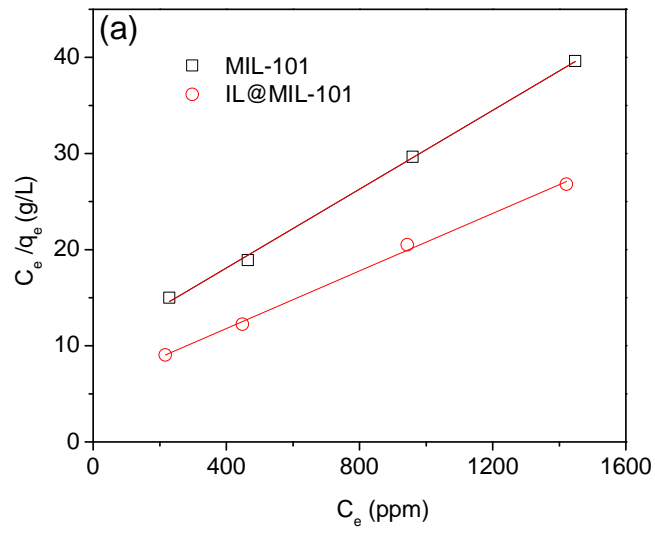
## Reference:

1. N. A. Khan, Z. Hasan and S. H. Jhung, *Chem. Eur. J.*, 2014, **20**, 376.
2. Q.-X. Luo, M. Ji, M.-H. Lu, C. Hao, J.-S. Qiu and Y.-Q. Li, *J. Mater. Chem. A*, 2013, **1**, 6530.
3. A. S. Shaplov, P. S. Vlasov, E. I. Lozinskaya, O. A. Shishkan, D. O. Ponkratov, I. A. Malyshkina, F. Vidal, C. Wandrey, I. A. Godovikov and Y. S. Vygodskii, *Macromol. Chem. Phys.* 2012, **213**, 1359.
4. B. H. Hameed and A.A. Rahman, *J. Hazard. Mater.* 2008, **160**, 576.
5. S.-H. Lin and R.-S. Juang, *J. Environ. Manag.* 2009, **90**, 1336.
6. T. W. Weber and R.K. Chakkravorti, *AIChE J.* 1974, **20**, 228.
7. Y. Önal, C. Akmil-Basar and C. Sarıcı-Özdemir, *J. Hazard. Mater.* 2007, **148**, 727.
8. K. P. Singh, D. Mohan, S. Sinha, G.S. Tondon, *Ind. Eng. Chem. Res.* 2003, **42**, 1965.

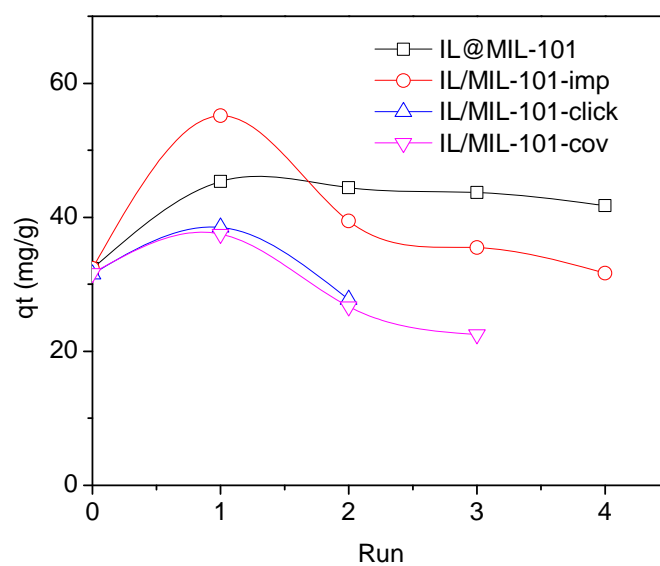


**Fig. S1.** (a) XRD patterns; (b) nitrogen adsorption-desorption isotherms and (c) BJH pore size distributions of the adsorbents.

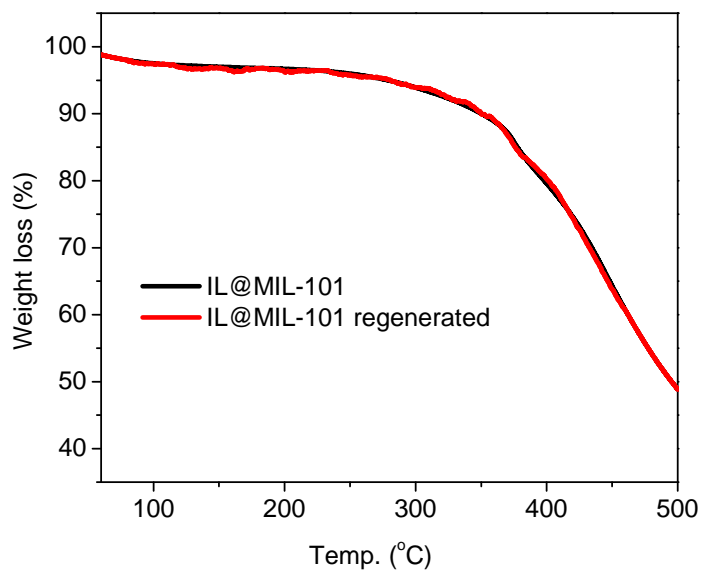




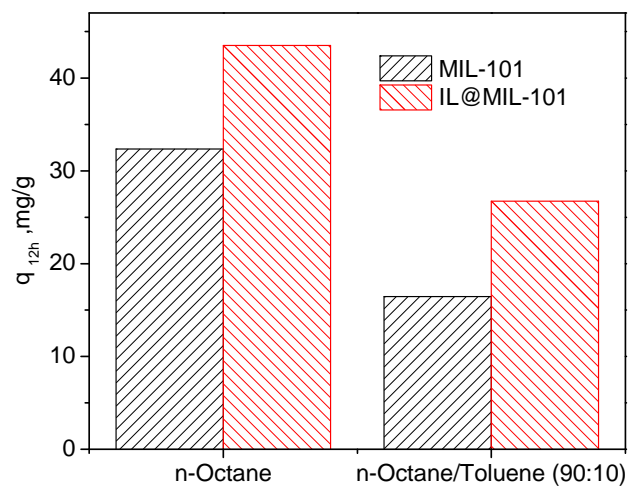
**Fig. S2.** (a) Langmuir plots and (b) effect of initial BT concentrations on the separation factor  $R_L$  for the adsorption.



**Fig. S3.** Reusability of the adsorbents for the adsorption of BT. The initial BT concentration was 1000 ppm.



**Fig. S4.** Results of thermogravimetric analyses of the fresh and regenerated (after use once) IL@MIL-101.



**Fig. S5.** Effect of co-presence of toluene in solvent on the adsorption of BT with MIL-101 and IL@MIL-101. The initial BT concentration was 1000 ppm.