

Supporting Information

The Role of MnO_x Doped in CeO₂ for Catalytic Synthesis of Aliphatic Carbamate from CO₂

Ran Zhang, Li Guo, Chen Chen, Jizhong Chen, Angjun Chen, Xiuge Zhao,
Xuerui Liu, Yuhe Xiu, Zhenshan Hou*

Key Laboratory for Advanced Materials, Research Institute of Industrial Catalysis,
East China University of Science and Technology, Shanghai, 200237, China.

E-mail: houzhenshan@ecust.edu.cn

Table S1. Relative molar sensitivity of all the products toward toluene (internal standard)

Reactants or products	Relative molar sensitivity
<i>n</i> -butylamine (BA)	1.68
Dibutylurea (DBU)	2.51
dimethyl carbonate (DMC)	3.33
N-butylcarbamate (NBCB)	2.05

Table S2 The catalytic performance with the different ratios of BA to catalyst over MnO_x(0.03)-CeO₂ catalyst^a

Entry	Sub./Cat. (molar ratio)	Conv. (%)	Sel. _{NBCB} (%)	Sel. _{DBU} (%)
1	3	81.8	68.1	31.9
2	4	79.1	67.3	32.7
3	9	61.8	60.7	39.3

^aReaction condition: BA: CH₃OH = 5 mmol : 200 mmol, t = 16 h, T = 170 °C, P = 5.0 MPa

Table S3 The catalytic performance with the different ratios of BA to CH₃OH over MnO_x(0.03)-CeO₂ catalyst^a

Entry	BA/CH ₃ OH (molar ratio)	Conv. (%)	Sel. _{NBCB} (%)	Sel. _{DBU} (%)
1	5:100	80.6	53.7	46.3
2	5:200	86.5	74.5	25.5
3	5:400	88.4	87.4	12.6
4	5:500	91.1	89.3	10.7
5	5:600	91.3	92.7	7.3

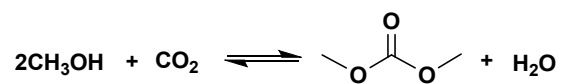
^aReaction condition: BA: 5 mmol, t = 8 h, T = 170 °C, P = 5.0 MPa, 0.3 g catalyst.

Table S4 BET surface area of CeO₂-based catalysts

Entry	Catalyst	BET surface /m ² ·g ⁻¹
1	Lab-com	8.0
2	Lab-CeO ₂	31.7
3 ^a	The spent Lab-CeO ₂	24.1
4	MnO _x (0.03)-CeO ₂	68.2
5 ^a	The spent MnO _x (0.03)-CeO ₂	52.9
6	MnO _x	14.9

^aThe BET surface area was measured after four catalytic recycles.

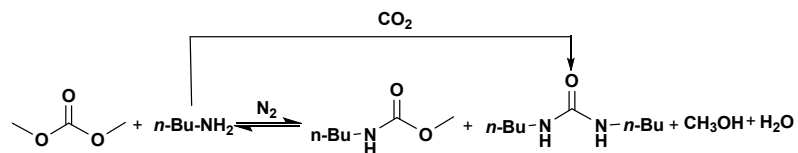
Table S5 The reaction of methanol with CO₂ over CeO₂-based catalysts^a



Entry	Catalyst	Reactants /mmol		n _{DMC}
		CH ₃ OH	CO ₂	/mmol
1	Lab-CeO ₂	500	5 MPa	0.21
2	MnO _x (0.03)-CeO ₂	500	5 MPa	0.28

^aReaction condition: T = 170 °C, P = 5.0 MPa, t = 8 h, catalyst 0.3 g. ^bDMC was detected as a sole product.

Table S6 The carbonylation of BA with DMC under the pressure of N₂ or CO₂^a.



Entry	Catalyst	Atmosphere	Reactants /mmol		Products /mmol	
			n _{BA}	n _{DMC}	n _{DBU}	n _{NBCB}
1	MnO _x (0.03)-CeO ₂	N ₂	5	2.5	0.058	0.65
^b 2	MnO _x (0.03)-CeO ₂	CO ₂	5	5	1.95	0.84

^aReaction condition: CH₃OH = 500 mmol, T = 170 °C, P = 5.0 MPa, t = 8 h, catalyst 0.3 g. ^bno solvent.

Table S7 Summary of the results of XPS analysis

Entry	Catalyst	u ^{'''} / total area	^a Mn/ Mn+Ce	Mn (%)	Ce (%)	O (%)	O distribution		
							O _L	O _s	O _a
1	Lab-CeO ₂	0.126	-	0	29.1	70.9	61.5	6.9	2.5
2	the spent Lab-CeO ₂	0.133	-	0	27.6	72.4	61.4	9.3	1.7
3	MnO _x (0.03)-CeO ₂	0.125	0.03	1.0	32.0	67.0	60.1	5.6	1.3
4	the spent MnO _x (0.03)-CeO ₂	0.126	0.037	1.2	29.8	69.0	57.6	8.8	2.6

^a The values estimated by XPS analysis; The ICP value of Mn/Mn+Ce was 0.03

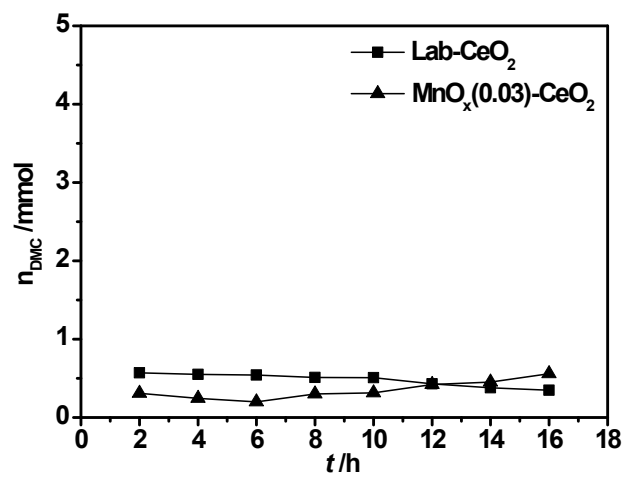


Figure S1 The n_{DMC} versus time profile over Lab- CeO_2 (A) and $\text{MnO}_x(0.03)\text{-CeO}_2$ (B) catalysts. Reaction condition: BA: CH_3OH = 5 mmol : 200 mmol, $T = 170\text{ }^\circ\text{C}$, $P = 5.0\text{ MPa}$, catalyst 0.3 g.

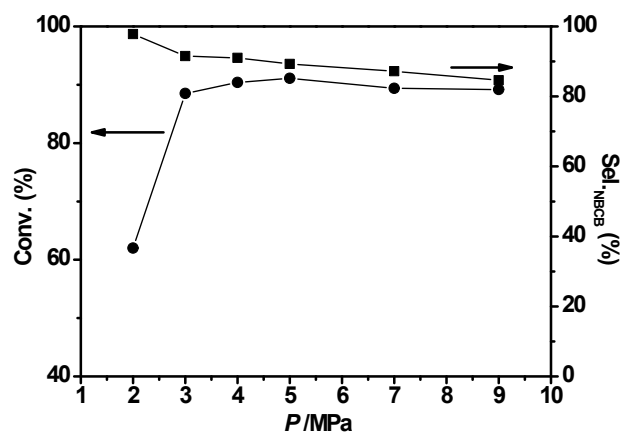


Figure S2 The effect of pressure on the reaction of BA+CO₂+CH₃OH over the MnO_x(0.03)-CeO₂ catalyst. Reaction condition: BA: CH₃OH = 5 mmol : 500 mmol, T = 170 °C, t = 8 h, catalyst 0.3 g.

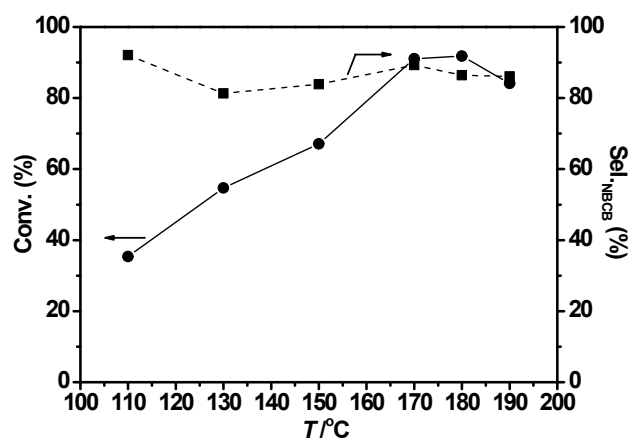


Figure S3 The effect of temperature in the reaction of BA+CO₂+CH₃OH over the MnO_x (0.03)-CeO₂ catalyst. Reaction condition: BA: CH₃OH = 5 mmol : 500 mmol, P = 5 MPa, t = 8 h, catalyst 0.3 g.

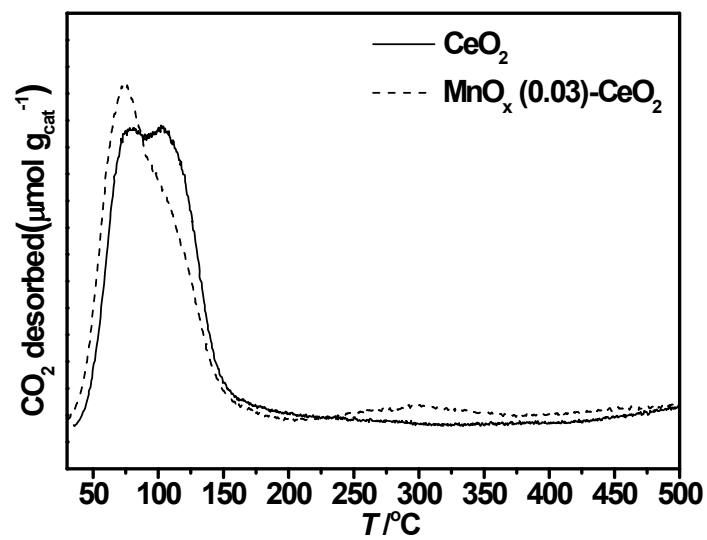


Figure S4 CO₂-TPD profiles of Lab-CeO₂ (solid line) and MnO_x(0.03)-CeO₂ (dashed line). Conditions: He 50 ml·min⁻¹; CO₂ adsorbed at 25 °C for 30 min.