

**Selective Hydrodeoxygenation of Bio-Oil Derived
Products: Ketones to Olefins**
Ayut Witsuthammakul and Tawan Sooknoi*

Supporting information

Table S1 % Metal content and surface area of metal catalysts and supports

Catalyst	Metal content wt%	BET surface area (m ² /g)	Catalyst	Metal content wt%	BET surface area (m ² /g)
2%Cr/SiO ₂	2.03	244	2%NiCu/SiO ₂ (25%Cu)	0.58(Cu);1.64(Ni)	240
10%Cr/SiO ₂	9.17	231	2%NiCu/SiO ₂ (50%Cu)	1.04(Cu);1.10(Ni)	241
2%Fe/SiO ₂	2.08	243	2%NiCu/SiO ₂ (70%Cu)	1.58(Cu);0.56(Ni)	238
10%Fe/SiO ₂	9.86	229	2%NiCu/SiO ₂ (80%Cu)	1.90(Cu);0.43(Ni)	238
2%Co/SiO ₂	1.81	245	SiO ₂	-	246
2%Pd/SiO ₂	1.70	238	5%Cu/HY (100)	5.08	568
2%Ni/SiO ₂	2.12	239	HY (100)	-	713
5%Ni/SiO ₂	5.01	234	5%Cu/HZSM-5 (250)	5.22	361
8%Ni/SiO ₂	8.05	212	HZSM-5 (250)	-	376
20%Ni/SiO ₂	20.3	208	H-β (14)	-	523
40%Ni/SiO ₂	42.0	137			
2%Cu/SiO ₂	2.05	242			
5%Cu/SiO ₂	5.08	240			
10%Cu/SiO ₂	10.7	220			
15%Cu/SiO ₂	16.4	214			
40%Cu/SiO ₂	36.1	144			

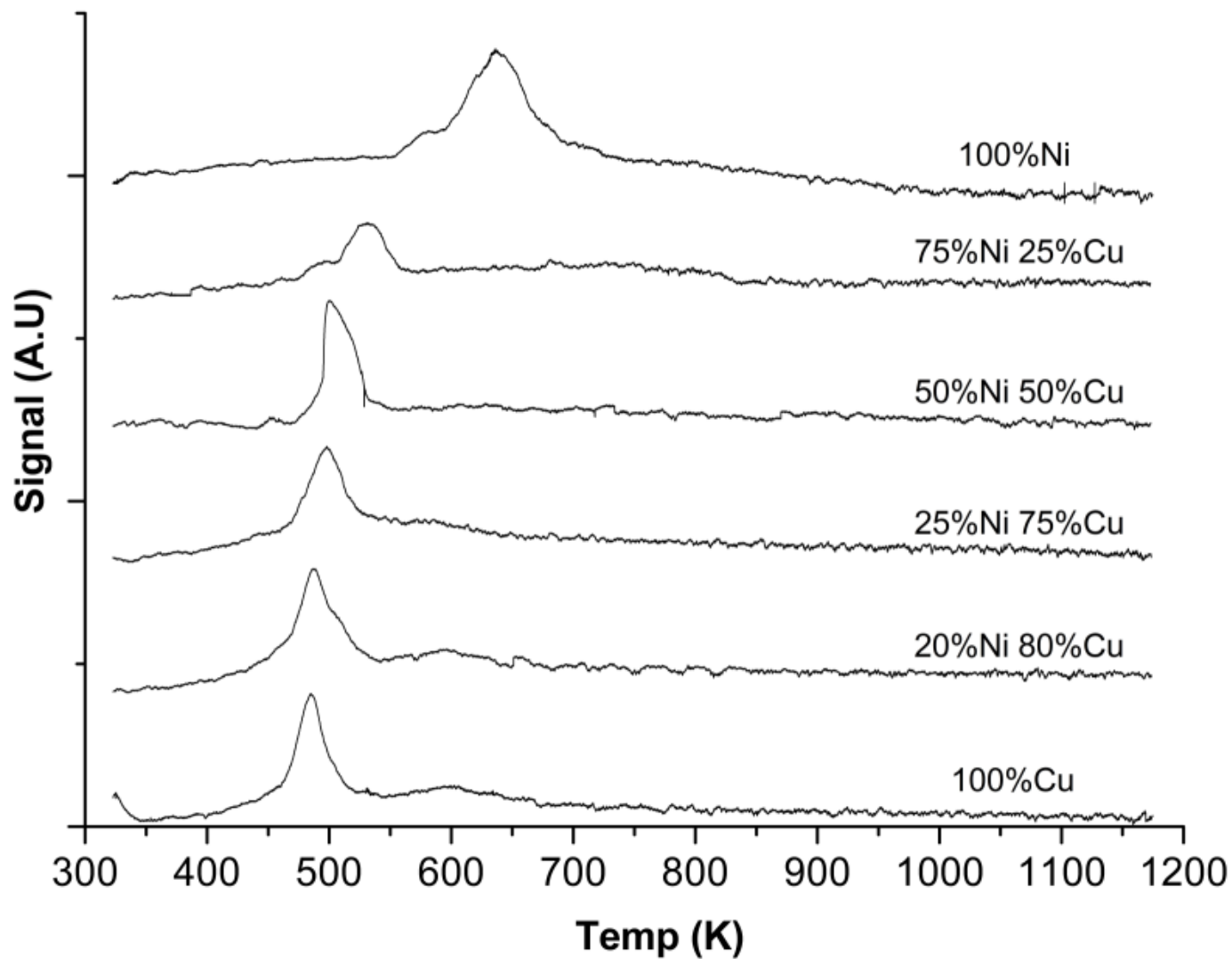


Figure S1 Temperature program reduction of 2% Ni-Cu alloy on SiO₂

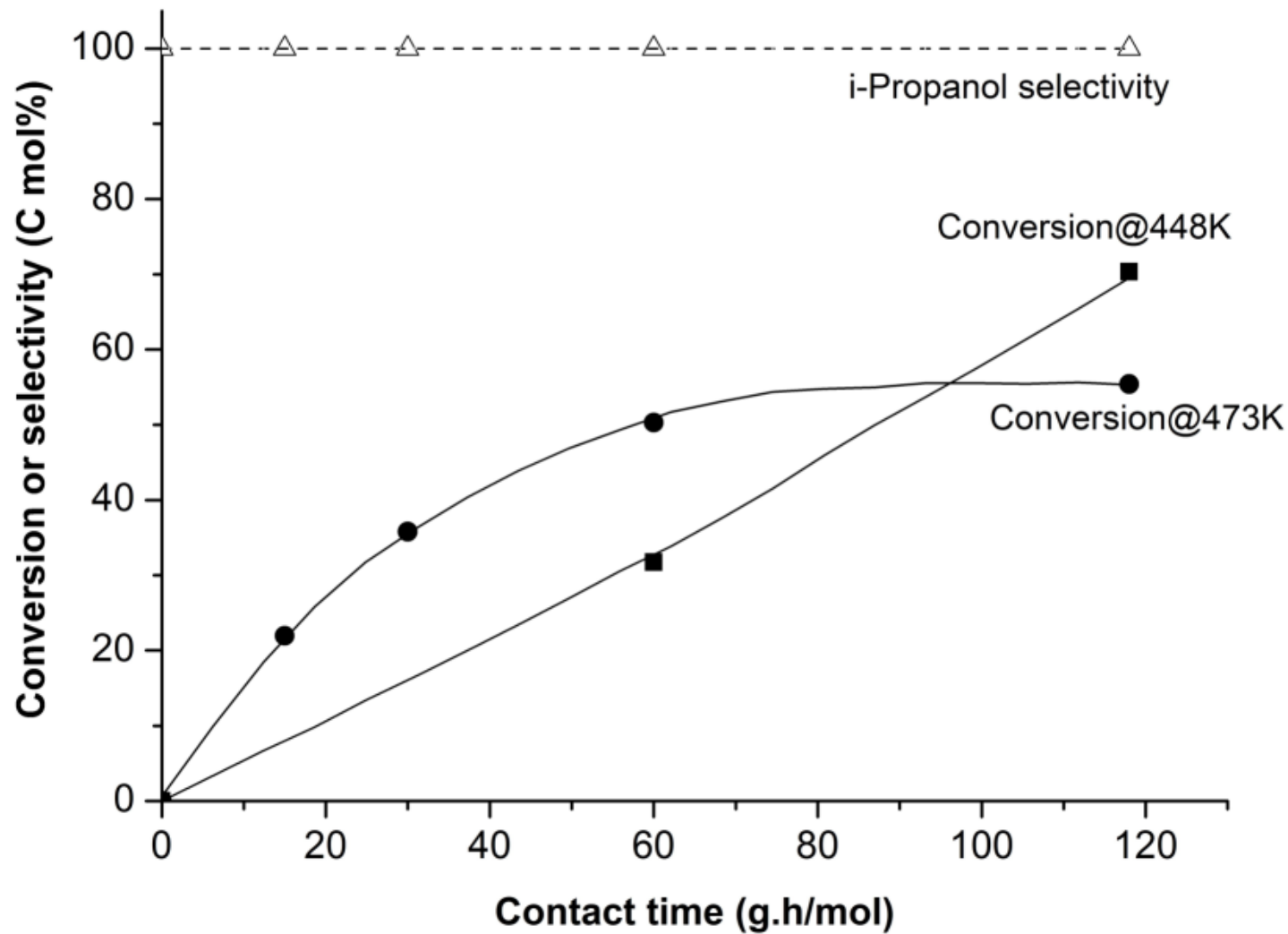


Figure S2 Effect of contact time for acetone hydrogenation on 2%Cu/SiO₂ at 448 and 473 K; H₂ as carrier 30 m/min

Table S2 Copper surface area and turnover frequency for acetone conversion

Catalyst	H₂ consumption mmol.g ⁻¹ _{Cu})	Cu area (m ² .g ⁻¹ _{Cu})	Contact time (g.h.mol ⁻¹)	TOF x10 ⁻³ (h ⁻¹)
2%Cu/SiO₂	0.51	257	30	n/a
5%Cu/SiO₂	1.6	646	30	2.5
10%Cu/SiO₂	3.3	437	30	2.1
15%Cu/SiO₂	7.1	220	30	2.7
5%Cu/HY (100)	1.7	499	19	7.2
5%Cu/HZSM-5 (250)	1.7	414	19	4.9

^aHydrogenation at 473 K

^bHydrodeoxygenation at 473 K