

### Electronic Supplementary Information

Methanation of CO<sub>2</sub> and reverse water gas shift reactions on Ni/SiO<sub>2</sub> catalysts: The  
influence of particle size on selectivity and reaction pathway

H.C. Wu<sup>a</sup>, Y.C. Chang<sup>b</sup>, J.H. Wu<sup>a</sup>, J.H. Lin<sup>c</sup>, I.K. Lin<sup>c</sup>, C.S. Chen<sup>a,\*</sup>

<sup>a</sup>Center for General Education, Chang Gung University, 259, Wen-Hua 1st Rd.,

Guishan Dist., Taoyuan City 33302, Taiwan, Republic of China

<sup>b</sup>Taiwan Power Research Institute, 84, Ta-An Road, Shu-Lin Taipei New City 23847

Taiwan, Republic of China

<sup>c</sup>Department of Materials Science, National University of Tainan, 33, Sec. 2, Shu-Lin

St., Tainan 700, Taiwan, Republic of China

Table S1 Characterization of the 0.5 wt% and 10 wt% Ni/SiO<sub>2</sub> catalysts

Catalyst	CO adsorption ( $\mu\text{mol/g cat.}$ )	Ni surface area <sup>a</sup> ( $\text{m}^2/\text{g}$ )	Ni particle size <sup>b</sup> (nm)
0.5 wt% Ni/SiO <sub>2</sub>	8.5	0.33	nd <sup>c</sup>
10 wt% Ni/SiO <sub>2</sub>	68.8	2.68	9

<sup>a</sup> Estimated from CO chemisorption.

<sup>b</sup> Estimated from the XRD spectra in Figure 1.

<sup>c</sup> The XRD pattern was too weak to be observed.

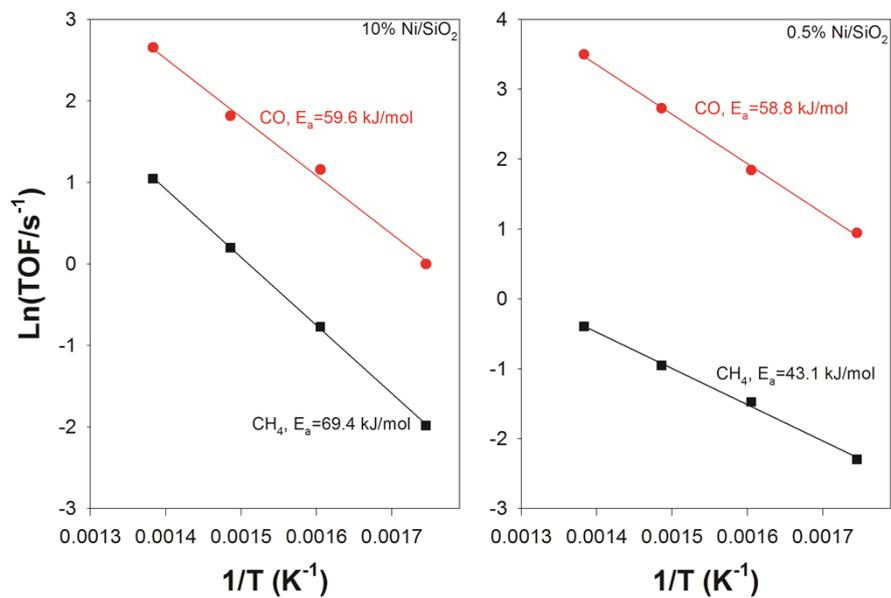


Fig. S1 Arrhenius plots for the TOF of CO CH<sub>4</sub> formation from CO<sub>2</sub> hydrogenation on Ni/SiO<sub>2</sub> catalysts.

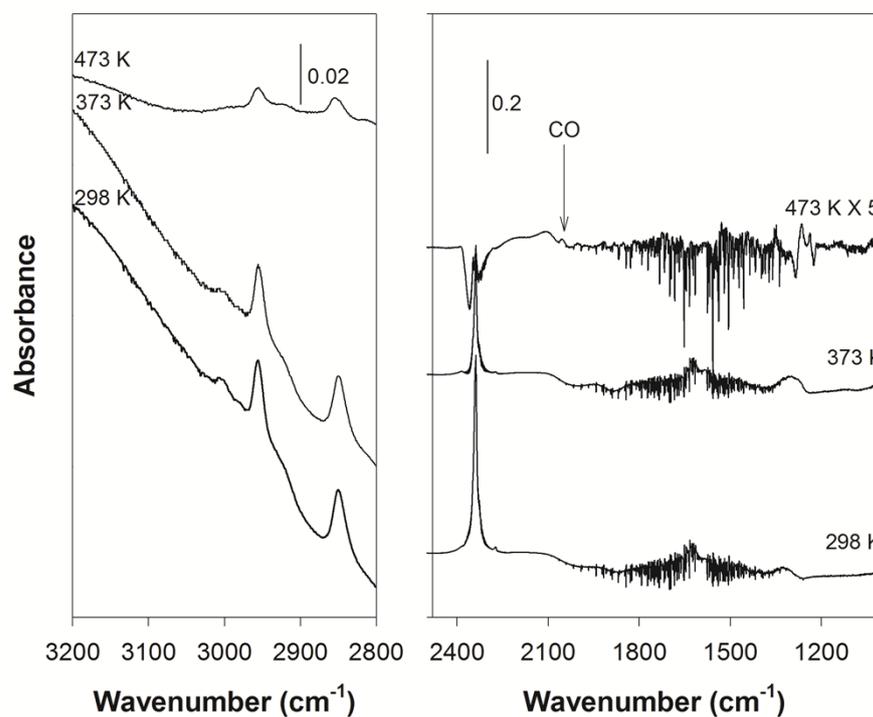


Fig. S2 IR spectra of  $\text{H}_2$  and  $\text{CO}_2$  co-adsorbed on the 0.5 wt% Ni/ $\text{SiO}_2$  catalyst at various temperatures. All experiments were performed by passing a pure  $\text{CO}_2$  stream (20 mL/min) over the catalysts for 20 min at 298 K, followed by purging the  $\text{CO}_2$  with a He stream (20 mL/min). The IR spectra were recorded to monitor the adsorbed  $\text{CO}_2$  on Ni/ $\text{SiO}_2$  under a  $\text{H}_2$  stream at elevated temperatures.

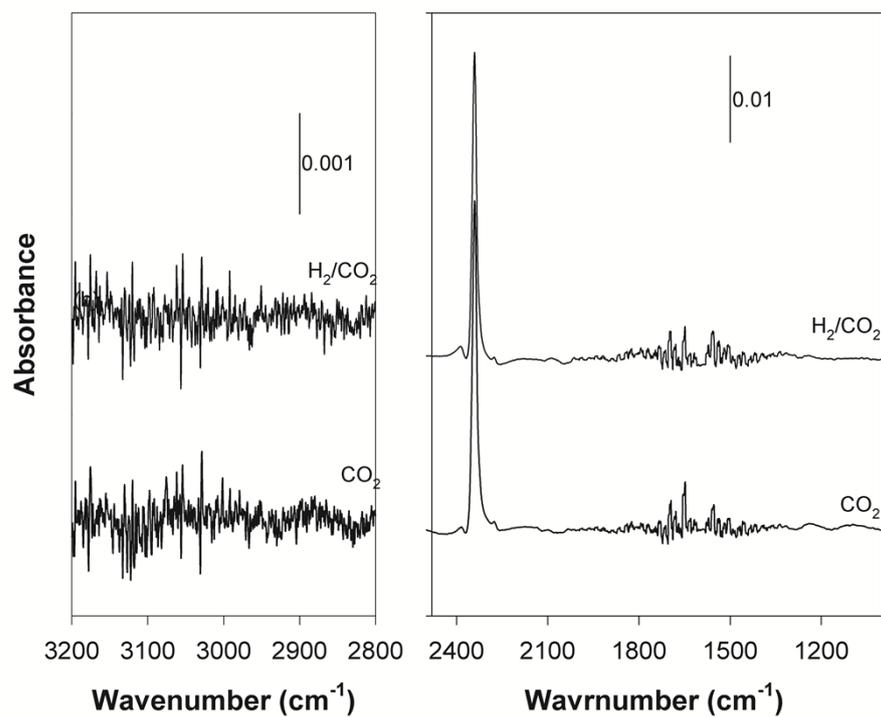


Fig. S3 IR spectra of CO<sub>2</sub> and H<sub>2</sub>/CO<sub>2</sub> adsorbed on the SiO<sub>2</sub> at room temperature. All experiments were performed by passing a pure CO<sub>2</sub> stream (20 mL/min) over the catalysts for 20 min at 298 K, followed by purging the CO<sub>2</sub> with a He stream (20 mL/min). The IR spectrum of H<sub>2</sub> and CO<sub>2</sub> co-adsorption was recorded to monitor the adsorbed CO<sub>2</sub> on SiO<sub>2</sub> under a H<sub>2</sub> stream at room temperature.

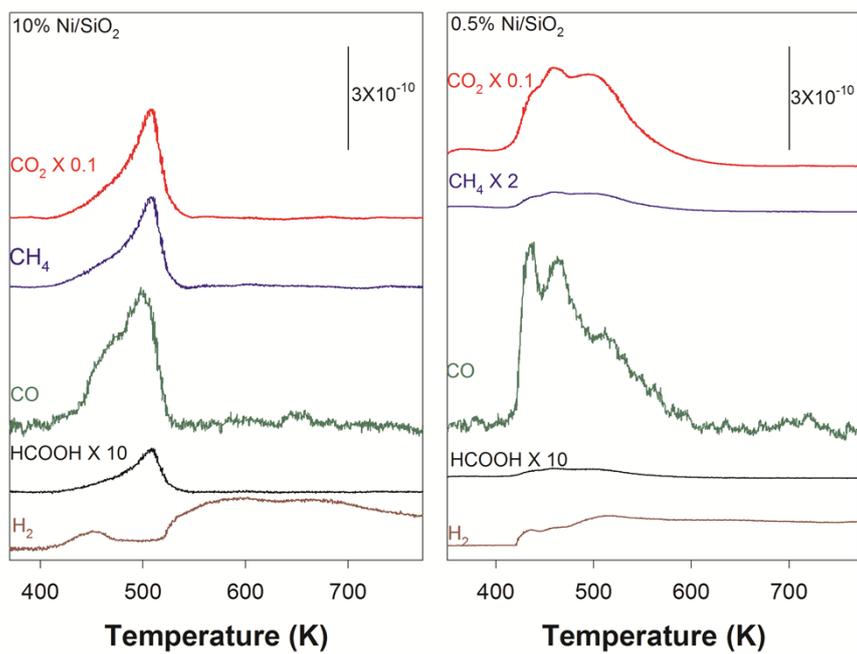


Fig.S4 TPD spectra of the 0.5 wt% and 10 wt% Ni/SiO<sub>2</sub> catalysts at 298 K after a 1-  
 μL dose of formic acid.

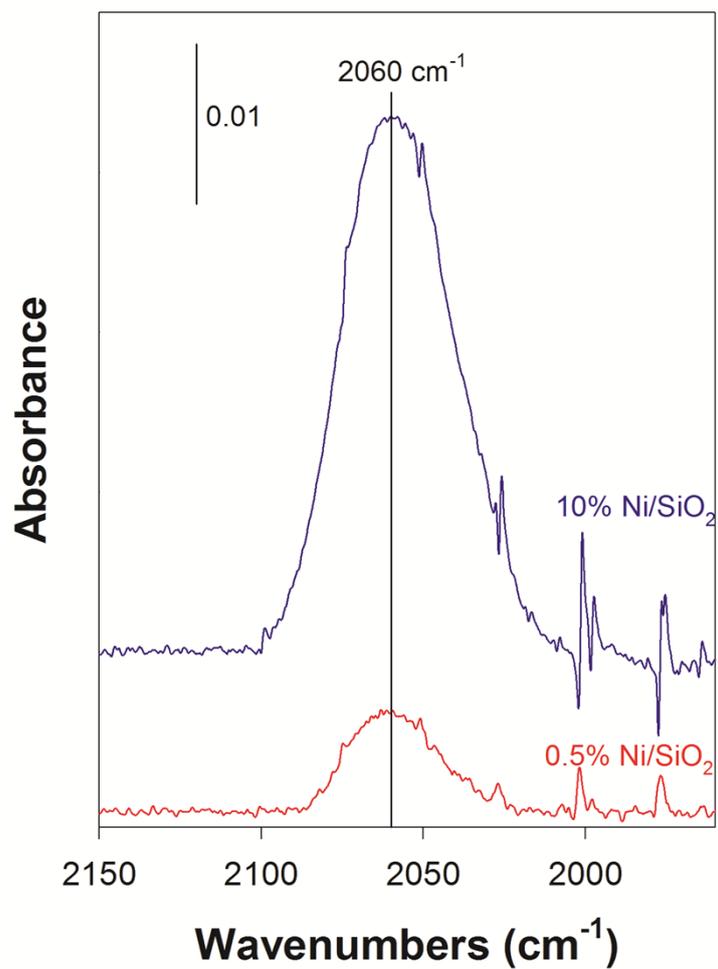
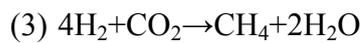
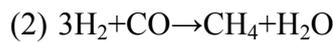
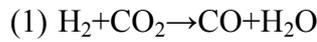


Fig. S5 IR spectra of the CO adsorbed on the reduced 0.5 wt% and 10 wt% Ni/SiO<sub>2</sub> catalysts at 298 K.

## Appendix

Far away from equilibrium conditions, the steady-state rate of CO<sub>2</sub> hydrogenation to form CO and CH<sub>4</sub> via parallel and consecutive reaction network is described by the following equations:

The possible reaction network of CO<sub>2</sub> hydrogenation can be described:



(A) parallel pathway:

$$\frac{r_{\text{CO}}}{r_{\text{CH}_4}} = \frac{k_1 P_{\text{H}_2}^{1.1} P_{\text{CO}_2}^{0.06}}{k_3 P_{\text{H}_2}^{1.1} P_{\text{CO}_2}^{0.06}} = \frac{k_1}{k_3}$$

$$\text{Selectivity of CH}_4: S_{\text{CH}_4} = \frac{r_{\text{CH}_4}}{r_{\text{CO}} + r_{\text{CH}_4}} = \frac{k_3}{k_1 + k_3}$$

(B) consecutive pathway:

$$\frac{r_{\text{CO}}}{r_{\text{CH}_4}} = \frac{k_1 P_{\text{H}_2}^{0.3} P_{\text{CO}_2}^{0.5} - k_2 P_{\text{H}_2}^{0.3} P_{\text{CO}_2}^{0.5} X_{\text{CO}_2}}{k_2 P_{\text{H}_2}^{0.3} P_{\text{CO}_2}^{0.5} X_{\text{CO}_2}} \quad (X_{\text{CO}_2} : \text{CO}_2 \text{ conversion})$$

$$\text{Selectivity of CH}_4: S_{\text{CH}_4} = \frac{r_{\text{CH}_4}}{r_{\text{CO}} + r_{\text{CH}_4}} = \frac{k_2 P_{\text{H}_2}^{0.3} P_{\text{CO}_2}^{0.5} X_{\text{CO}_2}}{k_1 P_{\text{H}_2}^{0.3} P_{\text{CO}_2}^{0.5} + k_2 P_{\text{H}_2}^{0.3} P_{\text{CO}_2}^{0.5} X_{\text{CO}_2}} = \frac{k_2}{k_1} X_{\text{CO}_2}$$