

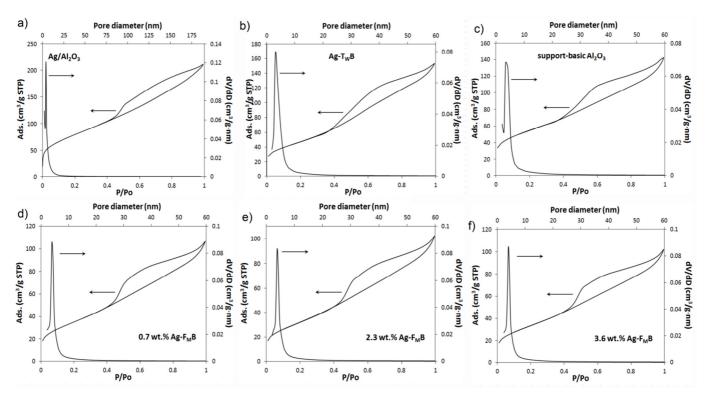
## **Catalysis Science & Technology**

**Electronic Supplementary Information (ESI)** 

# Performance of $Ag/Al_2O_3$ catalysts in the liquid phase oxidation of glycerol – effect of preparation method and reaction conditions

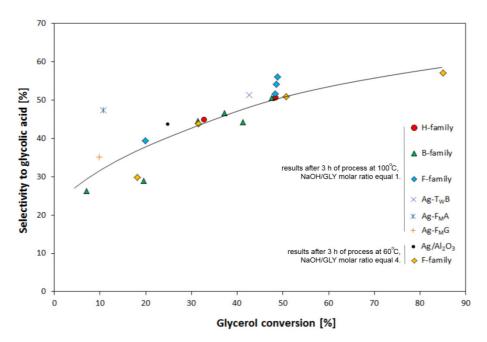
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#### ESI 1 - N<sub>2</sub> adsorption-desorption isotherms.



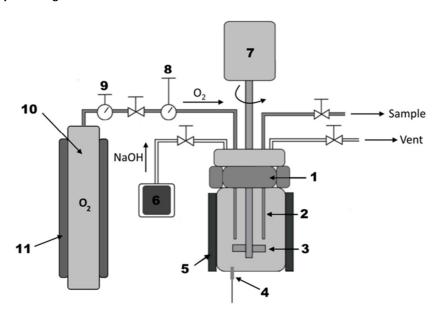
Nitrogen adsorption/desorption profiles and calculated pore diameter distribution (BJH method) of fresh catalyst samples: (a) commercial  $Ag/Al_2O_3$ ; (b) catalyst  $Ag-T_WB$  prepared by thermal reduction method; (c) basic alumina support; (d-f) catalysts prepared by formal dehyde reduction method with various silver loading.

### ESI 2 – Selectivity to glycolic acid as a function of glycerol conversion over the supported silver catalysts.



Selectivity to glycolic acid plotted as a function of glycerol conversion over all the tested catalysts. Main reaction conditions: 3 h of process, 5 bars of oxygen, 0.5 g of catalyst, 200 cm<sup>3</sup> of a 0.3 M pure glycerol solution, reaction temperature and NaOH/GLY molar ratio as stated on the figure.

### ESI 3 - Scheme of the catalytic test rig.

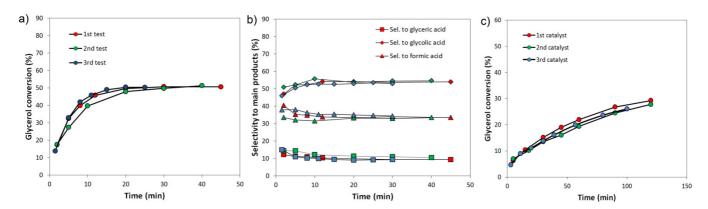


#### Elements on scheme:

- 1. Autoclave
- 2. Sampling line
- 3. Stirrer
- 4. Thermocouple

- 5. Heating ring for autoclave
- 6. High pressure pump
- 7. Stirrer controller
- 8. Reactor pressure controller
- 9. Oxygen reserve controller
- 10. Oxygen reserve
- 11. Heating ring for oxygen reserve

### ESI 4 – Reproducibility of the results.



Glycerol conversions and selectivities to the main products observed during three independent tests using the 3.6 wt.% Ag- $F_MB$  catalyst (figures a & b) at 100 °C and NaOH/GLY = 1 molar ratio, and comparison of the glycerol conversion using three different baths of 1.1 wt.% Ag- $F_MB$  catalyst (figure c) at 60 °C using NaOH/GLY molar ratio of 4. Other reaction conditions: 0.5 g of catalyst, 200 cm<sup>3</sup> of a 0.3 M pure glycerol solution, 5 bars of oxygen, 1500 rpm.