

Electronic Supporting Information

Improvement in the catalytic properties of ZSM-5 zeolite nanoparticles via mechanochemical and chemical modifications

Satoshi Inagaki,^{a,*} Shoma Shinoda,^a Shunsuke Hayashi,^a Toru Wakihara,^b Hiroshi Yamazaki,^c Junko N. Kondo,^c Yoshihiro Kubota^{a,*}

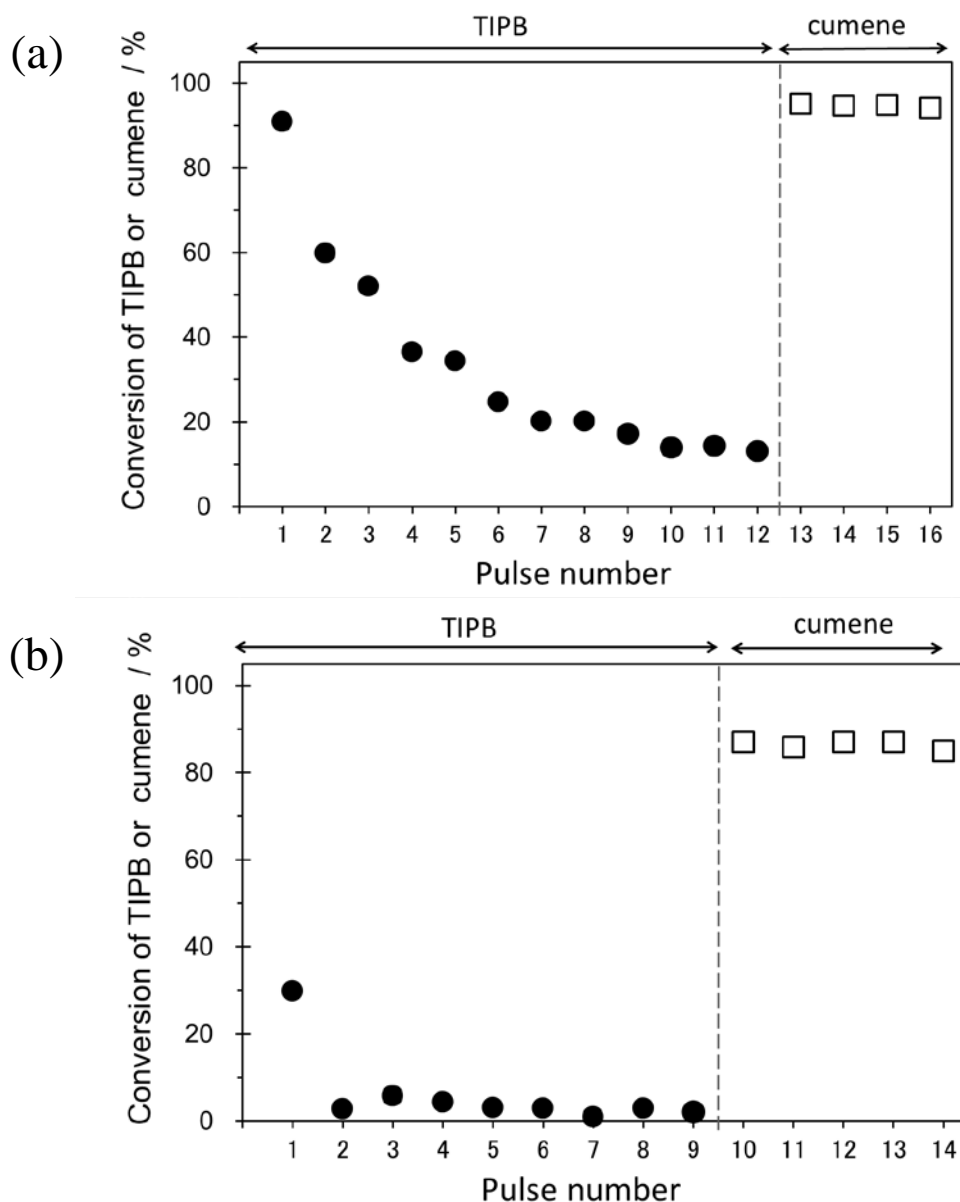


Figure S1 Catalytic cracking of 1,3,5-triisopropylbenzene or cumene at 300 °C over (a) ZSM-5 nanoparticles (Si/Al = 21.1), and (b) acid-treated ZSM-5 nanoparticles (Si/Al = 49.7). Reaction conditions: weight of catalyst, 20 mg; pellet size, 500–600 μm ; TIPB, 0.6 μL ; cumene, 0.8 μL ; He gas flow rate, 30.0 $\text{cm}^3(\text{N.T.P.}) \text{min}^{-1}$.

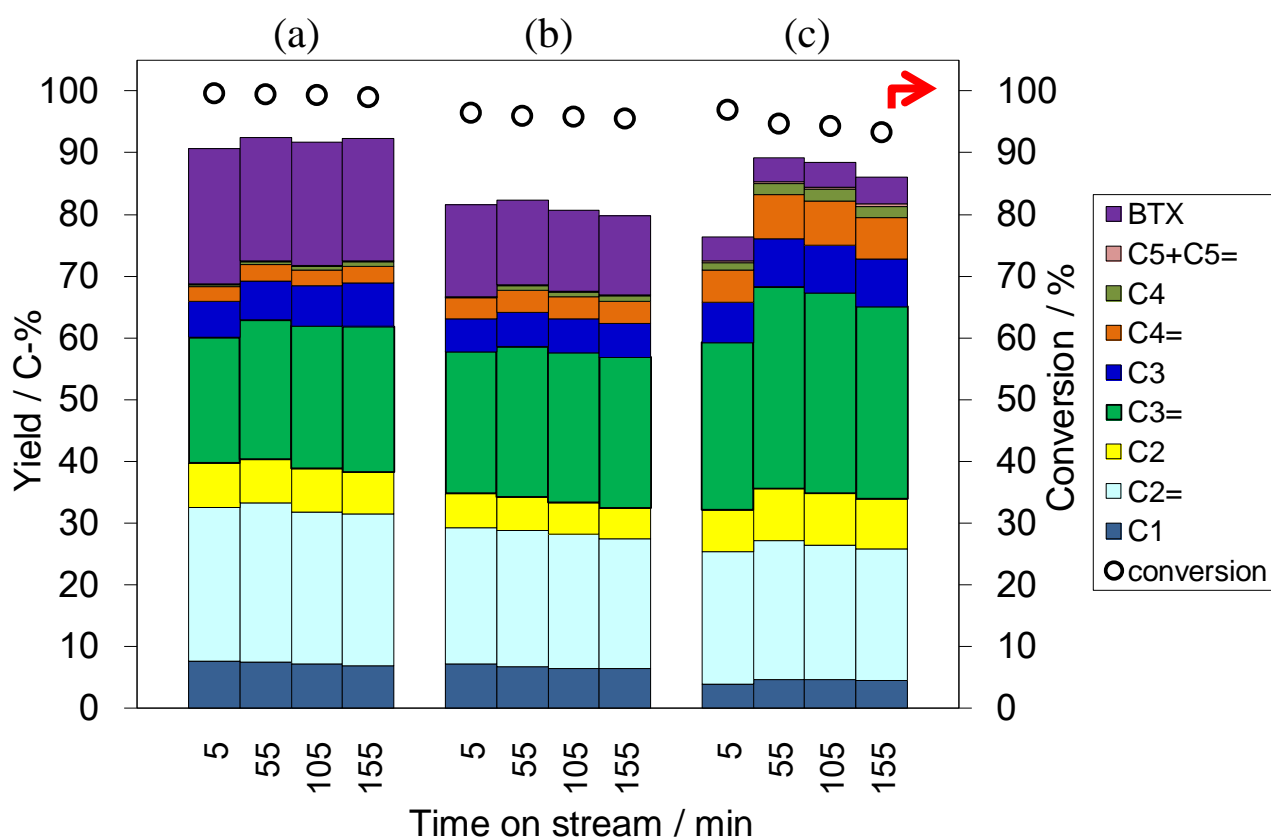


Figure S2 Product yields in hexane cracking at 650 °C over various ZSM-5 catalysts after adjusting the conversions at a similar level.

(a) Milled and recrystallized ZSM-5 nanoparticles (Si/Al = 21.1, 100 mg, W/F = 19.8 g h mol⁻¹); the same data as shown in Fig. 6e. The coke amount on the spent catalyst was 65.1 mg-coke/g-catalyst.

(b) Milled and recrystallized ZSM-5 nanoparticles (Si/Al = 21.1, 50 mg, W/F = 9.9 g h mol⁻¹). The coke amount on the spent catalyst was 23.9 mg-coke/g-catalyst.

(c) Milled, recrystallized and acid-treated ZSM-5 nanoparticles (Si/Al = 49.7, 100 mg, W/F = 19.8 g h mol⁻¹); the same data as shown in Fig. 6f. The coke amount on the spent catalyst was 7.2 mg-coke/g-catalyst.