

Supporting Information for

Observability of anammox activity in single-stage nitrification/anammox reactors using mass balances

Sarina Schielke-Jenni^a, Kris Villez^a, Eberhard Morgenroth^{a,b}, Kai M. Udert^{a*}

^aSwiss Federal Institute of Aquatic Science and Technology (EAWAG), 8600 Dübendorf, Switzerland, ^bInstitute of Environmental Engineering, ETH Zürich, 8093 Zürich, Switzerland

***Corresponding author:**

Kai M. Udert
Department of Process Engineering
Eawag- Swiss Federal Institute of Aquatic Science and Technology
Überlandstrasse 133
P.O.Box 611
8600 Dübendorf
Switzerland
Phone: +41-58-765-53-60
Fax: +41-58-765-58-02
E-mail: kai.udert@eawag.ch

S1 Mass balances with catabolic equations only

The equation system for mass balances with catabolic equations only is given in equation S1.

$$\begin{pmatrix} 0 & 0 & 0 & -1 & 0 & -1 \\ 0 & -8/3 & 0 & 1 & -1 & -1 \\ 0 & 0 & -8/5 & 0 & 1 & 0 \\ -1 & -1 & -1 & 0 & 0 & 0 \\ -1 & -11/3 & -13/5 & 2 & 0 & 0 \\ -2 & 0 & 0 & -3/2 & -1/2 & 0 \\ 2 & 2 & 2 & 0 & 0 & 0 \end{pmatrix} \cdot \begin{pmatrix} r_{R,HET,O2} \\ r_{R,HET,NO2} \\ r_{R,HET,NO3} \\ r_{R,AOB} \\ r_{R,NOB} \\ r_{R,AMX} \end{pmatrix} = \begin{pmatrix} r_{NH_4^+} \\ r_{NO_2^-} \\ r_{NO_3^-} \\ r_{C_2H_3O_2^-} \\ r_{H^+} \\ r_{O_2} \\ r_{TIC} \end{pmatrix} \quad (S1)$$

S2 Mass balances based on the activated sludge model

The equation system 2, where only mass balances for dissolved compounds were considered, is given in equation S2.

$$\begin{pmatrix} -0.587 & -0.820 & 0 & 0 & 0 & 0 & -15.3 & -0.820 & -23.8 & -0.820 \\ -1.59 & 0 & -1.85 & 0 & -1.85 & 0 & 0 & 0 & 0 & 0 \\ -0.0875 & 0.0803 & -0.0875 & 0 & -0.0875 & 0.0803 & -4.85 & 0.0803 & -0.0875 & 0.0803 \\ 0 & 0 & -0.298 & -0.287 & 0 & 0 & 0 & 0 & 21.7 & 0 \\ 0 & 0 & 0 & 0 & -0.497 & -0.478 & 4.76 & 0 & -21.7 & 0 \\ -0.0186 & -0.00574 & -0.0440 & -0.0262 & -0.058 & -0.0400 & 0.687 & -0.00574 & 0.00625 & -0.00574 \\ 0.220 & 0.308 & 0.319 & 0.308 & 0.319 & 0.3082 & -0.375 & 0.308 & -0.375 & 0.308 \end{pmatrix} \cdot \begin{pmatrix} \alpha_{R,HET,growth,O2} \\ \alpha_{R,HET,end.rep,O2} \\ \alpha_{R,HET,growth,NO3} \\ \alpha_{R,HET,end.resp,NO3} \\ \alpha_{R,HET,growth,NO2} \\ \alpha_{R,HET,end.resp,NO2} \\ \alpha_{R,AOB,growth} \\ \alpha_{R,AOB,end.resp} \\ \alpha_{R,NOB,growth} \\ \alpha_{R,NOB,end.resp} \\ \alpha_{R,AMX,growth} \\ \alpha_{R,AMX,end.resp} \end{pmatrix} = \begin{pmatrix} r_{O_2} \\ r_{C_2H_3O_2^-} \\ r_{NH_4^+} \\ r_{NO_3^-} \\ r_{NO_2^-} \\ r_{H^+} \\ r_{TIC} \end{pmatrix} \quad (S2)$$

The equation system 3, with one type of HET and including the concentrations for the bacterial groups and inert biomass, is given in equation S3.

$$\begin{pmatrix}
 -0.587 & -0.820 & 0 & 0 & 0 & 0 & -15.3 & -0.820 & -23.8 & -0.820 \\
 -1.59 & 0 & -1.85 & 0 & -1.85 & 0 & 0 & 0 & 0 & 0 \\
 -0.0875 & 0.0803 & -0.0875 & 0 & -0.0875 & 0.0803 & -4.85 & 0.0803 & -0.0875 & 0.0803 \\
 0 & 0 & -0.298 & -0.287 & 0 & 0 & 0 & 0 & 21.7 & 0 \\
 0 & 0 & 0 & 0 & -0.497 & -0.478 & 4.76 & 0 & -21.7 & 0 \\
 -0.0186 & -0.00574 & -0.0440 & -0.0262 & -0.058 & -0.0400 & 0.687 & -0.00574 & 0.00625 & -0.00574 \\
 0.220 & 0.308 & 0.319 & 0.308 & 0.319 & 0.3082 & -0.375 & 0.308 & -0.375 & 0.308 \\
 0 & 0.180 & 0 & 0.180 & 0 & 0.180 & 0 & 0.180 & 0 & 0.180 \\
 1 & -1 & 1 & -1 & 1 & -1 & 0 & 0 & 0 & 0 \\
 0 & 0 & 0 & 0 & 0 & 0 & 1 & -1 & 0 & 0 \\
 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 & -1 \\
 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0
 \end{pmatrix} \cdot
 \begin{pmatrix}
 r_{O_2} \\
 r_{C_2H_3O_2^-} \\
 r_{NH_4^+} \\
 r_{NO_3^-} \\
 r_{NO_2^-} \\
 r_{H^+} \\
 r_{TIC} \\
 r_{X_I} \\
 r_{X_{HET}} \\
 r_{X_{AOB}} \\
 r_{X_{NOB}} \\
 r_{X_{AMX}}
 \end{pmatrix} =
 \begin{pmatrix}
 \alpha_{R,HET,growth,O2} \\
 \alpha_{R,HET,end.rep,O2} \\
 \alpha_{R,HET,growth,NO3} \\
 \alpha_{R,HET,end.resp,NO3} \\
 \alpha_{R,HET,growth,NO2} \\
 \alpha_{R,HET,end.resp,NO2} \\
 \alpha_{R,AOB,growth} \\
 \alpha_{R,AOB,end.resp} \\
 \alpha_{R,NOB,growth} \\
 \alpha_{R,NOB,end.resp} \\
 \alpha_{R,AMX,growth} \\
 \alpha_{R,AMX,end.resp}
 \end{pmatrix}
 \quad (S3)$$

The equation system 4, with three types of HET and including the concentrations for the bacterial groups and inert biomass, is given in equation S4.

$$\begin{pmatrix}
 -0.587 & -0.820 & 0 & 0 & 0 & 0 & -15.3 & -0.820 & -23.8 & -0.820 \\
 -1.59 & 0 & -1.85 & 0 & -1.85 & 0 & 0 & 0 & 0 & 0 \\
 -0.0875 & 0.0803 & -0.0875 & 0 & -0.0875 & 0.0803 & -4.85 & 0.0803 & -0.0875 & 0.0803 \\
 0 & 0 & -0.298 & -0.287 & 0 & 0 & 0 & 0 & 21.7 & 0 \\
 0 & 0 & 0 & 0 & -0.497 & -0.478 & 4.76 & 0 & -21.7 & 0 \\
 -0.0186 & -0.00574 & -0.0440 & -0.0262 & -0.058 & -0.0400 & 0.687 & -0.00574 & 0.00625 & -0.00574 \\
 0.220 & 0.308 & 0.319 & 0.308 & 0.319 & 0.3082 & -0.375 & 0.308 & -0.375 & 0.308 \\
 0 & 0.180 & 0 & 0.180 & 0 & 0.180 & 0 & 0.180 & 0 & 0.180 \\
 1 & -1 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 \\
 0 & 0 & 1 & -1 & 0 & 0 & 0 & 0 & 0 & 0 \\
 0 & 0 & 0 & 0 & 1 & -1 & 0 & 0 & 0 & 0 \\
 0 & 0 & 0 & 0 & 0 & 0 & 1 & -1 & 0 & 0 \\
 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 1 & -1 \\
 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0 & 0
 \end{pmatrix} \cdot
 \begin{pmatrix}
 r_{O_2} \\
 r_{C_2H_3O_2^-} \\
 r_{NH_4^+} \\
 r_{NO_3^-} \\
 r_{NO_2^-} \\
 r_{H^+} \\
 r_{TIC} \\
 r_{X_I} \\
 r_{X_{HET,O2}} \\
 r_{X_{HET,NO3}} \\
 r_{X_{HET,NO2}} \\
 r_{X_{AOB}} \\
 r_{X_{NOB}} \\
 r_{X_{AMX}}
 \end{pmatrix}
 =
 \begin{pmatrix}
 \alpha_{R,HET,growth,O2} \\
 \alpha_{R,HET,end.rep,O2} \\
 \alpha_{R,HET,growth,NO3} \\
 \alpha_{R,HET,end.resp,NO3} \\
 \alpha_{R,HET,growth,NO2} \\
 \alpha_{R,HET,end.resp,NO2} \\
 \alpha_{R,AOB,growth} \\
 \alpha_{R,AOB,end.resp} \\
 \alpha_{R,NOB,growth} \\
 \alpha_{R,NOB,end.resp} \\
 \alpha_{R,AMX,growth} \\
 \alpha_{R,AMX,end.resp}
 \end{pmatrix}
 \quad (S4)$$

S3 Mass balances based on the activated sludge model including kinetics

The equation system 5, i.e. the mass balances to calculate the activities of the involved bacteria in a nitrification/anammox process *with* heterotrophic activity based on the activated sludge model and including kinetics, is given in equation S5.

$$\begin{pmatrix} -0.0351 & 0 & 0 & -0.189 & -0.00404 & 0 \\ -0.0490 & -0.0572 & -0.0487 & 0 & 0 & 0 \\ -0.00103 & -0.00103 & -0.000877 & -0.0592 & 0.0000664 & -0.0764 \\ 0 & -0.0152 & 0 & 0 & 0.00295 & 0.0185 \\ 0 & 0 & -0.0216 & 0.0583 & -0.00295 & -0.101 \\ -0.000691 & -0.00190 & -0.00224 & 0.00839 & -0.00000474 & -0.000412 \\ 0.0132 & 0.0163 & 0.0139 & -0.000389 & 0.000249 & -0.00340 \end{pmatrix} \cdot \begin{pmatrix} X_{HET,O2} \\ X_{HET,NO3} \\ X_{HET,NO2} \\ X_{AOB} \\ X_{NOB} \\ X_{AMX} \end{pmatrix} = \begin{pmatrix} r_{O_2} \\ r_{C_2H_3O_2^-} \\ r_{NH_4^+} \\ r_{NO_3^-} \\ r_{NO_2^-} \\ r_{H^+} \\ r_{TIC} \end{pmatrix} \quad (S5)$$

The equation system 6, i.e. the mass balances to calculate the activities of bacteria in a nitrification/anammox reactor without heterotrophic activity based on the activated sludge model and including kinetics, is given in equation S6.

$$\begin{pmatrix} -0.667 & -0.594 & 0 \\ -0.200 & -0.000979 & -0.104 \\ 0 & 0.531 & 0.0253 \\ 0.199 & -0.531 & -0.140 \\ 0.0285 & 0.0000699 & -0.000706 \\ -0.00588 & -0.00472 & -0.00366 \end{pmatrix} \cdot \begin{pmatrix} X_{AOB} \\ X_{NOB} \\ X_{AMX} \end{pmatrix} = \begin{pmatrix} r_{O_2} \\ r_{NH_4^+} \\ r_{NO_3^-} \\ r_{NO_2^-} \\ r_{H^+} \\ r_{TIC} \end{pmatrix} \quad (S6)$$

S4 Mass balances based on the activated sludge model including kinetics and a biomass balance

The equation system 7, for mass balances based on the activated sludge model and including both kinetics and a biomass balance, is given in equation S7.

$$\begin{pmatrix} -0.0351 & 0 & 0 & -0.189 & -0.00404 & 0 \\ -0.0490 & -0.0572 & -0.0487 & 0 & 0 & 0 \\ -0.00103 & -0.00103 & -0.000877 & -0.0592 & 0.0000664 & -0.0764 \\ 0 & -0.0152 & 0 & 0 & 0.00295 & 0.0185 \\ 0 & 0 & -0.0216 & 0.0583 & -0.00295 & -0.101 \\ -0.000691 & -0.00190 & -0.00224 & 0.00839 & -0.00000474 & -0.000412 \\ 0.0132 & 0.0163 & 0.0139 & -0.000389 & 0.000249 & -0.00340 \\ 0.0138 & 0.0138 & 0.0118 & 0.0104 & -0.000664 & 0.0103 \end{pmatrix} \cdot \begin{pmatrix} X_{HET,O2} \\ X_{HET,NO3} \\ X_{HET,NO2} \\ X_{AOB} \\ X_{NOB} \\ X_{AMX} \end{pmatrix} = \begin{pmatrix} r_{O_2} \\ r_{C_2H_3O_2^-} \\ r_{NH_4^+} \\ r_{NO_3^-} \\ r_{NO_2^-} \\ r_{H^+} \\ r_{TIC} \\ r_{X_{tot}} \end{pmatrix} \quad (S7)$$

S5 Initial conditions and influent concentrations

The initial conditions and the influent concentrations of the modelled compounds are given in Table S1.

Table S1 Initial conditions and influent concentrations of the modelled compounds.

	Unit	Initial condition	Influent concentration
S_H	$10^3 \text{ mol} \cdot \text{m}^{-3}$	$5.97 \cdot 10^{-7}$	$2.42 \cdot 10^{-9}$
S_{HCO3}	$\text{mol} \cdot \text{m}^{-3}$	0.63	31.7
S_{H2CO3}	$\text{mol} \cdot \text{m}^{-3}$	0.62	0.12
S_{HNO2}	$\text{g N} \cdot \text{m}^{-3}$	0	0
S_{HPO4}	$\text{g P} \cdot \text{m}^{-3}$	7.6	43.2
S_{H2PO4}	$\text{g P} \cdot \text{m}^{-3}$	36.4	0.7
$S_{N2,AMX}$	$\text{g N} \cdot \text{m}^{-3}$	0	0
$S_{N2,HET}$	$\text{g N} \cdot \text{m}^{-3}$	0	0
S_{NH3}	$\text{g N} \cdot \text{m}^{-3}$	0.11	132
S_{NH4}	$\text{g N} \cdot \text{m}^{-3}$	8.29	566
S_{NO2}	$\text{g N} \cdot \text{m}^{-3}$	0.1	0
S_{NO3}	$\text{g N} \cdot \text{m}^{-3}$	6.5	0
S_{O2}	$\text{g O}_2 \cdot \text{m}^{-3}$	0	0
S_S	$\text{g COD} \cdot \text{m}^{-3}$	0	0
S_{Sneg}	$\text{g COD} \cdot \text{m}^{-3}$	0	890
$S_{S,NO2}$	$\text{g COD} \cdot \text{m}^{-3}$	0	0
$S_{S,NO3}$	$\text{g COD} \cdot \text{m}^{-3}$	0	0
$S_{S,O2}$	$\text{g COD} \cdot \text{m}^{-3}$	0	0
X_{AMX}	$\text{g COD} \cdot \text{m}^{-3}$	100	0
X_{AOB}	$\text{g COD} \cdot \text{m}^{-3}$	100	0
$X_{H,NO2}$	$\text{g COD} \cdot \text{m}^{-3}$	100	0
$X_{H,NO3}$	$\text{g COD} \cdot \text{m}^{-3}$	100	0
$X_{H,O2}$	$\text{g COD} \cdot \text{m}^{-3}$	100	0
X_I	$\text{g COD} \cdot \text{m}^{-3}$	2000	0
X_{NOB}	$\text{g COD} \cdot \text{m}^{-3}$	100	0

S6 Modelled compounds

The modelled compounds are listed in Table S2.

Table S2 Dissolved and particulate compounds of the dynamic model.

		unit	i_N [g N]	i_{COD} [g COD]	i_C [mol C]	i_{charge} [mol]
S_H	dissolved hydrogen proton	$10^3 \text{ mol} \cdot \text{m}^{-3}$	0	0	0	1000
$S_{H_2CO_3}$	dissolved carbonic acid	$\text{mol} \cdot \text{m}^{-3}$	0	0	1	0
$S_{H_2PO_4}$	dissolved dihydrogen phosphate	$\text{g P} \cdot \text{m}^{-3}$	0	0	0	- 1/30.97
S_{HCO_3}	dissolved bicarbonate	$\text{mol} \cdot \text{m}^{-3}$	0	0	1	-1
S_{HNO_2}	dissolved nitrous acid	$\text{g N} \cdot \text{m}^{-3}$	1	-48/14	0	0
S_{HPO_4}	dissolved hydrogen phosphate	$\text{g P} \cdot \text{m}^{-3}$	0	0	0	- 2/30.97
$S_{N_2,AMX}$	dissolved dinitrogen produced by AMX	$\text{g N} \cdot \text{m}^{-3}$	1	-24/14	0	0
$S_{N_2,HET}$	dissolved dinitrogen produced by HET	$\text{g N} \cdot \text{m}^{-3}$	1	-24/14	0	0
S_{NH_3}	dissolved ammonia	$\text{g N} \cdot \text{m}^{-3}$	1	0	0	0
S_{NH_4}	dissolved ammonium	$\text{g N} \cdot \text{m}^{-3}$	1	0	0	1/14
S_{NO_2}	dissolved nitrite	$\text{g N} \cdot \text{m}^{-3}$	1	-48/14	0	-1/14
S_{NO_3}	dissolved nitrate	$\text{g N} \cdot \text{m}^{-3}$	1	-64/14	0	-1/14
S_{O_2}	dissolved oxygen	$\text{g O}_2 \cdot \text{m}^{-3}$	0	-1	0	0
S_S	dissolved acetic acid	$\text{g COD} \cdot \text{m}^{-3}$	0	1	2/64	0
$S_{S,neg}$	dissolved acetate	$\text{g COD} \cdot \text{m}^{-3}$	0	1	2/64	-1/64
S_{S,NO_2}	dissolved acetic acid degraded by X_{HET,NO_2}	$\text{g COD} \cdot \text{m}^{-3}$	0	1	2/64	0
S_{S,NO_3}	dissolved acetic acid degraded by X_{HET,NO_3}	$\text{g COD} \cdot \text{m}^{-3}$	0	1	2/64	0
S_{S,O_2}	dissolved acetic acid degraded by X_{HET,O_2}	$\text{g COD} \cdot \text{m}^{-3}$	0	1	2/64	0
X_{AOB}	ammonia oxidising bacteria	$\text{g COD} \cdot \text{m}^{-3}$	14/160	1	5/160	0
X_{AMX}	anammox bacteria	$\text{g COD} \cdot \text{m}^{-3}$	0.15·14/36.4	1	1/36.4	0
X_{H,NO_2}	heterotrophic bacteria using nitrite	$\text{g COD} \cdot \text{m}^{-3}$	14/160	1	5/160	0

$X_{H,NO3}$	heterotrophic bacteria using nitrate	g COD·m ⁻³	14/160	1	5/160	0
$X_{H,O2}$	heterotrophic bacteria using oxygen	g COD·m ⁻³	14/160	1	5/160	0
X_I	inert particulate matter	g COD·m ⁻³	0.035	1	5/160	0
X_{NOB}	nitrite oxidising bacteria	g COD·m ⁻³	14/160	1	5/160	0

S7 Simulation of pH equilibria and aeration

Parameters and process rates for the simulation of the pH equilibria and the aeration are listed in Table S3 and Table S4, respectively.

Table S3 Parameters for the simulation of pH equilibria and aeration.

Symbol	Characterisation	Value / formula	Unit
cond	Conductivity	22	mS·cm ⁻¹
f₁	Activity coefficient for ions with charge 1	$10^{\left(-0.5 \cdot 1 \cdot \frac{\sqrt{ionicstrength}}{\sqrt{ionicstrength} + 1} - 0.2 \cdot io\right)}$	-
f₂	Activity coefficient for ions with charge 2	$10^{\left(-0.5 \cdot 4 \cdot \frac{\sqrt{ionicstrength}}{\sqrt{ionicstrength} + 1} - 0.2 \cdot io\right)}$	-
H_{H2CO3}	Henry coefficient of H ₂ CO ₃	$\frac{1}{k_{H,T,H2CO3} \cdot 0.082057 \cdot (T + 273.15)}$	-
H_{NH3}	Henry coefficient of NH ₃	$\frac{1}{k_{H,T,NH3} \cdot 0.082057 \cdot (T + 273.15)}$	-
ionicstrength	Ionic strength	$0.01001047 \cdot cond + 0.0005188$	mol·L ⁻¹
k_{H,T,H2CO3}	Temperature dependency of H _{H2CO3}	$0.0345294 \cdot \exp\left(2428.57 \cdot \left(\frac{1}{T + 273.15} - \frac{1}{298.15}\right)\right)$	K ⁻¹
k_{H,T,NH3}	Temperature dependency of H _{NH3}	$55.8125 \cdot \exp\left(3708.33 \cdot \left(\frac{1}{T + 273.15} - \frac{1}{298.15}\right)\right)$	K ⁻¹
K_La_{H2CO3}	K _L a value of H ₂ CO ₃	$0.862 \cdot K_L a_{O2}$	d ⁻¹
K_La_{O2}	K _L a value of O ₂	70	d ⁻¹
k_{aeq}	Rate constant for equilibrium processes	10 ¹⁰	d ⁻¹

pCO_{2,air}	Partial pressure of CO ₂	0.000335	atm
pK_{H₂CO₃}	pK value of H ₂ CO ₃ ↔ HCO ₃	$-\log\left(10^{-6.37} \cdot \exp\left(7.6 \cdot \frac{1000}{8.314472} \cdot \left(\frac{1}{298.15} - \frac{1}{T}\right)\right)\right)$	
pK_{H₂PO₄}	pK value of H ₂ PO ₄ ↔ HPO ₄	$-\log\left(10^{-7.21} \cdot \exp\left(4.2 \cdot \frac{1000}{8.314472} \cdot \left(\frac{1}{298.15} - \frac{1}{T}\right)\right)\right)$	
pK_{HNO₂}	pK value of HNO ₂ ↔ NO ₂	$-\log\left(10^{-3.34} \cdot \exp\left(15.2 \cdot \frac{1000}{8.314472} \cdot \left(\frac{1}{298.15} - \frac{1}{T}\right)\right)\right)$	
pK_{NH₄}	pK value of NH ₄ ↔ NH ₃	$-\log\left(10^{-9.25} \cdot \exp\left(52.21 \cdot \frac{1000}{8.314472} \cdot \left(\frac{1}{298.15} - \frac{1}{T}\right)\right)\right)$	
pK_{SS}	pK value of S ↔ S _{neg}	$-\log\left(10^{-4.75} \cdot \exp\left(-0.2 \cdot \frac{1000}{8.314472} \cdot \left(\frac{1}{298.15} - \frac{1}{T}\right)\right)\right)$	
pO_s	Parameter for calculation of S _{O₂,sat}	$1.2 \cdot 10^{-6} \cdot T^4 + 0.00935467 \cdot T^2 - 0.41289$	-
pw	Parameter for calculation of S _{O₂,sat}	$4.79 \cdot 10^{-6} \cdot T^4 + 0.00021623 \cdot T^3 + 0.0148$	-
Q_{air}	Airflow rate	$0.195 \cdot \frac{1013}{971} \cdot \frac{273.14 + T}{273.14}$	m ³ ·d ⁻¹
Q_{in}	Influent flow rate	0.003	m ³ ·d ⁻¹
Q_{eff}	Effluent flow rate	0.003	m ³ ·d ⁻¹
SRT	Sludge retention time	50 <i>resp.</i> 100	d
S_{H₂CO₃,air}	Concentration of H ₂ CO ₃ in the air	$p_{CO2} \cdot 1000 \cdot \frac{1}{0.082057} \cdot \frac{1}{(T + 273.15)}$	mol·m ⁻³
S_{N₂,tot}	Total produced N ₂	$S_{N2,AMX} + S_{N2,HET}$	gN·m ⁻³
S_{O₂,sat}	Saturation concentration of dissolved oxygen	$pO_s \cdot \frac{975 - pw}{1013 - pw}$	gO ₂ ·m ⁻³
S_{S,tot}	Total degraded S _s	$S_{S,O2} + S_{S,NO3} + S_{S,NO2}$	gCOD·m ⁻³
T	Temperature	26	°C
V	Volume	0.01	m ³

Table S4 Process rates for the simulation of pH equilibria and aeration.

	Reaction	Reaction rate
aeration	H ₂ CO ₃ strip	$(H_{H_2CO_3} \cdot S_{H_2CO_3} - S_{H_2CO_3,air}) \cdot \frac{Q_{air}}{V} \cdot \left(1 - \exp\left(\frac{K_L a_{H_2CO_3} \cdot V}{H_{H_2CO_3} \cdot Q_{air}}\right)\right)$
	O ₂ input	$K_L a_{O_2} \cdot (S_{O_2,sat} - S_{O_2})$
pH equilibriums	HCO ₃ forward	$k_{aeq} \cdot S_{H_2CO_3}$
	HCO ₃ backward	$k_{aeq} \cdot 10^{pK_{H_2CO_3}} \cdot f_1 \cdot S_H \cdot f_1 \cdot S_{HCO_3}$
	HPO ₄ forward	$k_{aeq} \cdot f_1 \cdot S_{H_2PO_4}$
	HPO ₄ backward	$k_{aeq} \cdot 10^{pK_{H_2PO_4}} \cdot f_1 \cdot S_H \cdot f_2 \cdot S_{HPO_4}$
	NH ₃ forward	$k_{aeq} \cdot f_1 \cdot S_{NH_4}$
	NH ₃ backward	$k_{aeq} \cdot 10^{pK_{NH_4}} \cdot f_1 \cdot S_H \cdot S_{NH_3}$
	NO ₂ forward	$k_{aeq} \cdot S_{HNO_2}$
	NO ₂ backward	$k_{aeq} \cdot 10^{pK_{HNO_2}} \cdot f_1 \cdot S_H \cdot f_1 \cdot S_{NO_2}$
	S forward	$k_{aeq} \cdot S_S$
	S backward	$k_{aeq} \cdot 10^{pK_{SS}} \cdot f_1 \cdot S_H \cdot f_1 \cdot S_{Sneg}$

S8 Structural observability with one type of HET

To test whether the lack of observability is not only practical but also structural, we performed Monte Carlo simulations: 10,000 simulations were done with uniformly and randomly distributed parameter values in a range of $\pm 50\%$ of the default values. This was done with the following Matlab code:

```
clc
clear all
close all

disp('Defining default or sampled parameter values')

a_def = 0.630 ; % YH,O2
b_def = 0.566 ; % YH,NO3
c_def = 0.566 ; % YH,NO2
d_def = 14/160 ; % iN,AOB,NOB,HET
e_def = 0.15*14/36.4 ; % iN,AMX
f_def = 0.035 ; % iN,XI
g_def = 0.180 ; % fxi
h_def = 0.210 ; % YAOB
i_def = 0.046 ; % YNOB
k_def = 0.150 ; % YAMX

approach = 'randomized' ;
switch approach
case 'default'
    a = 0.630 ; % YH,O2
    b = 0.566 ; % YH,NO3
    c = 0.566 ; % YH,NO2
    d = 14/160 ; % iN,AOB,NOB,HET
    e = 0.15*14/36.4 ; % iN,AMX
    f = 0.035 ; % iN,XI
    g = 0.180 ; % fxi
    h = 0.210 ; % YAOB
    i = 0.046 ; % YNOB
    k = 0.150 ; % YAMX
case 'randomized'
    n_rand = 100 ; % number of repetitions

    a = rand(1,n_rand)*a_def+1/2*a_def ;
    b = rand(1,n_rand)*b_def+1/2*b_def ;
    c = rand(1,n_rand)*c_def+1/2*c_def ;
    d = 14/160 ; % iN,AOB,NOB,HET
    e = 0.15*14/36.4 ; % iN,AMX
    f = 0.035 ; % iN,XI
    g = rand(1,n_rand)*g_def+1/2*g_def ;
    h = rand(1,n_rand)*h_def+1/2*h_def ;
    i = rand(1,n_rand)*i_def+1/2*i_def ;
    k = rand(1,n_rand)*k_def+1/2*k_def ;

end

n_reagent = 12 ;
n_reactions = 12 ;
n_rep = length(a) ; % length of vector a = number of repetitions
```

```

for i_rep=1:n_rep
    disp(['Repetition ' num2str(i_rep) ' of ' num2str(n_rep)])
    % =====
    % Setup matrix:
    Matrix = nan(n_reagent,n_reactions) ;% initialize matrix

    % -----
    % reaction 1
    Matrix(:,1) = [      -1/(32*a(i_rep))+1/32 ;
                     -1/(64*a(i_rep)) ;
                     -d/14 ;
                     0 ;
                     0 ;
                     -1/(64*a(i_rep))+d/14 ;
                     2/(64*a(i_rep))-1/32 ;
                     0 ;
                     1/160 ;
                     0 ;
                     0 ;
                     0 ];

    % -----
    % reaction 2
    Matrix(:,2) = [      g(i_rep)/32-1/32      ;
                     0 ;
                     d/14-g(i_rep)*f/14 ;
                     0 ;
                     0 ;
                     (g(i_rep)*f-d)/14 ;
                     1/32-g(i_rep)/32 ;
                     g(i_rep)/160 ;
                     -1/160 ;
                     0 ;
                     0 ;
                     0 ];

    % -----
    % reaction 3
    Matrix(:,3) = [      0 ;
                     -1/(64*b(i_rep)) ;
                     -d/14 ;
                     1/40*(1-1/b(i_rep)) ;
                     0 ;
                     d/14-1/(64*b(i_rep))+1/40*(1-1/b(i_rep)) ;
                     1/(32*b(i_rep))-1/32 ;
                     0 ;
                     1/160 ;
                     0 ;
                     0 ;
                     0 ];

    % -----
    % reaction 4
    Matrix(:,4) = [      0 ;
                     0 ;
                     d/14-g(i_rep)*f/14 ;
                     (g(i_rep)-1)*1/40 ;
                     0 ;
                     (g(i_rep)*f-d)/14+(g(i_rep)-1)*1/40 ;
                     1/32-g(i_rep)/32 ;
                     g(i_rep)/160 ;

```

```

                                -1/160 ;
                                0 ;
                                0 ;
                                0 ] ;
% -----
% reaction 5

Matrix(:,5) = [      0 ;
                 -1/(64*c(i_rep)) ;
                 -d/14 ;
                 0 ;
                 1/24*(1-1/c(i_rep)) ;
                 d/14-1/(64*c(i_rep))+1/24*(1-1/c(i_rep)) ;
                 1/(32*c(i_rep))-1/32 ;
                 0 ;
                 1/160 ;
                 0 ;
                 0 ;
                 0 ] ;

% -----
% reaction 6

Matrix(:,6) = [      0 ;
                 0 ;
                 d/14-g(i_rep)*f/14 ;
                 0 ;
                 (g(i_rep)-1)*1/24 ;
                 (g(i_rep)*f-d)/14+(g(i_rep)-1)*1/24 ;
                 1/32-g(i_rep)/32 ;
                 g(i_rep)/160 ;
                 -1/160 ;
                 0 ;
                 0 ;
                 0 ] ;

% -----
% reaction 7

Matrix(:,7) = [      1/32-3/(28*h(i_rep)) ;
                 0 ;
                 -1/(14*h(i_rep))-d/14 ;
                 0 ;
                 1/(14*h(i_rep)) ;
                 1/(7*h(i_rep))+d/14 ;
                 -1/32 ;
                 0 ;
                 0 ;
                 1/160 ;
                 0 ;
                 0 ] ;

% -----
% reaction 8

Matrix(:,8) = [      g(i_rep)/32-1/32 ;
                 0 ;
                 d/14-g(i_rep)*f/14 ;
                 0 ;
                 0 ;
                 (g(i_rep)*f-d)/14 ;
                 1/32-g(i_rep)/32 ;
                 g(i_rep)/160 ;

```

```

0      ;
-1/160  ;
0      ;
0      ];
% -----
% reaction 9

Matrix(:,9) = [    1/32-1/(28*i(i_rep))      ;
0      ;
-d/14      ;
1/(14*i(i_rep)) ;
-1/(14*i(i_rep)) ;
d/14 ;
-1/32      ;
0      ;
0      ;
0      ;
1/160      ;
0      ];
% -----
% reaction 10

Matrix(:,10) = [    g(i_rep)/32-1/32      ;
0      ;
d/14-g(i_rep)*f/14      ;
0      ;
0      ;
(g(i_rep)*f-d)/14 ;
1/32-g(i_rep)/32      ;
g(i_rep)/160      ;
0      ;
0      ;
-1/160      ;
0      ];
% -----
% reaction 11

Matrix(:,11) = [    0      ;
0      ;
-1/(14*k(i_rep))-e/14      ;
0.192/(14*k(i_rep))+1/40      ;
-1.32/(14*k(i_rep)) ;
e/14+1/40-0.064/(7*k(i_rep)) ;
-1/36.4 ;
0      ;
0      ;
0      ;
0      ;
1/36.4  ];
% -----
% reaction 12

Matrix(:,12) = [    0      ;
0      ;
e/14-g(i_rep)*f/14      ;
0      ;
(g(i_rep)-1)*1/24      ;
(g(i_rep)*f-e)/14+(g(i_rep)-1)*1/24      ;
1/36.4-g(i_rep)/32      ;
g(i_rep)/160      ;
0      ;

```

```

0      ;
0      ;
-1/36.4 ];

% =====
% Analyze matrix:
rank(Matrix)
[U,S,V]=svd(Matrix);
BooleanInclude = diag(S)<=1e-10 ;
disp(V(:,BooleanInclude))

end

```

S9 Structural observability with three types of HET

To test whether the lack of observability is not only practical but also structural, we performed Monte Carlo simulations: 10,000 simulations were done with uniformly and randomly distributed parameter values in a range of $\pm 50\%$ of the default values. This was done with the following Matlab code:

```

clc
clear all
close all

disp('Defining default or sampled parameter values')

a_def = 0.630      ; % YH,O2
b_def = 0.566      ; % YH,NO3
c_def = 0.566      ; % YH,NO2
d_def = 14/160     ; % iN,AOB,NOB,HET
e_def = 0.15*14/36.4 ; % iN,AMX
f_def = 0.035      ; % iN,XI
g_def = 0.180      ; % fxi
h_def = 0.210      ; % YAOB
i_def = 0.046      ; % YNOB
k_def = 0.150      ; % YAMX

approach = 'randomized' ;
switch approach
case 'default'
    a = 0.630      ; % YH,O2
    b = 0.566      ; % YH,NO3
    c = 0.566      ; % YH,NO2
    d = 14/160     ; % iN,AOB,NOB,HET
    e = 0.15*14/36.4 ; % iN,AMX
    f = 0.035      ; % iN,XI
    g = 0.180      ; % fxi
    h = 0.210      ; % YAOB
    i = 0.046      ; % YNOB
    k = 0.150      ; % YAMX
case 'randomized'
    n_rand = 100 ; % number of repetitions

    a = rand(1,n_rand)*a_def+1/2*a_def ;

```

```

b = rand(1,n_rand)*b_def+1/2*b_def ;
c = rand(1,n_rand)*c_def+1/2*c_def ;
d = 14/160 ; % iN,AOB,NOB,HET
e = 0.15*14/36.4 ; % iN,AMX
f = 0.035 ; % iN,XI
g = rand(1,n_rand)*g_def+1/2*g_def ;
h = rand(1,n_rand)*h_def+1/2*h_def ;
i = rand(1,n_rand)*i_def+1/2*i_def ;
k = rand(1,n_rand)*k_def+1/2*k_def ;

end

n_reagent = 14 ;
n_reactions = 12 ;
n_rep = length(a) ; % length of vector a = number of repetitions

for i_rep=1:n_rep
disp(['Repetition ' num2str(i_rep) ' of ' num2str(n_rep)])
% =====
% Setup matrix:
Matrix = nan(n_reagent,n_reactions) ;% initialize matrix

% -----
% reaction 1
Matrix(:,1) = [ -1/(32*a(i_rep))+1/32 ;
-1/(64*a(i_rep)) ;
-d/14 ;
0 ;
0 ;
-1/(64*a(i_rep))+d/14 ;
2/(64*a(i_rep))-1/32 ;
0 ;
1/160 ;
0 ;
0 ;
0 ;
0 ;
0 ] ;

% -----
% reaction 2
Matrix(:,2) = [ g(i_rep)/32-1/32 ;
0 ;
d/14-g(i_rep)*f/14 ;
0 ;
0 ;
(g(i_rep)*f-d)/14 ;
1/32-g(i_rep)/32 ;
g(i_rep)/160 ;
-1/160 ;
0 ;
0 ;
0 ;
0 ;
0 ] ;

% -----
% reaction 3

Matrix(:,3) = [ 0 ;
-1/(64*b(i_rep)) ;
-d/14 ;
1/40*(1-1/b(i_rep)) ;

```

```

0 ;
d/14-1/(64*b(i_rep))+1/40*(1-1/b(i_rep)) ;
1/(32*b(i_rep))-1/32 ;
0 ;
0 ;
1/160 ;
0 ;
0 ;
0 ;
0 ;
0 ];

% -----
% reaction 4

Matrix(:,4) = [ 0 ;
0 ;
d/14-g(i_rep)*f/14 ;
(g(i_rep)-1)*1/40 ;
0 ;
(g(i_rep)*f-d)/14+(g(i_rep)-1)*1/40 ;
1/32-g(i_rep)/32 ;
g(i_rep)/160 ;
0 ;
-1/160 ;
0 ;
0 ;
0 ;
0 ];

% -----
% reaction 5

Matrix(:,5) = [ 0 ;
-1/(64*c(i_rep)) ;
-d/14 ;
0 ;
1/24*(1-1/c(i_rep)) ;
d/14-1/(64*c(i_rep))+1/24*(1-1/c(i_rep)) ;
1/(32*c(i_rep))-1/32 ;
0 ;
0 ;
0 ;
1/160 ;
0 ;
0 ;
0 ];

% -----
% reaction 6

Matrix(:,6) = [ 0 ;
0 ;
d/14-g(i_rep)*f/14 ;
0 ;
(g(i_rep)-1)*1/24 ;
(g(i_rep)*f-d)/14+(g(i_rep)-1)*1/24 ;
1/32-g(i_rep)/32 ;
g(i_rep)/160 ;
0 ;
0 ;
-1/160 ;
0 ;
0 ];

```

```

0    ];
% -----
% reaction 7

Matrix(:,7) = [    1/32-3/(28*h(i_rep))    ;
0    ;
-1/(14*h(i_rep))-d/14    ;
0    ;
1/(14*h(i_rep))    ;
1/(7*h(i_rep))+d/14    ;
-1/32    ;
0    ;
0    ;
0    ;
0    ;
1/160    ;
0    ;
0    ];
% -----
% reaction 8

Matrix(:,8) = [    g(i_rep)/32-1/32    ;
0    ;
d/14-g(i_rep)*f/14    ;
0    ;
0    ;
(g(i_rep)*f-d)/14    ;
1/32-g(i_rep)/32    ;
g(i_rep)/160    ;
0    ;
0    ;
0    ;
-1/160    ;
0    ;
0    ];
% -----
% reaction 9

Matrix(:,9) = [    1/32-1/(28*i(i_rep))    ;
0    ;
-d/14    ;
1/(14*i(i_rep))    ;
-1/(14*i(i_rep))    ;
d/14;
-1/32    ;
0    ;
0    ;
0    ;
0    ;
0    ;
1/160    ;
0    ];
% -----
% reaction 10

Matrix(:,10) = [    g(i_rep)/32-1/32    ;
0    ;
d/14-g(i_rep)*f/14    ;
0    ;
0    ;
(g(i_rep)*f-d)/14    ;

```

```

1/32-g(i_rep)/32      ;
g(i_rep)/160          ;
0      ;
0      ;
0      ;
0      ;
-1/160      ;
0      ];

% -----

% reaction 11

Matrix(:,11) = [      0      ;
                  0      ;
                  -1/(14*k(i_rep))-e/14      ;
                  0.192/(14*k(i_rep))+1/40      ;
                  -1.32/(14*k(i_rep))      ;
                  e/14+1/40-0.064/(7*k(i_rep))      ;
                  -1/36.4      ;
                  0      ;
                  0      ;
                  0      ;
                  0      ;
                  0      ;
                  0      ;
                  1/36.4      ];

% -----

% reaction 12

Matrix(:,12) = [      0      ;
                  0      ;
                  e/14-g(i_rep)*f/14      ;
                  0      ;
                  (g(i_rep)-1)*1/24      ;
                  (g(i_rep)*f-e)/14+(g(i_rep)-1)*1/24      ;
                  1/36.4-g(i_rep)/32      ;
                  g(i_rep)/160      ;
                  0      ;
                  0      ;
                  0      ;
                  0      ;
                  0      ;
                  0      ;
                  -1/36.4      ];

% =====
% Analyze matrix:
rank(Matrix)
[U,S,V]=svd(Matrix);
BooleanInclude = diag(S)<=1e-10 ;
disp(V(:,BooleanInclude))

```

end