

Supporting Information

Lignosulfonate-based acidic resin for the synthesis of renewable diesel and jet fuel range alkanes with 2-methylfuran and furfural

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1. Method for the calculation of carbon yields in the HDO step:

The carbon yields of different alkanes in the HDO process were calculated according to the following formulas:

Carbon yield of C₉-C₁₅ diesel and jet fuel range alkanes (%) = Total carbon of C₉-C₁₅ alkanes in the liquid products/Total carbon of feedstock pumped into the reactor × 100%

Carbon yield of C₅-C₈ gasoline range alkanes (%) = Total carbon of C₅-C₈ alkanes in the gas products per unit time/Total carbon of feedstock pumped into the reactor per unit time × 100% + Total carbon of the C₅-C₈ alkanes in liquid phase products/Total carbon of feedstock pumped into the reactor × 100%

Carbon yield of C₁-C₄ light alkanes (%) = Total carbon of the C₁-C₄ alkanes in the gas products per unit time/Total carbon of feedstock pumped into the reactor per unit time × 100%

2. Characterization

2.1 N₂-adsorption

The physical adsorption of N₂ was conducted on ASAP 2010 (Micromeritics). The specific surface areas of the acidic resins (see Table S2) were measured by Brunauer–Emmett–Teller (BET) method via nitrogen adsorption at 77 K. The nitrogen sorption isotherms and pore size distributions were measured according to the Barrett–Joyner–Halenda (BJH) method from the desorption branch of the isotherms. Before each measurement, the sample was evacuated at 393 K to eliminate the adsorbents.

2.2 Fourier Transform Infrared Spectroscopy (FT-IR)

The FT-IR spectrum of LF resin was collected a Bruker Equinox 55 spectrometer equipped with a deuterated triglycine sulphate (DTGS) detector and extended KBr beam splitter. The spectrometer was operated in the absorbance mode at a resolution of 4 cm^{-1} . Before the test, the LF resin was mixed with KBr at a mass ratio of 1/100 and pressed to self-supporting tablets.

From the FT-IR spectrum of LF resin illustrated in Figure S3, we can see that this material has many functional groups. According to literature,¹ the peaks at 2847 cm^{-1} and 2939 cm^{-1} can be attributed to stretching vibration of $-\text{CH}_2-$ which was formed during the phenol-aldehyde condensation lignosulfonate and formaldehyde. The bands at 1218 cm^{-1} and 1034 cm^{-1} can be assigned to the sym-stretching of $\text{O}=\text{S}=\text{O}$ and $\text{SO}_3\text{-H}$ stretching in SO_3H groups, respectively.² The peaks at 1113 cm^{-1} and 1312 cm^{-1} represent the in-plane bending vibration of aromatic C-H^3 and syringyl ring breathing with C-O stretching,⁴ respectively. The peaks at 1425 cm^{-1} , 1500 cm^{-1} and 1612 cm^{-1} can be attributed to the characteristic vibrations of benzene ring.^{1, 3, 5} The wavenumber at 1709 cm^{-1} indicated the existence of COOH group on the surface of LF resin.^{2c, 6} The broad peak at 3420 cm^{-1} can be attributed to the OH groups which are linked with the neighbor oxygen atom or SO_3H group by hydrogen-bond.¹ That is, the acidic groups (*i.e.* $-\text{SO}_3\text{H}$, $-\text{COOH}$ and phenolic $-\text{OH}$) on the LF resin are adjacent to each other.

2.3 Titration of $-\text{SO}_3\text{H}$, $-\text{COOH}$ and phenolic $-\text{OH}$

The amounts of acidic groups (*i.e.* -SO₃H, -COOH and phenolic -OH) on the surfaces of LF, Amberlyst-15, Amberlyst-36 and Nafion-212 resins (see Table S2) were measured by the acid-base titration method described in the literature.¹⁻²

In the first step, we measured the amount of -SO₃H sites on the surface of catalyst. To do this, 0.1 g catalyst was dispersed into 20 mL 2 mol L⁻¹ NaCl solution, sonicated for 1.5 h, and then centrifuged. The resulting liquid was titrated with 8 mmol L⁻¹ NaOH solution (pre-calibrated with a standard potassium hydrogenphthalate solution) using phenolphthalein as indicator. The molar amount of -SO₃H sites per gram of catalyst was obtained according to consumption of NaOH solution.

In the second step, we measured the total amount of -SO₃H and -COOH sites on the surface of the catalyst. To do this, 0.05 g catalyst was dispersed into 20 mL 80 mmol L⁻¹ NaHCO₃ solution. The liquid as obtained was titrated with 0.1 mol L⁻¹ HCl (pre-calibrated by a standard NaOH solution) using methyl orange as indicator. The molar amount of -COOH sites per gram of catalyst was calculated by subtracting the molar amount of -SO₃H sites per gram of catalyst from the total amount of -SO₃H and -COOH sites per gram of catalyst.

In the third step, the overall amount of -SO₃H, -COOH and phenolic -OH sites on the surface of the catalyst was measured. To do this, 0.05 g catalyst was dispersed into 20 mL 8 mmol L⁻¹ NaOH solution, sonicated for 1.5 h and then centrifuged. The resulting filtrate was titrated with 1 mmol L⁻¹ potassium hydrogenphthalate solution using phenolphthalein as indicator. The molar amount of phenolic -OH sites per gram of catalyst was calculated by subtracting the total amount of -SO₃H and -COOH sites

per gram of catalyst from the overall amount of $-\text{SO}_3\text{H}$, $-\text{COOH}$ and phenolic $-\text{OH}$ sites per gram of catalyst.

2.4 Microcalorimetric measurement of NH_3 adsorption

The microcalorimetric measurements of ammonia adsorption for the different solid acid catalysts used in the HAA reaction were performed at 353 K using a BT2.15 heat-flux calorimeter (France, Setaram) connected to a gas-handling and a volumetric system employing MKS Baratron Capacitance Manometers for precision pressure measurement ($\pm 0.5 \times 10^{-4}$ Torr). Before each measurement, ammonia (purity > 99.9%) was purified by successive freeze–pump–thaw cycles. The specific mass of sample with similar amount of acid sites was evacuated in a quartz cell at 353 K overnight under high vacuum to remove the physically adsorbed substance. The differential heat was measured as a function of acid site coverage by repeatedly introducing small dosage of ammonia onto the samples until the equilibrium pressure reached about 5-6 torr. Then the system was evacuated overnight to remove the physically adsorbed ammonia, and a second adsorption was performed. The amount of irreversible adsorbed ammonia was determined by the difference between the isotherms of the first and second adsorption cycles.

2.5 X-ray Diffraction (XRD)

XRD patterns of different catalysts were recorded with a PW3040/60X' Pert PRO (PANalytical) diffractometer using a $\text{Cu K}\alpha$ radiation source ($\lambda = 0.15432$ nm) at 40 kV and 40 mA. From the XRD patterns of Ni catalysts (see Figure S9 in supporting

information), we can only observe the peaks of H-ZSM-5 support and metallic Ni. No peak of nickel oxide was noticed.

2.6 H₂-O₂ titration

The nickel dispersions (ratio of surface nickel atoms to the total amount of nickel atoms in each catalyst) of the Ni catalysts were obtained with a Micromeritics AutoChem II 2920 Automated Catalyst Characterization System by H₂-O₂ titration. In a typical measurement, the sample was firstly reduced in H₂ flow at 773 K for 2 h and then purged in Ar flow at 783 K for 30 min to remove adsorbed H₂. After that, the catalyst was cooled down in Ar flow to 393 K and purged with a constant flow of 2% O₂/He (V/V) for 30 min for O₂ adsorption. Subsequently, the sample was heated to 773 K in a constant Ar flow. After the stabilization of baseline, the H₂ adsorption was then conducted by dosage of 10% H₂/Ar (V/V) pulse at 773 K. Finally, the metal dispersion of Ni catalyst was calculated on the basis of the amounts of adsorbed H₂ and total Ni loading under the assumption that the stoichiometry of H₂ to surface Ni atom is 1.5 (mol/mol).

2.7 Transmission Electron Microscopy (TEM)

The TEM images of the Ni-based HDO catalysts were obtained by a FEI TECNAI G² Spirit Transmission Electron Microscope operated at an accelerating voltage of 120 kV. Before the tests, the catalysts were reduced by H₂ at 773 K for 2 h. From the TEM images showed in the Figure S10, the utilization of complex agents obviously decreases the Ni particle sizes over the Ni/H-ZSM-5 catalysts. This result is consistent with what we observed in H₂-O₂ titration tests.

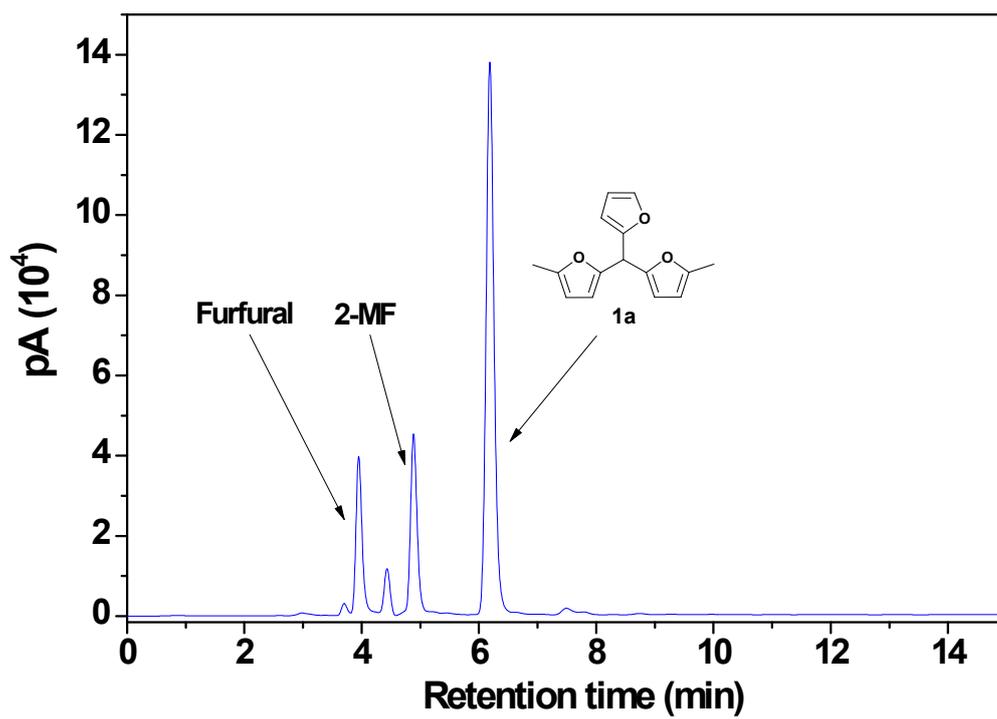


Figure S1. HPLC chromatogram of the liquid products from the HAA of 2-MF with furfural.

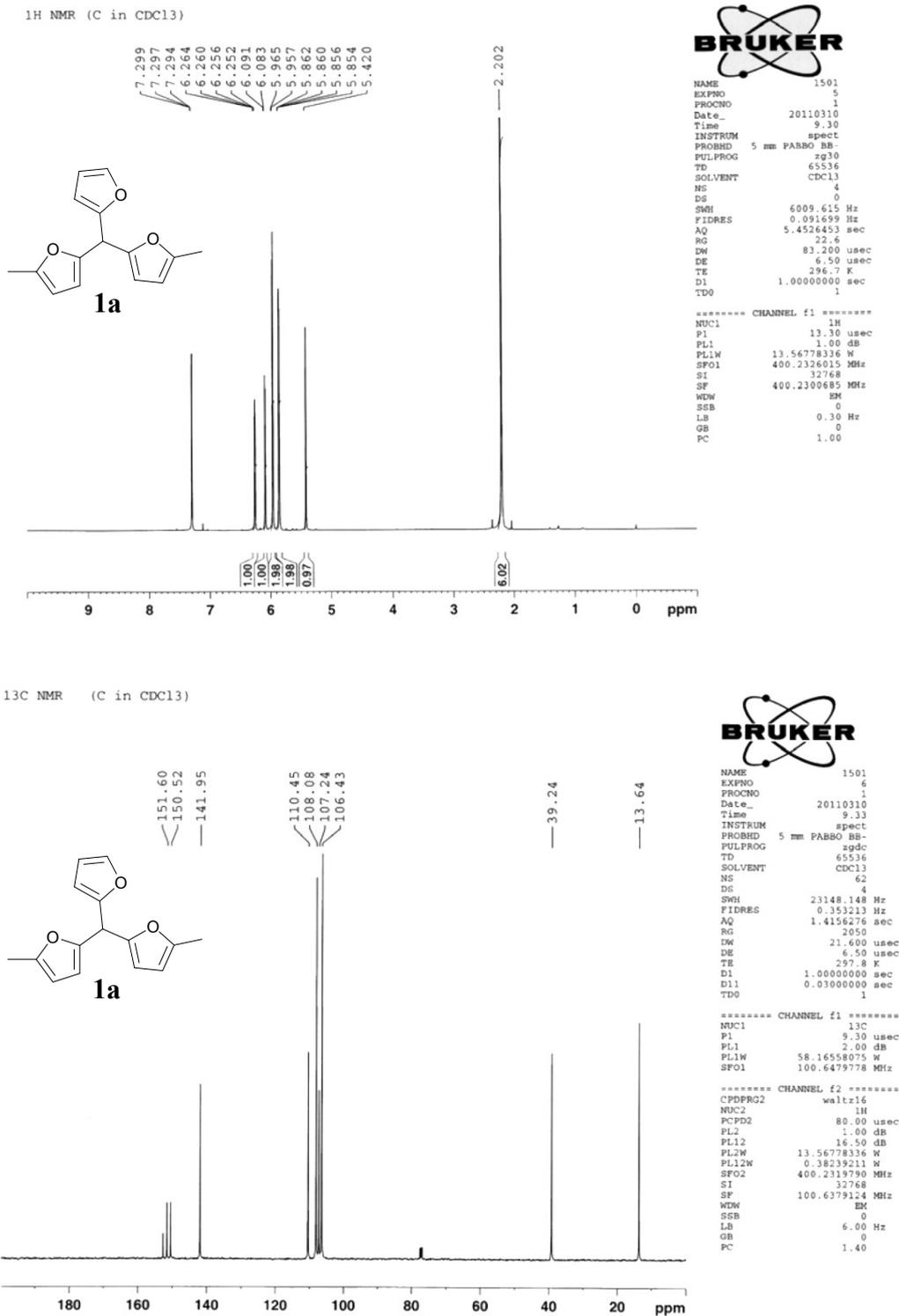


Figure S2. ^{13}C and ^1H NMR spectra of the **1a** produced by HAA of 2-MF with furfural.

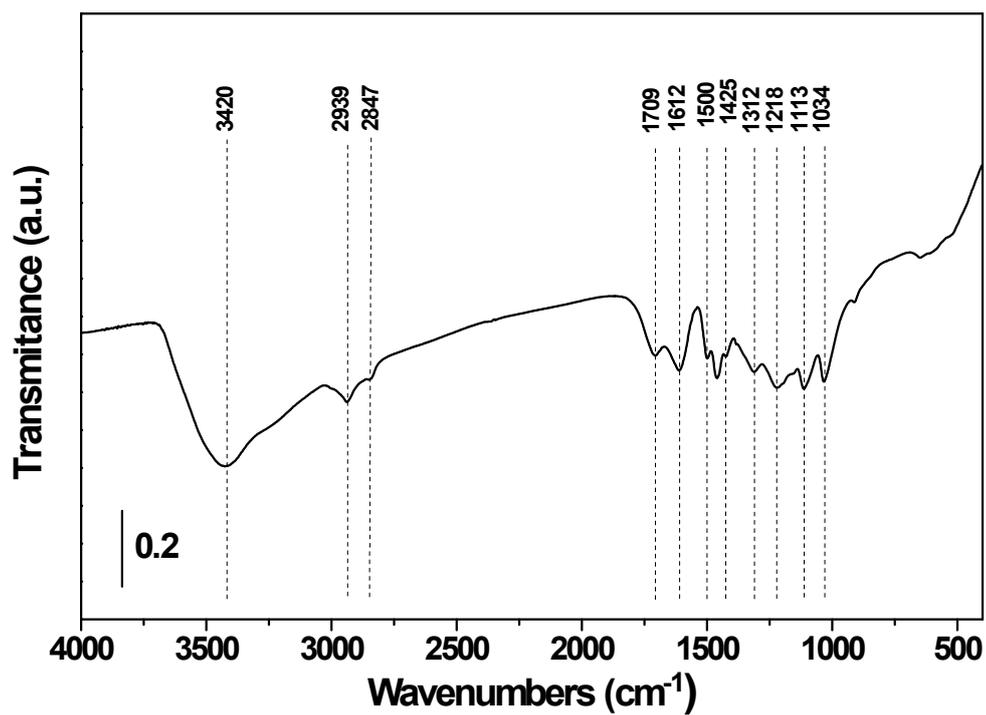


Figure S3. FT-IR spectrum of LF resin which was prepared by the protonation of the condensation product of sodium lignosulfonate and formaldehyde.

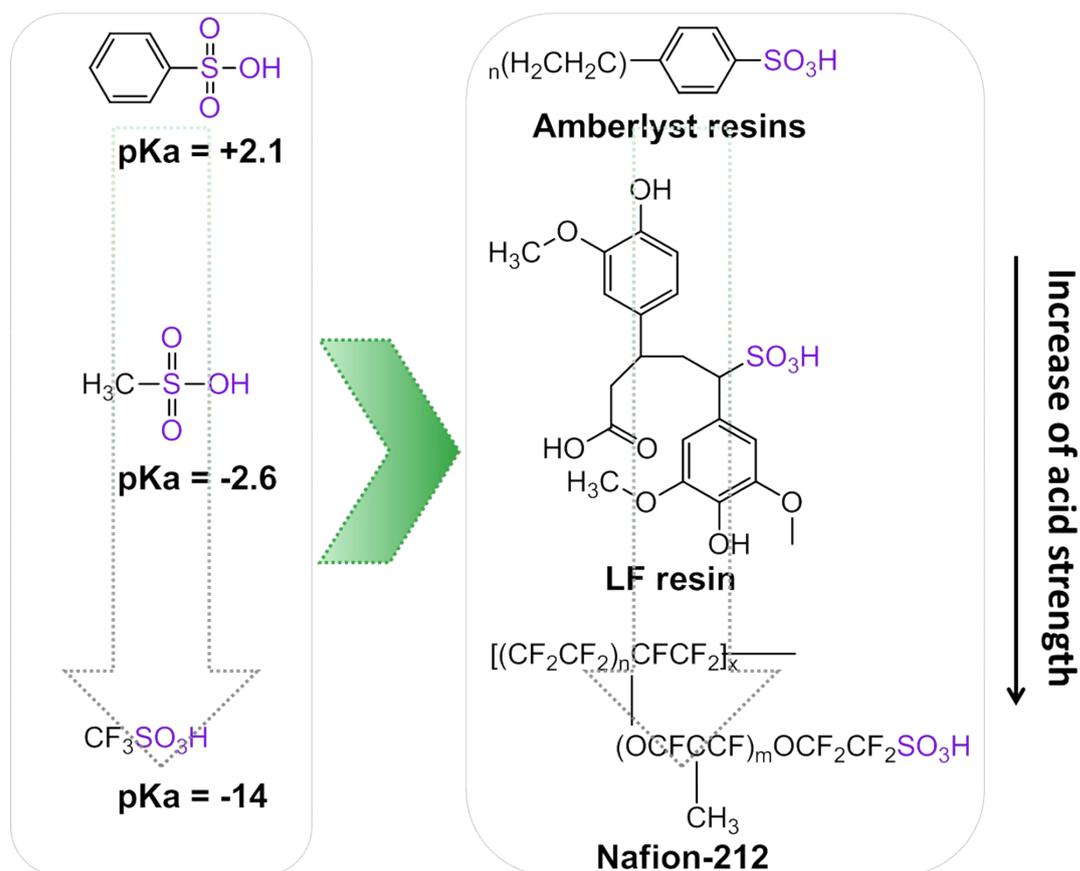


Figure S4. Chemical structures and the acid strengths of different organic acids and solid acids.⁷

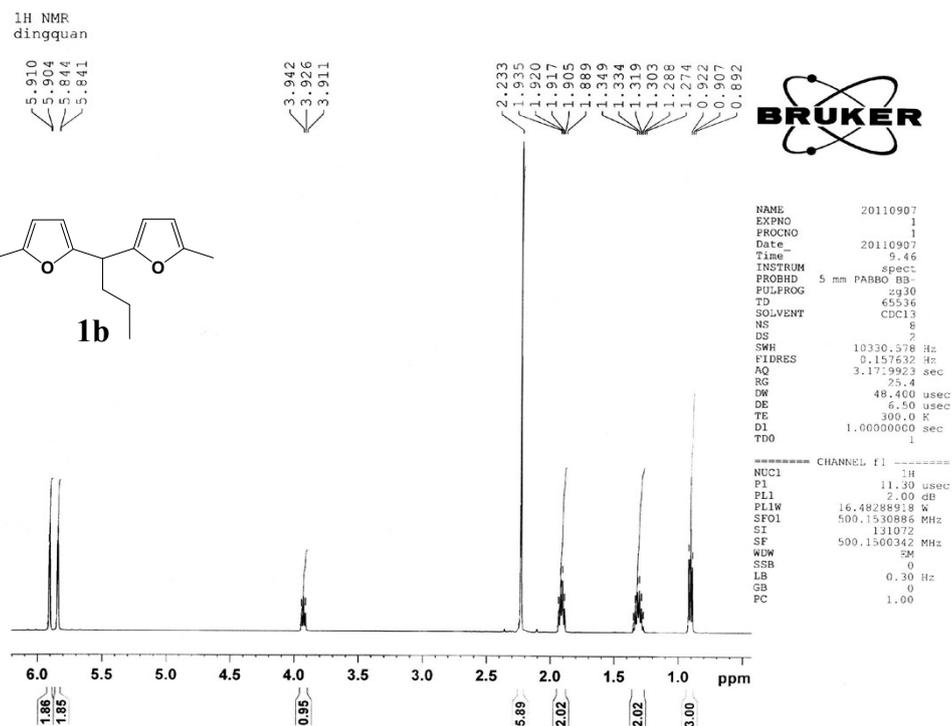
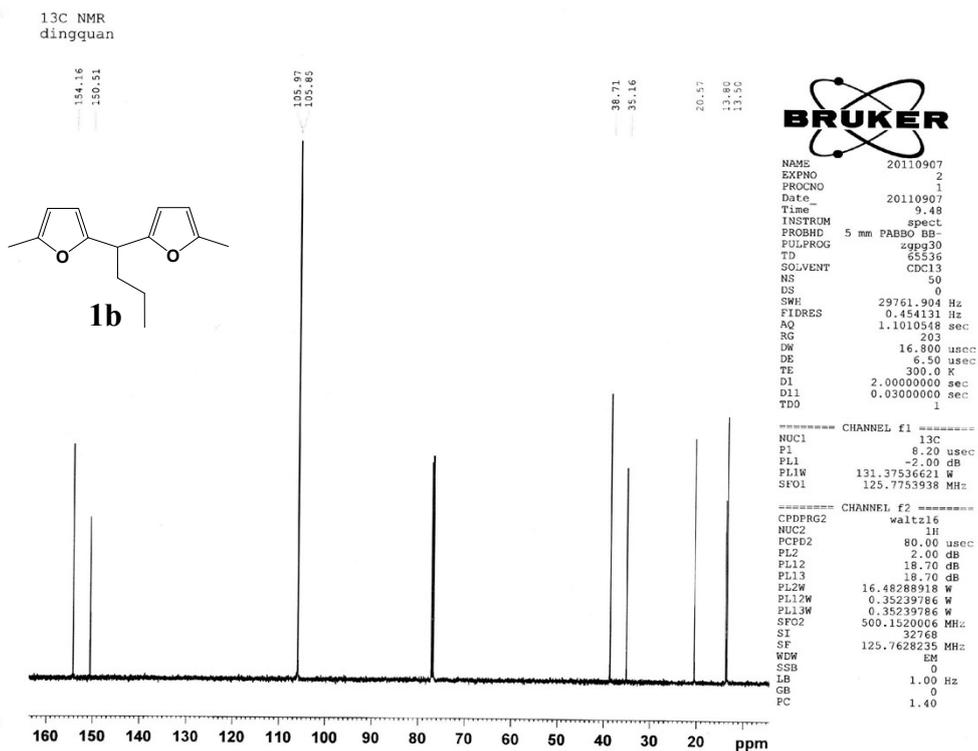


Figure S5. ^{13}C and ^1H NMR spectra of the **1b** produced by HAA of 2-MF with *n*-butanal.

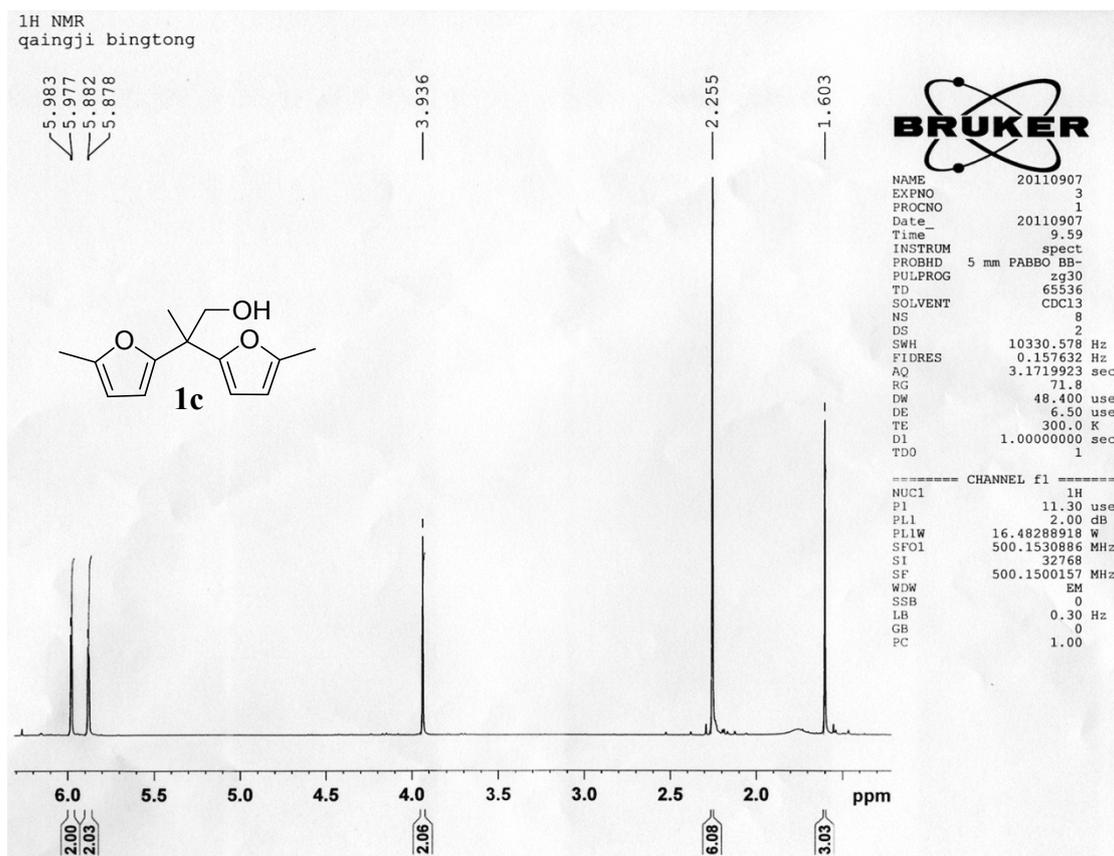
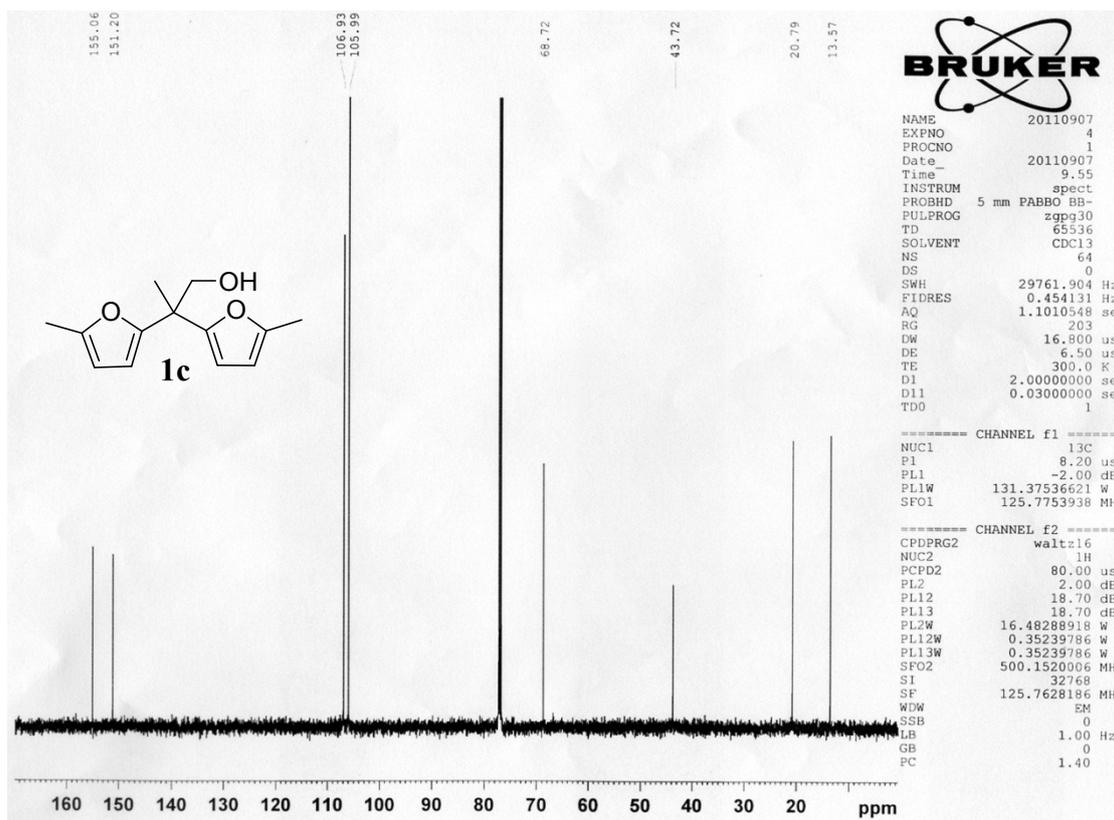
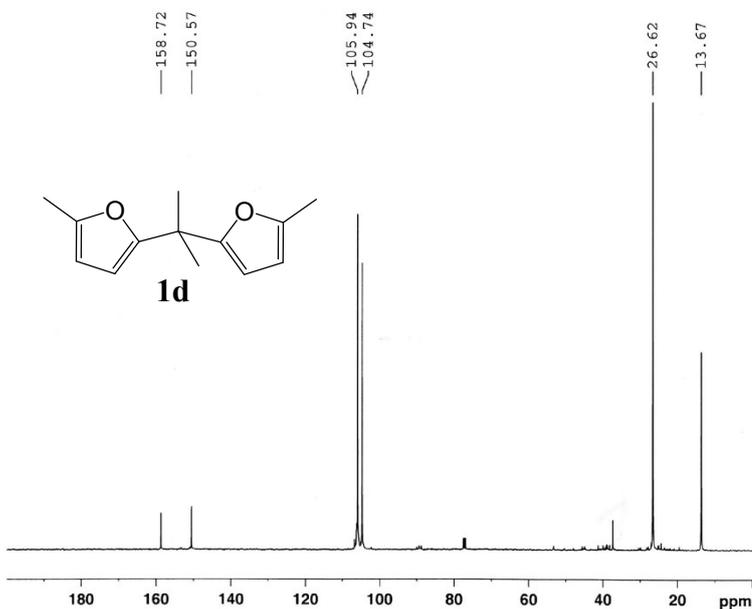


Figure S6. ¹³C and ¹H NMR spectra of the **1c** produced by the HAA of 2-MF with acetol.

¹³C NMR (A in CDCl₃)

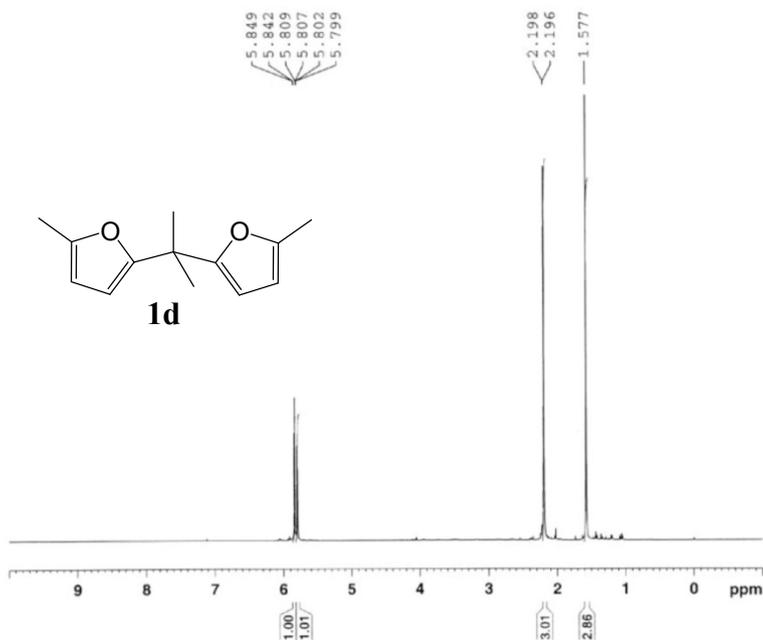


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¹H NMR (A in CDCl₃)



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Figure S7. ¹³C and ¹H NMR spectra of the **1d** produced by HAA of 2-MF with acetone.

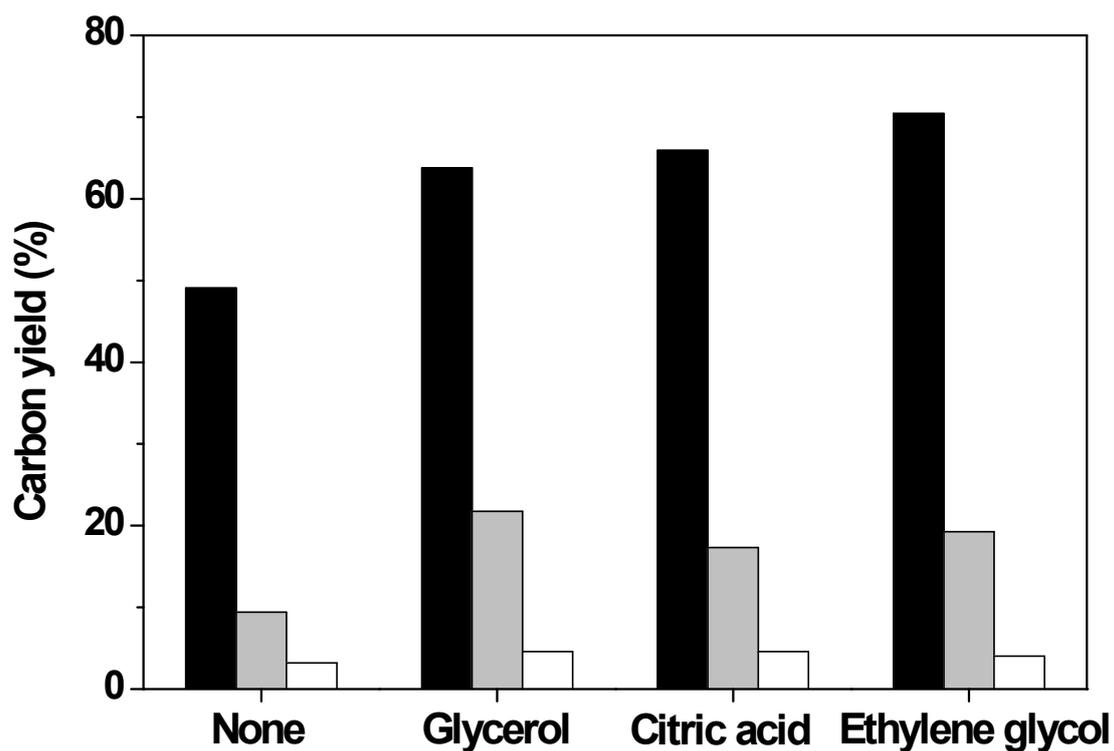


Figure S8. Carbon yields of C₉-C₁₅ diesel and jet fuel range alkanes (black bars), C₅-C₈ gasoline range alkanes (grey bars) and C₁-C₄ light alkanes (white bars) over the Ni/H-ZSM-5 catalysts prepared with different complex agents. Reaction conditions: 533 K, 6 MPa, 1.8 g HDO catalyst; flow rate of liquid feedstock: 0.04 mL min⁻¹ (WHSV = 1.3 h⁻¹); H₂ flow rate: 120 mL min⁻¹.

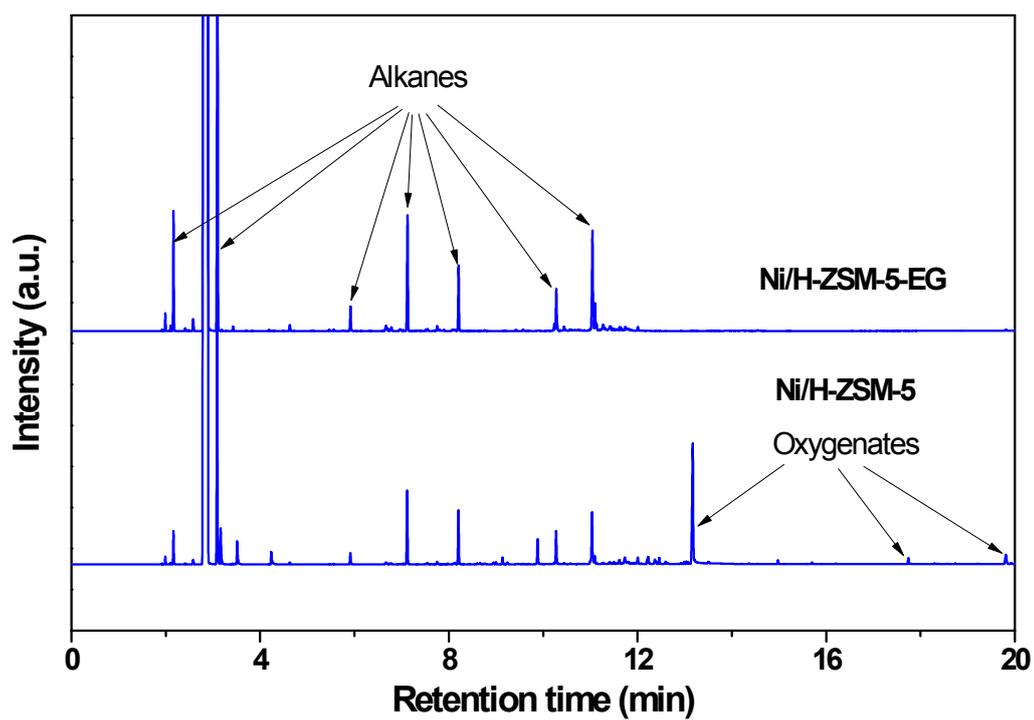


Figure S9. Gas chromatograms of the liquid products from the HDO of **1a** over the Ni/H-ZSM-5 and Ni/H-ZSM-5-EG catalysts. Reaction conditions: 533 K, 6 MPa H₂, 1.8 g catalyst; liquid feedstock flow rate of 0.04 mL min⁻¹ (WHSV = 1.3 h⁻¹); H₂ flow rate of 120 mL min⁻¹.

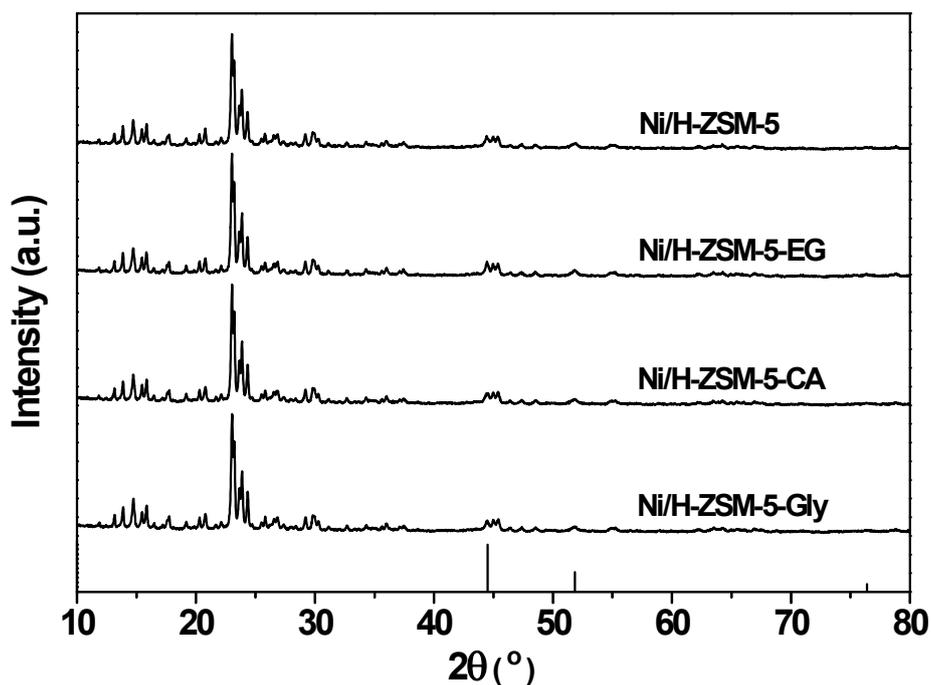


Figure S10. XRD patterns of different Ni/H-ZSM-5 catalysts. Ni/H-ZSM-5, Ni/H-ZSM-5-EG, Ni/H-ZSM-5-CA and Ni/H-ZSM-5-Gly denote the Ni/H-ZSM-5 catalyst prepared by conventional incipient wetness impregnation method (without using complex agent) and the Ni/H-ZSM-5 catalysts prepared by incipient wetness complexation impregnation method using ethylene glycol, citric acid or glycerol as the complex agent, respectively. The pattern at the bottom is that of metallic nickel from the JCPD standards (No. 00-004-0850).

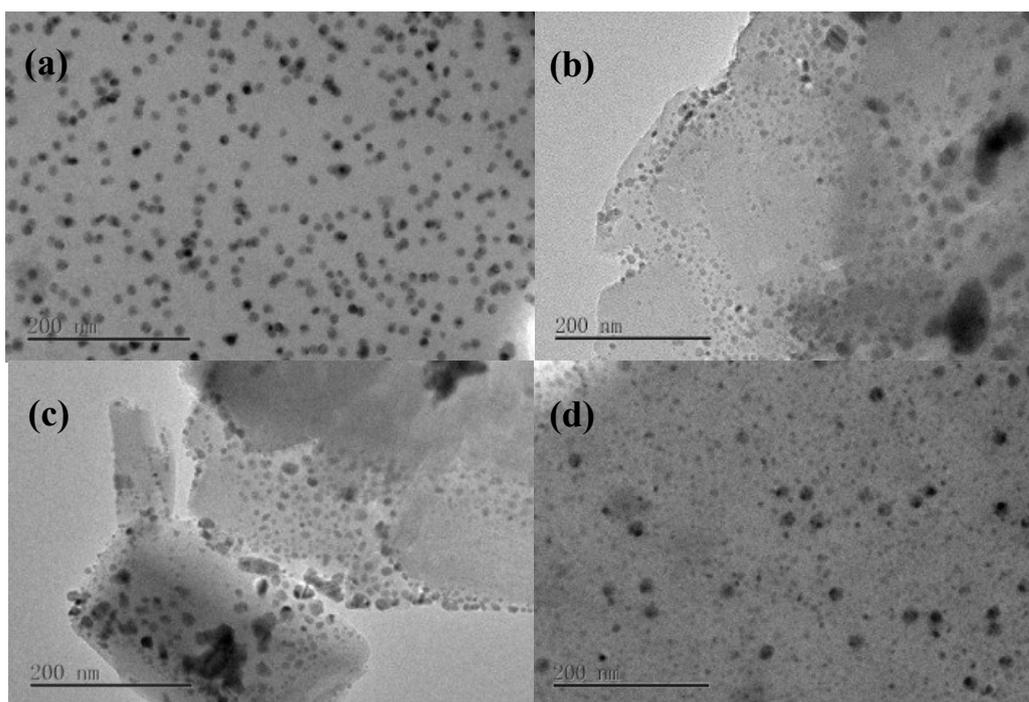


Figure S11. TEM images of the Ni/H-ZSM-5 (a), Ni/H-ZSM-5-Gly (b), Ni/H-ZSM-5-CA (c) and Ni/H-ZSM-5-EG (d) catalysts.

Table S1. Conversions of 2-methylfuran (2-MF) and carbon yields of **1a** under the catalysis of *p*-toluenesulfonic acid, acetic acid and phenol. Reaction conditions: 3.28 g (40 mmol) 2-MF, 1.92 g (20 mmol) furfural, 0.1 mL catalyst; 323 K, 2 h.

Catalyst ^a	Mole of acid (mmol)	Conversion of 2-MF (%)	Carbon yield of 1a (%)
<i>p</i> -Toluenesulfonic acid	0.2	57.1	45.9
Acetic acid	0.2	4.9	0
Phenol	0.2	3.8	0

^a The concentrations of the acid solutions are 2 mol L⁻¹.

Table S2. Specific BET surface areas, average pore sizes and the amount of acid sites of the LF, Amberlyst-15, Amberlyst-36, and Nafion-212 resins which were used as catalysts for the hydroxyalkylation/alkylation (HAA) of 2-MF and furfural.

Catalysts	Specific BET surface area (m ² g ⁻¹)	Average pore size (nm) ^a	Amount of acid sites on the surface of catalyst (mmol g _{cat} ⁻¹) ^b		
			-SO ₃ H group	-COOH group	Phenolic -OH group
LF	2	5.7	1.02	0.25	1.11
Amberlyst-15	41	29	4.61 (4.7)	—	—
Amberlyst-36	13	24	5.33 (5.4)	—	—
Nafion-212	2	4.0	1.08 (1.1)	—	—

^a Average pore sizes were measured by N₂-adsorption according to the Barrett–Joyner–Halenda (BJH) method. ^b The amounts of acid sites were obtained by titration method. The values in the brackets were the ones provided by supplier.

Table S3. Effect of calcium lignosulfonate concentration on the conversion of 2-MF and the carbon yield of **1a** over the LF resin. Reaction conditions: 3.28 g (40 mmol) 2-MF, 1.92 g (20 mmol) furfural, 0.15 g catalyst; 323 K, 2 h.

Catalyst ^a	Amount of acid sites on the surface of catalyst (mmol g _{cat} ⁻¹) ^b	Conversion of 2-MF (%)	Carbon yield of 1a (%)
LF	1.02	70.4	65.4
LF-Ca-1	0.97	64.4	60.9
LF-Ca-5	0.93	63.4	59.4
LF-Ca-10	0.87	58.9	55.1

^a LF-Ca-1, LF-Ca-5 and LF-Ca-10 denote the LF resins prepared with the mixture of sodium lignosulfonate and calcium lignosulfonate at the mass ratio of 99:1, 19:1 and 9:1, respectively.

^b Measured by the chemical titration described in the supporting information.

Table S4. Effect of sugar concentration on the conversion of 2-MF and the carbon yield of **1a** over the LF resin. Reaction conditions: 3.28 g (40 mmol) 2-MF, 1.92 g (20 mmol) furfural, 0.15 g catalyst; 323 K, 2 h.

Catalyst ^a	Amount of acid sites on the surface of catalyst (mmol g _{cat} ⁻¹) ^b	Conversion of 2-MF (%)	Carbon yield of 1a (%)
LF	1.02	70.4	65.4
LF-Sugars-1	1.00	64.7	62.2
LF-Sugars-5	0.92	62.2	58.6
LF-Sugars-10	0.79	57.6	54.1

^a LF-Sugars-1, LF-Sugars-5 and LF-Sugars-10 denote the LF resins prepared with the mixture of sodium lignosulfonate, glucose and xylose at the mass ratio of 198:1:1, 38:1:1 and 18:1:1, respectively.

^b Measured by the chemical titration described in the supporting information.

Table S5. Metal dispersions and the amounts of chemical accessible Ni sites over the different catalyst measured by H₂-O₂ titration.

Catalyst ^a	Metal dispersion (%)	Amount of chemical accessible Ni sites (μmol g ⁻¹)
Ni/H-ZSM-5	6.7	64.1
Ni/H-ZSM-5-Gly	10.0	77.4
Ni/H-ZSM-5-CA	9.8	76.1
Ni/H-ZSM-5-EG	11.4	96.8

^a The theoretical content of Ni in each catalyst was 5 wt.%. Ni/H-ZSM-5, Ni/H-ZSM-5-Gly, Ni/H-ZSM-5-CA, Ni/H-ZSM-5-EG account for the Ni/H-ZSM-5 catalysts prepared by conventional impregnation method or complexation impregnation method in the presence of glycerol, citric acid and ethylene glycol, respectively.

References

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