## Supporting Information

Tandem Catalytic Conversion of 1-Butene and Ethene to Propene over

Combined Mesoporous W-FDU-12 and MgO Catalysts

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Figure S1 XPS spectra of W-FDU-12 catalysts with various W contents.

Table S1. Binding energies and molar percentages of $\mathbf{W}^{6+}$ and $\mathbf{W}^{5+}$ species in different catalysts.

| Catalysts | Binding energies of $\mathrm{W}_{4 \mathrm{f}}(\mathrm{eV})$ |  |  |  | $\mathbf{W}^{5+}(\%)$ | $\mathbf{W}^{6+}(\%)$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
|  | $W^{6+4} f_{5 / 2}$ | $W^{6+} 4 f_{7 / 2}$ | $W^{5+} 4 f_{5 / 2}$ | $W^{5+4} \mathbf{f}_{7 / 2}$ |  |  |
| W-FDU-12-1.2 | 38.3 | 36.2 | 37.2 | 35.1 | 70.5 | 29.5 |
| W-FDU-12-2.2 | 38.2 | 36.2 | 37.3 | 35.1 | 77.0 | 23.0 |
| W-FDU-12-3.0 | 38.3 | 36.2 | 37.2 | 35.0 | 75.9 | 24.1 |
| W-FDU-12-5.2 | 38.4 | 36.3 | 37.2 | 35.1 | 40.3 | 59.7 |



Figure S2 TEM image of W-FDU-12-4.0\% (left panel) and corresponding EDX spectra (right panel).


Figure S3 1-butene conversion and propene selectivity over individual MgO or W -FDU-12-4.0\% catalyst. Reaction conditions: $\mathrm{T}=450^{\circ} \mathrm{C} ; \mathrm{P}=0.1 \mathrm{MPa} ; 1-\mathrm{C}_{4} \mathrm{H}_{8} / \mathrm{C}_{2} \mathrm{H}_{4}=1 / 2$; WHSV $\left(1-\mathrm{C}_{4} \mathrm{H}_{8}+\mathrm{C}_{2} \mathrm{H}_{4}\right)$ of $0.9 \mathrm{~h}^{-1}$.


Figure S4. 1-Butene conversion (left panel) and propene selectivity (right panel) over W-FDU-12-4.0\% catalysts at different reaction temperatures. Reaction conditions: $\mathrm{P}=0.1 \mathrm{MPa} ; 1-\mathrm{C}_{4} \mathrm{H}_{8} / \mathrm{C}_{2} \mathrm{H}_{4}=1 / 2$; WHSV $\left(1-\mathrm{C}_{4} \mathrm{H}_{8}+\mathrm{C}_{2} \mathrm{H}_{4}\right)$ of $0.9 \mathrm{~h}^{-1}$; W-contained catalyst $=1.0 \mathrm{~g}$.


Figure S5. 1-Butene conversion (left panel) and propene selectivity (right panel) over W-FDU-12-4.0\% catalysts at different calcinated temperatures. Reaction conditions: $\mathrm{T}=450{ }^{\circ} \mathrm{C} ; \mathrm{P}=0.1 \mathrm{MPa} ; 1-\mathrm{C}_{4} \mathrm{H}_{8} / \mathrm{C}_{2} \mathrm{H}_{4}=1 / 2$; WHSV $\left(1-\mathrm{C}_{4} \mathrm{H}_{8}+\mathrm{C}_{2} \mathrm{H}_{4}\right)$ of $0.9 \mathrm{~h}^{-1}$; Wcontained catalyst $=1.0 \mathrm{~g}$.


Figure S6. The TG curves of different used catalysts after 8 hours of reaction showing (a) W-FDU-12-4.0\%; (b) $\mathrm{WO}_{3} / \mathrm{FDU}-12-4.0 \%$; and (c) $\mathrm{WO}_{3} / \mathrm{SiO}_{2}-4.0 \%$.

