

Nb-doped VO_x/CeO₂ catalyst for NH₃-SCR of NO_x at low temperatures

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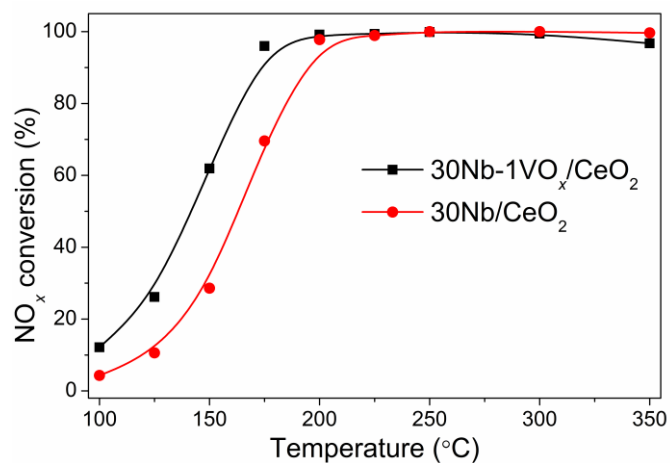


Fig. S1 NH₃-SCR activity over 30Nb-1VO_x/CeO₂ and 30Nb/CeO₂ catalysts.

Reaction conditions: [NO] = [NH₃] = 500 ppm, [O₂] = 5 vol. %, N₂ balance, total flow rate 500 ml/min and GHSV = 50 000 h⁻¹.

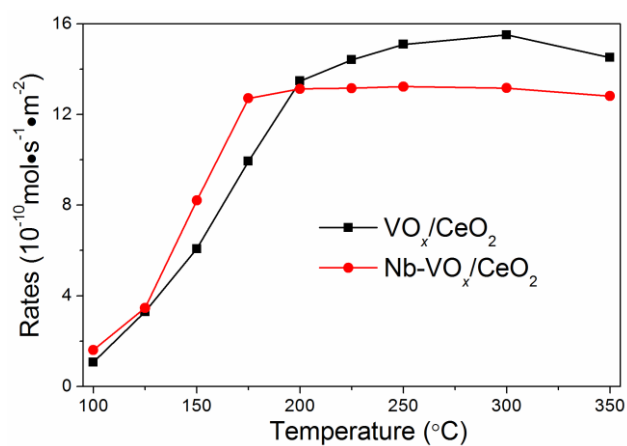


Fig. S2 The NH₃-SCR reaction rates normalized by surface area over VO_x/CeO₂ and 30Nb-VO_x/CeO₂ catalysts.

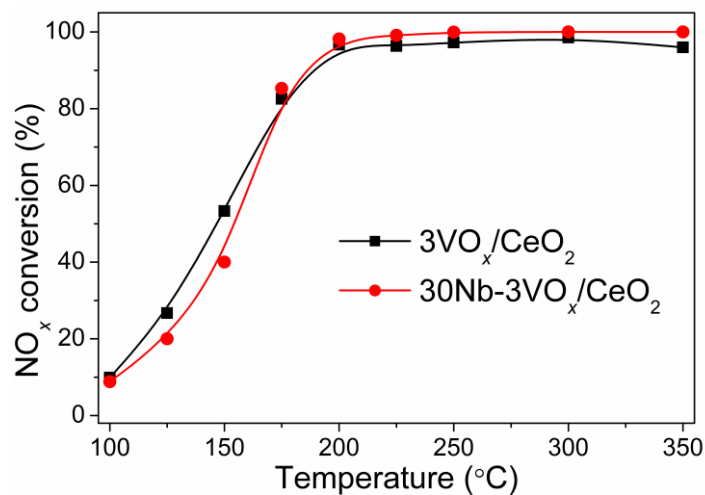


Fig. S3 NH₃-SCR activity over 3VO_x/CeO₂ and 30Nb-3VO_x/CeO₂ catalysts.

Reaction conditions: [NO] = [NH₃] = 500 ppm, [O₂] = 5 vol. %, N₂ balance, total flow rate 500 ml/min and GHSV = 50 000 h⁻¹.

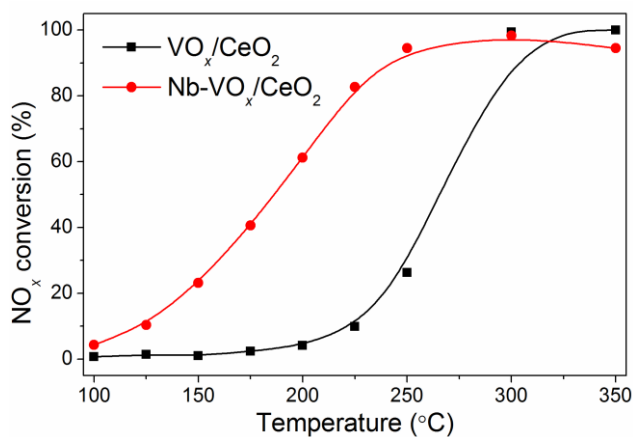


Fig. S4 NH₃-SCR activity over 1VO_x/CeO₂ and 30Nb-1VO_x/CeO₂ catalysts after 100 ppm SO₂ poisoning for 48 h.

Reaction conditions: [NO] = [NH₃] = 500 ppm, [O₂] = 5 vol. %, N₂ balance, total flow rate 500 ml/min and GHSV = 50 000 h⁻¹.

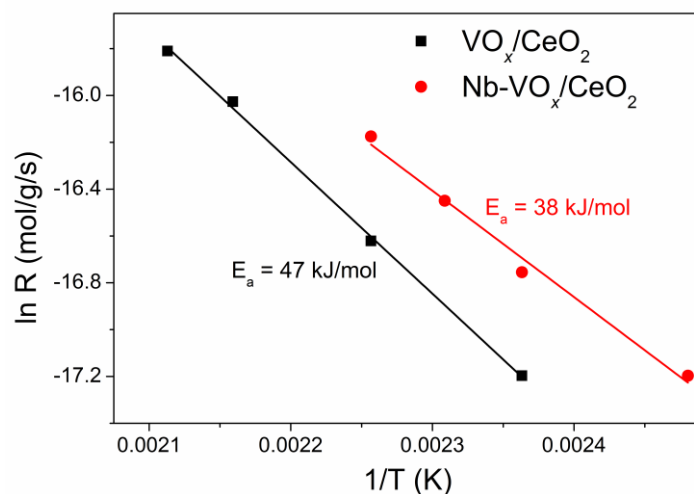


Fig. S5 Plots of rate (R) versus temperature of NO reduction over VO_x/CeO₂ and 30Nb-1VO_x/CeO₂ catalyst. Reaction conditions: total flow rate: 500 ml/min, mass of the catalyst: 100 mg (40-60 mesh), 500 ppm NO + 500 ppm NH₃ + 5% O₂.

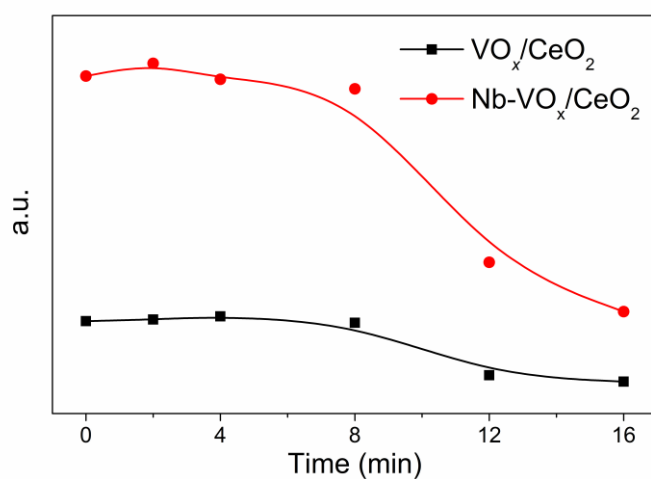


Fig. S6 The band intensities of adsorbed NH₃ species calculated from DRIFT spectra over 1VO_x/CeO₂ and 30Nb-1VO_x/CeO₂ pretreated by exposure to NH₃ followed by exposure to NO + O₂ at 175 °C.

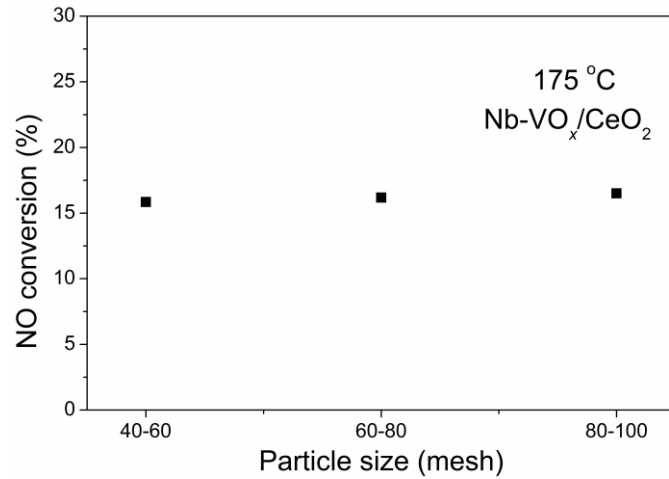


Fig. S7 Influence of particle-size-distribution on the NO conversion over 30Nb-1VO_x/CeO₂ catalyst. Reaction conditions: total flow rate: 500 ml/min, mass of the catalyst: 100 mg, temperature: 175 °C, 500 ppm NO + 500 ppm NH₃ + 5% O₂.

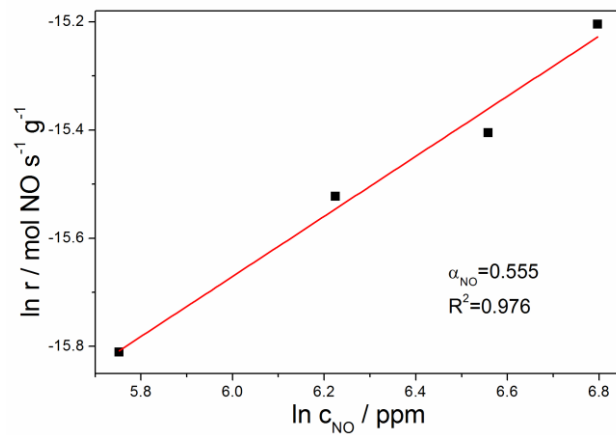


Fig. S8 Plot of $\ln r$ to $\ln c_{\text{NO}}$ over 30Nb-1VO_x/CeO₂ catalyst. Reaction conditions: total flow rate: 500 ml/min, mass of the catalyst: 100 mg (40-60 mesh), temperature: 175 °C, 200-900 ppm NO + 500 ppm NH₃ + 5% O₂.