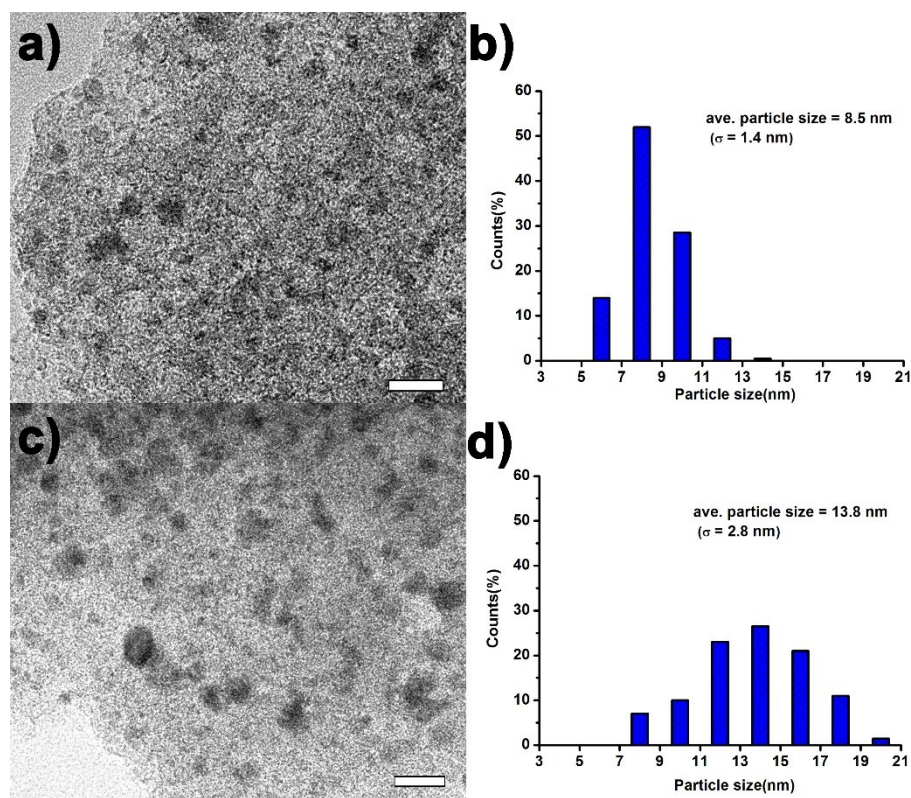


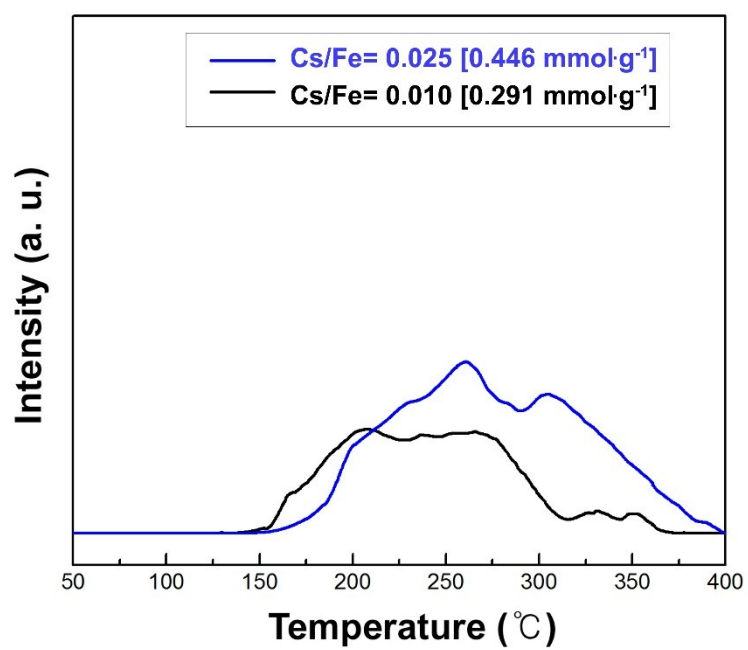
## Supporting Information

### Cs Promoted $\text{Fe}_5\text{C}_2$ /Charcoal Nanocatalysts for Sustainable Liquid Fuel Production

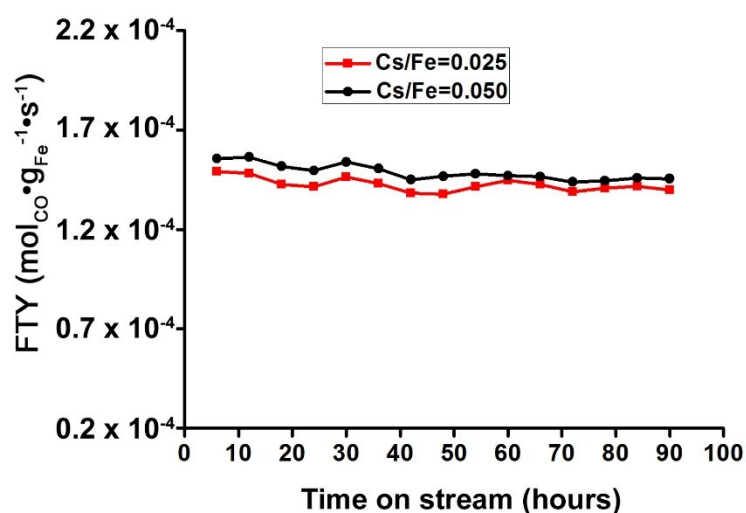
Ji Chan Park,\* Dong Hyun Chun, Jung-Il Yang, Ho-Tae Lee, Sungjun Hong, Geun Bae Rhim, Sanha Jang and Heon Jung\*



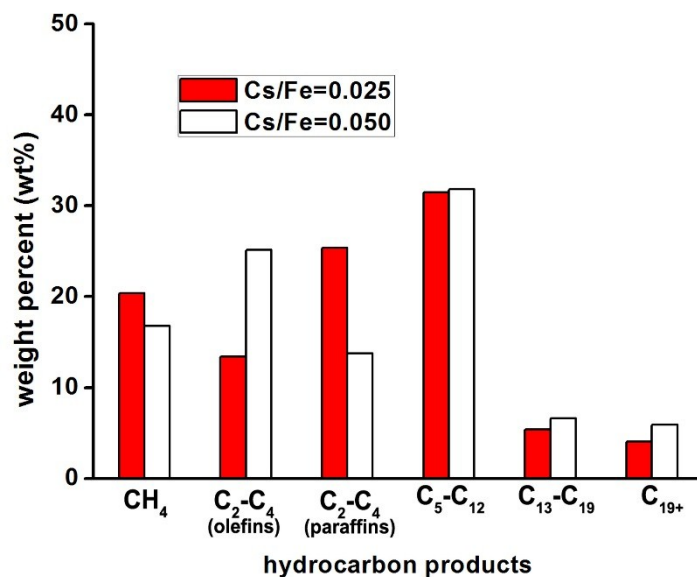
**Fig. S1** TEM images and particle size distribution histograms of Cs promoted  $\text{Fe}_5\text{C}_2$ /charcoal. (a,b) Cs/Fe = 0.025, (c,d) Cs/Fe = 0.050. More than 200 particles were counted for each sample. The bars (a,c) represent 20 nm.



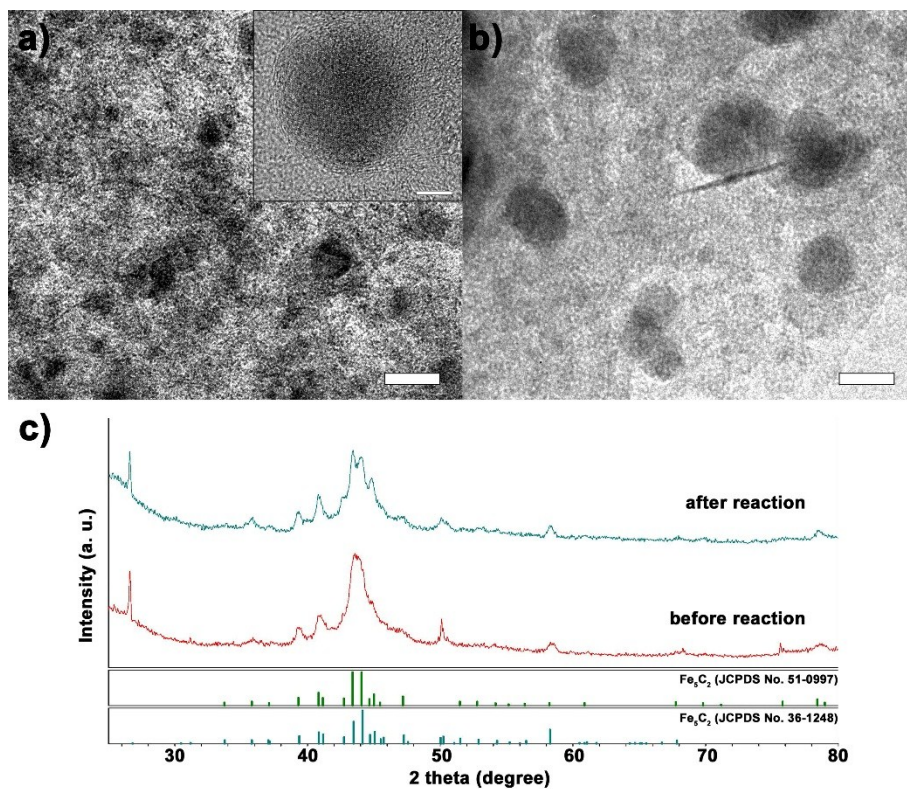
**Fig. S2** CO<sub>2</sub>-TPD profiles of Cs promoted catalysts and amount of CO<sub>2</sub> desorption measured by area under the peak.



**Fig. S3** Catalytic performance of Cs promoted  $\text{Fe}_5\text{C}_2$ /charcoal catalysts for high-temperature FT synthesis.



**Fig. S4** Hydrocarbon product distributions. The hydrocarbon distributions (wt%) for each sample were calculated from GC analysis of gas products ( $\text{C}_1\text{-C}_4$ ) and SIMDIS analysis of isolated liquid and solid products.



**Fig. S5** (a) TEM and HRTEM images (inset) of the recovered Cs promoted  $\text{Fe}_5\text{C}_2/\text{charcoal}$  catalyst (Cs/Fe=0.025) after the FT reaction, (b) TEM image and (c) XRD spectrum of the recovered Cs promoted  $\text{Fe}_5\text{C}_2/\text{charcoal}$  catalyst (Cs/Fe=0.050) after the FT reaction. The bars represent (a,b) 20 nm and (inset) 5 nm.

**Table S1** A comparison of the CO conversion and FT activity of Cs promoted Fe<sub>5</sub>C<sub>2</sub> catalysts with some literature Fe supported catalysts in high temperature FT reactions.

Catalyst	Total CO conv. (%)	FTY (mol <sub>CO</sub> •g <sub>Fe</sub> <sup>-1</sup> •s <sup>-1</sup> )	Ref.
Cs/Fe <sub>5</sub> C <sub>2</sub> /charcoal (Cs/Fe=0.025, Fe 20wt%)	97	1.40×10 <sup>-4</sup>	This work <sup>a</sup>
Cs/Fe <sub>5</sub> C <sub>2</sub> /charcoal (Cs/Fe=0.050, Fe 20wt%)	96	1.45×10 <sup>-4</sup>	This work <sup>a</sup>
Cs/Fe <sub>5</sub> C <sub>2</sub> /charcoal (Cs/Fe=0.100, Fe 20wt%)	63	9.0×10 <sup>-5</sup>	This work <sup>a</sup>
Fe/CNF (Fe 12wt%)	88	2.98×10 <sup>-5</sup>	
Fe-Cu-K-SiO <sub>2</sub> (Fe 32wt%)	79	1.12×10 <sup>-5</sup>	1) <sup>b</sup>
Fe/α-Al <sub>2</sub> O <sub>3</sub> (6wt% Fe)	77	8.48×10 <sup>-5</sup>	
Fe-Ru-K/CNT (9.8wt% Fe)	25	1.1×10 <sup>-4</sup>	2) <sup>c</sup>

Catalytic tests were carried out at <sup>a</sup>T = 320°C, P = 15 bar, H<sub>2</sub>/CO ratio=1, <sup>b</sup>T = 340°C, P = 20 bar, H<sub>2</sub>/CO ratio = 1, and <sup>c</sup>T = 275°C, P = 8 bar, H<sub>2</sub>/CO ratio= 2, respectively.

**Table S2** Liquid and solid hydrocarbon productivity of Cs promoted Fe<sub>5</sub>C<sub>2</sub> on charcoal catalysts.

Data	Catalyst	
	Cs/Fe=0.025	Cs/Fe=0.050
liquid oil productivity (g <sub>liq</sub> •g <sub>cat</sub> <sup>-1</sup> •h <sup>-1</sup> )	0.401	0.296
solid wax productivity (g <sub>sol</sub> •g <sub>cat</sub> <sup>-1</sup> •h <sup>-1</sup> )	0.026	0.164

The g<sub>cat</sub> is the weight sum of Fe and the charcoal support. The values of g<sub>liq</sub> and g<sub>sol</sub> indicate the weights of the isolated liquid oil and solid wax after reaction, respectively.

**Table S3** Gas product yields of Cs promoted Fe<sub>5</sub>C<sub>2</sub> on charcoal catalysts after 90 h on stream.

Catalyst	Gas product yield (10 <sup>-4</sup> g <sub>HC</sub> •g <sub>Fe</sub> <sup>-1</sup> •s <sup>-1</sup> )			
	CH <sub>4</sub>	C <sub>2</sub> -C <sub>4</sub> olefins	C <sub>2</sub> -C <sub>4</sub> paraffins	Total
Cs/Fe = 0.025	2.95	1.94	3.67	8.56
Cs/Fe = 0.050	2.42	3.62	1.99	8.03

#### References)

- 1) H. M. T. Galvis, J. H. Bitter, C. B. Khare, M. Ruitenbeek, A. I. Dugulan and K. P. de Jong, *Science*, 2012, **335**, 835.
- 2) M. C. Bahome, L. L. Jewell, K. Padayachy, D. Hildebrandt, D. Glasser, A. K. Datye and N. J. Coville, *Appl. Catal. A: Gen.*, 2007, **328**, 243.