

Supporting Information

New insight into the promotion effect of Cu doped V₂O₅/WO₃-TiO₂ for low temperature NH₃-SCR performance

Meiqing Shen,^{a,b,c} Chenxu Li,^a Jianqiang Wang,^{*a} Lili Xu,^a Wulin Wang^a and Jun Wang^{*a}

^a Key Laboratory for Green Chemical Technology of State Education Ministry, School of Chemical Engineering & Technology, Tianjin University, Tianjin 300072, PR China

^b Collaborative Innovation Center of Chemical Science and Engineering (Tianjin), Tianjin 300072, PR China

^c State Key Laboratory of Engines, Tianjin University, Tianjin 300072, PR China

* Corresponding author: Jun Wang, Jianqiang Wang

Postal address:

School of Chemical Engineering and Technology, Tianjin University, 92 Weijin Road, Nankai District, Tianjin 300072, China

Email: jianqiangwang@tju.edu.cn; wangjun@tju.edu.cn

Tel. /Fax. : (+86) 22-27407002

NH₃-SCR performance without H₂O

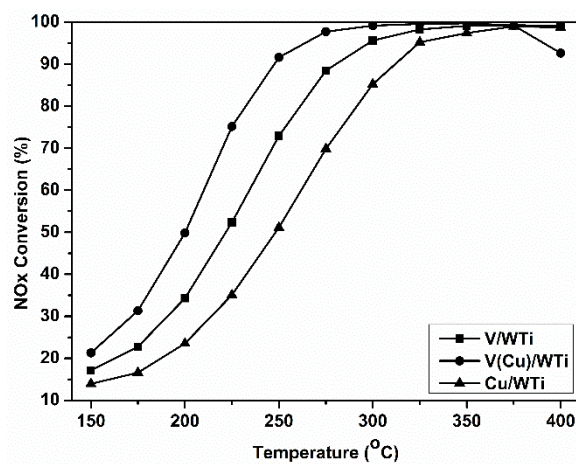


Fig.S1 NH₃-SCR performance on V/WTi, V(Cu)/WTi and Cu/WTi catalysts without H₂O. 500

ppm NH₃, 500 ppm NO, 5 % O₂ and N₂ balance, GHSV=10,000 h⁻¹.

Table S1 surface coverages of Vanadium species on catalysts

Samples	S _{BET} (m ² /g)	V (μmol/m ²)
V/WTi	41	2.7
V(Cu)/WTi	37	2.9

Raman

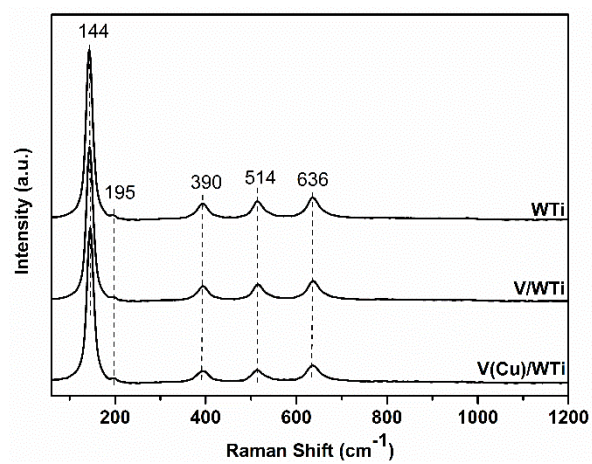


Fig.S2 Raman spectra of the catalysts

XPS

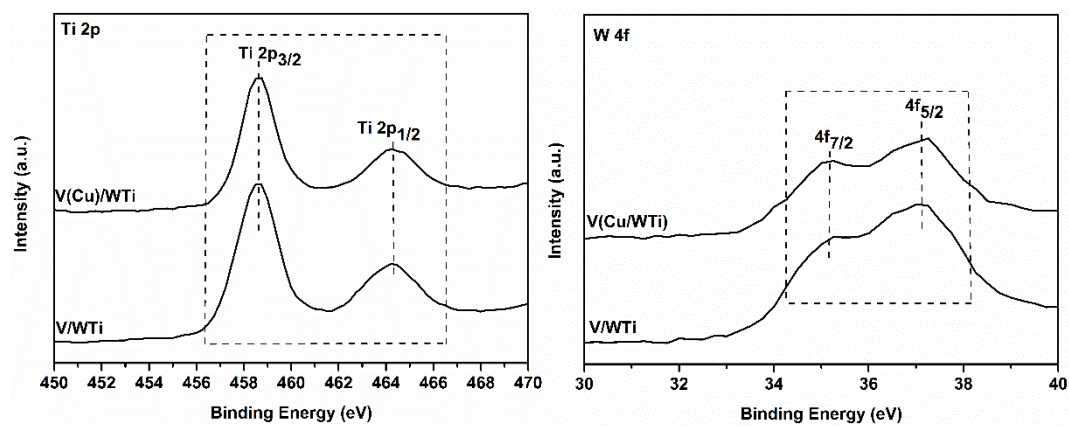


Fig.S3 XPS spectra of the obtained samples: Ti 2p, W 4f.

Reaction between NO+O₂ and adsorbed NH₃ species

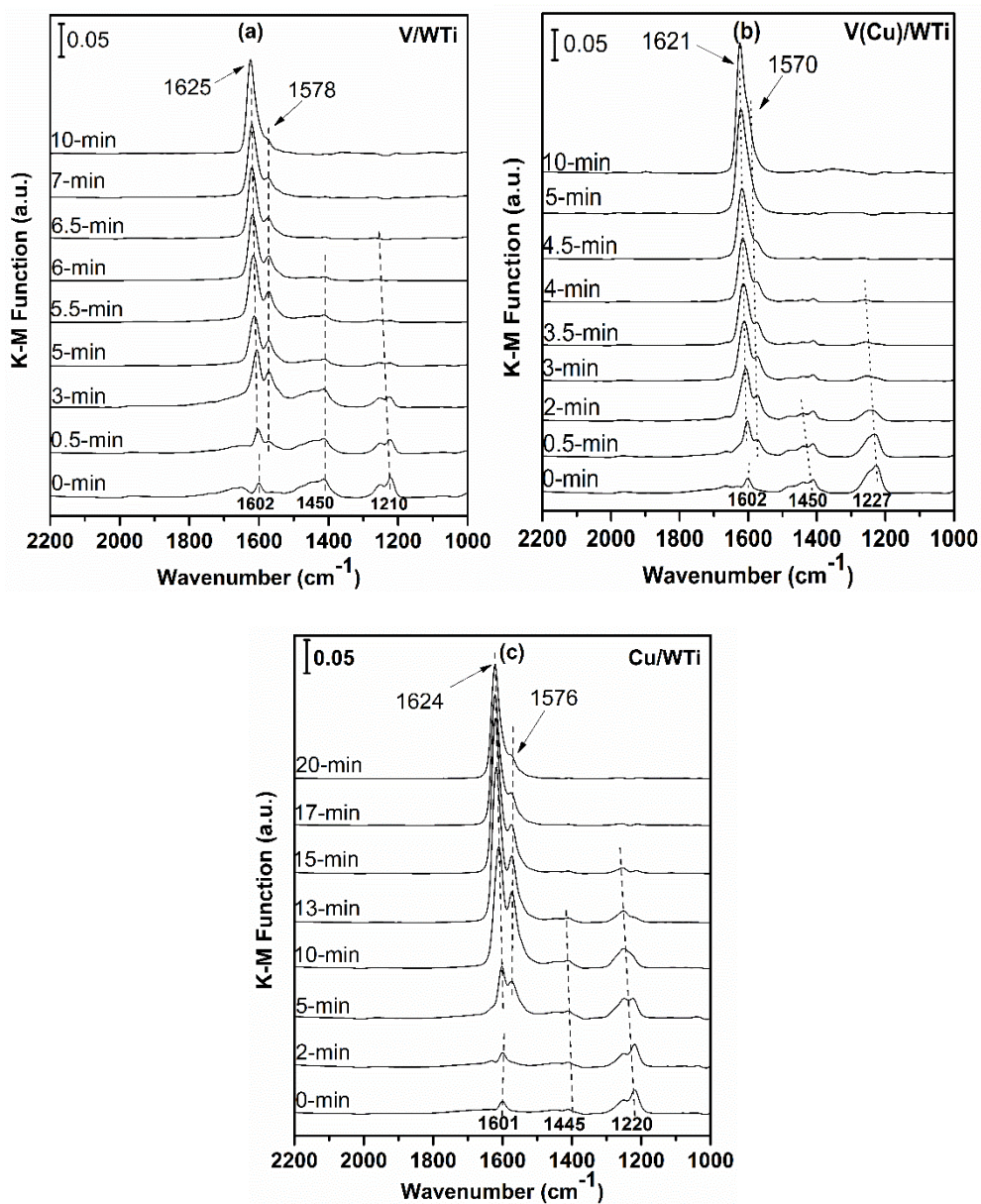


Fig.S4 DRIFTS spectra of catalysts pretreated with 3000 ppm NH₃, followed by exposed to 3000 ppm NO+4 % O₂ as a function of time at 200°C.

For V/WTi sample, after NH₃ were pre-adsorbed and N₂ purging for 30 min, the coordinate NH₃ lined to Lewis acid sites (1602 and 1210 cm⁻¹) and Brønsted (1672 and 1450 cm⁻¹) acid sites form on the surface. After NO+O₂ introduced, the intensities of

all bands assigned to NH_3 species decrease. Meanwhile, some new bands attributed to adsorbed nitrate species (1625 and 1578 cm^{-1}) appear. The result indicates the adsorbed NH_3 species are reactive in the NH_3 -SCR process. For Cu/WTi sample, similar bands due to NH_3 adsorption species are observed, introducing $\text{NO}+\text{O}_2$ results in the NH_3 adsorption species decreasing slowly, accompanying the appearance of nitrates species (1624 and 1576 cm^{-1}). For V(Cu)/WTi sample, the similar phenomenon can be observed during the process. But the consumption rate of the NH_3 adsorption species linked to the Lewis sites distinguishes from other catalysts.

$\text{NH}_3+\text{NO}+\text{O}_2$ reaction

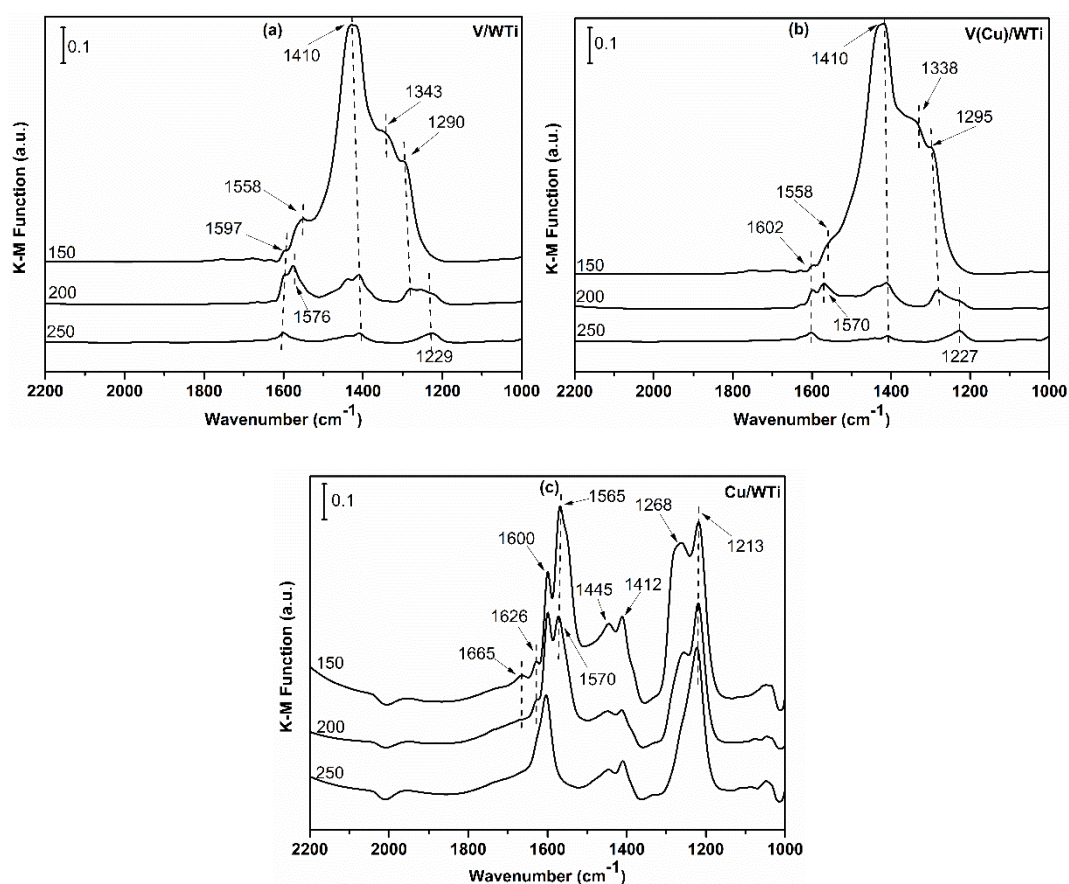


Fig.S5 DRIFTS spectra of catalysts in a flowing of $\text{NH}_3+\text{NO}+\text{O}_2$ at 150 , 200 and 250°C .

To investigate the surface species on the catalyst under the steady-state condition, DRIFTS spectra were recorded in a flow of $\text{NO}+\text{NH}_3+\text{O}_2$ from 150 to 250 °C. On the V/WTi sample, bands due to nitrates (1290 cm^{-1}), coordinated NH_4^+ (1434 cm^{-1}), $-\text{NH}_2$ species (1558 cm^{-1}) and NH_3 (1597 cm^{-1}) are observed at 150 °C. In addition, a new band appears at 1343 cm^{-1} , which is significantly different from the adsorbed nitrates and NH_3 species mentioned above, which can be attributed to the intermediates species converted by surface adsorbed NH_3 and NO_x species^{1, 2}. With the increasing of temperature to 250 °C, the intermediates species (1343 cm^{-1}) and the nitrates (1290 cm^{-1}) vanished completely with the NH_4^+ (1434 cm^{-1}) diminishing quickly. During the process, $-\text{NH}_2$ species (1558 cm^{-1}) disappear with nitrates (1576 cm^{-1}) appearing, and then only adsorbed NH_3 species (1597 and 1229 cm^{-1}) still exist at 250 °C. In regard with the V(Cu)/WTi sample, the similar process can be observed. While the intensities of $-\text{NH}_2$ species (1558 cm^{-1}) are obviously weaker than those of V/WTi sample, which indicates that $-\text{NH}_2$ species (1558 cm^{-1}) adsorbed on the V(Cu)/WTi are higher active than those of V/WTi sample. The intensities of $-\text{NH}_2$ species almost vanished at 200 °C due to the rapid consumption by the NO_x reagent, which is in agreement with the results of reaction between $\text{NO}+\text{O}_2$ and adsorbed NH_3 species. Meanwhile, the band of nitrates species at 1570 cm^{-1} appears and the intensities of them are obviously weaker than those of V/WTi sample, which may be caused by the competitive adsorption between NH_3 and $\text{NO}+\text{O}_2$ or the weaker adsorbed nitrates on the catalyst surface. Therefore it is beneficial for the reaction between adsorbed NH_3 species and the gas NO or weak

adsorbed NO according to the E-R mechanism imposed by Topsøe³. In view of Cu/WTi sample, it is clear that no intermediates species (1335 cm⁻¹) can be observed and large amounts of –NH₂ species (1565 cm⁻¹) exist on the catalyst surface at 150°C, which strongly indicates the weakest NH₃-SCR performance among the three catalysts at low temperature.

Notes and references

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2. X. Yao, L. Zhang, L. Li, L. Liu, Y. Cao, X. Dong, F. Gao, Y. Deng, C. Tang, Z. Chen, L. Dong and Y. Chen, *Appl. Catal., B*, 2014, **150–151**, 315-329.
3. J. A. Dumesic, N. Y. Topsøe, H. Topsøe, Y. Chen and T. Slabiak, *J. Catal.*, 1996, **163**, 409-417.