

High performance polydimethylsiloxane pervaporation
membranes with hyperbranched polysiloxane as crosslinker for
separation of *n*-butanol from water

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1. PV experiments method

The PV experiments were carried out at various temperatures using a pervaporation cell with the effective membrane area of 35.24 cm². In pervaporation operation, the pressure of downstream side (permeate side) was maintained at 200 ± 10Pa. The permeated mass was collected in a condensation trap cooled by liquid nitrogen. The composition in feed mixture and the corresponding permeate was detected by gas chromatography (GC) SP-6800A (Shangdong, China) equipped with a packed column and a thermal conductivity detector (TCD).

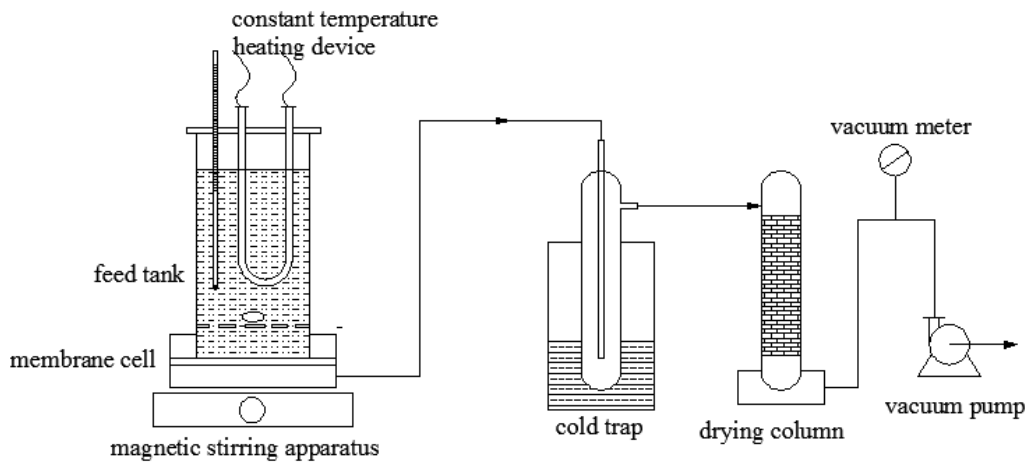


Fig.S1 Schematic diagram of the experimental equipment

2. Scanning electron microscope



Fig.S2 Surface morphology of HPSiO-c-PDMS membranes: (a) HPSiO-c-PDMS-1, (b) HPSiO-c-PDMS-2, (c) HPSiO-c-PDMS-3

3. Contact angle measurements of HPSiO-c-PDMS membranes

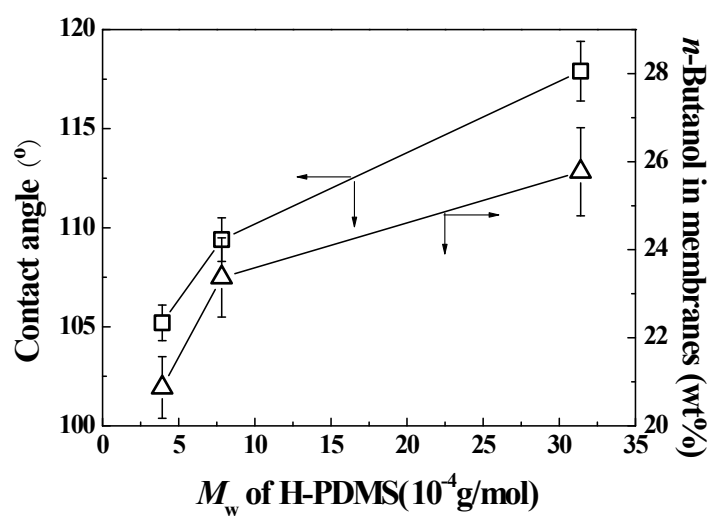


Fig.S3. Effect of H-PDMS molecular weight on *n*-butanol concentration in membranes and contact angle of HPSiO-c-PDMS membranes

4. GPC spectroscopy of PDMS

Table S1 Molecular weights and PDI of H-PDMS and HPSiO

Samples	Molecular weight		PDI ^c
	M_w^a	M_n^b	
H-PDMS-1	39250	24369	1.61
H-PDMS-2	78263	49437	1.58
H-PDMS-3	314043	195815	1.60
HPSiO	3513	1417	2.48

^a M_w , weight average molecular weight;

^b M_n , number average molecular weight;

^c Polydispersity index (PDI) = M_w/M_n