Supporting Information:

An active and stable Ni/Al $_2O_3$ nanosheet catalyst for dry reforming

of CH_4

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SI-1. Experimental details

Catalyst Preparation

Nickel 2, 4-pentanedionate and Al(NO₃)₃·9H₂O was used as nickel source and aluminum source respectively. Moreover, (NH₂)₂CO and TX-100 were used as alkali source and surfactant respectively. All chemicals were of analytical grade and used without further re-purification. Nickel 2, 4-pentanedionate (0.46g) was dissolved in deionized water (70 mL), and then (NH₂)₂CO (0.11g) and Triton X-100 (0.05g) were added to form a clear solution under stirring at 333K. The reactant mixture was then transferred into a 150 mL Teflon-lined autoclave and heated at 423K for 2 h. After the autoclave had been allowed to cool to room temperature, the Ni(OH)₂ nanoparticles were re-dispersed by ultrasonic treatment and then Al(NO₃)₃·9H₂O (6.62g), $(NH_2)_2CO$ (1.67g) were added to this solution in order. The mixture was then transferred into a 150 mL Teflon-lined autoclave and heated at 423K for 5 h. When the reaction was completed, the autoclave was cooled to room temperature. The products were collected and purified by repeated centrifugation and then dried at 393 K for 2 h. Calcination step was carried out by slowly increasing temperature from room temperature to 773 K (2 K/min) and keeping at 773 K for 3 h. The as-prepared sample Ni/Al₂O₃ was signed as fresh Ni/Al₂O₃ (T). The Ni/Al₂O₃ catalysts by one-step hydrothermal (signed as Ni/Al₂O₃ (O)) used a 150 mL Teflon-lined autoclave and heated at 423K for 5 h. For comparison, a conventional Ni/Al₂O₃ catalyst was prepared by impregnation method (signed as Ni/Al₂O₃ (I)) using Al₂O₃ support synthesized by hydrothermal method under the same reaction conditions. The nickel loading of all catalysts was 10 wt %, which was confirmed by EDX.

Characterization of catalysts

For characterization of reduced catalysts, the calcined catalysts were reduced by pure hydrogen at 1073 K for 2 h and then passivated by 1% O_2 in N_2 to form a metal oxide layer on the surface of metal particle in order to preventing oxidation of nickel metal when the catalysts were exposed to air. The surface area and the pore size distribution were determined via nitrogen adsorption, using AUTOSORB-IQ instrument. The surface area was calculated using the BET method, while the pore size distribution curve was obtained from the adsorption branch of the N_2 isotherm by the BJH method.

XRD patterns of Ni/Al₂O₃ catalysts were recorded on a D/Max 2500VB2+/PC diffracttometer with Cu K α radiation (λ = 0.154056 nm). The samples were scanned with a speed of 2 degree/min.

For the reduction behavior, temperature-programmed reduction (TPR) was carried out in a quartz tube reactor using 0.1 g calclined catalysts. The reducing gas, a mixture of 10% H₂ diluted by Ar, was fed via a mass flow controller at 30 cm³/min and then the sample was heated to 1173 K at a constant heating rate of 10 K/min. The signal of hydrogen consumption was detected by a thermal conduction detector (TCD). The effluent of reactor passed through a 5 A molecular sieve trap to remove produced water, before reaching TCD.

Scanning electron microscopy (SEM) was used to determine the catalyst granule morphology, using a JEOL JSM-7600F scanning electron microscope.

Thermo gravimetric thermal analysis (TG-DTA) was carried on a HTG-1 (henven) instrument from 323 K and 1073 K at a heating rate of 10 K/min to determine the carbon deposition of used catalysts.

Transmission electron microscopy (TEM) and High-resolution transmission electron microscopy (HRTEM) images of the catalysts were determined by JEM-2100 microscope. The specimen was prepared by ultrasonically suspending the catalyst powder in ethanol. A drop of the suspension was deposited on a carbon grid and dried in air.

Scanning transmission electron microscopy (STEM) was carried on a Tecnai G2 F20 S-TWIN instrument. The specimen was prepared in a similar way adopted in TEM characterization.

In order to study the thickness of Ni/Al_2O_3 (T) catalyst, Atomic force microscopy (AFM) observations were performed by a DMFASTSCAN2-SYS instrument.

Catalysts testing in dry reforming of CH₄

The catalytic activity in CO₂ reforming of CH₄ was tested using a quartz tube reactor (7 mm in diameter) at atmospheric pressure. The 100 mg catalysts were loaded into reactor and reduced by hydrogen at 1073 K for 2h and then purged by N₂. The dry reforming of methane reaction was carried out at 973 K or 1073 K under atmospheric pressure (Ar/CH₄/CO₂=4/48/48, where Ar is inner reference, GHSV=21000cm³·g⁻¹·h⁻¹). The products were analyzed by on-line gas chromatograph equipped with a thermal conductivity detector (TCD). **SI-2.** Figure S1 TEM images of catalyst at different stage of experiments and XRD pattern of products of first step hydrothermal process



Fig.S1 TEM images of catalyst at different stage of experiments: (a) after the first step hydrothermal, (b) second step hydrothermal for 1h, (c) second step hydrothermal for 2h, (d) second step hydrothermal for 3h, (a*)XRD pattern of products of first step hydrothermal process.

For the formation of leaf like nano structured Ni/Al₂O₃ (T) catalyst, it is considered that the Ni(OH)₂ particles would partially dissolved into the solution of second hydrothermal reaction, leading to modifying the crystallization of Al₂O₃. As reported by Msharrafieh and Langer, ^{1, 2} the possible chemical reactions during secondary hydrothermal reaction could be presented as eq. (1)–(4).

$$(NH_2)_2CO+3H_2O\rightarrow 2 NH_4OH + CO_2$$
(1)

$$Ni(OH)_2 + 6NH^{4+} + 4OH^{-} \rightleftharpoons Ni(NH_3)_6^{2+} + 6H_2O$$
 (3)

$$2AI^{3+}+6NH_4OH=3NH^{4+}+2AI(OH)_3\downarrow+3H_2O$$
 (4)

Under the secondary hydrothermal conditions, the $Ni(OH)_2$ nanoparticles were gradually dissolved to generate $Ni(NH_3)_6^{2+}$ and reacted with the $Al(OH)_3$ or AlOOH,

resulting in that redissolved $Ni(OH)_2$ entered the lattice of generated $Al(OH)_3$ or co-precipitated with the $Al(OH)_3$.

Figure S1 exhibited the TEM images of Ni(OH)₂ particles after the first step hydrothermal process and products of secondary hydrothermal reaction at 423 K for 1 h, 2 h, and 3 h, respectively. The image of Ni(OH)₂ particles synthesized in the first step hydrothermal process (Fig. S1a) showed that the particles dispersed very well and diameters of the sphere-like particles were about 5 nm. As shown in Fig. S1a*, the peaks attributed to Ni(OH)₂ (PDF#01-1047) were observed for the product of first step hydrothermal process. After 1h reaction of the second hydrothermal process, partial dissolution of Ni(OH)₂ particles and generation of Al(OH)₃ or AlOOH were observed as shown in Figure S1b. With increasing reaction time, it can be found that three or more particles are linked together each other at the certain principle in Fig. S1c. After 3h reaction (Fig. S1d), Ni(OH)₂ particles highly dispersed on Al(OH)₃ or AlOOH and the diameter of Ni(OH)₂ particles formed in the first step hydrothermal process.

In recent years, the oriented attachment (OA) growth of crystals ³ has shown great potential in controlling and designing materials of various nanostructures. The structure is grown from small primary nanoparticles through an oriented attachment mechanism, in which the adjacent nanoparticles are self-assembled by sharing a common crystallographic orientation and docking of these particles at a planar interface. It is reported that the CuO nanoleaves ⁴ and well-defined CuO nano architectures ⁵ have been synthesized based on the OA growth of crystal. Therefore, it is considered that the leaf like nanosheet of Ni/Al₂O₃ (T) catalyst (Fig. 2a) might be formed following the oriented attachment (OA) growth of crystals.



SI-3. Figure S2 XRD patterns of catalysts: (a) fresh, (b) passivated.

Fig.S2 XRD patterns of catalysts: (a) fresh, (b) passivated

SI-4. Figure S3 H_2 -TPR profiles of the samples.



Fig. S3 H₂-TPR profiles of three catalysts.

SI-5. Figure S4 TEM image of Ni/Al_2O_3 (T) after 50 h reaction.



Fig. S4 TEM image of Ni/Al₂O₃ (T) after 50 h reaction.

SI-6. Figure S5 TG/DTA profiles of Ni/Al₂O₃ (T) after 50 h reaction.



Fig. S5 TG/DTA profiles of Ni/Al₂O₃ (T) after 50 h reaction.



SI-7. Figure S6 XRD patterns of used catalysts

Fig. S6 XRD patterns of used catalysts

SI-8. Figure S7 TG / DTA profiles of used catalysts.



Fig. S7 TG / DTA profiles of used catalysts after CO₂/CH₄ reforming at 973 K for 10 h.

SI-9. Table S1 Textural and structural characteristics of the synthesized samples.

Catalysts	S_{BET} $(m^2/g)^a$	Pore volume (cc/g) ^b	Pore size (nm) ^b	Ni cluster size (nm) ^c		Ni particle size (nm) ^c	
				passivated	used	passivated	used
Ni/Al ₂ O ₃ (T)	508	0.64	2.4	9.62	9.78	2.15	2.21
$Ni/Al_2O_3(O)$	141	0.22	2.9	6.81	8.14	1.81	2.32
Ni/Al ₂ O ₃ (I)	258	0.59	6.1	8.02	12.15	2.32	3.84

Table S1 Physiochemical properties of various catalysts.

^{*a*} BET surface area; ^{*b*} Calculated by BJH method; ^{*c*} Average cluster size calculated from TEM images.

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