

Electronic Supplementary Information (ESI) for

**Multi-hydroxyl-containing porous organic
polymers based on phenol formaldehyde resin
chemistry with high carbon dioxide capture
capacity**

Shi-Hui Jia,^a Xuesong Ding,^{*,b} Hai-Tao Yu,^{*,a} and Bao-Hang Han^{*,b}

*^a School of Chemistry and Materials Science, Hebei Normal University,
Shijiazhuang 050024, China*

*^b National Center for Nanoscience and Technology, Beijing 100190,
China*

Tel.: +86 10 8254 5576. Email: hanbh@nanoctr.cn

Tel.: +86 10 8254 5708. Email: dingxs@nanoctr.cn

Tel.: +86 311 8078 7402. Email: haitaoyu@mail.hebtu.edu.cn

A. Elemental analysis data

Table S1 Elemental analysis data of **PFPOP-1–3**.

PFPOPs		C	N	H
PFPOP-1	Exp. (%)	68.13	0	3.62
(C ₄₅ H ₃₀ O ₁₂)	Cal. (%)	70.86	0	3.96
PFPOP-2	Exp. (%)	72.53	0	4.04
(C ₆₃ H ₄₂ O ₁₂)	Cal. (%)	76.36	0	4.27
PFPO-3	Exp. (%)	68.09	1.24	4.25
(C ₅₇ H ₃₉ O ₁₂ N)	Cal. (%)	73.62	1.51	4.23

B. Solid-state ^{13}C NMR spectra

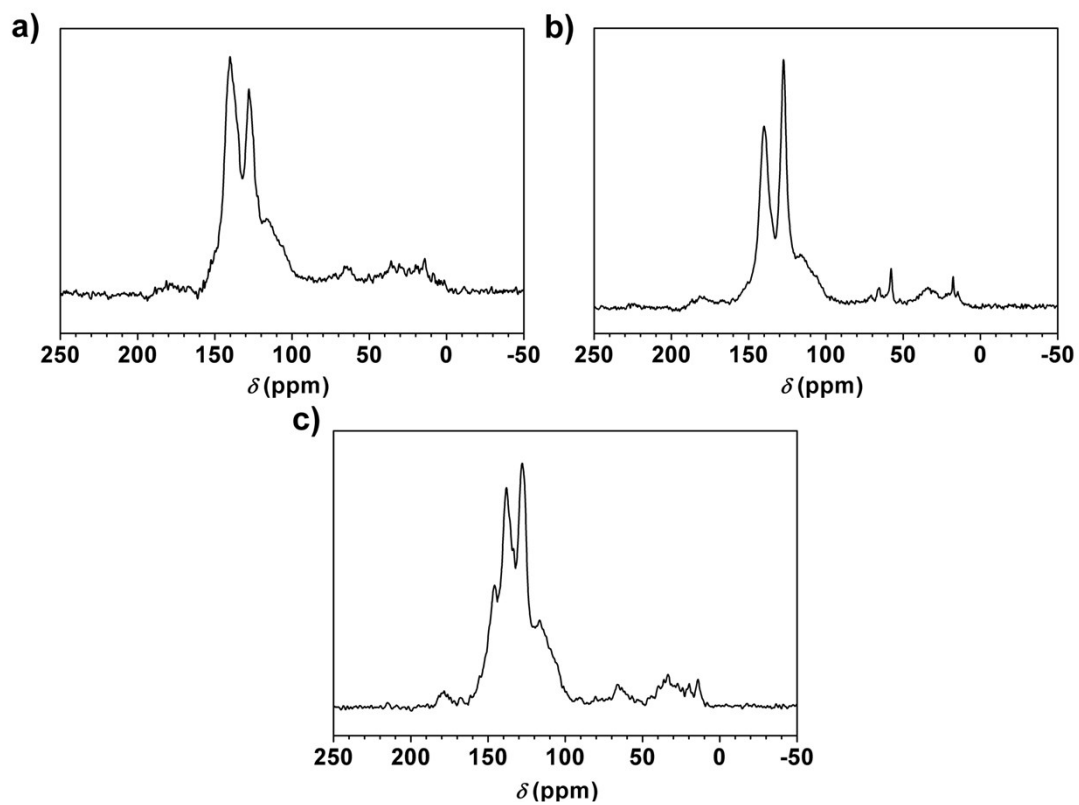


Fig. S1 Solid-state ^{13}C NMR spectra of (a) **PFPOP-1**, (b) **PFPOP-2** and (c) **PFPOP-**

3.

C. TEM images

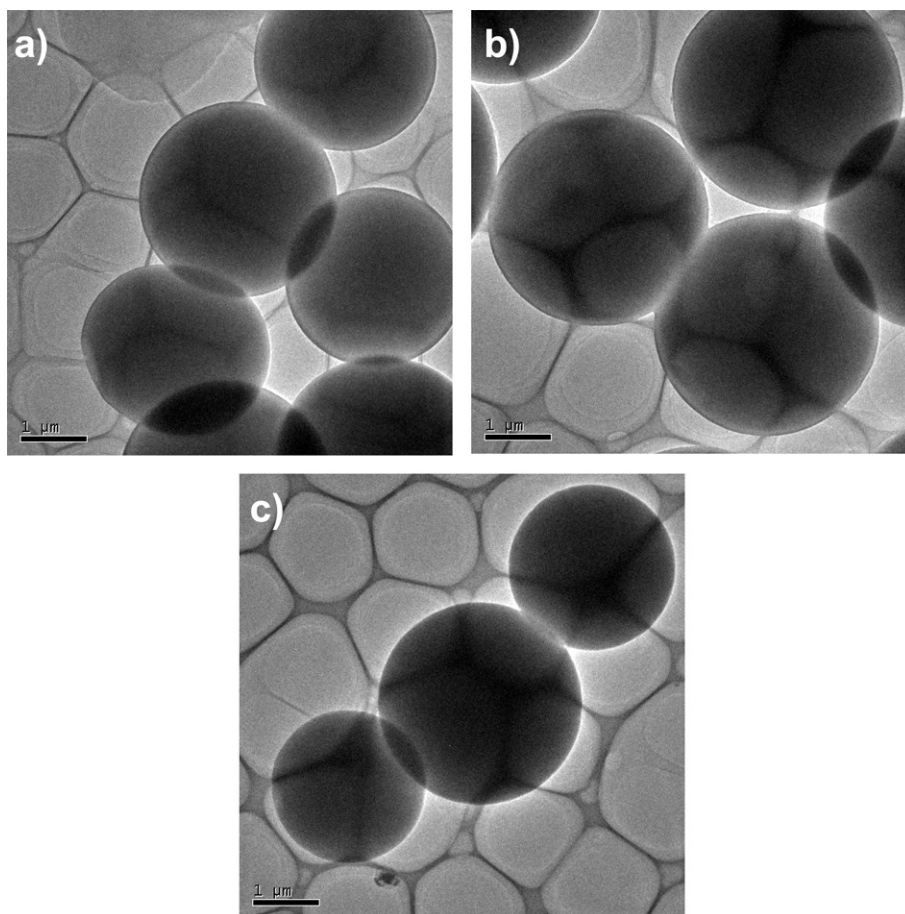


Fig. S2 TEM images of (a) **PFPOP-1**, (b) **PFPOP-2**, and (c) **PFPOP-3**.

D. Corresponding data of porosity properties

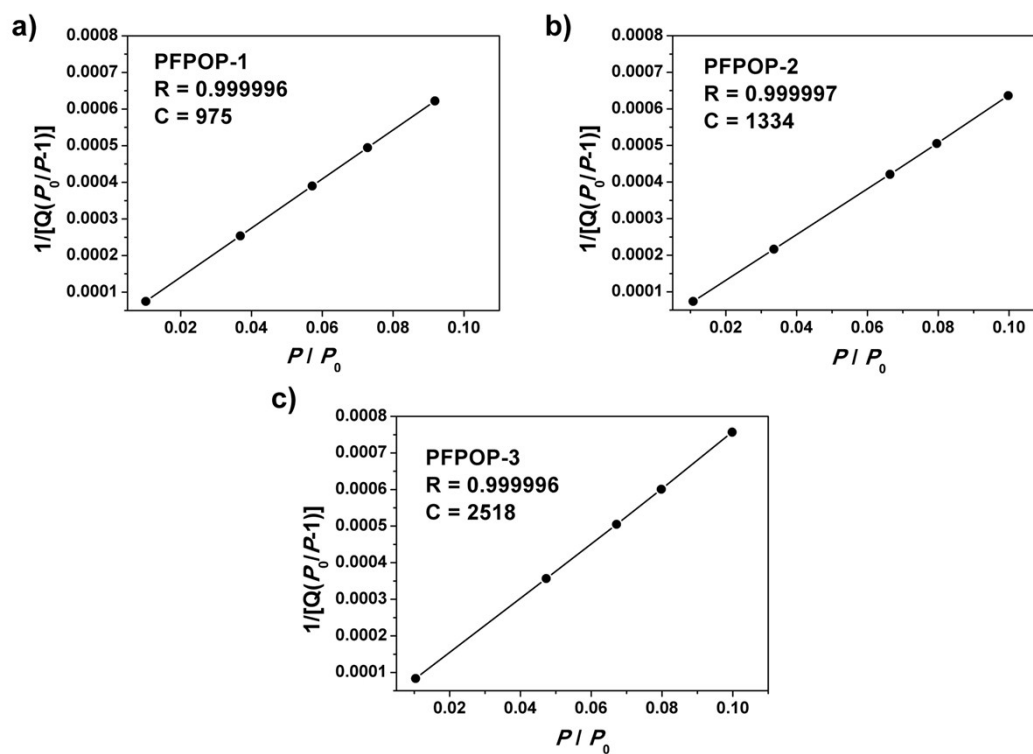


Fig. S3 BET plots of PFPOP-1 (a), PFPOP-2 (b), and PFPOP-3 (c) from nitrogen adsorption data.

E. Corresponding data of gas adsorption and selectivities

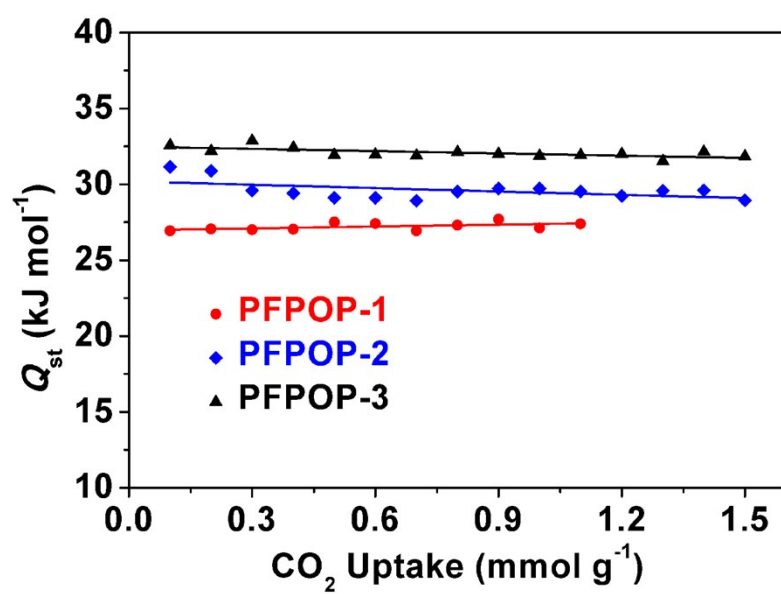


Fig. S4 The isosteric heats of adsorption of CO₂ for PFPOP-1–3.

Ideal adsorbed solution theory (IAST) selectivity studies

In order to evaluate the efficiency of PFPOPs for CO₂ over N₂ separation, we used the Ideal Adsorbed Solution Theory (IAST) of Myers and Prausnitz along with the pure component isotherm fits to determine the molar loadings in the mixture for specified partial pressures in the bulk gas phase.

The pure component isotherms of CO₂ measured at 273 K were fitted with the dual-site Langmuir (DSL) model:

$$q = q_A + q_B = q_{\text{sat,A}} \frac{b_A p}{1 + b_A p} + q_{\text{sat,B}} \frac{b_B p}{1 + b_B p}$$

The pure component isotherms of N₂ measured at 273 K were fitted with the single-site Langmuir (SSL) model:

$$q = q_{\text{sat,A}} \frac{b_A p}{1 + b_A p}$$

where, q is molar loading of adsorbate (mmol g⁻¹), q_{sat} is saturation loading (mmol g⁻¹), b is parameter in the pure component Langmuir isotherm (bar⁻¹), p is bulk gas phase pressure (bar).

Pure-component isotherm fitting parameters were then used for calculating IAST binary-gas adsorption selectivities (S_{ads}). S_{ads} is defined as:

$$S_{\text{ads}} = \frac{q_1/q_2}{p_1/p_2}$$

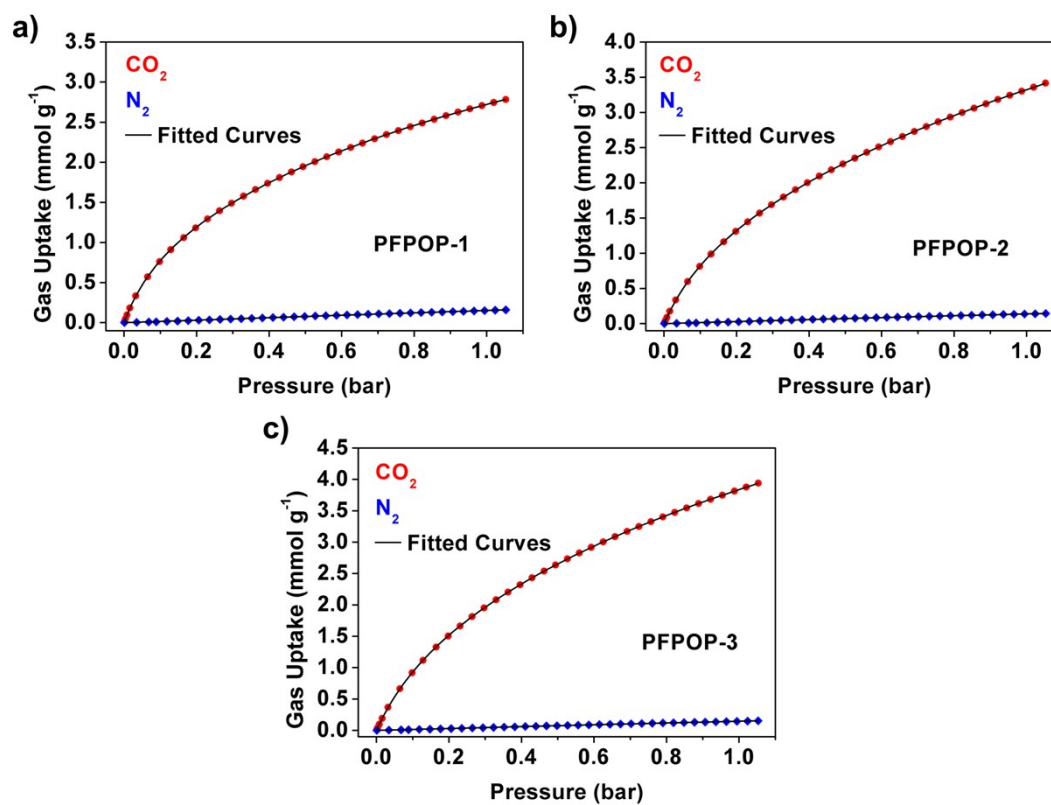


Fig. S5 The corresponding isotherm fits (solid black lines) dual-site Langmuir model fits for CO₂ and single-site Langmuir model for N₂ of **PFPOP-1** (a), **PFPOP-2** (b), and **PFPOP-3** (c) based on experimental pure component isotherms for CO₂ (red) and N₂ (blue) at 273 K.

Table S2 Langmuir fitting parameters of CO₂ and N₂ adsorption isotherms of **PFPOP-1–3** at 273 K.

PFPOPs	Gas	$q_{\text{sat,A}}$ (mmol g ⁻¹)	b_{A} (bar ⁻¹)	$q_{\text{sat,B}}$ (mmol g ⁻¹)	b_{B} (bar ⁻¹)
PFPOP-1	CO ₂	4.78740	0.55962	1.11936	8.68132
	N ₂	6.12831	0.02553		
PFPOP-2	CO ₂	8.12292	0.34526	1.43774	6.22190
	N ₂	1.62911	0.09268		
PFPOP-3	CO ₂	7.99534	0.44457	1.61727	5.72241
	N ₂	3.14180	0.04877		