

**Supplementary Information for**

**Nitric oxide emission during the reductive heterogeneous photocatalysis of aqueous nitrate  
with TiO<sub>2</sub>**

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## Experimental section

### Chemicals

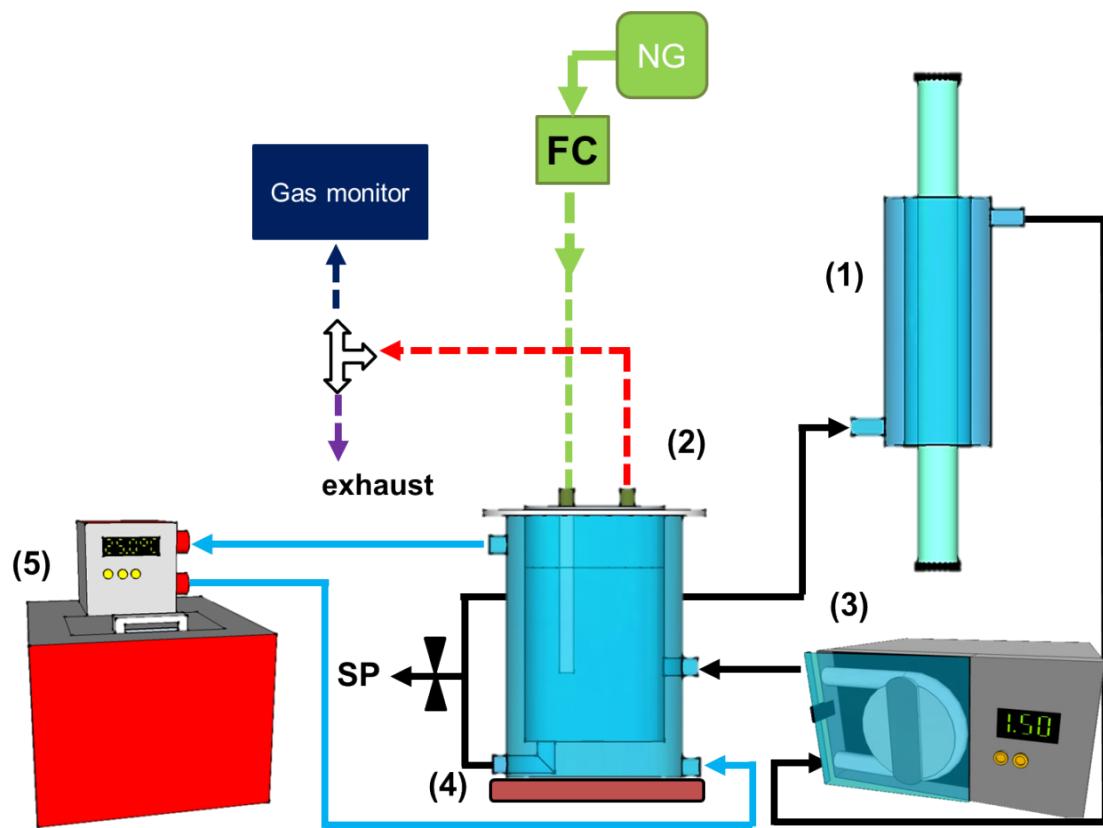
$\text{KNO}_3$  (> 99%, Mallinkrodt), concentrated  $\text{HClO}_4$  (70%, Biopack) and  $\text{HCOOH}$  (88%, Biopack) were used without further purification. Analytical calibration standards of  $\text{KNO}_3$ ,  $\text{NaNO}_2$  and  $\text{NH}_4\text{Cl}$  were obtained from ChemLab and  $\text{TiO}_2$  Aerioxide P25 was provided by Evonik. All experiments were done with MilliQ water (resistivity = 18  $\text{M}\Omega \text{ cm}$ ) and all mentioned chemicals were analytical grade or superior.

### Photocatalytic experiments

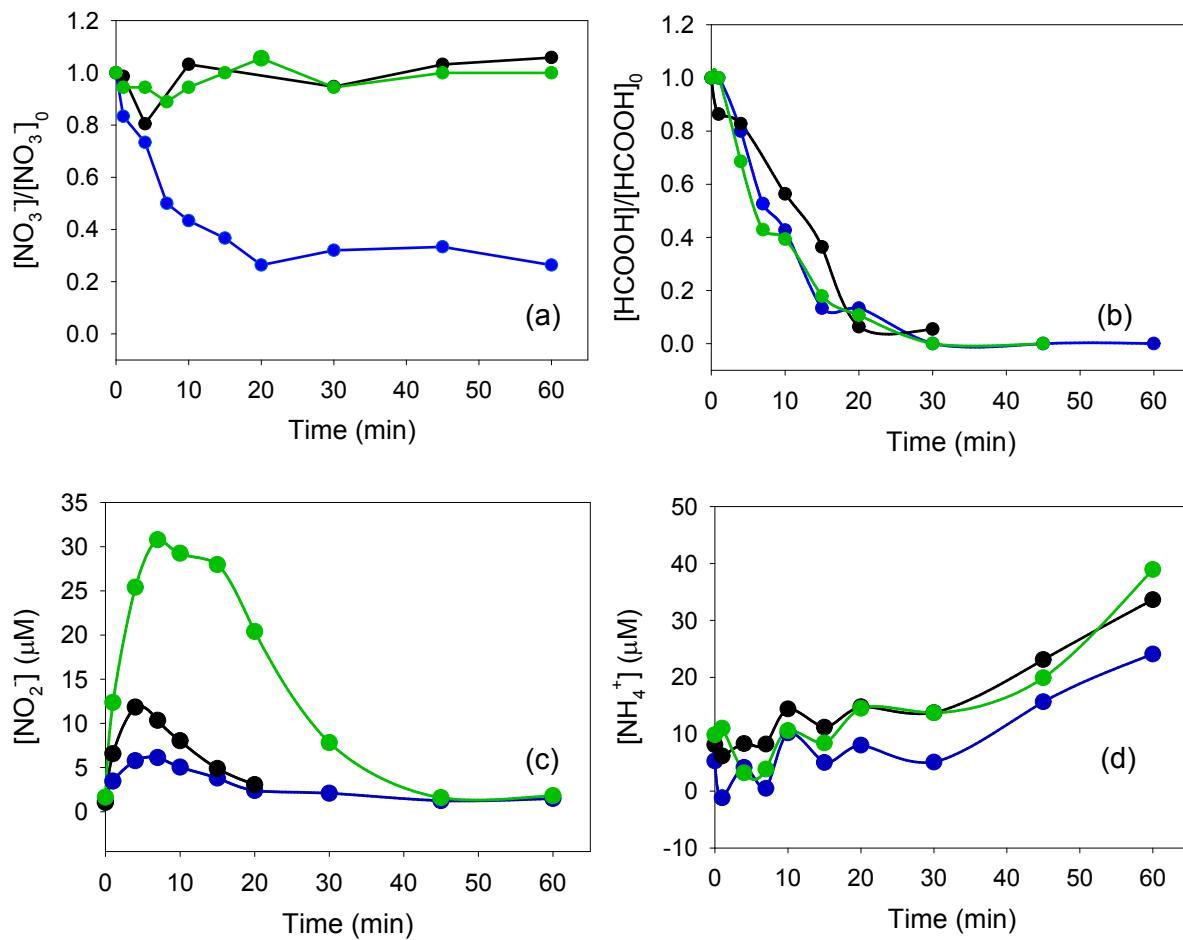
Photocatalytic removal of nitrate was carried out in a recirculating batch reactor (Figure S1) consisting in a glass jacketed reservoir, a recirculation peristaltic pump and a tubular Pyrex® glass photoreactor with annular section, equipped with a 15 W actinic lamp (Phillips TL-D,  $\lambda_{\text{max}} = 366$  nm). In each experiment, 500 mL of  $\text{TiO}_2$  suspension at pH 2.8 (adjusted with  $\text{HClO}_4$ ), with the desired concentrations of  $\text{KNO}_3$  ( $[\text{NO}_3^-]_0 = 80\text{--}8000 \mu\text{M}$ ) and  $\text{HCOOH}$  ( $[\text{HCOOH}]_0 = 100\text{--}1000 \mu\text{M}$ ), was added into the reactor, recirculated during 30 min in the dark to reach the adsorption equilibrium on the catalyst surface, and then irradiated for at least 60 min. Adsorption of nitrate and formic acid on the photocatalyst was negligible, as found previously by Wehbe et al.<sup>1</sup> All the experiments were made at  $25.0 \pm 0.1^\circ\text{C}$  and under continuous  $\text{N}_2$  bubbling at  $600 \text{ mL min}^{-1}$ .

Samples were periodically withdrawn, filtered through 0.22  $\mu\text{m}$  cellulose acetate filters and conditioned to determine  $[\text{NO}_3^-]$ ,  $[\text{NO}_2^-]$ ,  $[\text{NH}_4^+]$  and  $[\text{HCOOH}]$ . The concentrations of  $\text{NO}_3^-$ ,  $\text{NO}_2^-$  and  $\text{NH}_4^+$  were measured spectrophotometrically using the standard methods SM-4500-NO3-E,<sup>2</sup> SM-4500-NO2-B<sup>3</sup> and SM-4500-NH3-F,<sup>4</sup> respectively, employing a HP8453A spectrophotometer (Hewlett-Packard) with UV detection.  $\text{HCOOH}$  concentration was determined using a Shimadzu 5000 A TOC analyzer in the non-purgeable organic carbon (NPOC) mode.

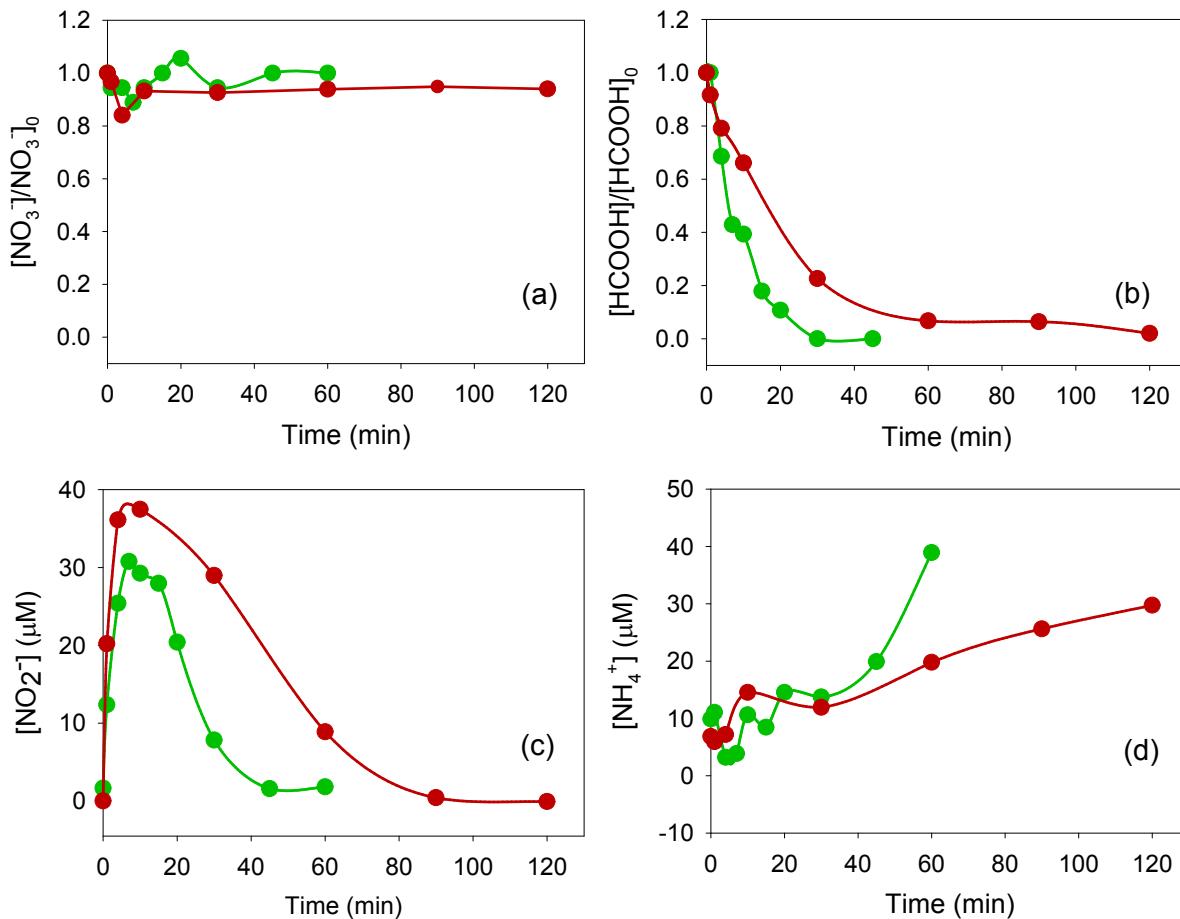
$\text{NO}_x$  concentration during the photocatalytic runs was monitored using a Horiba PG-250 gas phase analyzer based on the chemiluminescent reaction between  $\text{NO}$  and  $\text{O}_3$ .<sup>5</sup>



**Figure S1.** Recirculating batch reactor: (1) Pyrex® tubular photoreactor, (2) glass jacketed reservoir, (3) peristaltic pump, (4) magnetic stirrer, (5) thermocirculator. FC is the flow controller, NG the nitrogen generator and SP is the liquid sampling port used to collect samples during the photocatalytic runs.



**Figure S2.** Time evolution for (a)  $[\text{NO}_3^-]/[\text{NO}_3^-]_0$ , (b)  $[\text{HCOOH}]/[\text{HCOOH}]_0$ , (c)  $[\text{NO}_2^-]$  and (d)  $[\text{NH}_4^+]$  during the treatment of  $\text{NO}_3^-$  by HP in aqueous phase with  $\text{TiO}_2$  in the presence of  $[\text{HCOOH}] = 0.1 \text{ mM}$  and  $[\text{NO}_3^-]_0 = 0.08 \text{ mM}$  (blue),  $0.8 \text{ mM}$  (black) and  $8 \text{ mM}$  (green).



**Figure S3.** Time evolution for (a)  $[\text{NO}_3^-]/[\text{NO}_3^-]_0$ , (b)  $[\text{HCOOH}]/[\text{HCOOH}]_0$ , (c)  $[\text{NO}_2^-]$  and (d)  $[\text{NH}_4^+]$  during the treatment of  $\text{NO}_3^-$  by HP in aqueous phase with  $\text{TiO}_2$  in the presence of  $[\text{HCOOH}]_0 = 0.1$  (green) and 1 mM (red) and  $[\text{NO}_3^-]_0 = 8$  mM.

## REFERENCES

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