

Electronic Supplementary Information

**Unprecedented performance of N-doped activated hydrothermal carbon towards
C₂H₆/CH₄, CO₂/CH₄, and CO₂/H₂ separation**

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Fitting of adsorption isotherms with Toth model

The pure-component adsorption isotherms of C₂H₆, CO₂, CH₄, and H₂ were well fitted with Toth model:

$$q = \frac{q_m (bP)^t}{(1 + (bP)^t)^{1/t}}$$

Here, q is the amount of gas uptake (mmol g⁻¹), q_m is the maximum amount of gas uptake (mmol g⁻¹), P is the equilibrium pressure (kPa), b (kPa⁻¹) and t are constants. The fitting parameters are summarized in Table S3 along with the average relative deviation (ARD) defined by the following equation:

$$ARD = \frac{100}{N} \sum_i^N \left| \frac{q_{\text{exp}} - q_{\text{fit}}}{q_{\text{exp}}} \right|,$$

where N is the total number of experimental data points, and q_{exp} and q_{fit} are the experimental and fitted gas uptake at the same equilibrium pressure, respectively.

Selectivity calculation using the ideal adsorbed solution theory (IAST)

The pure-component adsorption isotherms were first fitted with Toth equation (see above information). The selectivity for a binary mixture was calculated using the following equation:

$$S_{1,2} = \frac{x_1/y_1}{x_2/y_2}$$

where x_i and y_i are the molar fractions of component i ($i = 1, 2$) in the adsorbed phase and bulk phase, respectively.

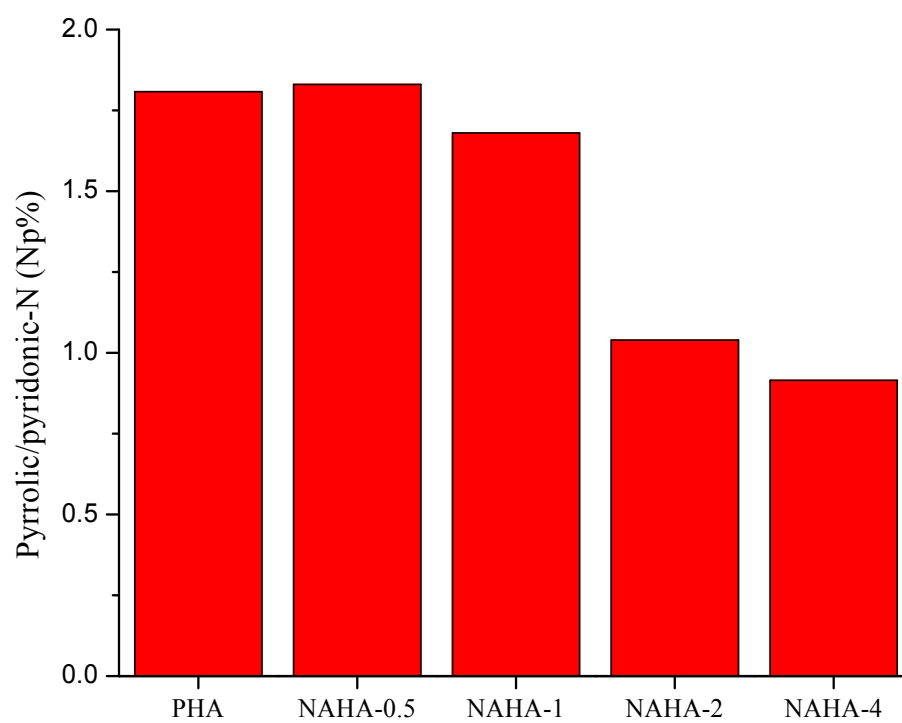


Fig. S1 Pyrrolic/pyridonic-N content by atom, i.e. the percentage of nitrogen atom in the form of pyrrolic/pyridonic-N with respect to all the atoms (C, O, and N) determined by XPS. This value is denoted as Np%.

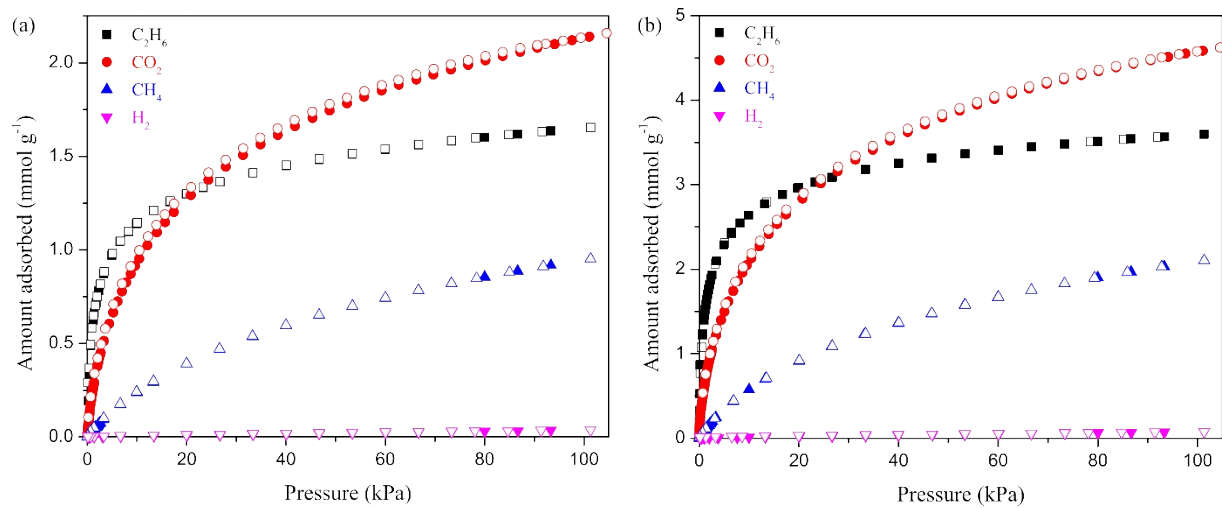


Fig. S2 Representative adsorption and desorption isotherms of CO₂, C₂H₆, CH₄, and H₂ on (a) pyrolyzed carbon (PHA) and (b) activated carbon (NAHA-0.5).

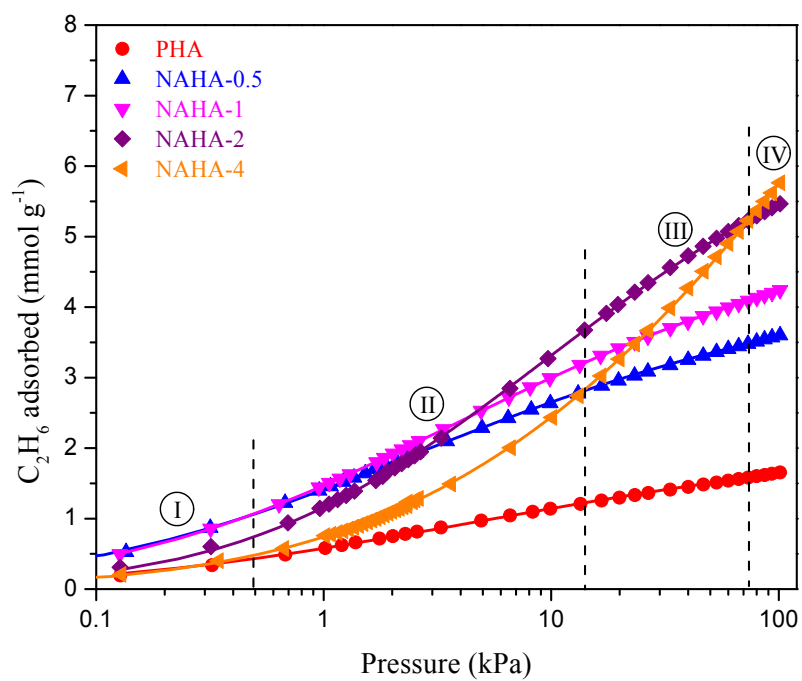


Fig. S3 C_2H_6 adsorption isotherms of the investigated carbons at 273 K. The lines represent Toth isotherm fitting.

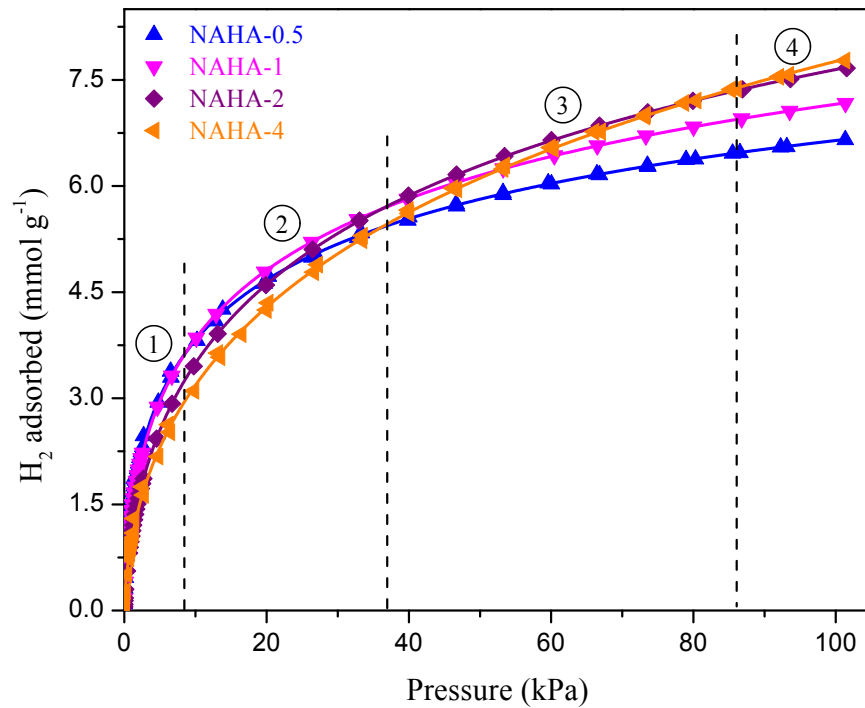


Fig. S4 H₂ adsorption isotherms of the investigated carbons at 87 K. The lines represent Toth isotherm fitting.

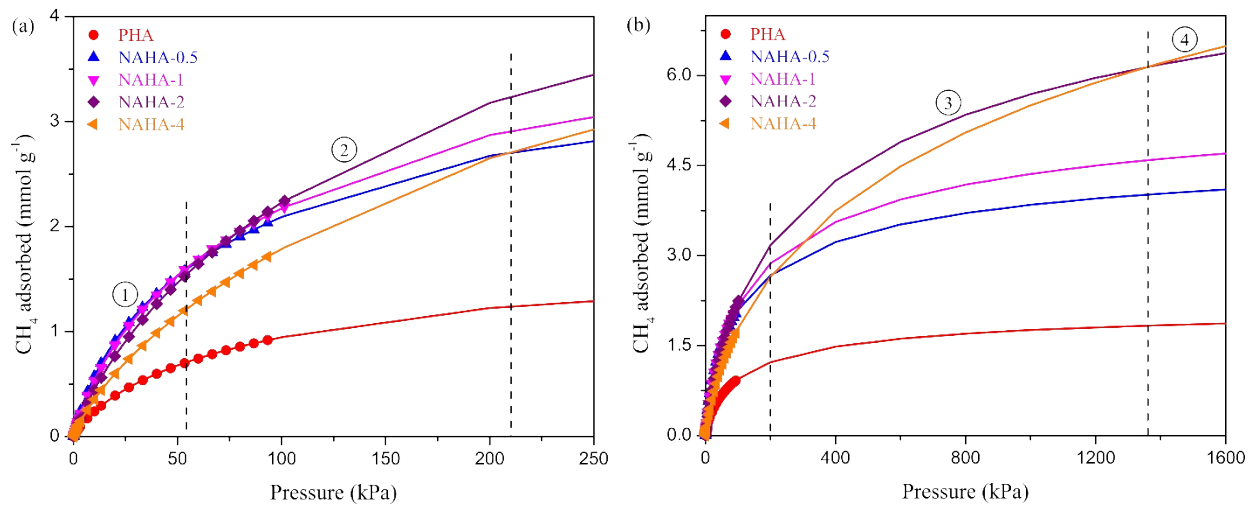


Fig. S5 CH₄ adsorption isotherms of the investigated carbons at 273 K. The lines represent Toth isotherm fitting.

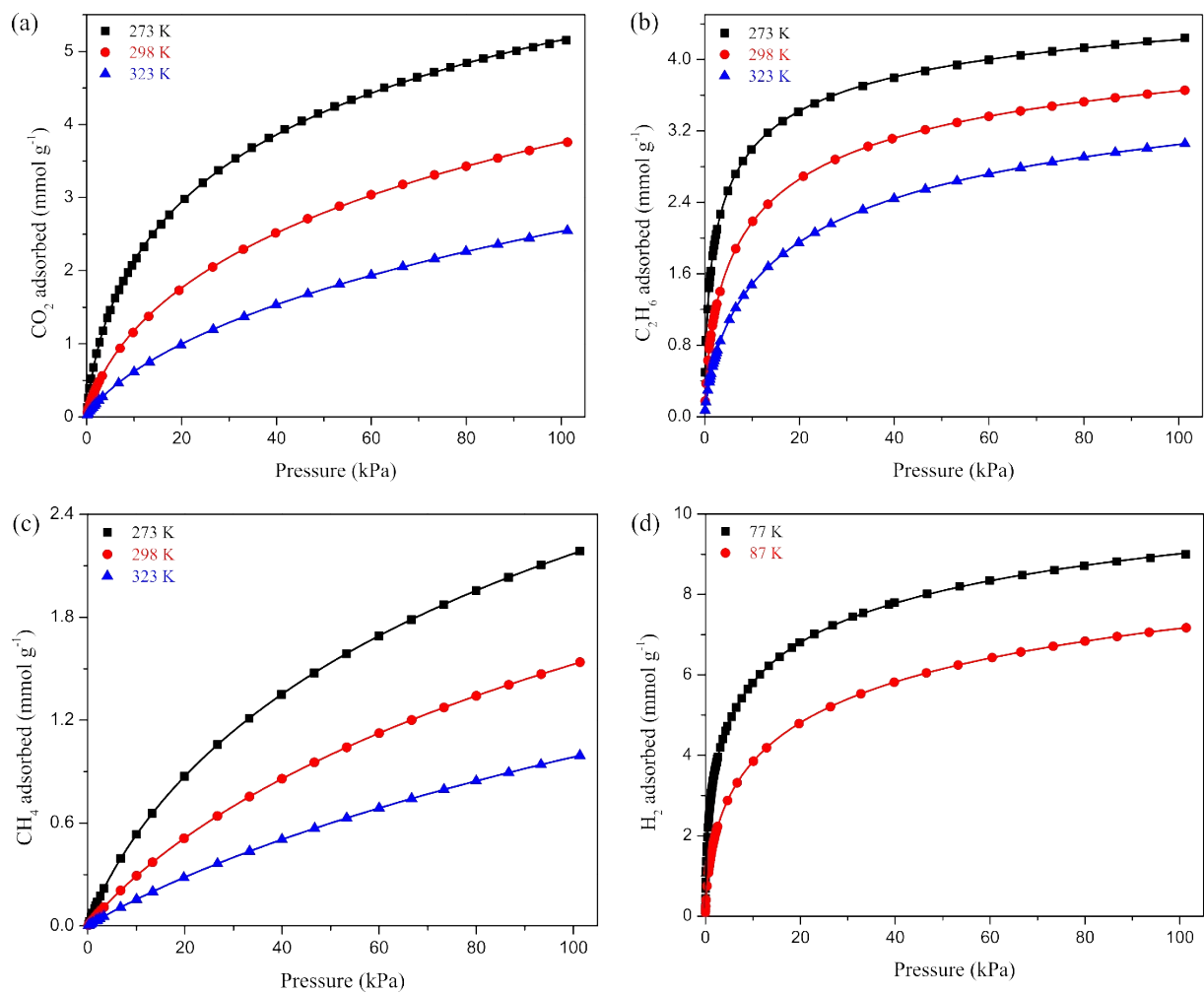


Fig. S6 CO₂ (a), C₂H₆ (b), and CH₄ (c) isotherms of NAHA-1 at 273, 298, and 323 K. H₂ (d) isotherms of NAHA-1 at 77 and 87 K. The lines represent Toth isotherm fitting.

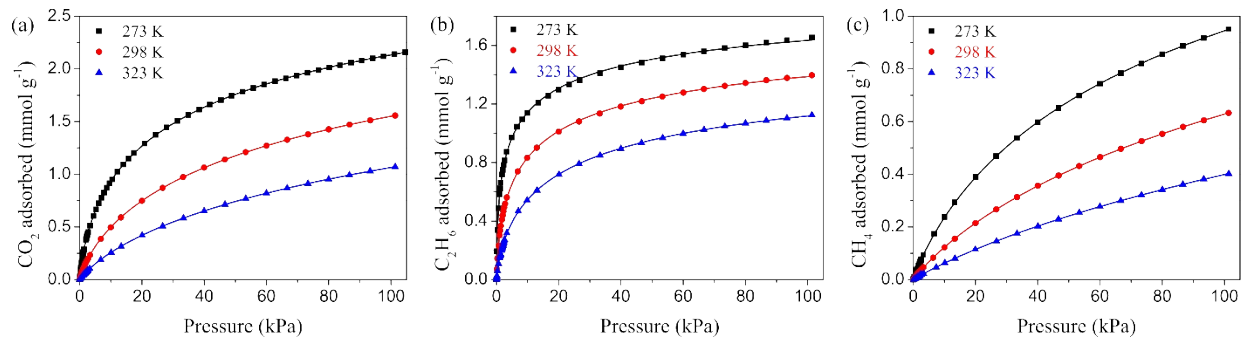


Fig. S7 CO₂ (a), C₂H₆ (b), and CH₄ (c) isotherms of PHA at 273, 298, and 323 K. The lines represent Toth isotherm fitting.

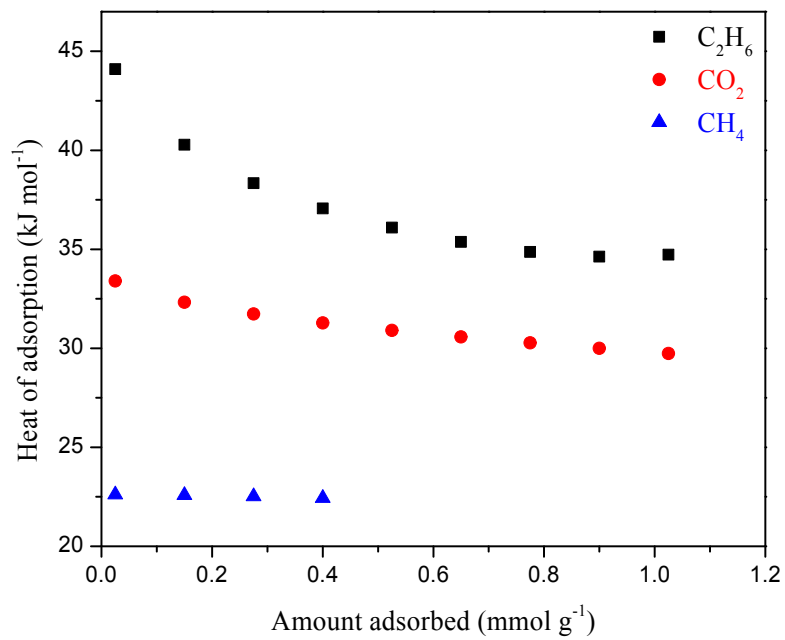


Fig. S8 Isosteric heat of adsorption for PHA at different gas loadings.

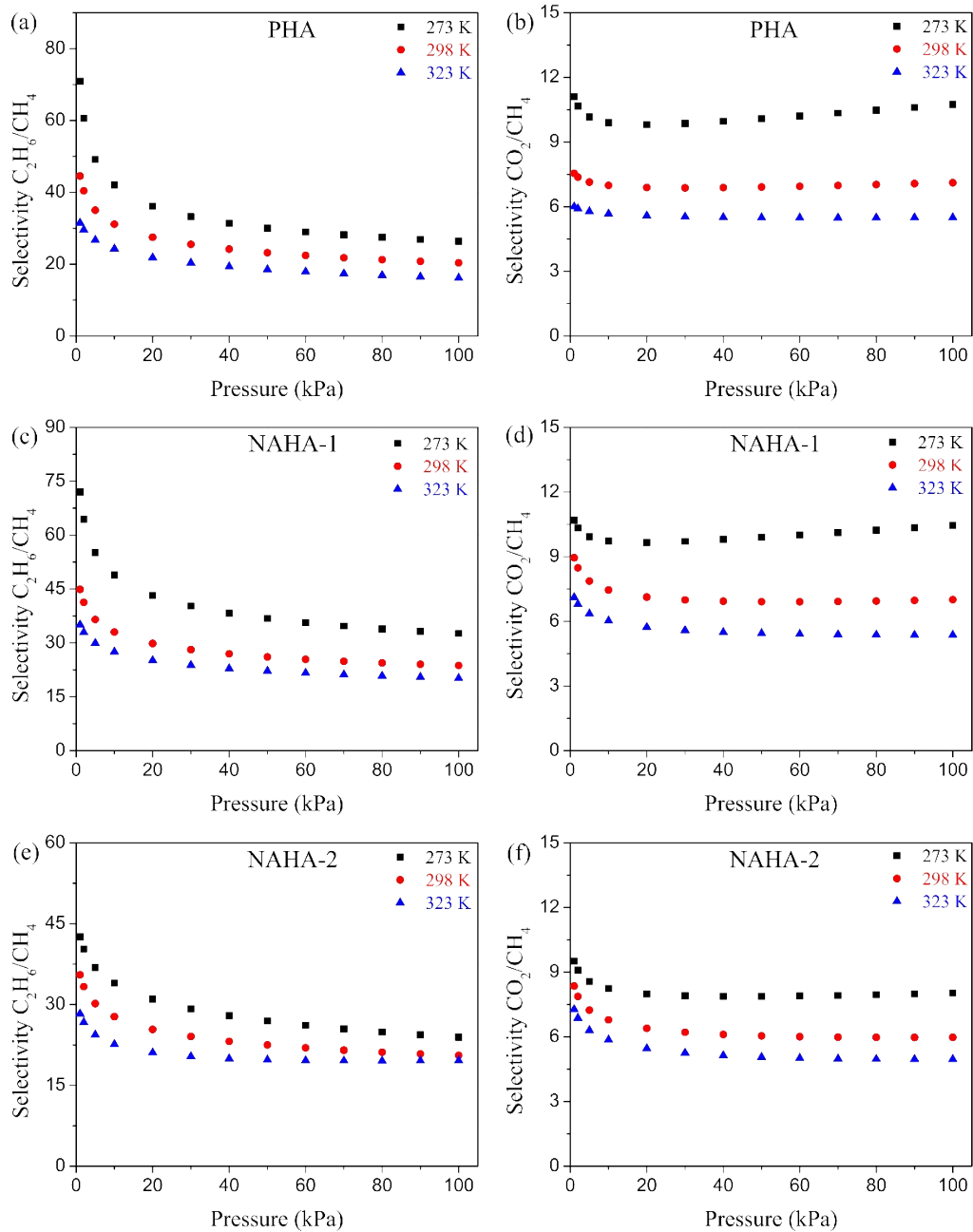


Fig. S9 IAST predicted selectivities of C_2H_6 over CH_4 (a,c,e) and CO_2 over CH_4 (b,d,f) for equimolar binary mixtures at 273, 298, and 323 K in PHA (a,b), NAHA-1 (c,d), and NAHA-2 (e,f).

Table S1 Comparison of CO₂ uptakes of various carbons at 100 kPa

Sample	CO ₂ uptake (mmol g ⁻¹)		Reference
	273 K	298 K	
NAHA-2	6.0	4.0	This study
commercial activated carbon (e.g. BPL, Maxsorb, Norit R1 Extra)	< 5	< 2.5	(1)
RFL-500	–	3.1	(2)
CEM750	6.9	4.4	(3)
CN500	4.4	3.1	(4)
AS-2-700	6.6	4.3	(5)
CP-2-600	6.2	3.9	(6)
SK-0.5-700	–	4.2	(7)
C _{RHC111-DES} after thermally treated at 800 C	–	3.1	(8)
VR-5-M	8.6	4.2	(9)
CS*-P-A	8.9	4.6 (296 K)	(10)
micro-TiC chlorinated at 700 C and then annealed in H ₂ at 600 C	7.1	4.1	(11)
ACM-5	11.5	5.1	(12)
HCM-ZC-1	5.4	3.8	(13)
HCM-DAH-1-900-1	4.8	3.2	(14)
CPC-550	8.3	5.8	(15)
SC800	–	3.4	(16)
AC-2-635	5.9	3.9	(17)
NC800	5.7	3.8	(18)
Bamboo-3-873	7.0	4.5	(19)
HPC74-1000	–	3.4 (300 K)	(20)
NC900	5.1	3.9	(21)
AG-2-700	7.4	4.5	(22)
PCN-71	4.5	2.9	(23)
EBI-B	4.1	2.7	(24)
activated carbon monoliths	–	< 3	(25)
K4-700	–	3.5	(26)
CSA-800	6.6	3.2	(27)
N-HCSs	–	2.7	(28)
KNC-A-HCl	6.0	4.0	(29)

Table S2 Comparison of C₂H₆ uptakes of various sorbents at 100 kPa

Sample	C ₂ H ₆ uptake (mmol g ⁻¹)		Reference	
	273 K	298 K		
Carbons	NAHA-2	5.5	4.6	This study (30)
	activated carbon	–	3.75 (293 K)	
	BPL	–	2.8 (301 K)	(31)
	BPL	4.7	3.6	(32)
	activated carbon	–	3.5	(33)
	kureha activated carbon	5.5	4.3	(34)
	date-pit activated carbon	–	2.6 (303 K)	(35)
	zeolite-templated carbon	4	–	(36)
	zeolite-templated carbon	10	6.5	(37)
	MSC-30 (Maxsorb)	10	6.5	(37)
	AC-40	–	2.2 (293 K)	(38)
	CMK-3	–	3.7	(39)
	Nuxit-AL	–	3.3 (293 K)	(40)
	coconut activated carbon	–	4.5	(41)
	Norit-activated carbon	–	3.3 (303 K)	(42)
	Ajax-activated carbon	4.9 (283 K)	4 (303 K)	(42)
Other adsorbents (MOFs, Polymeric Organic Frameworks, zeolites, ordered mesoporous silica, and clays)	UTSA-33a	3.5	2.7 (296 K)	(43)
	ZJU-60a	7.8	5.9 (296 K)	(44)
	Mg-MOF-74	7.8	–	(45)
	ZIF-7	–	1.9	(46)
	NOTT-300	–	0.9 (293 K)	(47)
	FJI-C1	5.5	3.9	(48)
	Fe ₂ (dobdc)	–	0.77 (318 K)	(49)
	La(BTB)H ₂ O	4.6	–	(50)
	mesoPOF-1	2.5	–	(51)
	PAF-40-Mn	2.8	2	(52)
	silicalite	2.2 (277 K)	–	(53)
	ETS-10	–	1.5 (300 K)	(54)
	zeolite 13X	–	3.4 (305 K)	(55)
	MCM-41	1.5	–	(56)
	SBA-15	–	0.6 (303K)	(57)
	clays	–	< 0.8	(58)

Table S3 Fitting parameters of Toth model for the pure-component isotherms on the as-prepared carbons

Sample	Gas	Temp. (K)	q_m	b	t	Adjusted R^2	ARD, %
NAHA-0.5	C ₂ H ₆	273	4.427	3.692	0.4057	0.99987	1.55
	CO ₂	273	9.875	0.1898	0.3750	0.99982	4.75
	CH ₄	273	5.153	0.0201	0.5694	1	1.81
	H ₂	273	62.51	2.65E-05	0.2532	0.99913	7.38
	H ₂	87	11.75	0.9989	0.3371	0.99977	1.99
NAHA-1	C ₂ H ₆	273	5.386	2.2836	0.4135	0.99998	0.19
	C ₂ H ₆	298	5.078	0.4837	0.4635	0.99998	0.59
	C ₂ H ₆	323	4.829	0.1632	0.4913	1	0.35
	CO ₂	273	11.19	0.1020	0.4161	0.99991	1.64
	CO ₂	298	14.17	0.03127	0.3772	0.99994	2.85
	CO ₂	323	16.84	0.00932	0.3733	0.99995	3.82
	CH ₄	273	6.130	0.01404	0.5780	1	0.96
	CH ₄	298	5.281	0.00707	0.6549	1	0.96
	CH ₄	323	5.051	0.00354	0.6756	1	1.33
	H ₂	273	1.408	5.21E-04	0.8330	0.99994	6.24
	H ₂	87	13.85	0.6292	0.3362	0.99998	2.20
H ₂	77	15.20	4.509	0.2938	0.99997	0.41	
NAHA-2	C ₂ H ₆	273	7.329	0.4591	0.4892	0.9999	1.03
	C ₂ H ₆	298	7.618	0.1628	0.4706	0.99997	0.52
	C ₂ H ₆	323	7.470	0.05654	0.4941	1	0.28
	CO ₂	273	25.80	0.03169	0.3497	0.99994	1.49
	CO ₂	298	38.88	0.00813	0.3188	0.99998	2.55
	CO ₂	323	49.58	0.00236	0.3187	0.99998	2.79
	CH ₄	273	10.02	0.00642	0.5461	1	1.47
	CH ₄	298	7.610	0.00356	0.6580	1	1.54
	CH ₄	323	3.870	0.00319	0.9412	0.99998	4.28
	H ₂	273	2.111	4.22E-04	0.6958	0.99989	9.92
	H ₂	87	19.04	0.2422	0.3292	0.99998	4.33
H ₂	77	20.93	1.672	0.2818	0.99988	3.31	
NAHA-4	C ₂ H ₆	273	23.11	0.2376	0.2610	0.99996	0.96
	CO ₂	273	4109	0.01571	0.1005	0.99985	1.98
	CH ₄	273	17.30	0.00352	0.4091	0.99997	8.22
	H ₂	273	132.2	2.47E-05	0.2128	0.99934	22.78
	H ₂	87	44.52	0.2117	0.2302	0.99999	1.81
PHA	C ₂ H ₆	273	2.239	3.689	0.3594	0.99946	1.17
	C ₂ H ₆	298	1.971	0.5833	0.4401	0.99987	1.16
	C ₂ H ₆	323	1.759	0.1638	0.4945	0.99995	8.48
	CO ₂	273	4.090	0.1216	0.4410	0.99999	1.84
	CO ₂	298	4.061	0.03372	0.4667	0.99999	1.86
	CO ₂	323	3.928	0.01188	0.4985	1	3.92
	CH ₄	273	2.246	0.0159	0.6415	0.99998	5.94
	CH ₄	298	2.292	0.00711	0.6220	0.99999	2.40
	CH ₄	323	2.431	0.00303	0.6306	0.99994	4.37
	H ₂	273	0.6428	6.55E-04	0.8238	0.99979	23.97

Table S4 Comparison of C₂H₆/CH₄, CO₂/CH₄, CO₂/H₂ separation performance (uptake capacity and selectivity) of various carbons for corresponding equimolar binary mixtures between 0–100 kPa or under similar conditions^a

Sample	C ₂ H ₆ uptake ^b	CO ₂ uptake ^b	C ₂ H ₆ /CH ₄ selectivity	CO ₂ /CH ₄ selectivity	CO ₂ /H ₂ selectivity	Ref.
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	273 K	298 K	273 K	298 K	273 K	298 K	273 K	298 K	273 K	298 K	
NAHA-1	4.2	3.7	5.2	3.8	33–72	24–45	9.7–10.7	6.9–9.0	2.0×10 ⁴		This study
NAHA-2	5.5	4.6	6.0	4.0	24–43	21–36	7.9–9.5	6.0–8.4	3.5×10 ³		This study
SC700P				3.0				4.3–7			(16)
PAF-1-450 ^c			4.5				8.5		400		(59)
C125-220 ^d				2.1				14.8			(60)
Zeolite templated carbon				< 2.5				< 2.7		17–18	(61)
AC35				< 2.5				2.4			(61)
BG-ENO				< 2.5				3.4			(61)
activated carbon ^e										< 90	(62)
BPL ^f		2.8				17					(31)
N-doped carbon			1.4				8–13				(63)
ACB-5				2.2				< 2			(64)
A35/4 ^g				2.2				3.5			(65)
CMK-3		3.7		2.3		12–16		< 2.1			(39)
JX101 ^h				1.5						< 100	(66)
Norit				2.0				2			(67)
Maxorb				2.2				2			(67)
N-doped carbon			5.1				11				(21)
activated carbon ⁱ		3.8				<i>11</i>					(30)
BPL ^j				< 2				2.5		91	(68)
BPL				1.0				4.5			(69)
N-Doped Carbon			8.3	5.8			<i>13</i>	<i>12</i>			(15)
FCDTPA-K-500			4.4				<i>8</i>				(70)
Norit R1 Extra, Maxsorb			< 5	< 2.5			< 3.2	< 2.2			(1)

^a A cell is left blank if the data is not available for that cell, selectivity values in italics are Henry's law selectivities. ^b Gas uptake at 100 kPa in mmol g⁻¹. ^c At a CO₂:CH₄ ratio of 15:85, CO₂:H₂ ratio of 20:80. ^d At 120 kPa, a CO₂:CH₄ ratio of 30:70 ^e At a CO₂:H₂ ratio of 1:8, pressure of 1.11 MPa. ^f At 301 K. ^g At 293 K. ^h At 313 K, a CO₂:H₂ ratio of 20:80. ⁱ At 293 K. ^j At 303 K.

Table S5 Comparison of C₂H₆/CH₄, CO₂/CH₄, CO₂/H₂ separation performance (uptake capacity and selectivity) of the carbons prepared in this study with those of various adsorbents (carbons are not included here) for corresponding equimolar binary mixtures between 0–100 kPa or under similar conditions^a

Sample	C ₂ H ₆ uptake ^b		CO ₂ uptake ^b		C ₂ H ₆ /CH ₄ selectivity		CO ₂ /CH ₄ selectivity		CO ₂ /H ₂ selectivity		Ref.
	273 K	298 K	273 K	298 K	273 K	298 K	273 K	298 K	273 K	298 K	
NAHA-1	4.2	3.7	5.2	3.8	33–72	24–45	9.7–10.7	6.9–9.0	2.0×10 ⁴		This study
NAHA-2	5.5	4.6	6.0	4.0	24–43	21–36	7.9–9.5	6.0–8.4	3.5×10 ³		This study
bio-MOF-11 ^c				4.1						< 300	(71)
SUMOF-4 ^d				3.2						< 180	(72)
Zn ₅ (BTA) ₆ (TDA) ₂ ^e				2				10			(73)
UTSA-25a ^e				3.2				8			(73)
Cu(BDC-OH) ^e				1.9				6.5			(73)
UTSA-33a ^e				2.5				6.5			(73)
UTSA-34b ^e				2.6				4.5			(73)
Yb(BPT) ^e				0.7				3			(73)
UTSA-33a ^e		2.7				16–20					(43)
UTSA-34b ^e		4.4				17–18					(74)
UTSA-34a ^e		2.8				19–25					(74)
IIFP-5			< 2				7.5				(75)
NOTT-300 ^f		0.9				5–6					(47)
MCOF-1		2				50–88					(76)
MOF	4.6		2.3		12–22		4.7–8				(50)
FJI-C1		3.9				13–24					(48)
FIR-7a-ht		4				14–15					(77)
FIR-51	5.4	4.7			14–19	10–14.5					(78)
Cu-TDPAT		6.7				15–46					(79)
2a	5.2				18–20						(80)
Mg ₂ (dobdc) ^g				8						< 900	(66)
Zeolite 13X ^g				4.3						< 400	(66)
Na-ETS-10 ^h		1.4				46–52					(81)
MCM-41		0.5		0.8		5–5.7		5.8–6.8			(82)
MCM-41				0.7						< 35	(83)
SBA-15				0.5				4.9–5.5			(39)
mesoPOF-2	1.6		1.7		25–40		10–15				(51)
ZnP-CTF-500		4				21–40					(84)
PAF-40-Mn		2				30–35					(52)
CoMo ₃ S ₁₃ aerogel			0.9						85–120		(85)
Ge-rich chalcogenide			< 1						< 90		(86)
PCH		0.4		0.7		4.5–5	5.8–7				(82)
Zr _w		0.3		0.4		18–25		14–35			(87)
MOF-177				1.6				4.4			(88)
Compound 1A			1.7						266		(89)
UTSA-36 a	2.8	2.1			24.7	16.6					(90)
CG-9			8.3				7.3				(91)
ZIF-100				1				5.9			(92)
ZIF-78				2.7				10.5			(69)
NOTT-202a			2.3				2.9		10 ⁵		(93)
ZJU-30	2.8	2.1			29.8	19.5					(94)
ZJU-61	6	4.7			12.3	11					(95)

^a A cell is left blank if the data is not available for that cell, selectivity values in italics are Henry's law selectivities. ^b Gas uptake at 100 kPa in mmol g⁻¹. ^c At a CO₂:H₂ ratio of 10:90. ^d At a CO₂:H₂ ratio of 15:85. ^e At 296 K. ^f At 293 K. ^g At 313 K, CO₂:H₂ ratio of 80:20. ^h At a C₂H₆:CH₄ ratio of 95:5.

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