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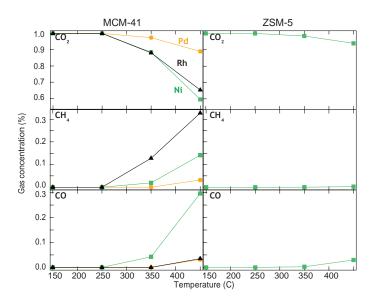
## Supplementary Information for Article: Catalytic hydrogenation of CO<sub>2</sub> to methane over supported Pd, Rh and Ni catalysts

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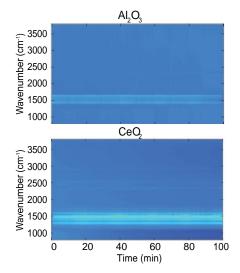


**Fig. S1** Steady-state outlet concentration of CO<sub>2</sub> (top), CH<sub>4</sub> (middle) and CO (bottom) as a function of temperature during the reaction between 1 % CO<sub>2</sub> and 5 % H<sub>2</sub> in Ar gas with a total flow rate of 2000 ml/min at atmospheric pressure over the Pd (orange), Ni (green) and Rh (black) catalysts supported on MCM-41 (left panel) and over the Ni/ZSM-5 (right panel) catalyst.

Figure S1 shows the catalytic performance of the metal-promoted MCM-41 and ZSM-5 catalysts for CO<sub>2</sub> hydrogenation. The inlet gas concentrations to the flow reactor are 1% CO<sub>2</sub> and 5% H<sub>2</sub> in Ar and each marker in the figure represents the calculated average value over a 10 min period. The main reaction products formed during CO<sub>2</sub> hydrogenation are CH<sub>4</sub>, CO and H<sub>2</sub>O. No hy-

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**Fig. S2** Transient hydrogenation of 0.2% CO<sub>2</sub> over Al<sub>2</sub>O<sub>3</sub> (upp) and CeO<sub>2</sub> (bottom) during periodic variation of the feed gas composition between 0.8% H<sub>2</sub>+0.2% CO<sub>2</sub> and 0.2% CO<sub>2</sub> at 350 °C for 10 min. The panels show the color coded intensities (blue corresponds to low intensity, red to high intensity) of the IR bands in the region 790-3800 cm<sup>-1</sup> versus time.

drocarbon compounds except methane are observed.

Figure S2 shows the DRIFTS results for the hydrogen pulse experiments under a continuous flow of CO<sub>2</sub> for alumina and ceria at 350  $^\circ$  C.