

## Supporting Information

# A multicomponent assembly approach for the design of deep desulfurization heterogeneous catalysts

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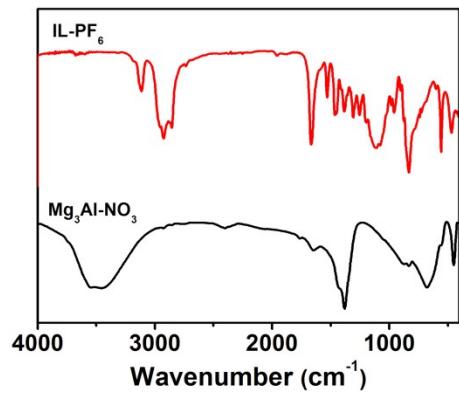
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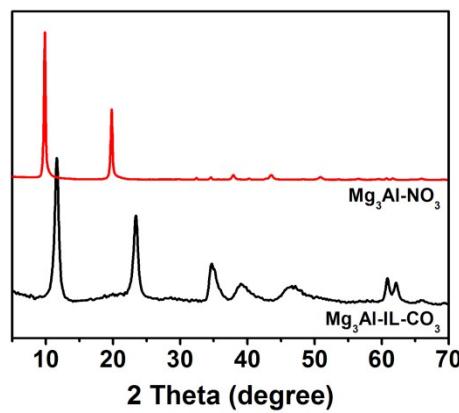
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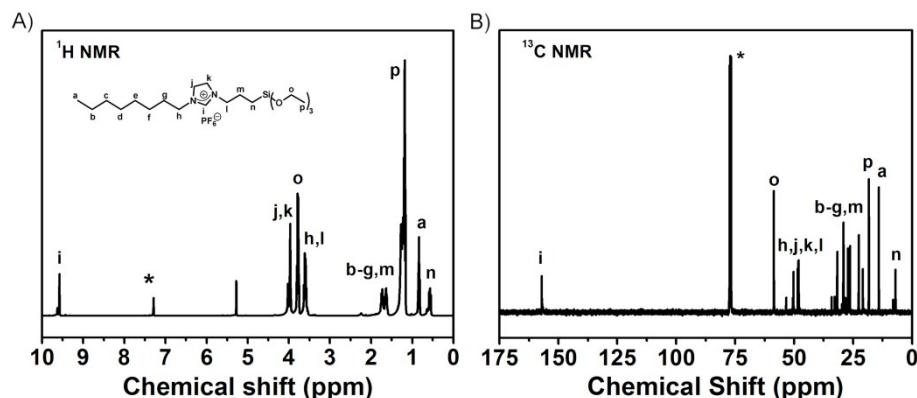
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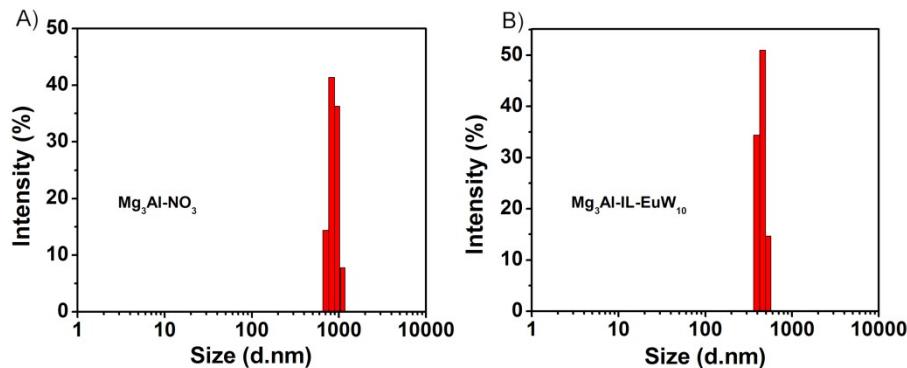
**Fig. S1.** FT-IR spectra of Mg<sub>3</sub>Al-NO<sub>3</sub> and IL-PF<sub>6</sub>.



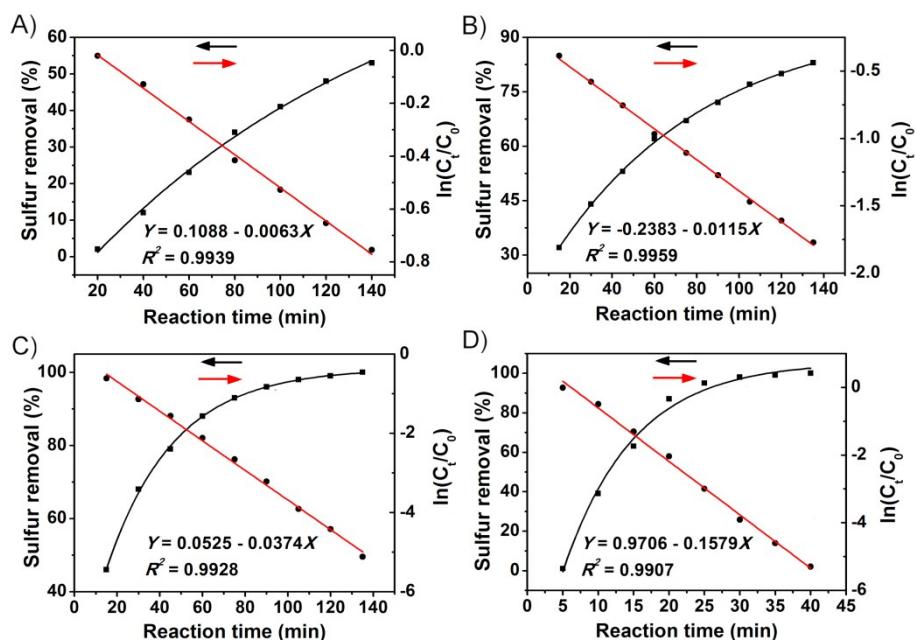
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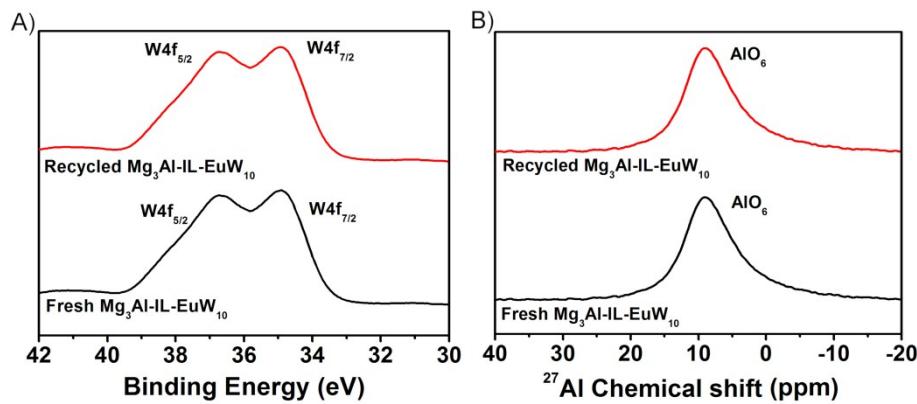
**Fig. S3.** A) The <sup>1</sup>H NMR and B) <sup>13</sup>C NMR (CDCl<sub>3</sub>) spectra of IL-PF<sub>6</sub>.



**Fig. S4.** Particle size distributions of A)  $\text{Mg}_3\text{Al}-\text{NO}_3$  and B)  $\text{Mg}_3\text{Al-IL-EuW}_{10}$ .



**Fig. S5.** Sulfur removal of DBT;  $\ln(C_t/C_0)$  as a function of reaction time at A) 30, B) 40, C) 50 and D) 60 °C, respectively. Reaction conditions:  $\text{H}_2\text{O}_2/\text{DBT/EuW}_{10} = 40:8:1$ , ( $\text{H}_2\text{O}_2 = 0.08 \text{ mL}$ , model oil = 5 mL, S = 1000 ppm).



**Fig. S6.** The XPS and B) <sup>27</sup>Al CP/MAS NMR spectra of recycled and fresh Mg<sub>3</sub>Al-IL-EuW<sub>10</sub>.

**Table S1.** Comparison of physicochemical properties of Mg<sub>3</sub>Al-EuW<sub>10</sub> and Mg<sub>3</sub>Al-IL-EuW<sub>10</sub>.

| Entry | Catalyst                                | Surface area/m <sup>2</sup> g <sup>-1</sup> | Pore volume/cm <sup>3</sup> g <sup>-1</sup> | Pore size/nm |
|-------|-----------------------------------------|---------------------------------------------|---------------------------------------------|--------------|
| 1     | Mg <sub>3</sub> Al-EuW <sub>10</sub>    | 33.61                                       | 0.31                                        | 4.20         |
| 2     | Mg <sub>3</sub> Al-IL-EuW <sub>10</sub> | 41.82                                       | 0.58                                        | 5.78         |