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Supporting Information







Figure S2 (a) Nitrogen adsorption-desorption isotherm and (b) the corresponding pore size



distribution of the Cu-BTC; (c) Nitrogen adsorption-desorption isotherm and (d) the corresponding pore size distribution of the [Cu-BTC][HPM].

Figure S3 The characterization of the reaction products. (a) The general GC-MS image of the reaction products. The MS of (b) EMF and (d) EL.



Figure S4 MS of the main by-product DEEF.



Figure S5 Catalyst recycling (Reaction conditions: 120 °C for 12 h).



Figure S6 The XRD patterns of the catalyst before the reaction (a) and after the reaction with the reaction temperature of 140 °C (b), the peaks in red pane correspond to the characteristicpeak of Cu.

Elements	[Cu-BTC][HPM]	[Cu-BTC][HPM]		
(ug/ml)	before the reaction	after the reaction		
Cu	23.4	24.1		

Мо	13.5	12.9

 Table S1 The ICP results of [Cu-BTC][HPM] before and after the reaction.

Entry	Catalyst	Reaction condition	con.(%)	EMF yield(%)
1[30]	NH4-S5.5	140°C/5h	69	21
2[33]	cellulose sulfuric acid	120°C/10h	100	67
3[34]	Ag1H2PW	120°C/6h	93	87
4[35]	20 wt.% MCM-41-HPW	100°C/12h	56.5	49
5[36]	Fe3O4@SiO2-HPW	120°C/10h	89.5	77
6[37]	MCM-41-H4SiW12O40	90°C/2h	92	77
7[38]	Fe3O4@SiO2–SH–Im–HSO4	120°C/12h	89	82.7
8[39]	K-10 clay-Al	100°C/8h	78	73
9[40]	20 wt.% K-10 clay-HPW	100°C/6h	60	54
10[in this work]	[Cu-BTC][HPM]	100°C/12h	100	44
11[in this work]	[Cu-BTC][HPM]	120°C/12h	100	55

Table S2 The comparison of the catalytic performance of the present work with reported literatures.