## **Supplementary Information**

## Multi-functional polydopamine coating: simultaneous enhancement of interfacial adhesion and CO<sub>2</sub> separation performance of mixed

## matrix membranes

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Fig.S1 Experimental apparatus for gas sorption

The gas sorption isotherms of the prepared membranes were investigated using the barometric pressure decay method with a dual-volume, comprised of a sample container and a reference volume where the chambers were connected in series. The volumes of both chambers were carefully calibrated before the measurements. The device was placed in a temperature-controlled water bath to minimize the effect of environmental temperature on the gas sorption behavior. In this study, the temperature was maintained at 25 °C. The membranes were introduced into the sample chamber and degassed for more than 3 h to remove all adsorbed species. Feed gas was firstly charged into the reference chamber and then the pressure decay was immediately initiated after opening the valve between the sample and reference chamber. The gas sorption reached equilibrium once no further pressure decay was observed. The

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concentration of gas adsorbed in prepared membranes was evaluated by using the equation of state and the Soave-Redlich-Kwong (SRK) equation of state.<sup>1</sup> In this work, the sorption test  $CO_2$  saturated with water vapor or not was conducted to investigate the difference of  $CO_2$  sorption under at humidified and dry states. But for  $N_2$ , under humid conditions, both water and nitrogen are present in the system. Because the  $N_2$  sorption was quite low, the pressure drop upon  $N_2$  sorption would also be very small. Therefore, the relative pressure fluctuation caused by water evaporation and condensation cannot be neglected; accordingly, we cannot accurately measure the amount of  $N_2$  sorbed under humid conditions. Hence, the  $N_2$  sorption tests were carried out under dry conditions.

[1] S. Kanehashi and K. Nagai, J. Membr. Sci., 2005, 253, 117-138.



Fig.S2 Experimental apparatus for gas permeability



Fig.S3 Photographs of dispersion stability of ZIF-8 (white) and PDA@ZIF-8 (black) versus time



Fig. S4 Nitrogen sorption isotherms of ZIF-8 (b) and PDA@ZIF-8 (a) at 77K. Red and black data

correspond to the adsorption and desorption branches, respectively.

Sample		BET Surface Area			Langmuir Surface		t-Plot micropore	
		$(m^2/g)$			Area (m <sup>2</sup> /g)		volume (cm <sup>3</sup> /g)	
PDA@ZIF-8	1139			1465		0.51		
ZIF-8		1360			1785		0.60	
(a-1)	С	(a-2)		N	(a-3)	0	(a-4)	Zn
20 um		20 um			20 um		20 um	
(b-1)	C	(b-2)		Ν	(b-3)	0	(b-4)	Zn
20 um		20 um			20 um		20 um	na Maga na dua anti.

Table S1 BET and micropore volume of ZIF-8 and PDA@ZIF-8

Fig. S5 EDAX maps of Peabx/ZIF-8-15 (a) and Peabx/PDA@ZIF-8-15 (b).



Fig. S6 Sorption isotherms of  $N_2$  on pure Pebax control and MMMs at 25  $^\circ\text{C}$ 

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