

Electronic Supplementary Information

Two-Dimensional Metal-Organic Frameworks for Selective Separation of CO₂/CH₄ and CO₂/N₂

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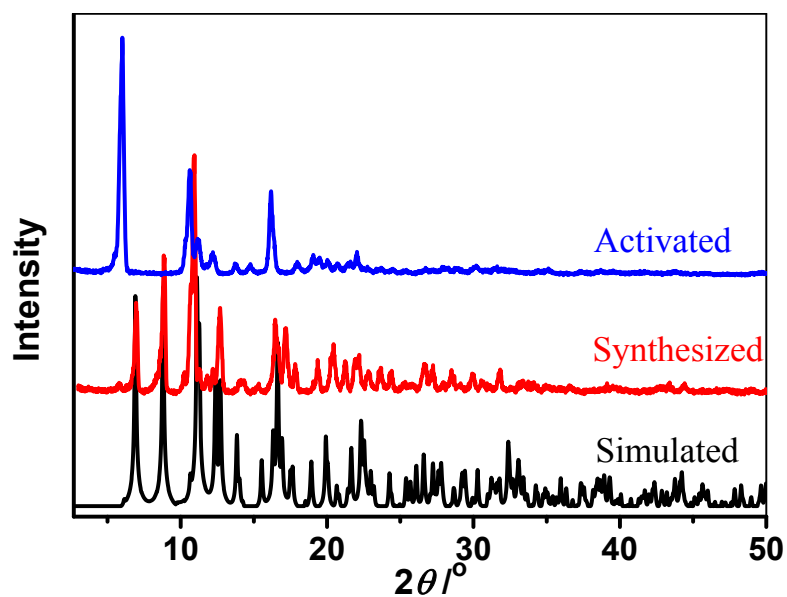


Figure S1. Powder X-ray diffraction patterns of **1** (red) and activated **1a** (blue), in comparison with a simulated powder pattern based on the reported $[\text{Zn}_2(\text{TMTA})(\text{H}_2\text{O})_2]\cdot\text{NO}_3\cdot 6\text{H}_2\text{O}\cdot\text{DEF}$ structure (black line).

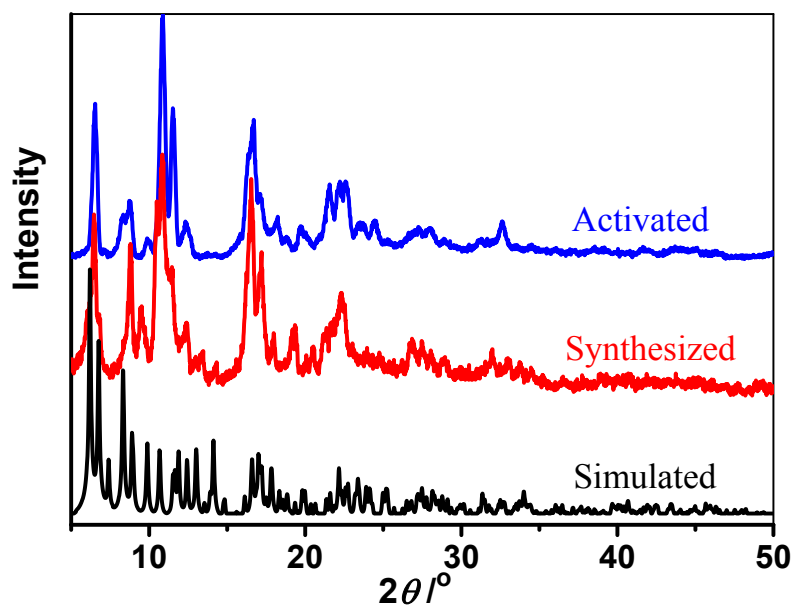


Figure S2. Powder X-ray diffraction patterns of **2** (red) and activated **2a** (blue), in comparison with a simulated powder pattern based on the single-crystal $[\text{Zn}_3(\text{TETA})_2(\text{DMF})_4]\cdot 3\text{DMF}$ structure (black line).

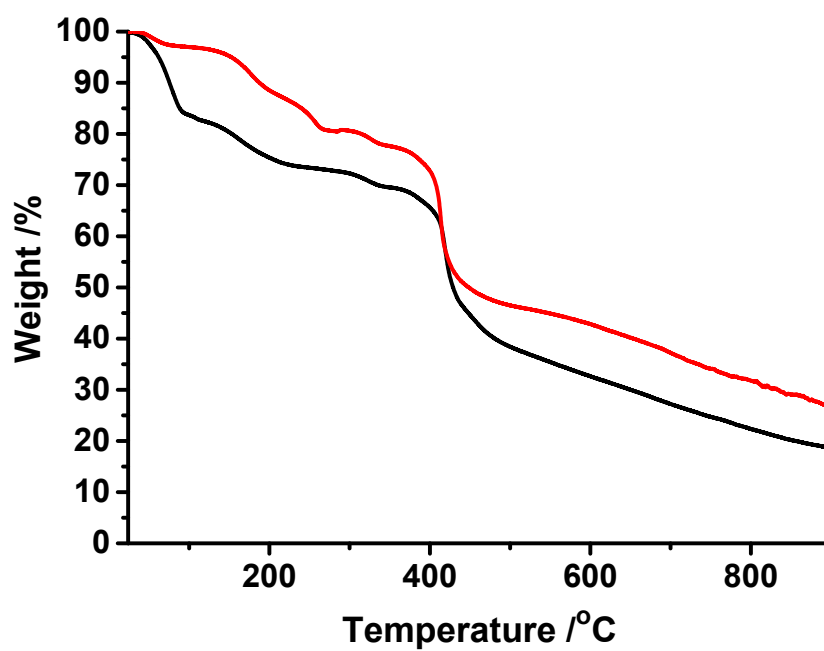


Figure S3. TGA curves of **1** (black) and activated **1a** (red)

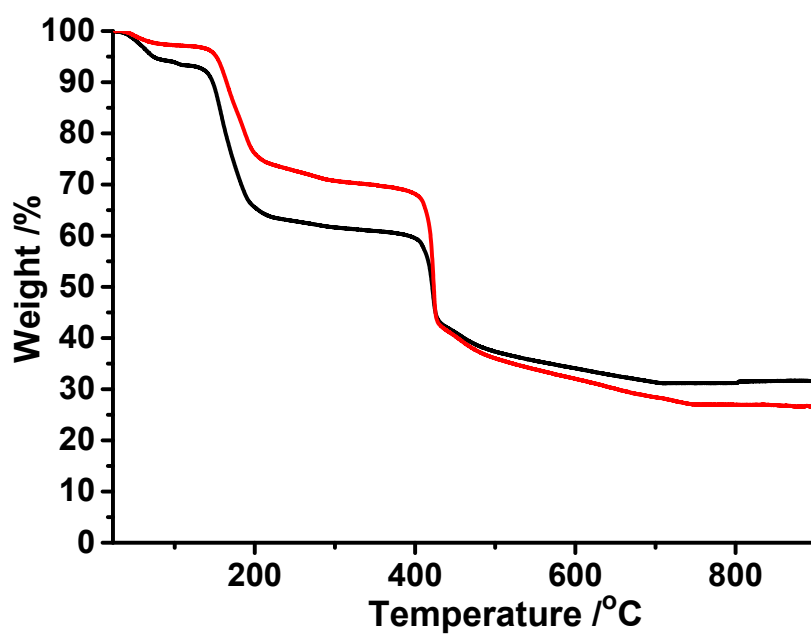


Figure S4. TGA curves of **2** (black) and activated **2a** (red)

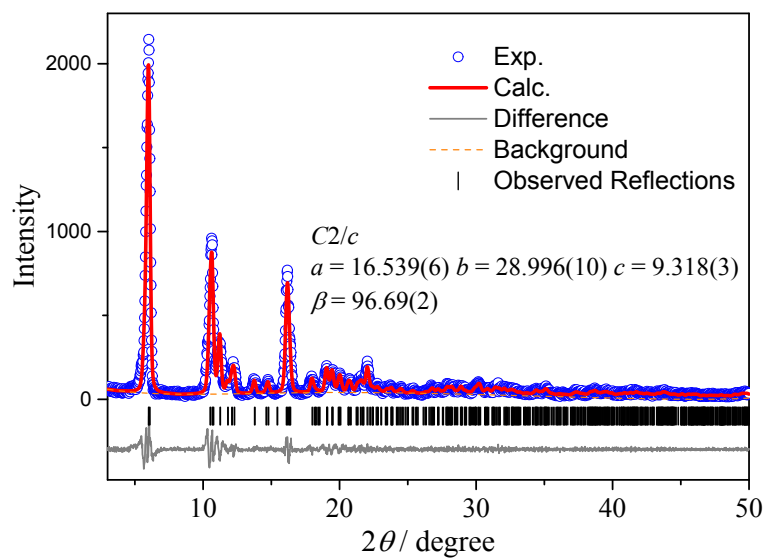


Figure S5. Pawley refinements of the PXRD patterns for **1a** ($R_{wp} = 14.71\%$, $R_p = 10.96\%$).

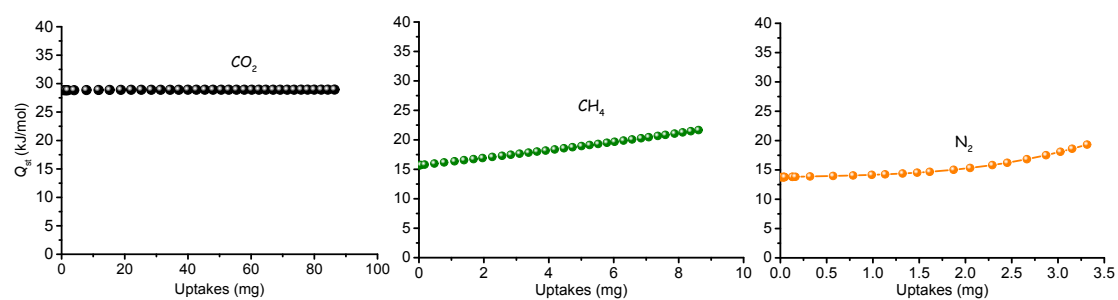


Figure S6. The coverage-dependent adsorption enthalpies of **1a** towards CO_2 , CH_4 , and N_2 .

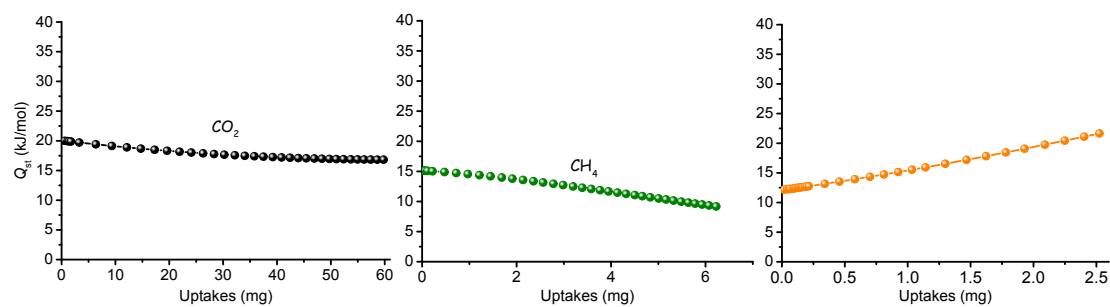


Figure S7. The coverage-dependent adsorption enthalpies of **2a** towards CO_2 , CH_4 , and N_2 .

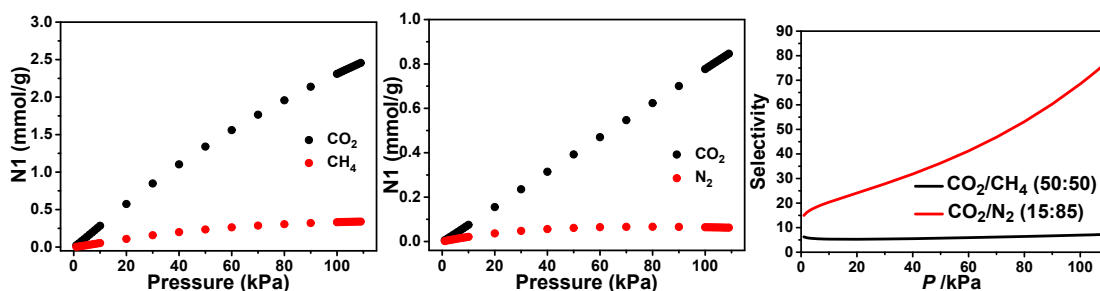


Figure S8. Mixture adsorption isotherms and adsorption selectivity predicted by IAST of **1a** for mixed CO_2/CH_4 ($\text{CO}_2/\text{CH}_4 = 50:50$) and CO_2/N_2 ($\text{CO}_2/\text{N}_2 = 15:85$) at 273 K, respectively.

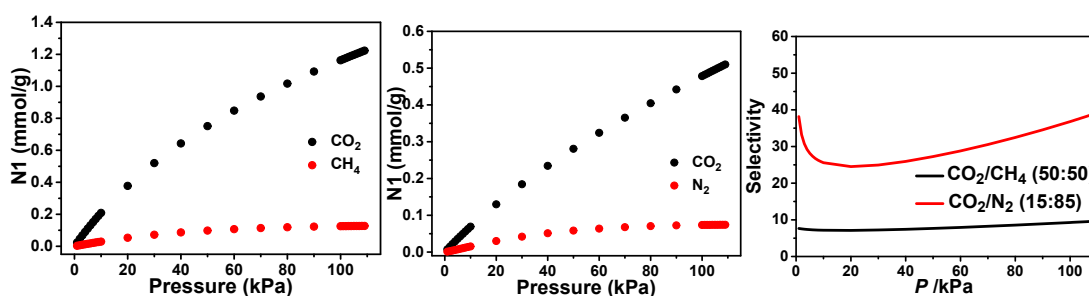


Figure S9. Mixture adsorption isotherms and adsorption selectivity predicted by IAST of **2a** for mixed CO_2/CH_4 ($\text{CO}_2/\text{CH}_4 = 50:50$) and CO_2/N_2 ($\text{CO}_2/\text{N}_2 = 15:85$) at 273 K, respectively.

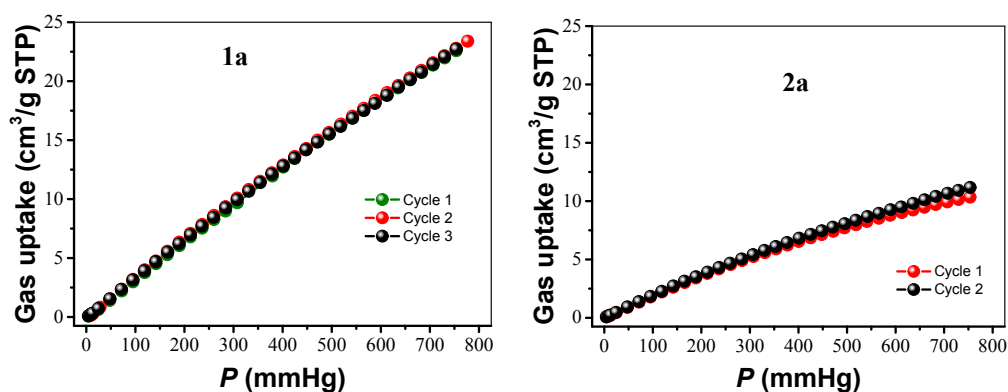


Figure S10. Repeatability of CH_4 adsorption at 273 K for **1a** (black) and **2a** (red).

Table S1. Crystal data and structure refinements of **2**.

Complex	2
Formula.	C ₇₈ H ₈₂ N ₄ O ₁₆ Zn ₃
F.W.	1527.65
Crystal system	Triclinic
Space group	<i>P</i> -1
<i>a</i> / Å	11.4427(17)
<i>b</i> / Å	14.514(2)
<i>c</i> / Å	16.196(3)
α /°	65.694(5)
β /°	69.783(5)
γ /°	73.998(5)
volume/Å ³	2272.2(6)
<i>Z</i>	1
<i>D</i> _{calcd} /g cm ⁻³	1.116
μ / mm ⁻¹	0.842
<i>F</i> 000	796
<i>R</i> ₁ ^{<i>a</i>} <i>I</i> > 2 θ	0.1319
<i>R</i> _{w2} ^{<i>b</i>} <i>I</i> > 2 θ	0.3180
<i>R</i> ₁ ^{<i>a</i>}	0.1720
<i>R</i> _{w2} ^{<i>b</i>}	0.3495

$$^a R_1 = \Sigma |F_o - |F_c|| / \Sigma |F_o|, \quad ^b R_{w2} = [\Sigma w(F_o^2 - F_c^2)^2 / \Sigma w(F_o^2)^2]^{1/2}.$$

Table S2. IAST selectivities of CO₂/CH₄ (CO₂/CH₄ = 50:50) and C₂H₂/N₂ (C₂H₂/N₂ = 15:85).

mixture	Temperature (K)	component proportion	IAST selectivity
1a			
CO ₂ /CH ₄	273	50:50	7.0
CO ₂ /N ₂	273	15:85	69.4
CO ₂ /CH ₄	296	50:50	5.8
CO ₂ /N ₂	296	15:85	39.3
2a			
CO ₂ /CH ₄	273	50:50	9.3
CO ₂ /N ₂	273	15:85	37.0
CO ₂ /CH ₄	296	50:50	6.4
CO ₂ /N ₂	296	15:85	38.4

Table S3. Equation parameters for the DSLF isotherm model.

Adsorbates	$N_1^{\max}$ (mmol/g)	b_1 (kPa ⁻¹)	$1/n_1$	$N_2^{\max}$ (mmol/g)	b_2 (kPa ⁻¹)	$1/n_2$
1a						
CO ₂ (273 K)	5.84212	0.00312	1.09163	3.90591	0.00808	1.09707
CH ₄ (273 K)	1.8189	0.00247	1.21258	0.69688	0.00278	1.16592
N ₂ (273 K)	0.33714	0.00717	0.97884	0.10463	0.00214	1.32019
CO ₂ (296 K)	3.70703	0.00279	1.11011	1.81594	0.01085	0.90231
CH ₄ (296 K)	0.81515	0.00114	1.37365	0.51875	0.00357	1.13232
N ₂ (296 K)	0.20737	0.00376	1.23743	0.04827	9.73155E-4	1.2096
2a						
CO ₂ (273 K)	3.29637	2.88732E-4	1.36359	2.20458	0.02105	0.97376
CH ₄ (273 K)	0.75567	0.00176	1.30619	0.36853	0.01383	0.90577
N ₂ (273 K)	0.2728	0.00219	1.19577	0.13969	0.0033	1.28087
CO ₂ (296 K)	2.77073	0.00906	0.96235	1.13709	0.00103	1.06798
CH ₄ (296 K)	0.5847	0.00452	1.08803	0.30156	0.0028	1.27058
N ₂ (296 K)	0.19832	0.00207	1.15664	0.087	0.00645	0.9631

Note: Dual-site Langmuir-Freundlich (DSLF) model is listed as below:

$$N = N_1^{\max} \times \frac{b_1 p^{1/n_1}}{1 + b_1 p^{1/n_1}} + N_2^{\max} \times \frac{b_2 p^{1/n_2}}{1 + b_2 p^{1/n_2}}$$

Where p (unit: kPa) is the pressure of the bulk gas at equilibrium with the adsorbed phase, N (unit: mol/kg) is the adsorbed amount per mass of adsorbent, $N_1^{\max}$ and $N_2^{\max}$ (unit: mol/kg) are the saturation capacities of sites **1** and **2**, b_1 and b_2 (unit: 1/kPa) are the affinity coefficients of sites **1** and **2**, and n_1 and n_2 represent the deviations from an ideal homogeneous surface.