## **Supplementary Information**

## The hydrogenation performance control of MoP and Ni<sub>2</sub>P catalysts

## by electronegativity modification method

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Samples	Mo [wt%]	Ni [wt%]	P [wt%]	W [wt%]	Cu [wt%]
MoP	75.36	-	24.64	-	-
Mo <sub>8</sub> WP <sub>9</sub>	60.81	-	19.73	19.46	-
Mo <sub>8</sub> CuP <sub>9</sub>	70.08	-	22.28	-	7.64
Ni <sub>2</sub> P	-	87.21	12.79	-	-
$Ni_{38}W_2P_2$	-	66.08	19.99	14.29	-

**Table S1.** The element content of different catalysts measured by SEM-EDS.

Table S2. Results of EXAFS model fitting of different catalysts<sup>a</sup>.

Samples	Element	Shell	R (Å)	CN	ss <sup>2</sup> /10 <sup>3</sup>	$s_0^2$	E <sub>0</sub> /eV	R- factor(%)
MoP	Mo	Mo-P	2.45	5.7	3.73	0.93	0.3	0.22
		Mo-Mo	3.21	6.8	3.95	0.79	-0.7	0.22
Mo <sub>8</sub> WP <sub>9</sub>	Mo	Mo-P	2.46	5.9	3.72	0.91	1.5	0.51
		Mo-Mo	3.21	7.3	4.56	0.72	-0.7	0.51
	W	W-P	2.45	5.5	2.94	0.81	7.5	0.89
		W-M	3.21	5.3	4.78	0.44	5.8	0.89
Ni <sub>2</sub> P	Ni	Ni-P	2.24	2.4	9.09	0.53	0.7	0.37
		Ni-Ni	2.62	4.3	7.53	0.54	3.5	0.37
$Ni_{38}W_2P_{20}$	Ni	Ni-P	2.24	4.1	8.94	0.54	0.8	0.32
		Ni-Ni	2.62	8.1	7.96	0.55	3.8	0.32
	W	W-P	2.46	4.6	8.61	1.15	5.7	0.19
		W-Ni	2.72	3.7	5.32	0.46	3.2	0.19

<sup>a</sup>R: Interatomic distance; CN: Coordination number; ss<sup>2</sup>: Disorder factor. The errors in the fitted parameters are estimated to be within CN  $\pm$  10 %, R  $\pm$  0.02-0.05

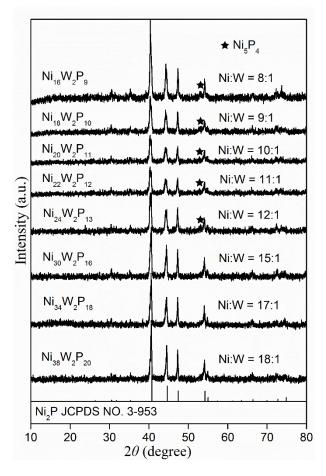


Figure S1. The XRD patterns of Ni-W-P catalysts with different Ni/W ratio.

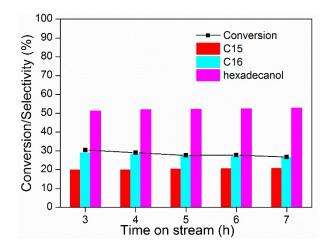


Figure S2. The methyl palmitate conversion and products selectivity of MoP catalysts

(reaction conditions: 3 MPa, 300 °C, WHSV = 6  $h^{-1}$ ,  $H_2/oil = 1000$ ).

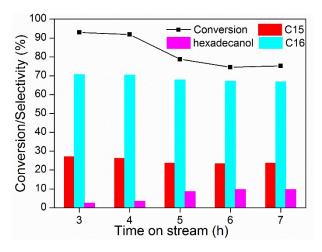


Figure S3. The methyl palmitate conversion and products selectivity of  $Mo_8WP_9$ 

catalysts (reaction conditions: 3 MPa, 300 °C, WHSV = 6  $h^{-1}$ ,  $H_2/oil = 1000$ ).

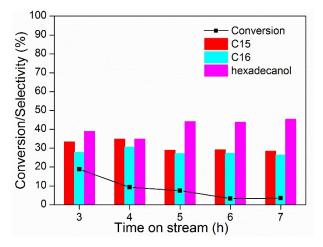


Figure S4. The methyl palmitate conversion and products selectivity of Mo<sub>8</sub>CuP<sub>9</sub>

catalysts (reaction conditions: 3 MPa, 300 °C, WHSV = 6  $h^{-1}$ ,  $H_2/oil = 1000$ ).

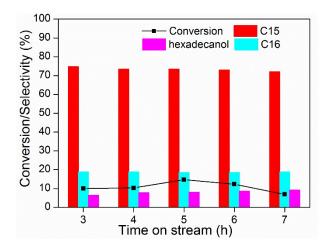
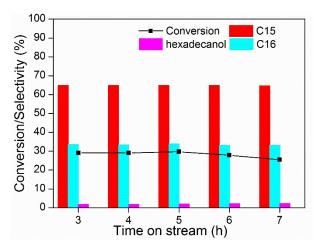


Figure S5. The methyl palmitate conversion and products selectivity of Ni<sub>2</sub>P catalysts

(reaction conditions: 3 MPa, 370 °C, WHSV = 3  $h^{-1}$ ,  $H_2/oil = 1000$ ).



**Figure S6.** The methyl palmitate conversion and products selectivity of Ni<sub>2</sub>P catalysts (reaction conditions: 3 MPa, 370 °C, WHSV = 3  $h^{-1}$ , H<sub>2</sub>/oil = 1000).