

Supporting Information for:

**Multimetallic Catalysts of RuO₂-CuO-Cs₂O-TiO₂/SiO₂ for Direct
Gas-Phase Epoxidation of Propylene to Propylene Oxide**

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Table S1 Detailed experiments for the Box–Behnken designs of experiment

Std.	Factor				Response		
	A: Temperature reactions (°C)	B: O ₂ /C ₃ H ₆ (ratio)	C: (O ₂ +C ₃ H ₆)/He (ratio)	D: Total flow rate (cc/min)	PO selectivity (%)	C ₃ H ₆ conversion (%)	PO formation rate (g _{PO} h ⁻¹ kg _{cat} ⁻¹)
1	190	0.7	0.05	50	31.6	0.2	43
2	310	0.7	0.05	50	8.4	9.0	464
3	190	6.7	0.30	50	35.1	0.7	89
4	310	6.7	0.30	50	10.0	33.5	1876
5	250	11.0	0.14	30	21.5	18.6	1572
6	250	2.2	0.19	30	11.7	29.1	3288
7	250	11.0	0.14	70	15.3	30.8	1753
8	250	2.2	0.19	70	9.4	32.7	2895
9	190	3.7	0.16	30	31.9	0.4	89
10	310	3.7	0.16	30	9.3	40.4	2209
11	190	3.7	0.16	70	35.6	0.2	49
12	310	3.7	0.16	70	7.4	43.8	1862
13	250	2.0	0.03	50	26.9	8.3	817
14	250	20.0	0.27	50	12.3	53.9	3050
15	250	0.4	0.08	50	17.2	5.1	796
16	250	4.0	0.33	50	34.8	7.7	2514
17	190	11.0	0.14	50	34.1	0.7	89
18	310	11.0	0.14	50	14.6	51.2	2190
19	190	2.2	0.19	50	34.5	0.3	128
20	310	2.2	0.19	50	8.4	63.6	1767
21	250	0.7	0.05	30	18.6	7.1	866
22	250	6.7	0.30	30	28.5	13.1	2265
23	250	0.7	0.05	70	18.0	5.9	668
24	250	6.7	0.30	70	20.0	16.9	1908
25	250	3.7	0.16	50	9.4	39.0	2433
26	250	3.7	0.16	50	11.6	32.2	2479
27	250	3.7	0.16	50	9.7	37.9	2435
28	250	3.7	0.16	50	10.8	34.1	2441
29	250	3.7	0.16	50	10.2	35.5	2408

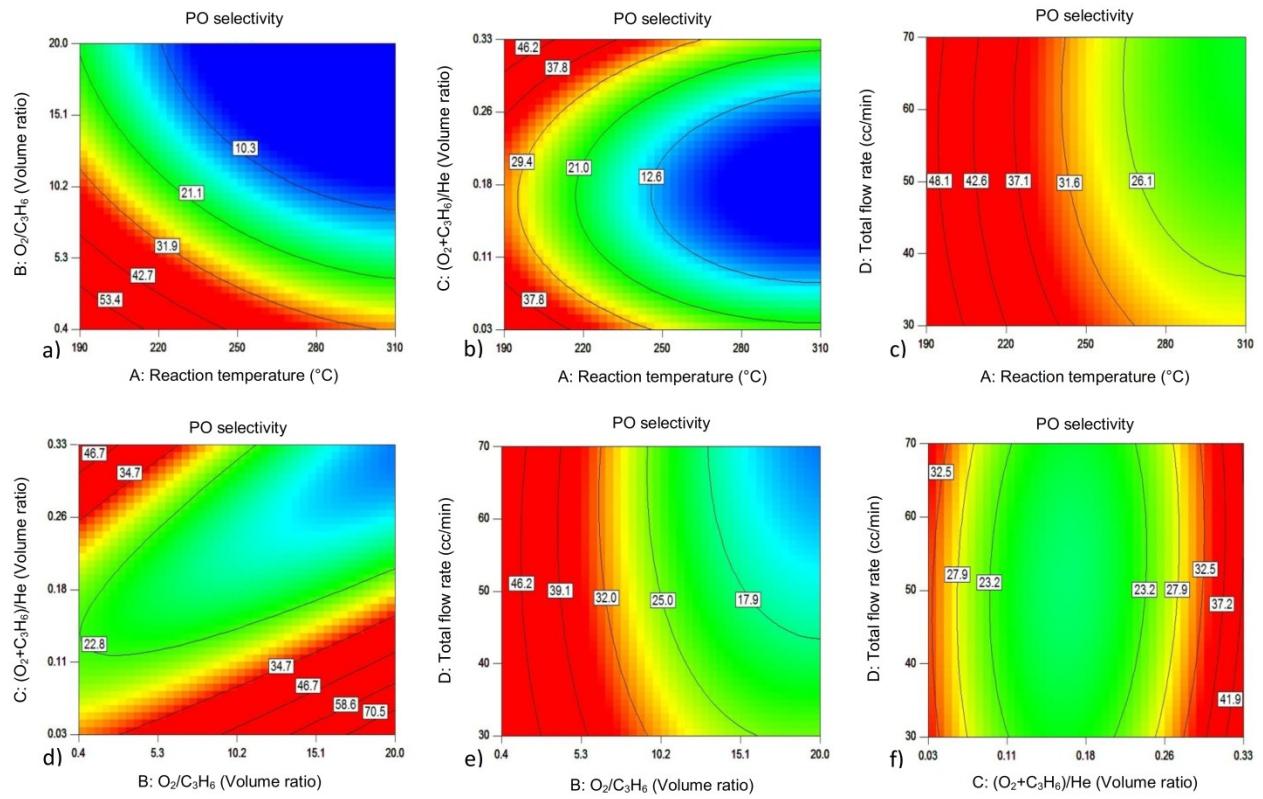


Fig. S1 a) – f) Contour plots showing % PO selectivity from all combinations of 4 parameters; a) A vs B, b) A vs C, c) A vs D, d) B vs C, e) B vs D, f) C vs D; where A = Reaction temperature (190–310 °C), B = $\text{O}_2/\text{C}_3\text{H}_6$ ratio (0.4–20), C = $(\text{O}_2+\text{C}_3\text{H}_6)/\text{He}$ ratio (0.03–0.33), and D = total feed gas flow rate (30–70 cc/min by using He as balance gas)]. When two parameters were studied, A, B, C and/or D were fixed at 219 °C, 4.1, 0.32, and/or 70 cc/min, respectively.

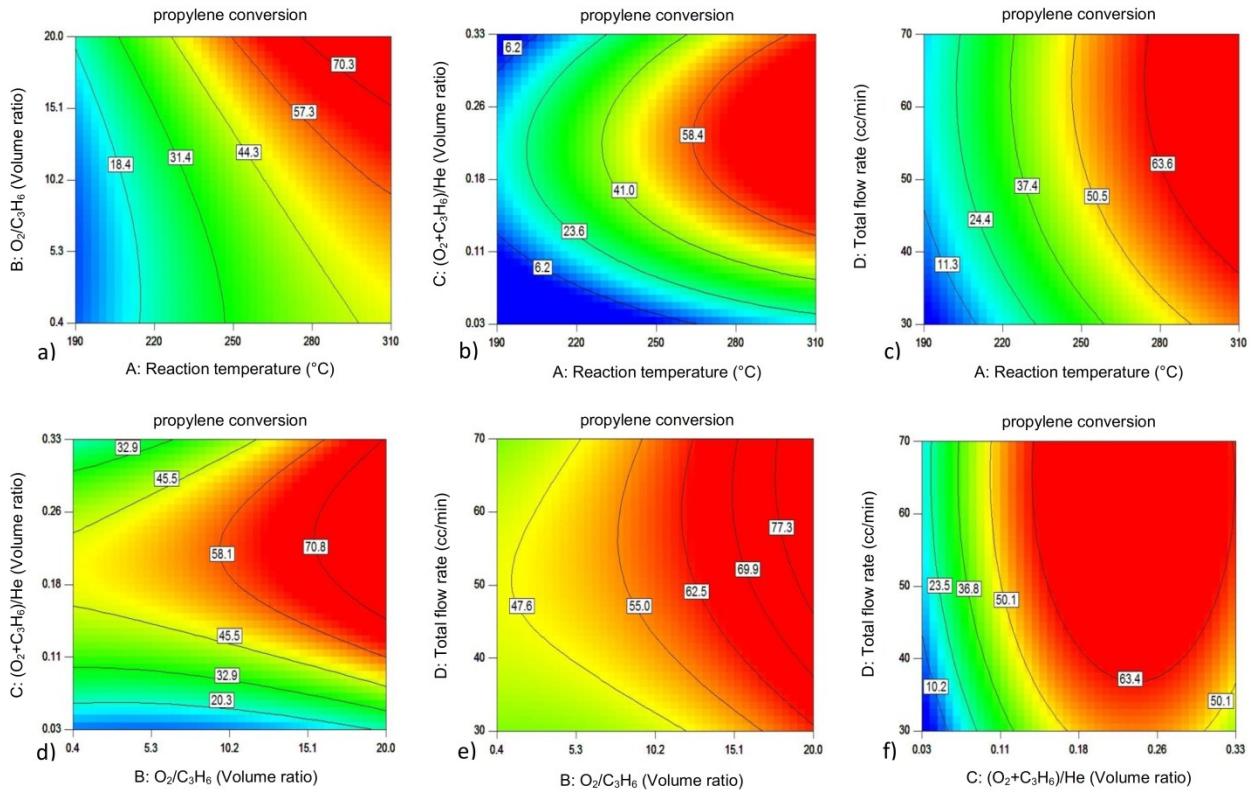


Fig. S2 Contour plots showing % propylene conversion from all combinations of 4 parameters; a) A vs B, b) A vs C, c) A vs D, d) B vs C, e) B vs D, f) C vs D; where A = Reaction temperature (190–310 °C), B = $\text{O}_2/\text{C}_3\text{H}_6$ ratio (0.4–20), C = $(\text{O}_2+\text{C}_3\text{H}_6)/\text{He}$ ratio (0.03–0.33), and D = total feed gas flow rate (30–70 cc/min by using He as balance gas)]. When two parameters were studied, A, B, C and/or D were fixed at 310 °C, 17.4, 0.23, and/or 57 cc/min, respectively.

Table S2 Predicted and experimental values of optimal PO selectivity and PO formation rate obtained from the Box–Behnken designs of experiment.

Optimization	Temperature (°C)	O ₂ /C ₃ H ₆ (ratio)	(O ₂ +C ₃ H ₆)/He (ratio)	Total flow rate (cc/min)	PO selectivity (%)		C ₃ H ₆ conversion (%)		PO formation rate (g _{PO} h ⁻¹ kg _{cat} ⁻¹)	
					Predict	Test	Predict	Test	Predict	Test
PO Selectivity	219	4.1	0.32	70	37.3	38.4	-	1.3	-	573
PO formation rate	272	3.1	0.26	34	-	7.1	-	40.1	2973	3015

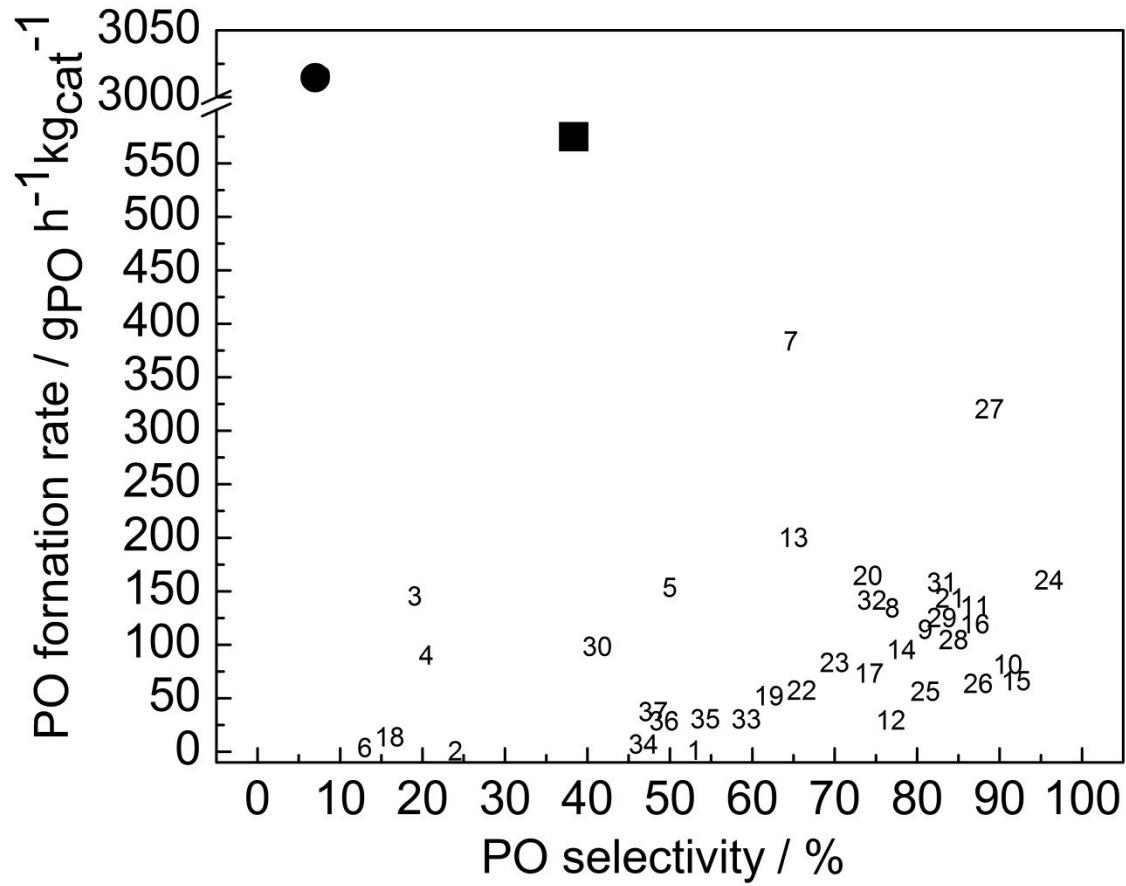


Fig. S3 PO formation vs PO selectivity of various catalysts for the direct gas-phase epoxidation of propylene to PO reported in literature from 2005 – present.

Table S3 Catalysts reported in literature for catalysts the direct gas-phase epoxidation of propylene to PO reported in literature from 2005 – present.

No.	Catalyst	Reactions	Temperature (°C)	Pressure (atm)	C ₃ H ₆ conversion (%)	PO selectivity (%)	PO formation rate (g _{PO} h ⁻¹ kg _{cat} ⁻¹)	Ref.
1	Cu/SiO ₂	Epoxidation	225	1	0.3	53.0	1	¹
2	K ⁺ –Cu/SBA–15	Epoxidation	350	1	2.2	24.0	1	²
3	(KAc)–Cu/SiO ₂	Epoxidation	325	1	0.3	19.1	145	³
4	K–Cu/m–SiO ₂	Epoxidation	350	1	2.9	20.5	90	⁴
5	RuO ₂ –CuO–NaCl/SiO ₂	Epoxidation	270	1	20.0	50.0	153	⁵
6	d–Cu ₂ O	Epoxidation	250	1	0.8	13.0	3	⁶
7	Ti–MoO ₃ –Bi ₂ SiO ₅ /SiO ₂	Epoxidation	400	1.4	20.5	64.7	383	⁷
8	Au/TS–1	Hydroperoxide	200	1	10.0	76.0	134	⁸
9	Au/TS–1(36)	Hydroperoxide	200	n/a	8.8	81.0	116	⁹
10	Au–Ba(NO ₃) ₃ /Ti–SiO ₂	Hydroperoxide	150	1	8.5	91.0	81	¹⁰
11	0.33Au/PCTS–1(28)	Hydroperoxide	200	n/a	9.7	87.0	132	¹¹
12	Au–Ba/Ti–TUD	Hydroperoxide	150	1	2.1	76.8	29	¹²
13	Au/TS–1	Hydroperoxide	212	n/a	16.0	65.0	200	¹³
14	0.09Au/TS–1(170)	Hydroperoxide	200	1	6.7	78.1	95	¹⁴
15	0.14Au/0.04Ge–TS–1(100)	Hydroperoxide	170	1	4.0	91.0	66	¹⁵
16	Au/TS–1(48)–Na1	Hydroperoxide	200	n/a	7.4	85.0	119	¹⁶
17	Ba(NO ₃) ₃ –Au/Ti–MCM–41	Hydroperoxide	150	n/a	5.4	74.2	73	¹⁷
18	VO _x –Cu	Hydroperoxide	230	1	2.7	16.0	13	¹⁸

19	Au-Ti(0.05) -M	Hydroperoxide	150	1	2.2	62.0	52	19
20	Au/TS-1(35)	Hydroperoxide	300	1	14.6	74.0	164	20
21	0.2Au/TS-1-Na	Hydroperoxide	200	n/a	8.3	84.0	127	21
22	Au-00	Hydroperoxide	200	1	4.8	66.0	57	22
23	Au/TS-1 ₃₅ /Si/1.0%	Hydroperoxide	300	1	12.6	70.0	83	23
24	0.081Au/TS-1(127)	Hydroperoxide	200	1	5.1	96.0	160	24
25	0.57Au/0.4In-TS-1	Hydroperoxide	170	1	3.8	81.0	56	25
26	0.05-Au/Ti-SiO ₂ -1L	Hydroperoxide	200	1	2.7	89.4	63	26
27	0.16Au/TS-1(121)Cs	Hydroperoxide	200	1	11.4	88.8	320	27
28	0.08Au/NTS-1-10	Hydroperoxide	150	1	6.8	84.4	105	28
29	Au/TS-1	Hydroperoxide	200	1	n/a	83.0	125	29
30	0.04Au/U-TS-1(119)	Hydroperoxide	200	1	3.2	41.2	98	30
31	0.13 wt% Au/TS-1-B(40)	Hydroperoxide	200	1	n/a	83.0	158	31
32	0.5Au/TS-1-15 g/L	Hydroperoxide	300	1	11.5	74.5	141	32
33	4.5Au/A-TiYNU-1	Hydroperoxide	225	1	3.3	59.3	30	33
34	V-Ti/MCM-41	Photo reaction	50	1	24.4	46.8	7	34
35	Au/TS-1	Photo reaction	50	1	56.1	54.3	30	35
36	V-Ti/MCM-41	Photo reaction	50	1	n/a	49.3	29	36
37	V _{0.2} Ti _{0.3} /MCM-41	Photo reaction	50	1	0.2	48.0	37	37
■	RuO ₂ -CuO-Cs ₂ O-TiO ₂ /SiO ₂	Epoxidation	219	1	1.3	38.4	573	This work
●	RuO ₂ -CuO-Cs ₂ O-TiO ₂ /SiO ₂	Epoxidation	273	1	40.1	7.1	3015	This work

* n/a = not available

Table S4 Multiple test runs of the optimal RuO₂-CuO-Cs₂O-TiO₂/SiO₂ catalyst with (w/) and without (w/o) treating with fumed HCl under the optimal operating condition for PO formation rate.

Run no.	PO selectivity (%)		AC selectivity (%)		C ₃ H ₆ conversion (%)		PO formation rate (g _{PO} h ⁻¹ kg _{cat} ⁻¹)	
	W/O	W/	W/O	W/	W/O	W/	W/O	W/
1	7.1	-	0.5	-	40.1	-	3015	-
2	10.5	7.6	0.8	0.7	18.8	34.9	2202	3010
3	15.0	7.7	1.2	0.5	6.9	34.1	1156	2997
4	12.5	7.7	1.2	0.7	6.7	34.0	935	2984
5	11.7	7.5	1.4	0.3	5.6	34.7	732	2965
6	10.8	8.0	1.4	0.3	5.8	32.5	696	2971

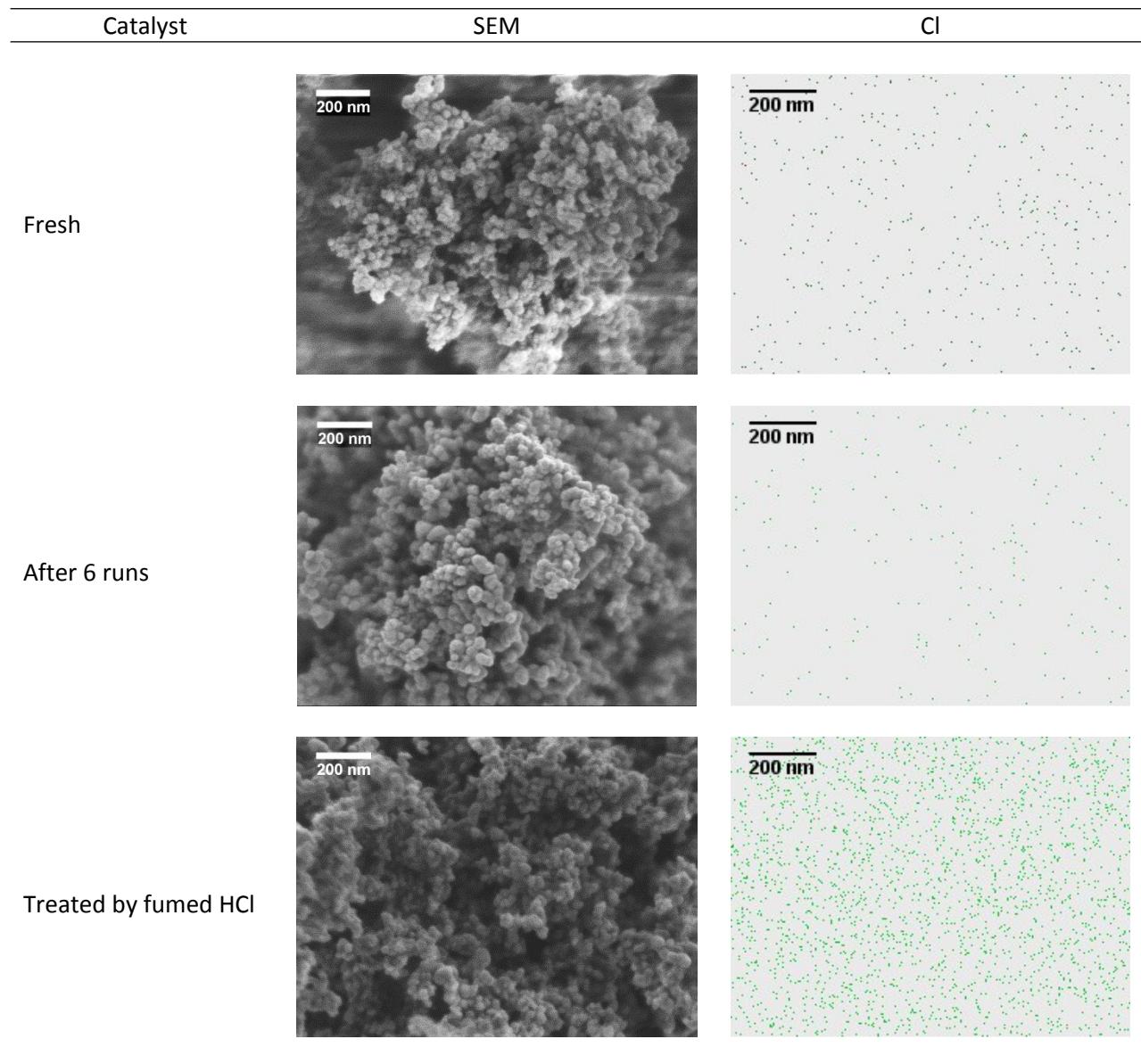


Fig. S4 SEM-EDS showing Cl of the optimal $\text{RuO}_2\text{-CuO}\text{-Cs}_2\text{O}\text{-TiO}_2/\text{SiO}_2$ catalyst; fresh catalyst, after 6 runs of testing, and after treated by fumed HCl.

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