

# **Supplementary information for**

## **Nanocrystalline MnO<sub>2</sub> on Activated Carbon Fiber for**

### **Catalytic Formaldehyde Removal**

Zijian Dai <sup>a</sup>, Xiaowei Yu <sup>b</sup>, Chen Huang <sup>a</sup>, Meng Li <sup>a</sup>, Jiafei Su <sup>b</sup>, Yaping Guo <sup>b</sup>, He Xu<sup>b</sup>, Qinfei Ke, <sup>\*, b, a</sup>

a Key Laboratory of Textile Science & Technology (College of Textiles, Donghua University), Ministry of Education, Shanghai 201620, P. R. China. E-mail address: [kqf@dhu.edu.cn](mailto:kqf@dhu.edu.cn)

b Environmental Materials Research Center, Shanghai Normal University, Shanghai 200234, P. R. China

**Table S1. Summary of catalytic oxidation for formaldehyde removal at ambient temperature in recent literature.**

Catalyst	Concentration	Temperature	Test method	Performance	Ref.
Pt/TiO <sub>2</sub> hollow chains	260 ± 5 ppm	Room temperature	Organic glass box reactor(4.4 L) catalyst weight: 0.1 g	HCHO decreased to 17.2 ppm after 60 min with R0.5Pt/TiO <sub>2</sub>	29
Eu/CeO <sub>2</sub>	500 ppm	20-350 °C	Tests were performed in a fixed-bed reactor GHSV =30,000 mL · h <sup>-1</sup> · g <sup>-1</sup>	The complete HCHO oxidation of 4% Eu/CeO <sub>2</sub> nanosheets can be obtained at 120°C	30
			Tests were	100% HCHO	

manganese oxides with different crystal structures	170 ppm	50-200 °C	performed in a fixed-bed quartz flow reactor (i.d. = 4 mm) catalyst: 60 mg GHSV = 100 000 mL (g <sub>cat</sub> h) <sup>-1</sup>	conversion occurs at 80 °C for δ-MnO <sub>2</sub> , 125 °C, 200 °C, and 150 °C for α-MnO <sub>2</sub> , β-MnO <sub>2</sub> and γ-MnO <sub>2</sub>	6
Pt/ceramics	140 ppm	Room temperature (25 °C)	Organic glass box reactor (6 L) catalyst weight: 21 g (300 mesh)	Best performance with 0.013 wt% Pt loaded at Pt/HC catalysts.	31
Pt/MnO <sub>2</sub>	460 ppm	20-200 °C	Test in fixed-bed reactor; catalyst: 0.1 g; GHSV: 20 000 h <sup>-1</sup>	~30% conversion of HCHO over 0.5-1 wt% Pt/MnO <sub>2</sub> 20 °C	27
Au <sub>0.5</sub> Pt <sub>0.5</sub> /MnO <sub>2</sub> /cotton	460 ppm;	20-200 °C	Fixed-bed reactor; (length = 500 mm, diameter = 4 mm) GHSV: 20 000 h <sup>-1</sup>	~30% HCHO conversion over (Au <sub>0.5</sub> Pt <sub>0.5</sub> /MnO <sub>2</sub> )(20 wt%)/cotton at 40 °C 100% conversion at 120 °C	32
MnO <sub>2</sub> /cellulose	100 ppm	60-180 °C	Tests were performed in a fixed-bed quartz flow reactor (length = 300 mm,	100 % conversion with 8.86% loading amount in MnO <sub>2</sub> /cellulose at 140 °C	

			diameter = 4 mm)	~16.7%	13
			GHSV = 50 000 <sup>-1</sup>	conversion at	
				60 °C	
			Performed with a	100% HCHO	
			fixed-bed quartz	conversion was	
			flow reactor	attained in the	
			(length = 300 mm,	space velocity of	
			diameter = 4 mm)	GHSV = 50,000	
		Room	GHSV: 50,000,	h <sup>-1</sup> , and about	
Pt/TiO <sub>2</sub>	100 ppm	temperature	100,000, 200,000	97% and 58%	33
		(25 °C)	h <sup>-1</sup> by changing the	HCHO	
			used catalyst	conversion in the	
			volume	space velocity of	
				GHSV = 100,000	
				and 200,000 h <sup>-1</sup> ,	

### Content of $\delta$ -MnO<sub>2</sub>.

**Table S2. Preparation of MnO<sub>2</sub>/ACF.**

Sample	Conc. of KMnO <sub>4</sub> solution (mol L <sup>-1</sup> )	Conc. of MnSO <sub>4</sub> solution (mol L <sup>-1</sup> )	MnO <sub>2</sub> content in MnO <sub>2</sub> /ACF (wt.%)
0.01-MnO <sub>2</sub> /ACF	0.013	0.010	5.62
0.02-MnO <sub>2</sub> /ACF	0.026	0.020	11.74
0.03-MnO <sub>2</sub> /ACF	0.040	0.030	16.12
0.04-MnO <sub>2</sub> /ACF	0.052	0.040	22.42
0.05-MnO <sub>2</sub> /ACF	0.066	0.050	29.33

Results illustrated that the amount of  $\delta$ -MnO<sub>2</sub> NPs attached in MnO<sub>2</sub>/ACF was determined by the initial concentration of MnSO<sub>4</sub> and KMnO<sub>4</sub> solution. By altering

the concentration of  $\text{MnSO}_4$  and  $\text{KMnO}_4$  solution, different  $\text{MnO}_2$  contents of  $\text{MnO}_2/\text{ACF}$  could be obtained. With the increasing of the concentration of  $\text{MnSO}_4$  and  $\text{KMnO}_4$  solution, the content of  $\delta\text{-MnO}_2$  was increasing.

### Calculation of formaldehyde removal amount

The removal capacity of formaldehyde was calculated according to the following equation (equation [1]):

where  $W$  is the removal amount of formaldehyde per unit weight of adsorbent (mol/g),  $P$  is atmospheric pressure (1 atm),  $V$  is volume of removal formaldehyde at 80% breakthrough time which was calculated from the integrated area over breakthrough curve  $\times 10^{-6} \times 0.2$  L/min,  $R$  is universal gas constant ( $0.08204 \text{ atm} \times \text{mol}^{-1} \times \text{K}^{-1}$ ),  $T$  is operating temperature (298.15 K), and  $m$  is mass of adsorbent.

Finally,  $W$  was converted to weight percentage of removed formaldehyde per unit weight of adsorbent and labelled as  $W_0$  (mg/g).

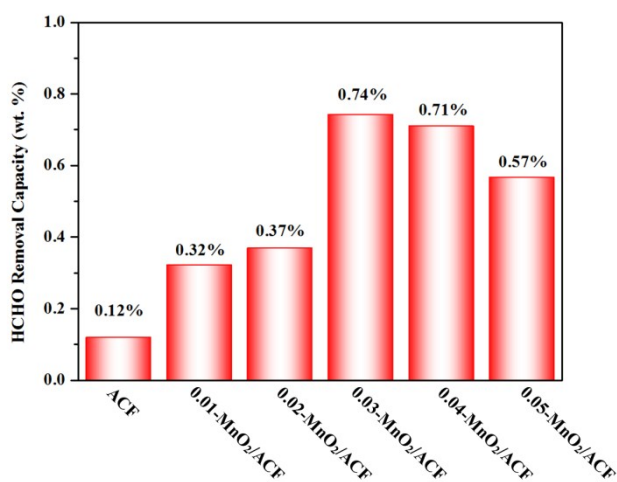


Fig. S1 HCHO removal capacities of ACF and  $\text{MnO}_2/\text{ACF}$  samples.

## References

[S1] Song Y, Qiao W, Yoon S-H, Mochida I, Guo Q, Liu L. Removal of formaldehyde at low concentration using various activated carbon fibers. *J Appl Polym Sci* 2007;106(4):2151-2157.