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## **Supplementary Information:**

## Effect on ceramic grade $CaF_2$ recovery quality from the etching wastewater under the optimum sulfate content

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## 1. Figures

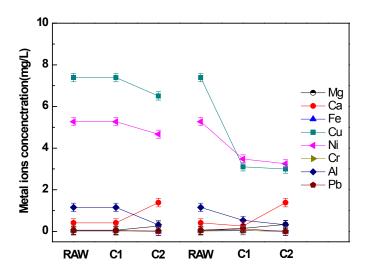


Fig.S1 Concentrations of metal ions adsorbed by 2 g/L AC ( $C_F$ =1613mg/L).

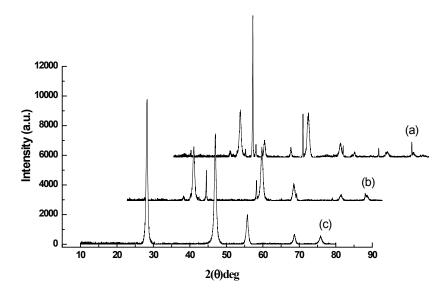
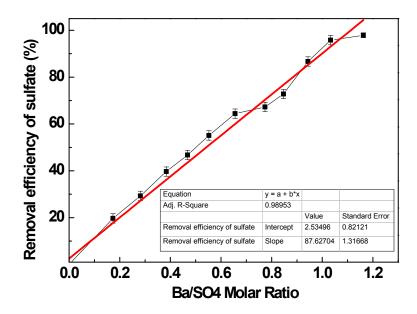


Fig.S2.XRD pattern: (a) calcium fluoride synthesized directly without pre-treatment; (b) calcium fluoride generated by calcium chloride after removal of metal ions by AC absorption (Ca/F=1.2, pH=7); (c) Ceramic grade CaF<sub>2</sub>.



**Fig.S3.** Variations of removal efficiency of sulfate with  $Ba^{2+}/SO_4^{2-}$  molar ratio after 30 min of mixing time.

## 2. Tables

 $\textbf{Table S1} \ \ \text{Chemical components of } CaF_2 \ \ \text{synthesized by } CaCl_2 \ \ \text{after } AC \ \ \text{adsorption}$ 

Components	Weight (%)		
	Control	Experiment	
CaF <sub>2</sub>	77.5	79.7	
$CaSO_4$	9.5	9.9	
$Ca_3(PO_4)_2$	0.6	0.7	
Other impurity	12.4	9.7	

 $\textbf{Table S2} \ \ \textbf{Settlement capability analysis of } CaF_2 \ \textbf{synthesized after } AC \ \textbf{adsorption}.$ 

Runs	Turbidity(NTU)		Zata matantial(my)	TOC(m~/I)	
	0h	1h	— Zeta potential(mv)	TOC(mg/L)	
Control	238	17.8	24.54	35.2	
Experiment	267	54.8	28.81	21.4	

 $\textbf{Table S3} \ \text{Experimental conditions and chemical composites of } CaF_2 \ production.$ 

Run	$C_{\mathrm{F}}$	[Ca]/[F]	рН	$C_{ m sulfate}$	CaF <sub>2</sub>	CaSO <sub>4</sub>
	mg/L			mg/L	%	%
Control	1181	1.2	6.9	398	78.6	12.4
Experiment	1181	1.2	7.1	36	92.4	0.6
Verification	1408	1.28	8.2	121	88.2	4.6