

Electronic Supplementary Information

Facile synthesis of low-cost biomass-based γ -Fe₂O₃/C for efficient adsorption and catalytic degradation of methylene blue in aqueous solution

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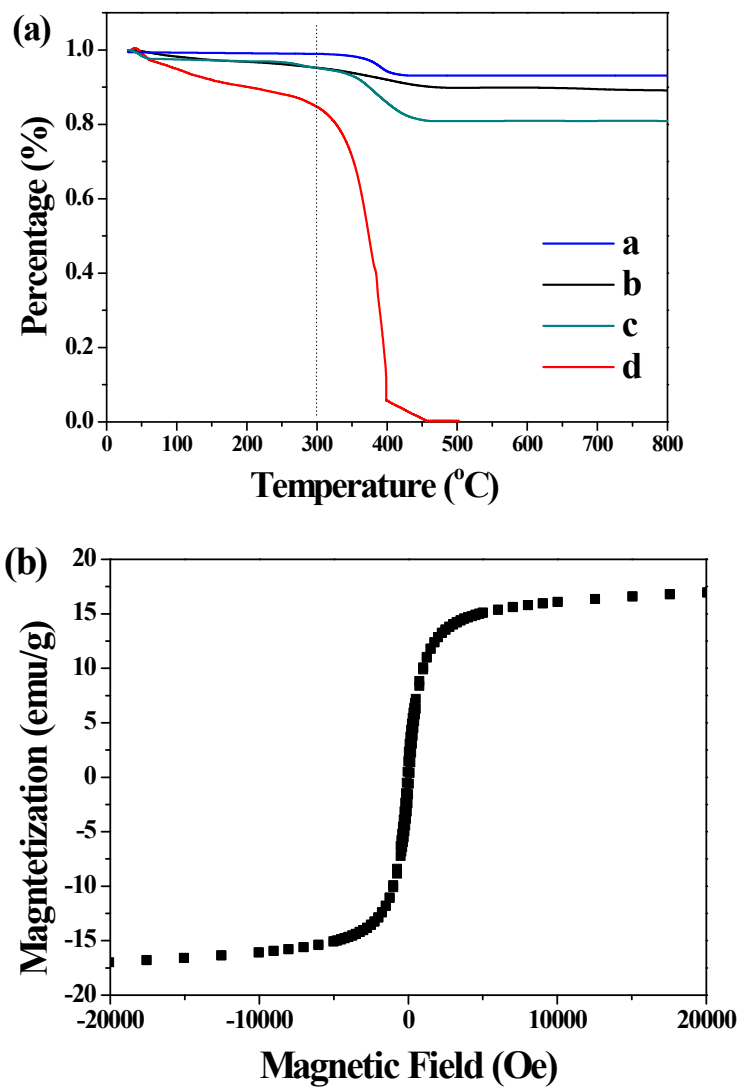


Fig.S1 (a) TGA curves of γ -Fe₂O₃/C, the FeCl₃ impregnation ratio was (a) 2:1; (b) 1.5:1; (c) 0.5:1; (d) 0:1;

(b) Magnetization curves of γ -Fe₂O₃/C (the FeCl₃ impregnation ratio=0.5:1; the carbonization time=4 min).

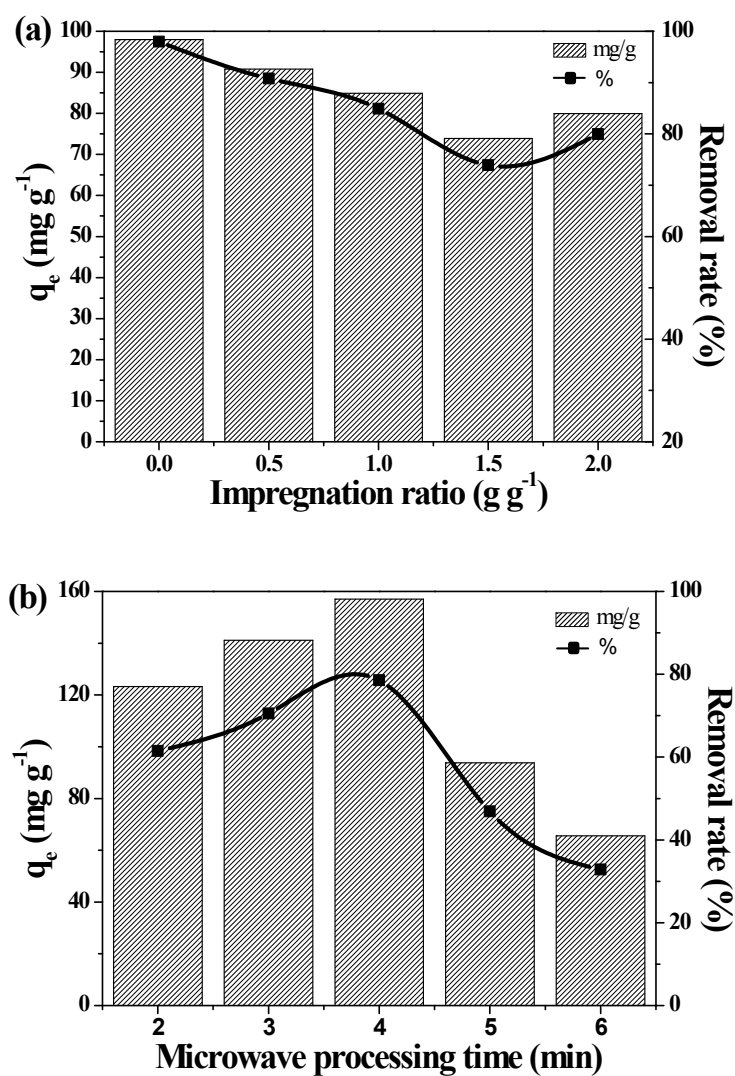


Fig.S2 a) Influence of the proportion of impregnation. b) Influence of the carbonization time. (C_{MB} : 50 mg L^{-1} ; T : 30°C ; pH : 7; the dosages of adsorbent: 10 mg)

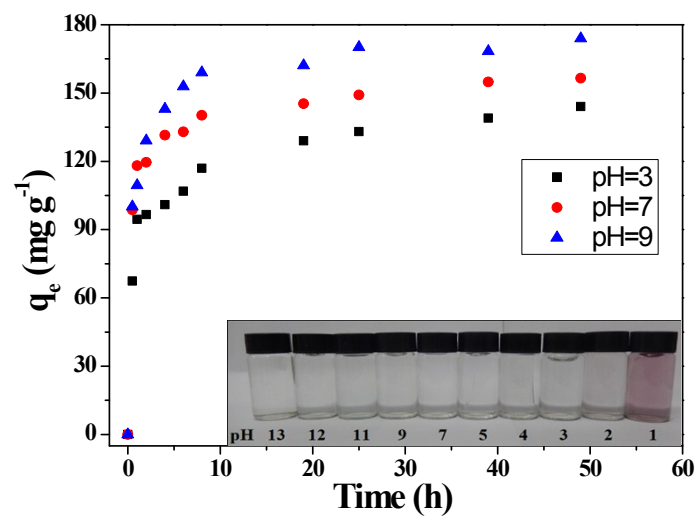


Fig.S3 Influence of pH value of the adsorption system. Insert: a series soak solution of different pH.(the dosages of adsorbent: 10 mg; C_{MB} : 200 mg L⁻¹; T: 30 30 °C)

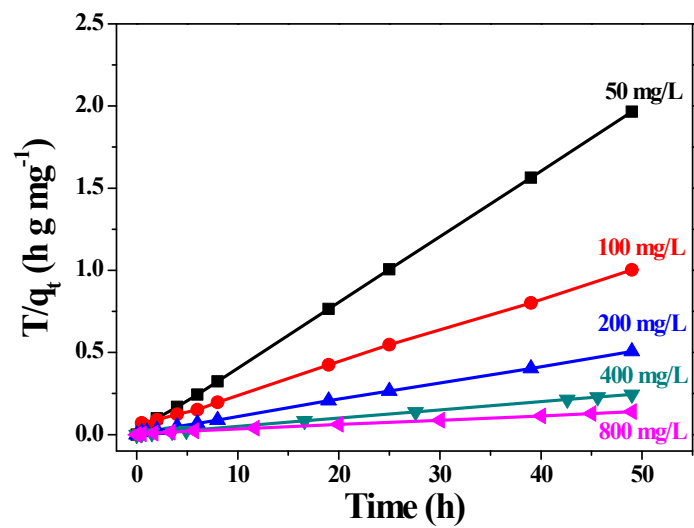


Fig.S4 The pseudo-second-order model of adsorption of MB at 30 °C.(pH: 7; the dosages of adsorbent: 10 mg)

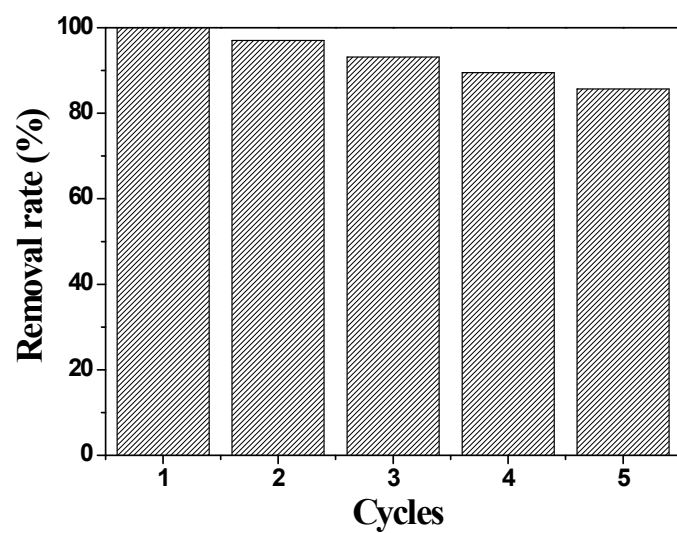


Fig.S5 The recycling performance of $\gamma\text{-Fe}_2\text{O}_3/\text{C}$. (C_{MB} : 50 mg L⁻¹; T: 30 °C; pH: 7; the dosages of adsorbent: 10 mg)

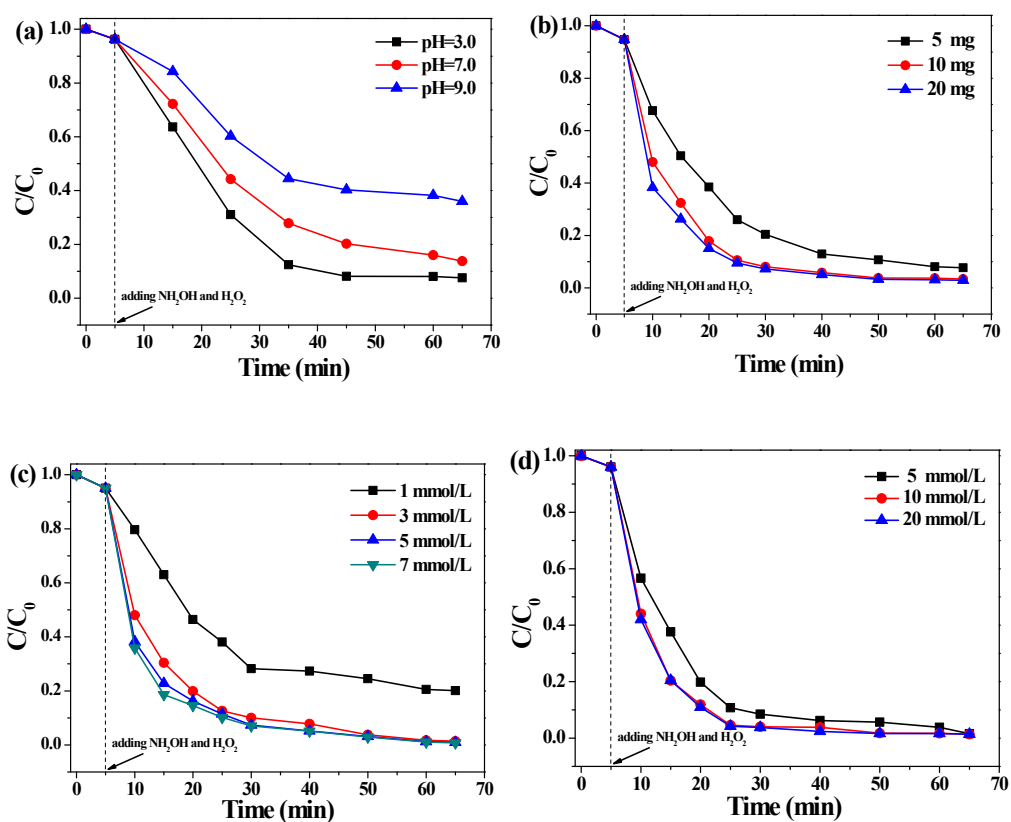


Fig.S6 Effect of different reaction conditions of degradation with MB (100 mg L^{-1}) at $30 \text{ }^{\circ}\text{C}$:

- a) pH (the dosages of catalyst: 5 mg ; NH_2OH : 10 mmol L^{-1} ; H_2O_2 : 1 mol L^{-1});
- b) the concentration of H_2O_2 (the dosages of catalyst: 5 mg ; NH_2OH : 10 mmol L^{-1} ; pH: 7);
- c) the concentration of NH_2OH ; (the dosages of catalyst: 5 mg ; H_2O_2 : 3 mol L^{-1} ; pH: 7);
- d) the dosages of catalyst (pH: 7; NH_2OH : 10 mmol L^{-1} ; H_2O_2 : 3 mol L^{-1})

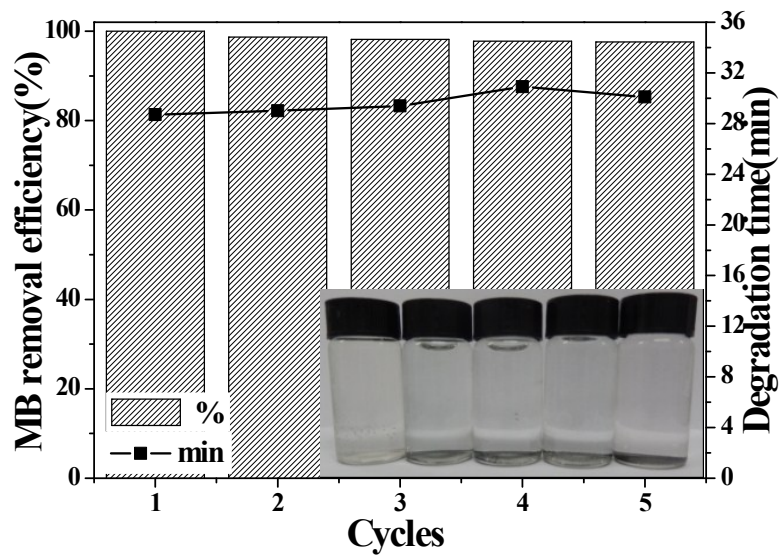


Fig.S7 The recycling performance of the catalytic. Insert: the stability of catalytic after 5 cycles. (C_{MB} : 50 mg L⁻¹; T: 30; pH: 7; the dosages of adsorbent: 10 mg; NH₂OH: 10 mmol L⁻¹; H₂O₂: 3 mol L⁻¹)

Table S1 Porosity analysis of γ -Fe₂O₃/C

γ -Fe ₂ O ₃ /C	BET Surface area (m ² g ⁻¹)	Average pore diameter (nm)	Total pore volumes (cm ³ g ⁻¹)
1	764.12	2.81	0.54
2	114.78	3.41	0.12

Notes: the FeCl₃ impregnation ratio and carbonization time of γ -Fe₂O₃/C-1 and 2 were 0.5:1, 2:1, and 4 min, 4min, respectively.

Table S2 Correlation coefficients of the dynamic equation at 30 °C and pH 7. (the dosages of adsorbent: 10 mg; the preparation condition of γ -Fe₂O₃/C: FeCl₃·6H₂O to bagasse ratio=0.5:1 (g g⁻¹); microwave processing time=4 min)

Pollutant	C ₀ (mg L ⁻¹)	q _{e(exp)} (mg g ⁻¹)	Pseudo-second-order kinetic model		
			q _{e(cal)} (mg g ⁻¹)	k ₂ (g mg ⁻¹ min ⁻¹)	R ²
MB	800	352.96	362.31	1.890×10 ⁻³	0.998
	400	199.75	200.40	2.546×10 ⁻²	0.999
	200	96.71	97.85	1.523×10 ⁻²	0.999
	100	48.90	50.58	1.021×10 ⁻²	0.997
	50	24.94	25.11	1.495×10 ⁻¹	0.999

Notes: C₀, initial concentration of MB; q_{e(exp)}, experimental adsorption capacity, q_{e(cal)}; calculated adsorption capacity; k₂, pseudo-second-order kinetic constant.

Table S3 Comparison of the adsorption capacity and degradation efficiency of various adsorbents for MB.

Sample	Adsorption capacity (mg g ⁻¹)	Degradation efficiency	References
Mesoporous organosilicon (BC-60)	556	--	[13]
Porous functional carbon material (HPFCMS-5-1-800)	385.12	--	[15]
ZnCl ₂ -molten salt synthesis (MSS)	353.1	--	[18]
Peanut shell magnetic carbon (PMC-2)	--	90 % (Time ≤ 30 min; C _{MB} = 40 mg g ⁻¹)	[19]
Manganese oxide (MO)	--	99 % (Time ≤ 10 min; C _{MB} = 100 mg g ⁻¹)	[22]
Graphene oxide-iron(III) based cellulose nanofibril (30 % GO-Fe-CNF)	143.96	30.4 % (Time ≤ 24 h; C _{MB} = 100 mg g ⁻¹)	[23]
Fe-based metal-organic framework (γ-Fe ₂ O ₃ /C)	303.95	--	[26]
Biomass-based γ-Fe ₂ O ₃ /C	352.96	99 % (Time ≤ 30 min; C _{MB} = 100 mg g ⁻¹)	This work