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Supporting Information

Ca²⁺ and Ga³⁺ doped LaMnO₃ perovskite as highly efficient and stable catalyst for two-step thermochemical water splitting

Lulu Wang,^a Mohammad Al-Mamun,^a Yu Lin Zhong,^a Lixue Jiang,^a Porun Liu,^a Yun Wang,^a

Hua Gui Yang^b and Huijun Zhao*ac

^aCentre for Clean Environment and Energy, Griffith University, Gold Coast Campus,

QLD 4222, Australia

^bKey Laboratory for Ultrafine Materials of Ministry of Education, School of Materials

Science and Engineering, East China University of Science and Technology, 130 Meilong Road, Shanghai 200237 China

°Centre for Environmental and Energy Nanomaterials, Institute of Solid State Physics, Chinese Academy of Sciences, Hefei 230031, P. R. China

E-mail: h.zhao@griffith.edu.au; Fax: +61 7 5552 8067; Tel: +61 7 5552 8261

I Experimental Section

Perovskites synthesis

All the perovskite oxides were synthesised by a modified Pechini method.¹ . In brief, stoichiometric amounts of metal nitrate precursors were dissolved in deionized water and heated at 70 °C with continuous stirring. Citric acid was then added to the solution with a molar ratio of 1.5:1 with respect to the metal cations. After 10 min, ethylene glycol (ethylene glycol: citric acid molar ratio = 1:1) was added to the mixture and heated at 90 °C until a brownish gel was obtained. The resulting gel was transferred to an electric oven and kept at 120 °C for 12 h to obtain a resin. The resin was then collected and ground with a mortar and pestle. The final perovskite oxide powder was prepared by calcining the resin at 1300 °C for 6 h to remove any remaining organics or nitrates.

Characterisations

The X-ray diffraction (XRD) patterns of the samples were collected with a Bruker D8 X-ray diffractometer operated at 40 kV with the current of 25 mA using a Cu K α radiation. The measurements of 2 θ symmetrical scans were carried out in the range of 20–80 ° with a step size of 0.02 ° and a scanning rate of 2 °/min, respectively. Phase identification was conducted through comparisons with the standard Inorganic Crystal Structure Database (ICSD). Scanning electron microscopy (SEM, JSM- JSM-7100), energy dispersive X-ray (EDX, JSM-7100) mapping and transmission electron microscope (TEM, Tecnai F20) techniques were also employed to characterise the surface morphology and elemental distribution within the samples.

Thermochemical H₂O splitting test

The two-step thermochemical H₂O splitting activity was investigated using a laboratory-scale fix-bed reactor, as shown in Fig. S4. To facilitate effective testing, the freshly-prepared perovskite samples (~ 0.5 g) were transferred into a solid porous monolith structure by mixing with isopropanol then fired at 1300 °C for 6 h in air.² The prepared redox sample was then packed at the centre of an alumina tubular reactor coupled within a high temperature programmable electric furnace (MTI, KSL-1800X-S60). Ar (ultra-high purity ~ 99.99%) was used as a carrier gas and the flow rate was controlled by a mass flow controller (Alicat Scientific). The thermal reduction step was carried out by heating the perovskite sample to 1300 °C and holding for 1 h under an Ar flow rate of 200 sccm (the oxygen partial pressure was ~20 ppm). The temperature was then allowed to decrease to 900 °C for H₂O splitting. The

temperature increase and decrease rates were fixed at 10 °C/min. The water was introduced into the chamber by a water pump (Easypump, BT100N), then vaporised and mixed with Ar gas (the volume ratio of vapour in the mixture gas was ~ 40%). The whole H₂O splitting process was maintained for 1 h to complete the re-oxidation process. During the thermal reduction and H₂O splitting processes, the O₂ and H₂ produced were detected by mass spectrometer (MS, Omni Star GSD 320). For quantitative measurement of evolved gas, the ion current signal of the MS result was calibrated by standard O₂ and H₂ gases.

The re-oxidation yield (α) of thermochemical H₂O splitting test was calculated as follow,

$$\alpha = (n_{H_2} / 2n_{O_2}) \times 100\%$$

where n_{O_2} and n_{H_2} repersent the total amount (mole weight) of O₂ and H₂ evolved during twostep thermochemical H₂O splitting process.

II Supporting Figures



Fig. S1 XRD patterns of LaMnO₃ based perovskites with the Ga³⁺ doping content of 0.2 (black) and red (0.3) on the B site. The square represents the impurity of Ga_2O_3 in the fabricated perovskite sample.



Fig. S2 XRD patterns of parent LaMnO₃ and A site (Ca²⁺, Sr²⁺, Ba²⁺) and B site (Al³⁺ and Ga³⁺) doped LaMnO₃ perovskites.



Fig. S3 SEM images of of parent LaMnO₃ and A site (Ca²⁺, Sr²⁺, Ba²⁺) and B site (Al³⁺ and Ga³⁺) doped LaMnO₃ perovskites..



Fig. S4 Two-step thermochemical H₂O splitting set-up for H₂ production.



Fig. S5 A comparison of O_2 evolution and H_2 production between perovskite powder and porous monolith during two-step thermochemical H_2O splitting process.



Fig.S6 O_2 and H_2 production results of CeO₂ from thermochemcial H₂O splitting operated between 1300 and 900 °C.



Fig. S7 (a) O_2 evolution and (b) H_2 production curves of $La_{0.6}Ca_{0.4}Mn_{0.8}Ga_{0.2}O_3$ perovskite oxide with the two-step thermochemical H_2O splitting carried out between 1400 and 900 °C.



Fig. S8 SEM images of $La_{0.6}Ca_{0.4}Mn_{0.8}Ga_{0.2}O_3$ perovskite oxide after thermally reduced at (a) 1300 °C and (b) 1400 °C.



Fig. S9 XRD patterns of LCMGO before (black) and after (red) the thermochemical cycling measurements



Fig. S10 SEM image of LCMGO after the two-step thermochemical H_2O splitting cycling test operated between 1300 and 900 °C.

Table S1 BET surface area of LaMnO3 based perovskites with various metal ions doped beforeand after two-step thermochemical H_2O splitting process.

Perovskite sample	BET surface area before thermochemical test (m^2/g)	BET surface area after thermochemical test (m ² /g)
$La_{0.6}Ba_{0.4}MnO_3$	10.4	7.9
$La_{0.6}Sr_{0.4}MnO_3$	11.5	9.4
$La_{0.6}Ca_{0.4}MnO_3$	14.2	11.5
$La_{0.6}Ca_{0.4}Mn_{0.8}Al_{0.2}O_{3}$	16.9	13.4
$La_{0.6}Ca_{0.4}Mn_{0.8}Ga_{0.2}O_3$	19.6	15.2

Redox Catalyst	Thermal	O ₂ evolution	H ₂ production	Re-	Ref.
	reduction	(µmol/g)	(µmol/g)	oxidation	
	temperature			yield (%)	
	(°C)				
$Ba_{0.5}Sr_{0.5}Co_{0.8}Fe_{0.2}O_{3}$	1000	600	83	7	3
$La_{0.6}Sr_{0.4}Cr_{0.8}Co_{0.2}O_{3}$	1200	154	50	16	4
$La_{0.5}Sr_{0.5}Co_{0.8}Fe_{0.2}O_{3}$	1200	503	90	9	3
$La_{0.6}Ca_{0.4}Mn_{0.8}Ga_{0.2}O_{3}\\$	1300	212	401	95	This
					study
LaSrCoO ₄	1300	268	161	30	3
$La_{0.6}Sr_{0.4}Mn_{0.4}Al_{0.6}O_{3}$	1350	120	220	92	5
$La_{0.5}Sr_{0.5}Mn_{0.95}Sc_{0.05}O_{3}$	1400	390	250	32	6
$La_{0.6}Sr_{0.4}MnO_3$	1400	219	397	91	7
$La_{0.5}Sr_{0.5}MnO_3$	1400	298	195	33	3
$La_{0.6}Ca_{0.4}MnO_3$	1400	272	407	75	8
Y _{0.5} Sr _{0.5} MnO ₃	1400	481	320	33	9
Y _{0.5} Ca _{0.5} MnO ₃	1400	593	310	26	9
CeO ₂	1400	66	144	109	10
CeO ₂	1640	111	178	80	11

Table S2 Comparison of thermochemical performances of the present study with those reportedby other perovskite type catalyst and benchmark CeO_2 in the literature.

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