

Design of CO₂ Sorbents using Functionalized Fibrous Nanosilica (KCC-1): Insights into the Effect of the Silica Morphology (KCC-1 vs MCM-41)

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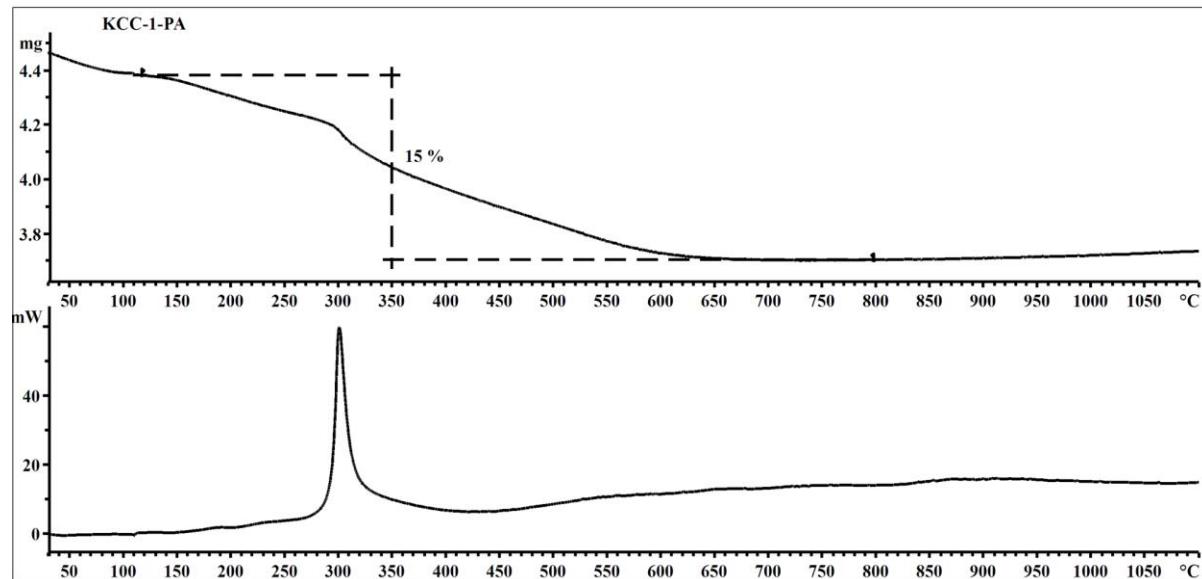


Figure S1. TGA-DTA profile of KCC-1-PA.

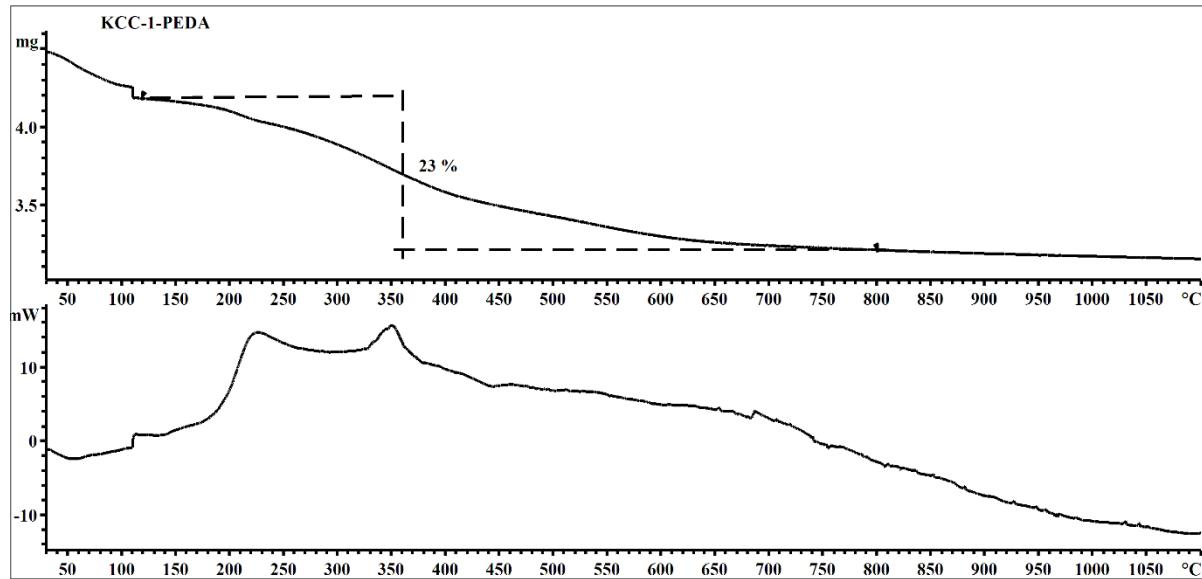


Figure S2. TGA-DTA profile of KCC-1-PEDA.

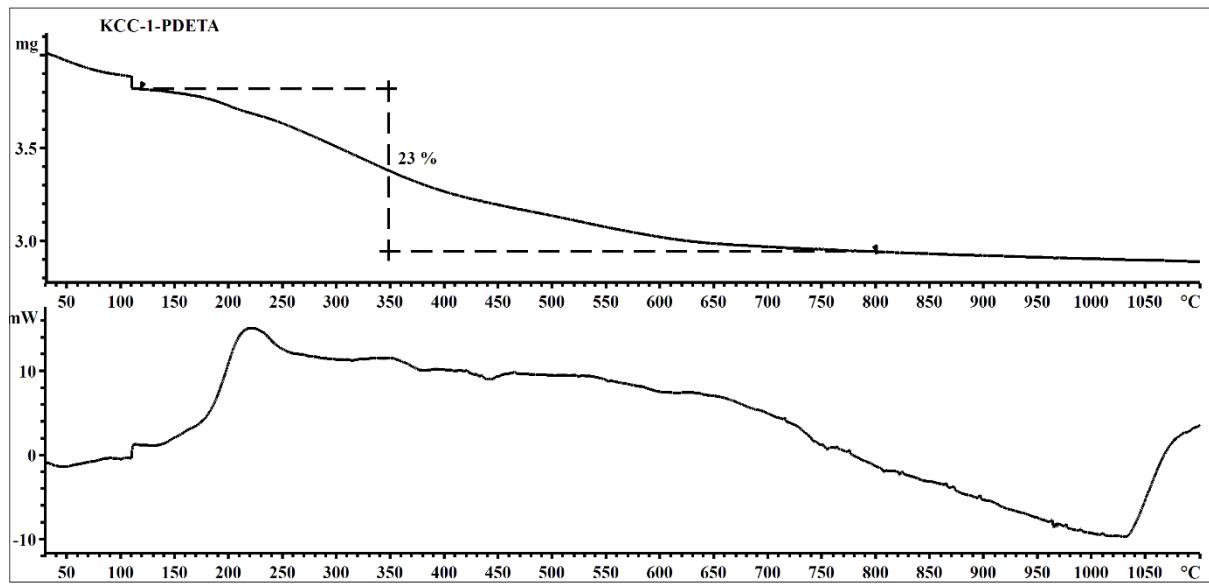


Figure S3. TGA-DTA profile of KCC-1-PDETA.

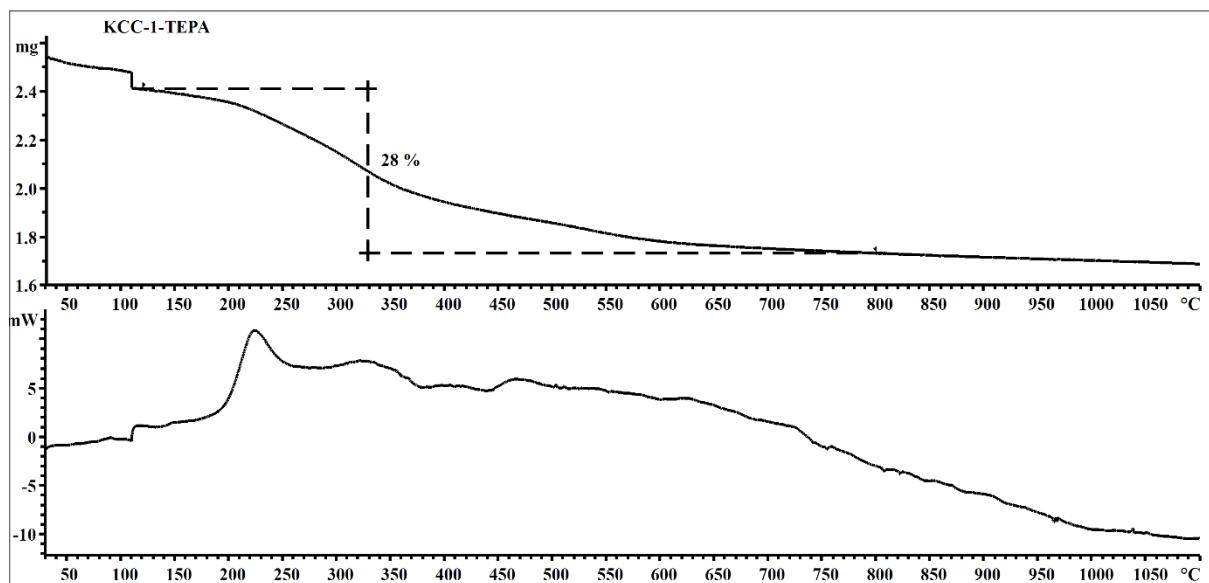


Figure S4. TGA-DTA profile of KCC-1-TEPA.

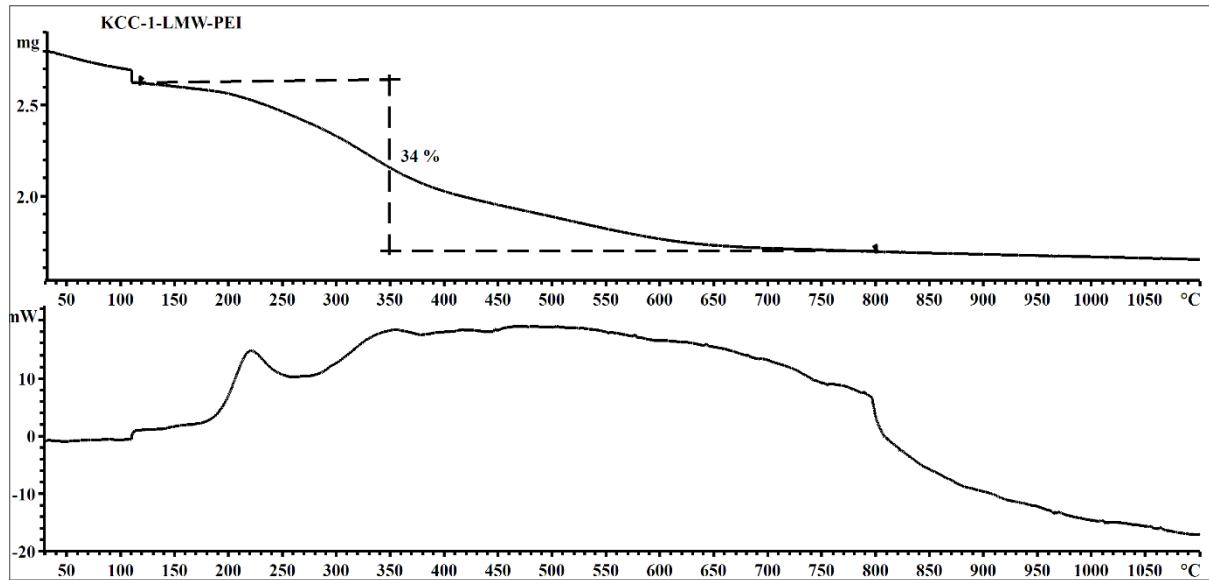


Figure S5. TGA-DTA profile of KCC-1-PEI-LMW.

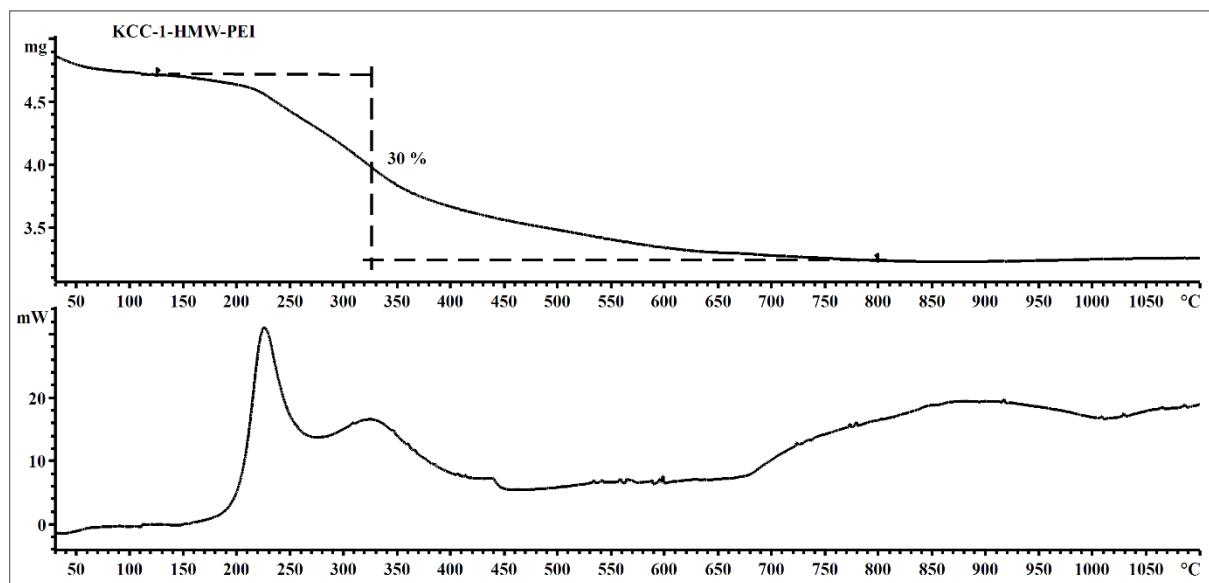


Figure S6. TGA-DTA profile of KCC-1-PEI-HMW.

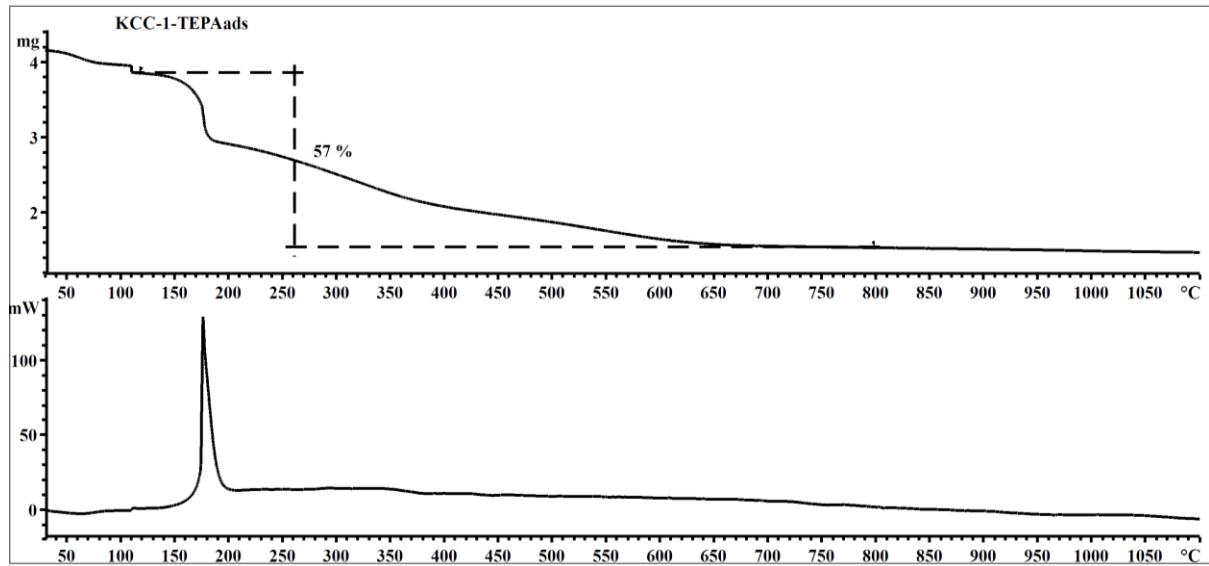


Figure S7. TGA-DTA profile of KCC-1-TEPA_{ads}.

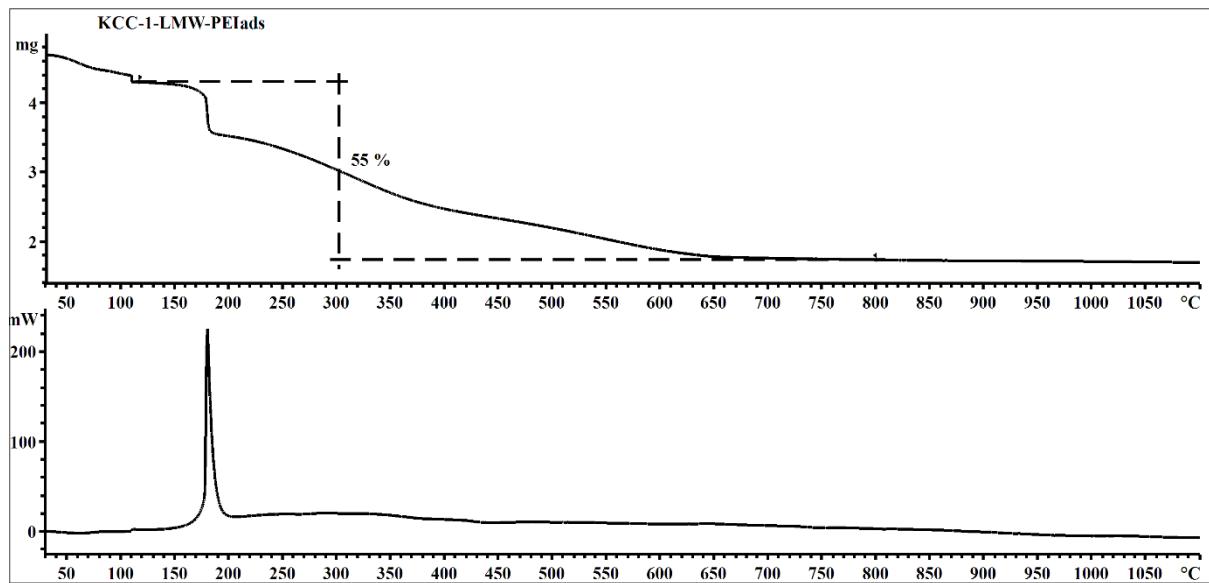


Figure S8. TGA-DTA profile of KCC-1-PEI-LMW_{ads}.

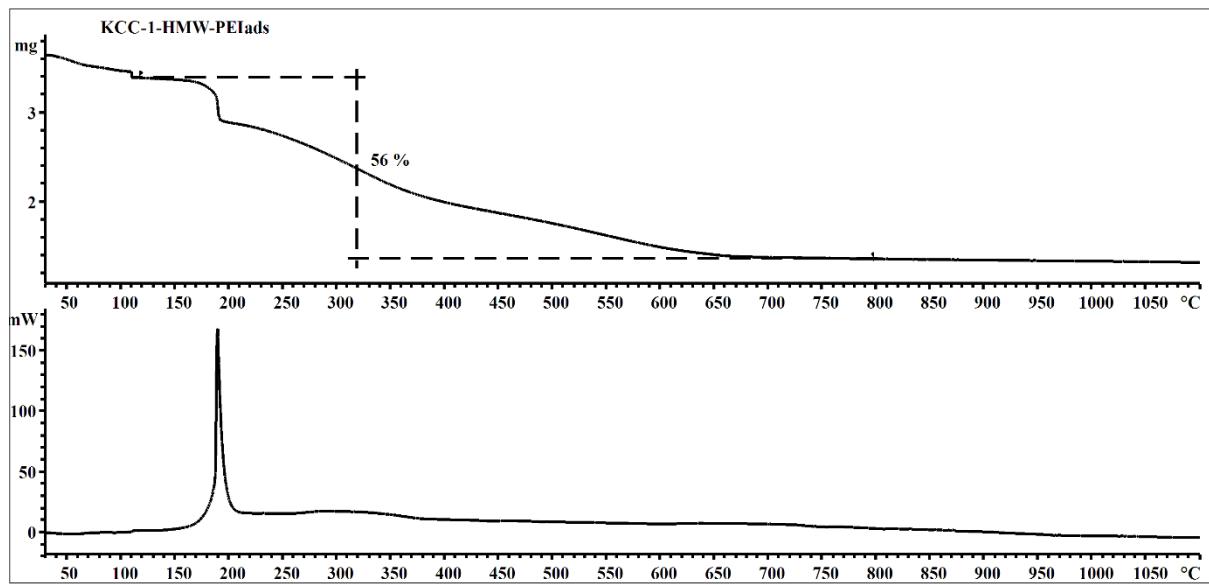


Figure S9. TGA-DTA profile of KCC-1-PEI- HMW_{ads}.

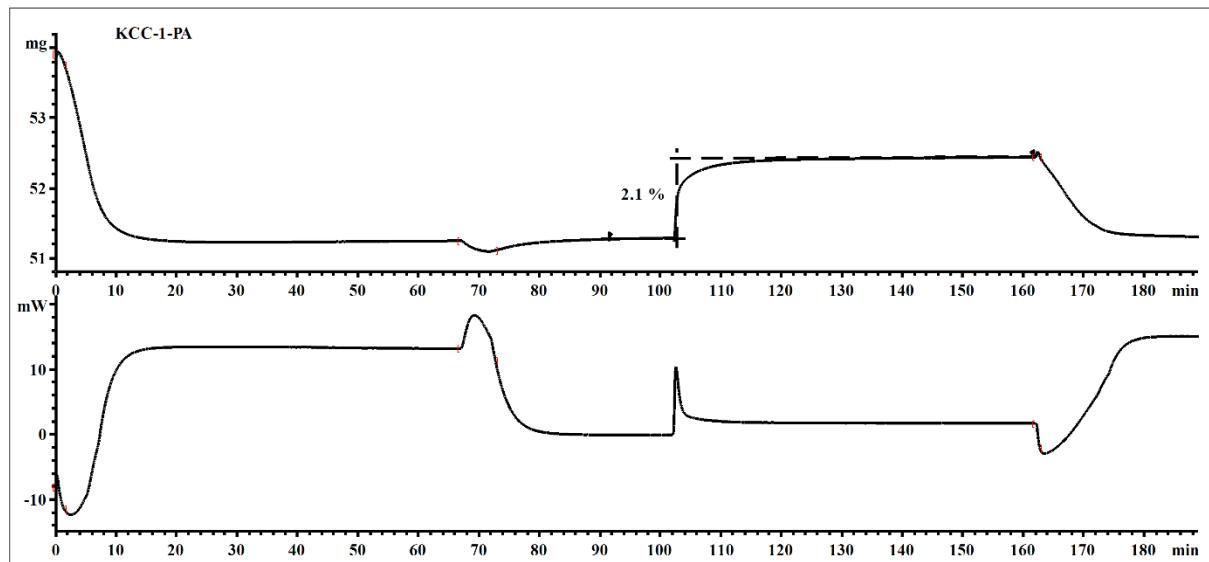


Figure S10. CO₂ adsorption/desorption by KCC-1-PA at 50 °C using 15% CO₂.

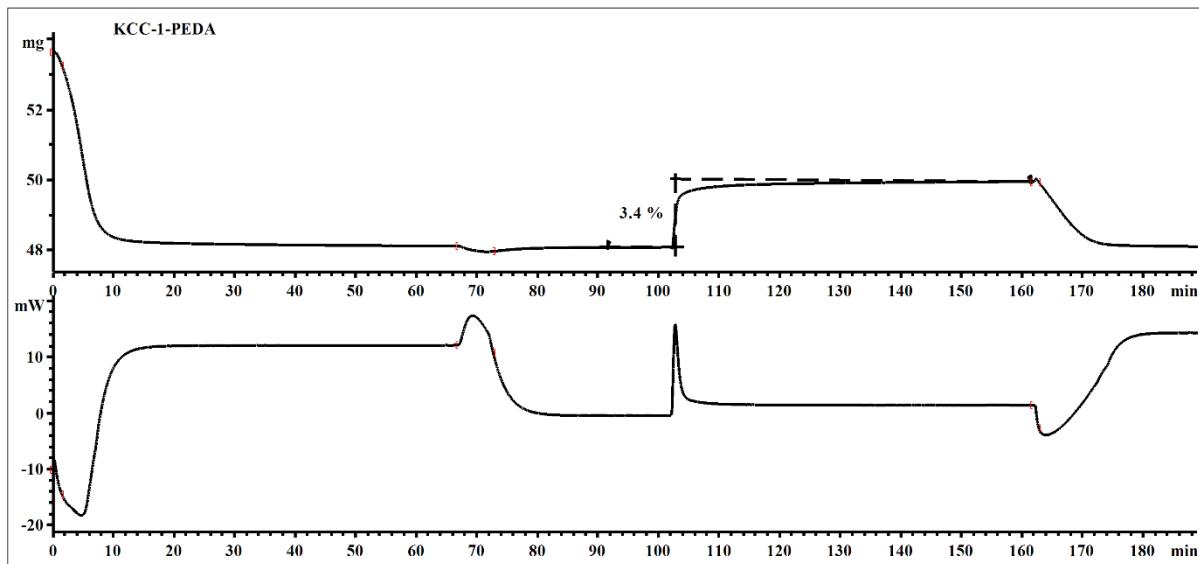


Figure S11. CO₂ adsorption/desorption by KCC-1-PEDA at 50 °C using 15% CO₂.

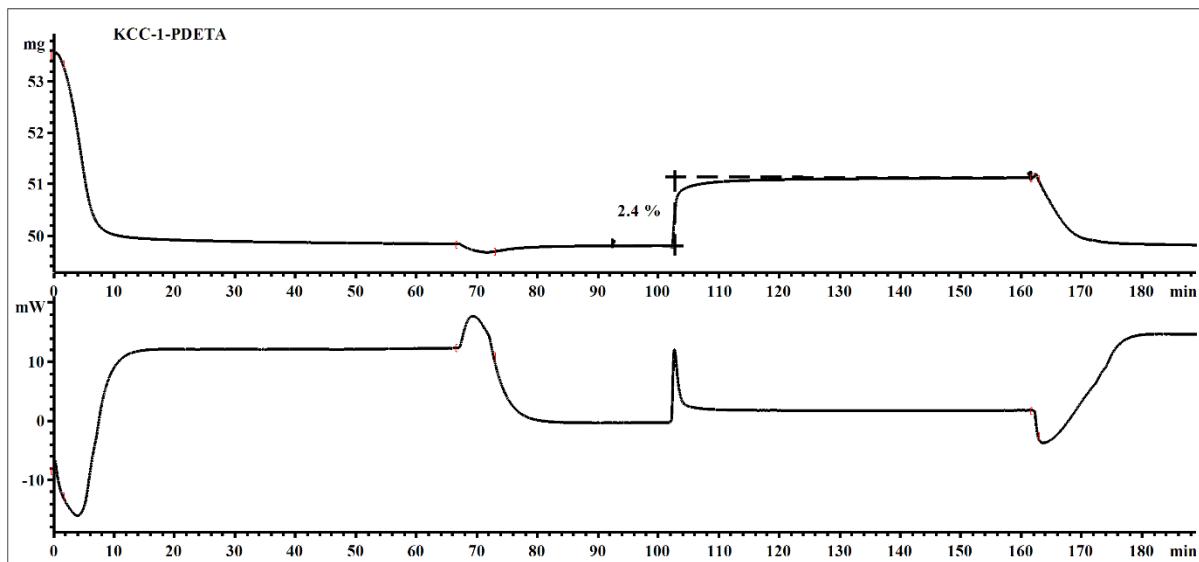


Figure S12. CO₂ adsorption by KCC-1-PDETA at 50 °C using 15% CO₂.

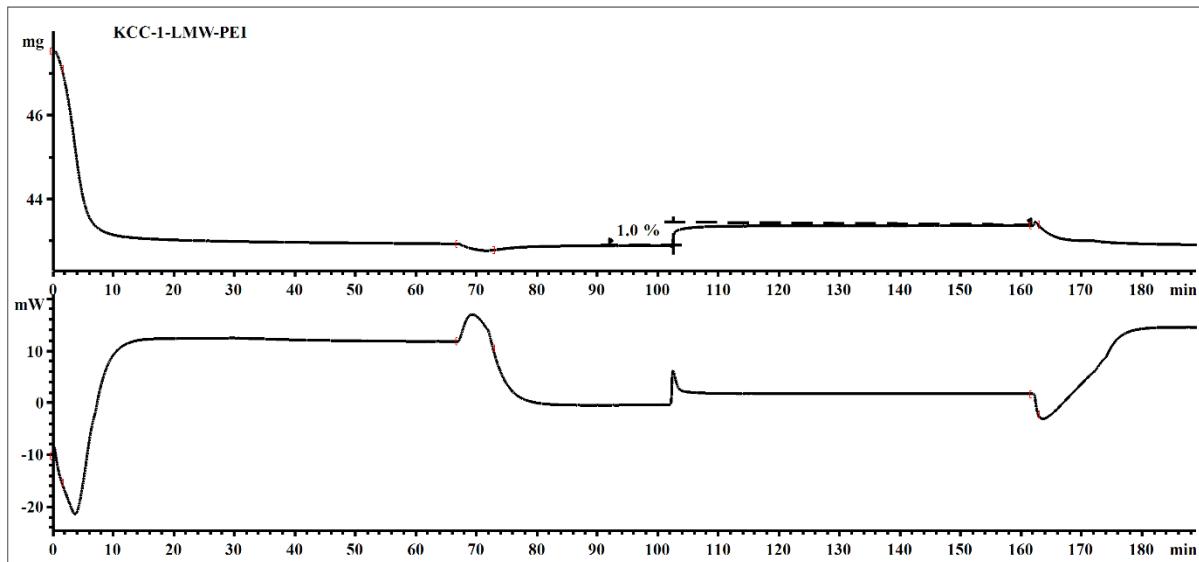


Figure S13. CO₂ adsorption by KCC-1-PEI-LMW at 50 °C using 15 % CO₂.

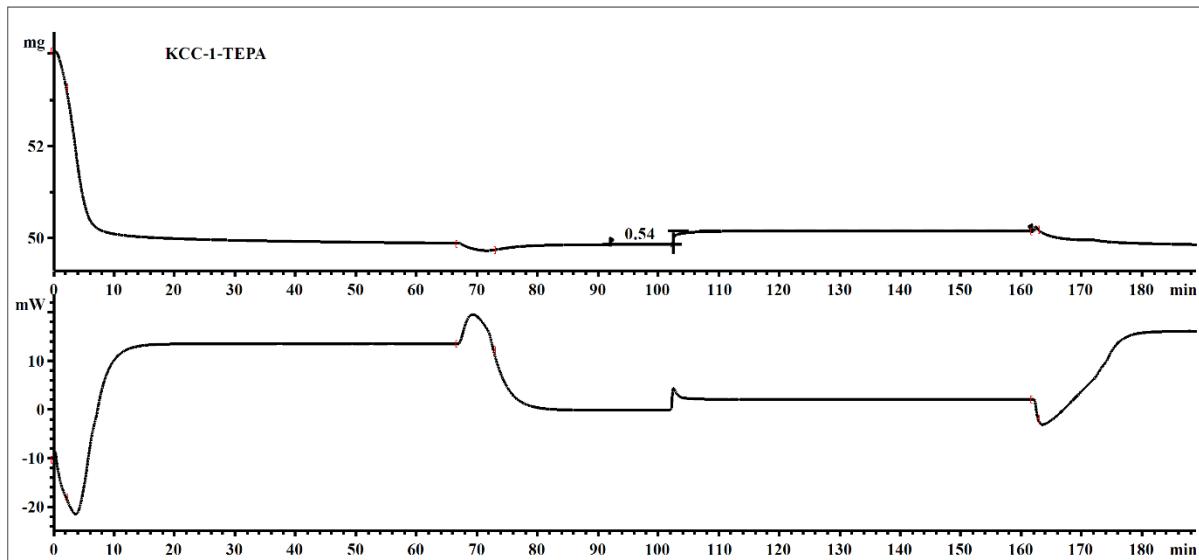


Figure S14. CO₂ adsorption by KCC-1-TEPA at 50 °C using 15 % CO₂.

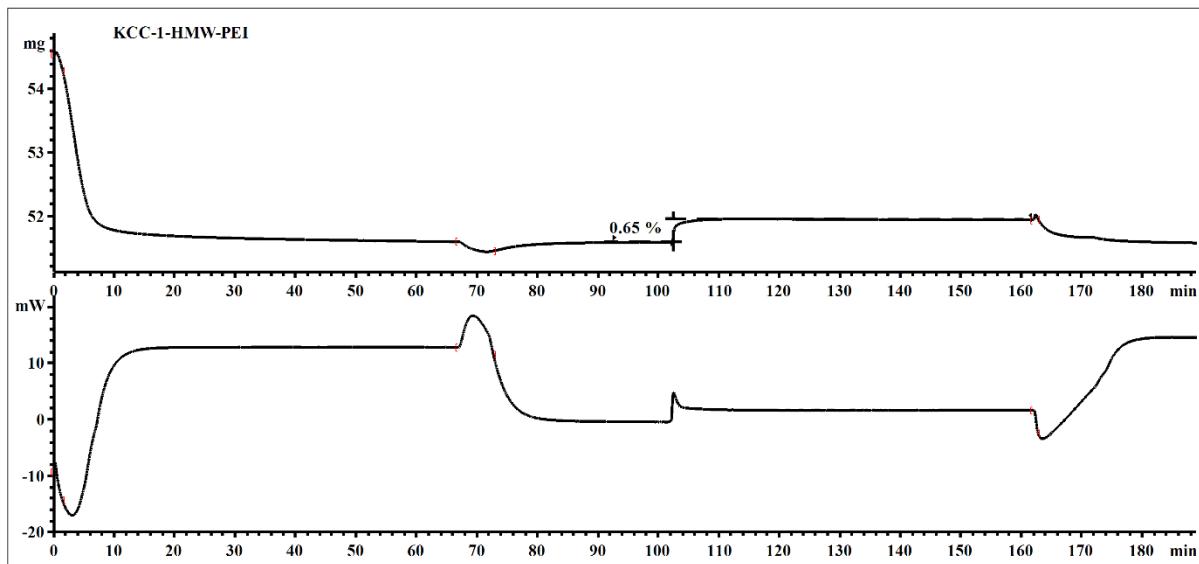


Figure S15. CO₂ adsorption by KCC-1-PEI-HMW at 50 °C using 15 % CO₂.

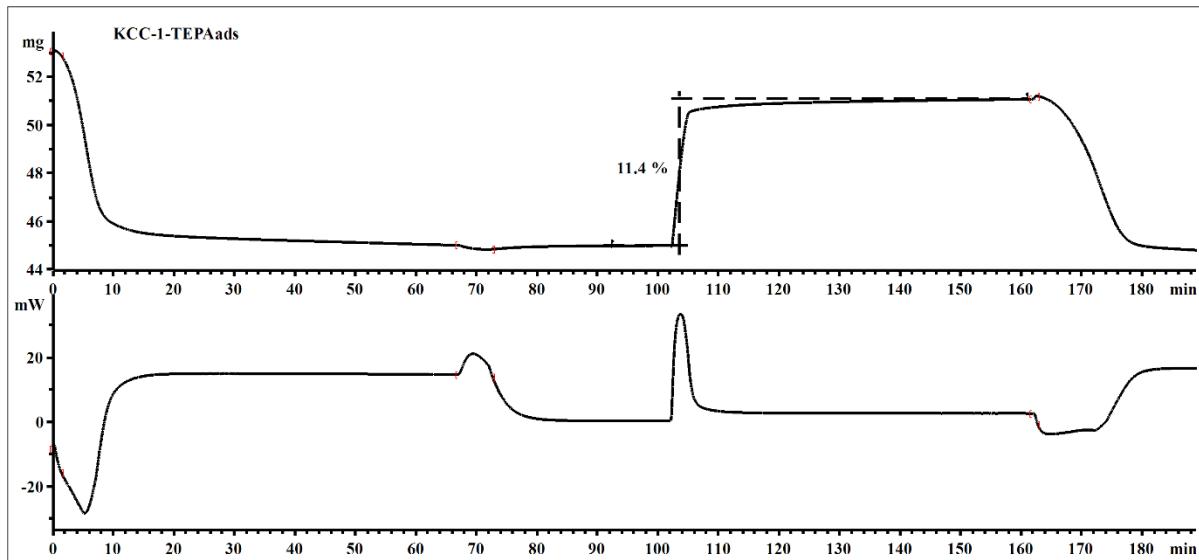


Figure S16. CO₂ adsorption by KCC-1-TEPA_{ads} at 50 °C using 15 % CO₂.

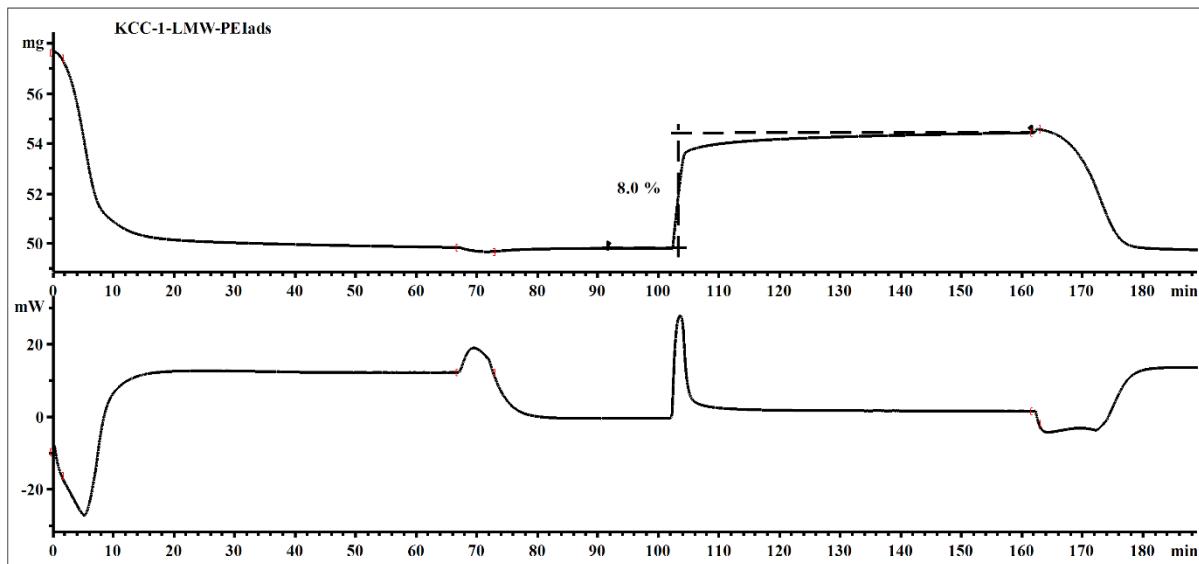


Figure S17. CO₂ adsorption by KCC-1-PEI--LMW_{ads} at 50 °C using 15 % CO₂.

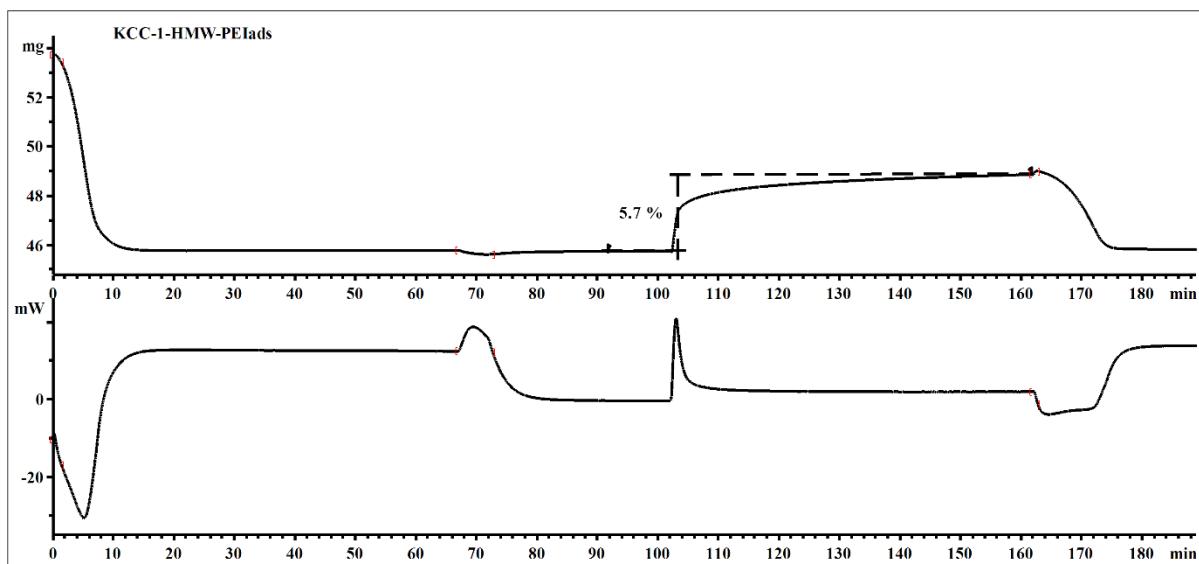


Figure S18. CO₂ adsorption by KCC-1-PEI-HMW_{ads} at 50 °C using 15 % CO₂.

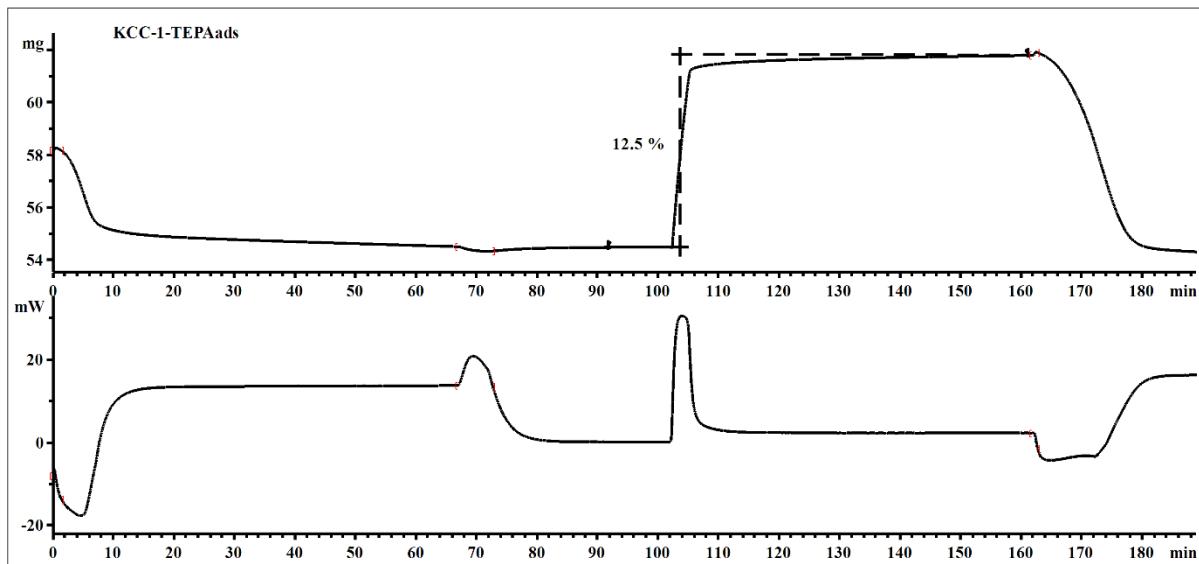


Figure S19. CO₂ adsorption by KCC-1-TEPA_{ads} (toluene as a solvent) at 50 °C using 15 % CO₂.

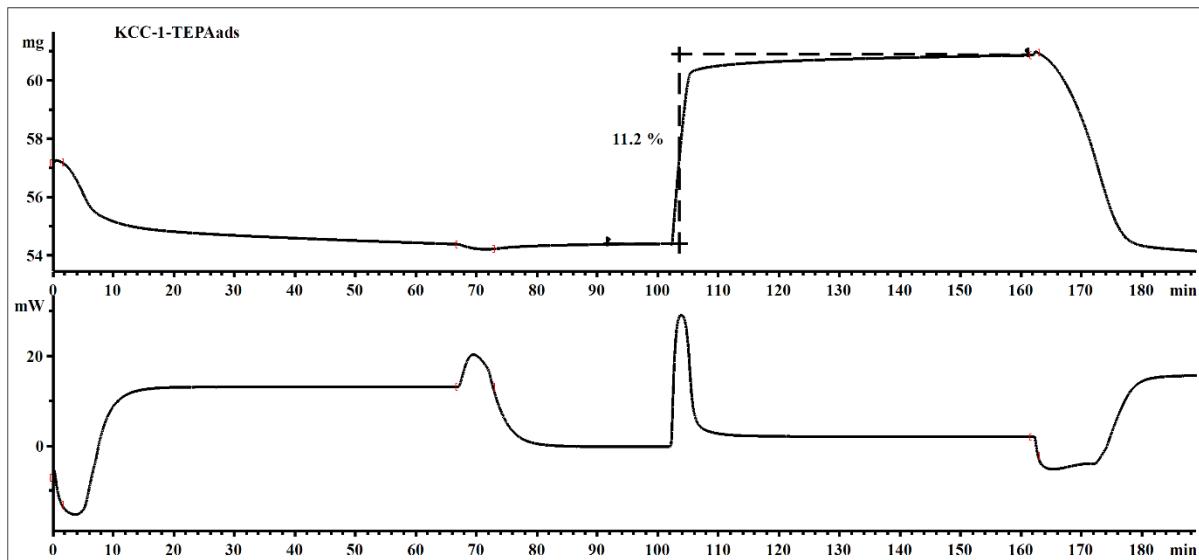


Figure S20. CO₂ adsorption by KCC-1-TEPA_{ads} (THF as a solvent) at 50 °C using 15 % CO₂.

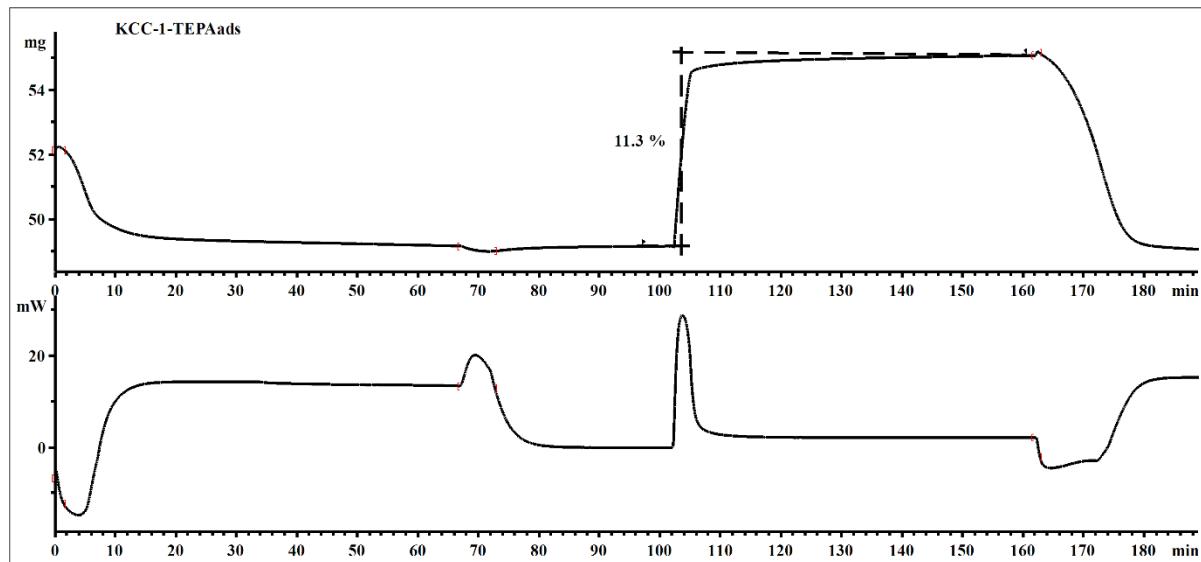


Figure S21. CO₂ adsorption by KCC-1-TEPA_{ads} (Methanol as a solvent) at 50 °C using 15 % CO₂.

Table S1. Synthesis of various TEPA loaded KCC-1 and MCM-41.

Types of support	Amount of support (mg)	TEPA used (mg)	Organic amine loading by TGA (wt. %)
KCC-1	500	1000	63.8
	500	850	61.0
	500	750	58.3
	500	350	44.4
	500	300	39.4
MCM-41	500	1000	67.3
	500	850	64.4
	500	750	57.6
	500	350	39.4
	500	300	36.6

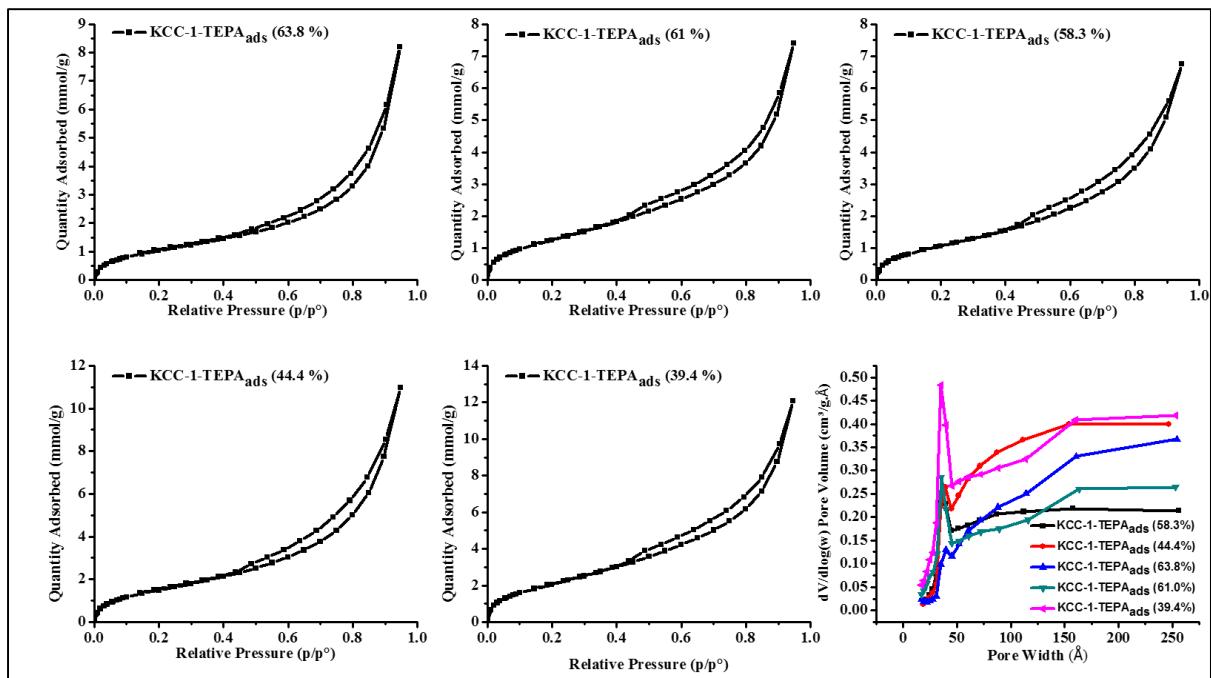


Figure S22. N₂ sorption isotherm of various KCC-1-TEPA_{ads}.

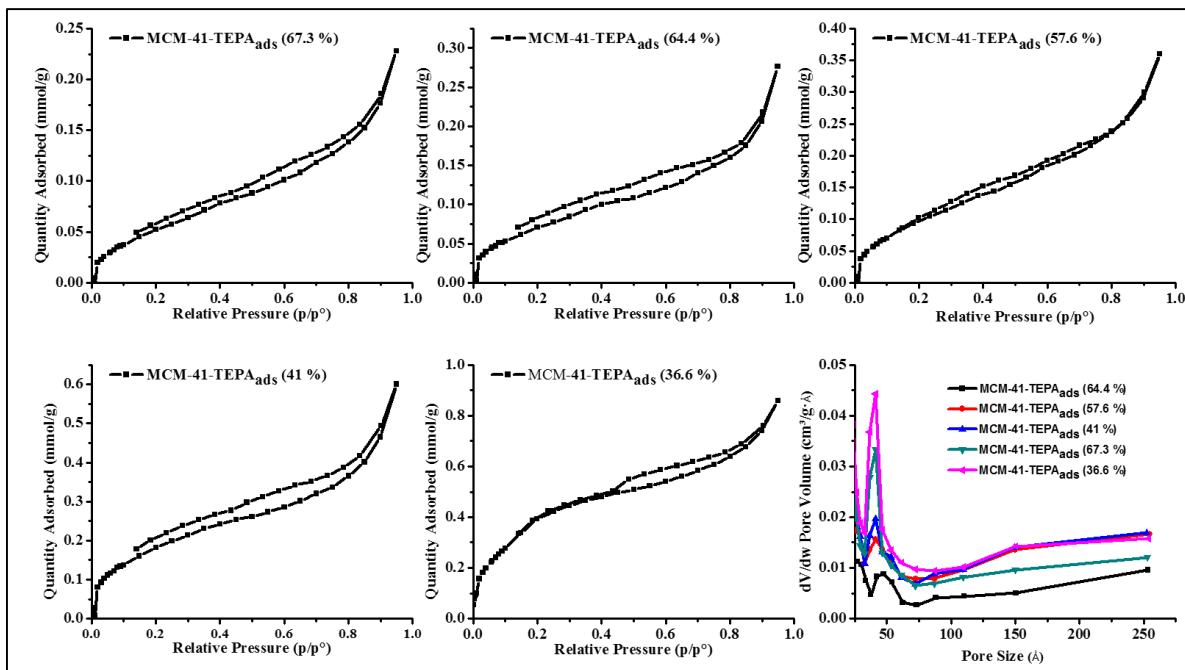


Figure S23. N₂ sorption isotherm of various MCM-41-TEPA_{ads}.

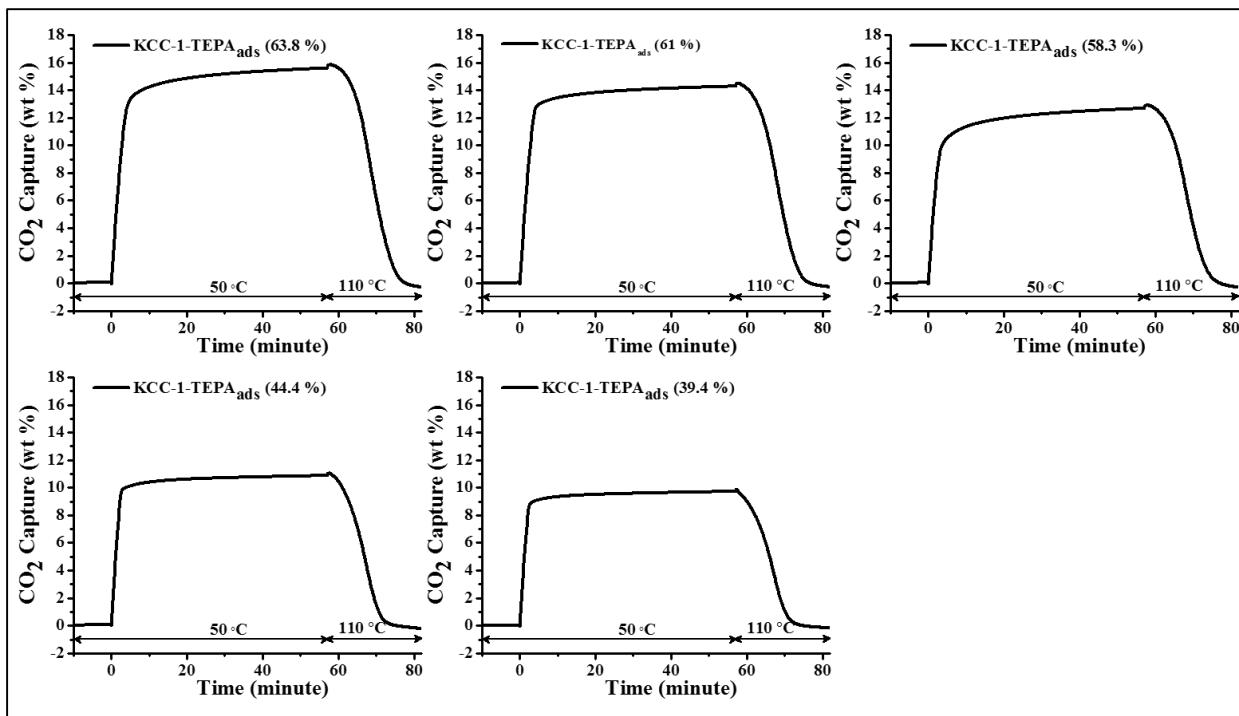


Figure S24. CO₂ adsorption by KCC-1-TEPA_{ads} at different loading (toluene as a solvent) at 50 °C using 15 % CO₂.

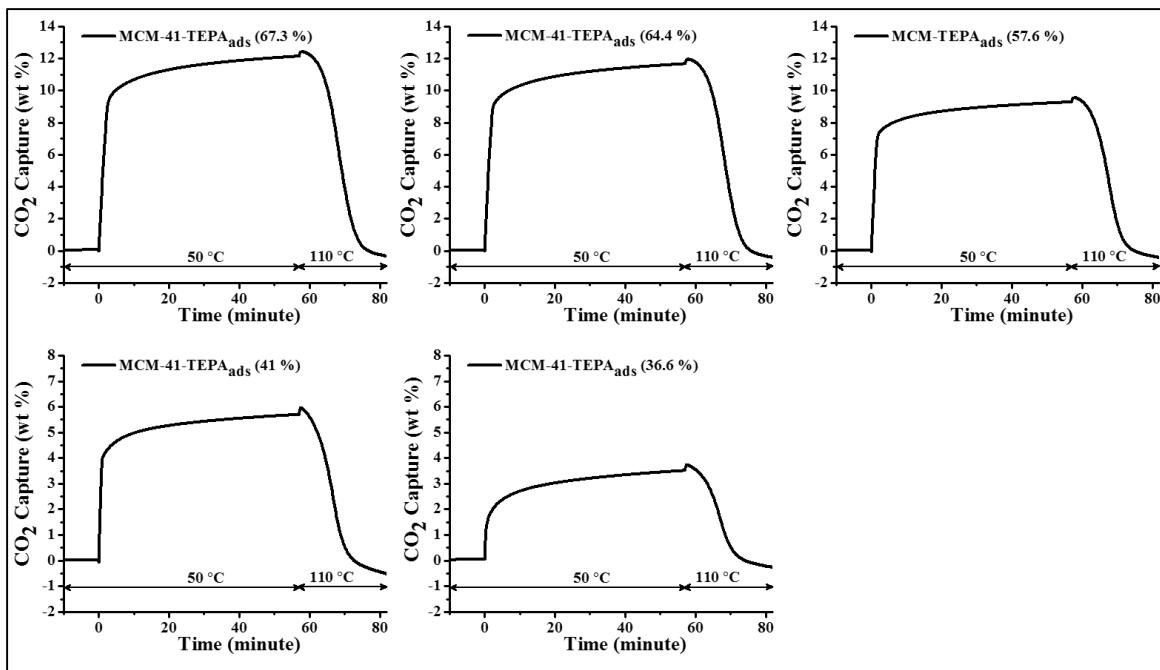


Figure S25. CO₂ adsorption by MCM-41-TEPA_{ads} at different loading (toluene as a solvent) at 50 °C using 15 % CO₂.

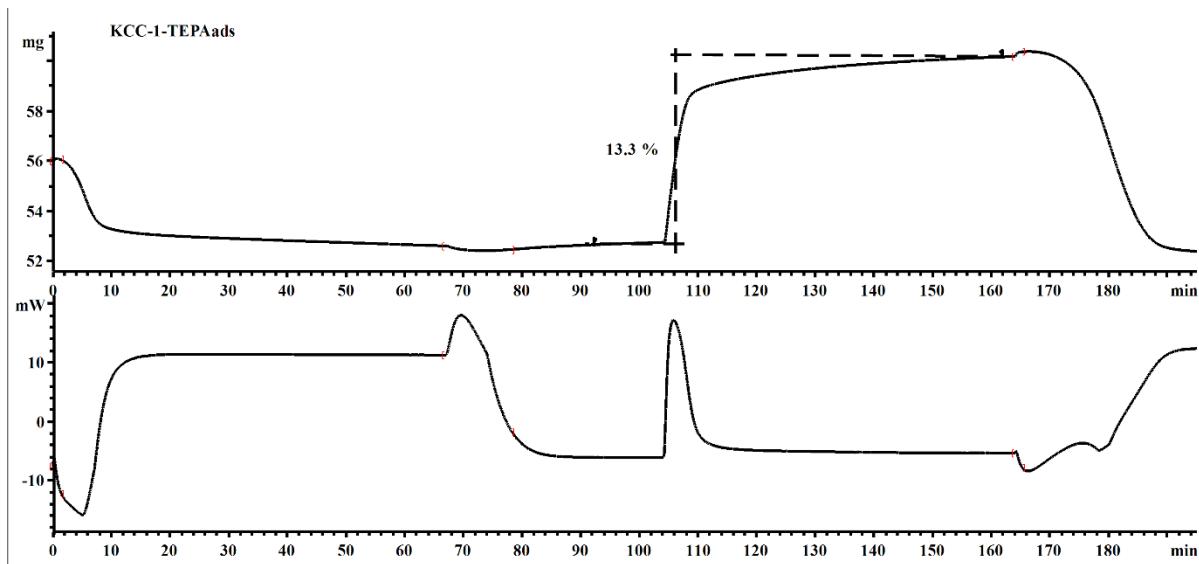


Figure S26. CO₂ adsorption by KCC-1-TEPA_{ads} (63.8 wt. %) at 30 °C using 15 % CO₂.

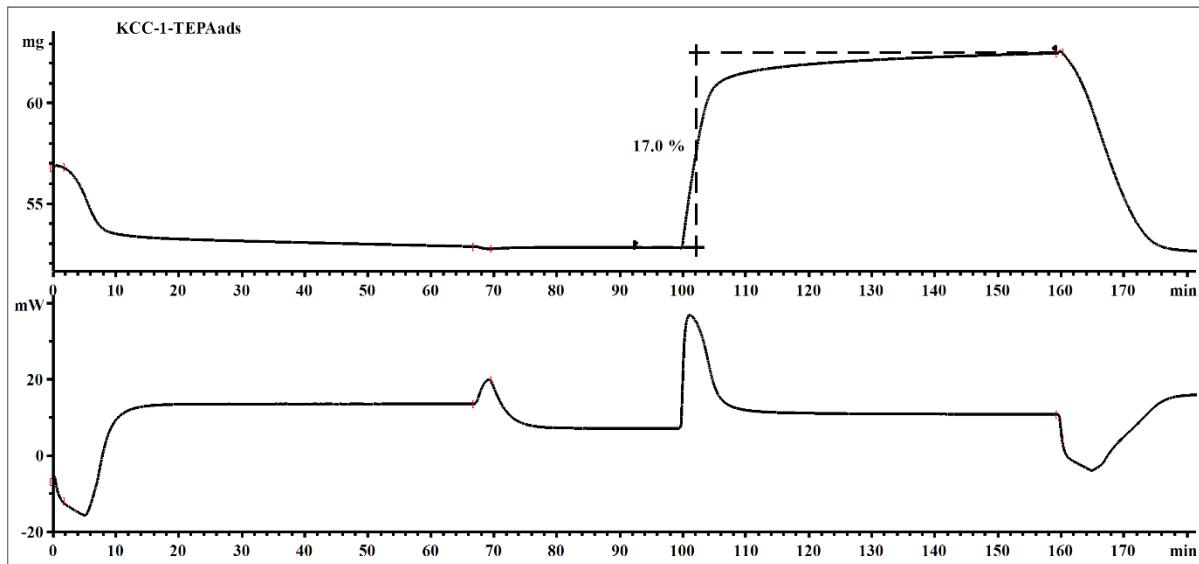


Figure S27. CO₂ adsorption by KCC-1-TEPA_{ads} (63.8 wt. %) at 75 °C using 15 % CO₂.

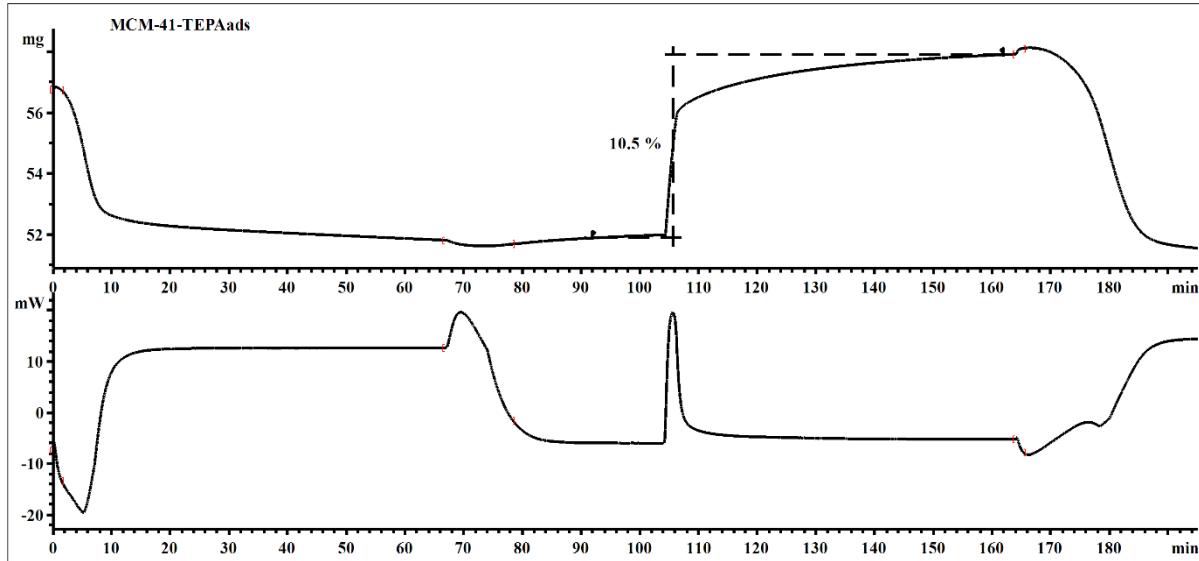


Figure S28. CO₂ adsorption by MCM-41-TEPA_{ads} (67.3 wt. %) at 30 °C using 15 % CO₂.

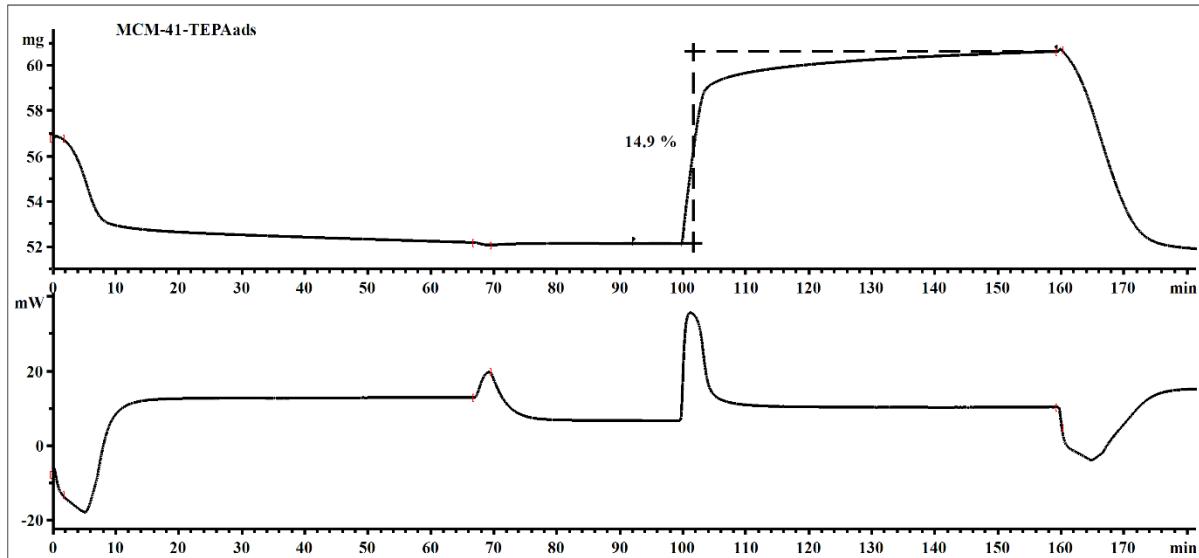


Figure S29. CO₂ adsorption by MCM-41-TEPA_{ads} (67.3 wt. %) at 75 °C using 15 % CO₂.

Table S2. CO₂ capture in each cycle for 21 cycles at 75 °C using 15 % CO₂.

No. of cycles	KCC-1-TEPA _{ads} (63.8 wt. %)		MCM-41-TEPA _{ads} (67.3 wt. %)	
	Under dry condition	Under humid Condition	Under dry condition	Under humid Condition
1	17.0	17.7	15.5	15.4
2	18.3	19.7	16.1	17.6
3	18	19.5	15.7	16.7
4	18.4	20.1	15.9	17.3

5	18.3	19.9	15.4	16.9
6	18.7	20.1	15.6	17
7	18.5	19.8	15.1	16.6
8	18.9	20.1	15	16.7
9	18.5	19.7	14.7	16.3
10	18.8	20	14.9	16.3
11	18.5	19.6	14.4	15.8
12	18.7	19.8	14.5	15.6
13	18.3	19.2	13.9	14.8
14	18.6	19.3	13.9	14.8
15	18.2	18.8	13.7	14.3
16	18.3	18.9	13.2	14.6
17	17.8	18.4	12.6	13.8
18	17.9	18.6	12.5	14
19	17.5	17.9	11.9	12.8
20	17.7	18.1	11.7	12.7
21	17.2	17.4	11.0	11.9
Total	383	402.65	297.2	321.9

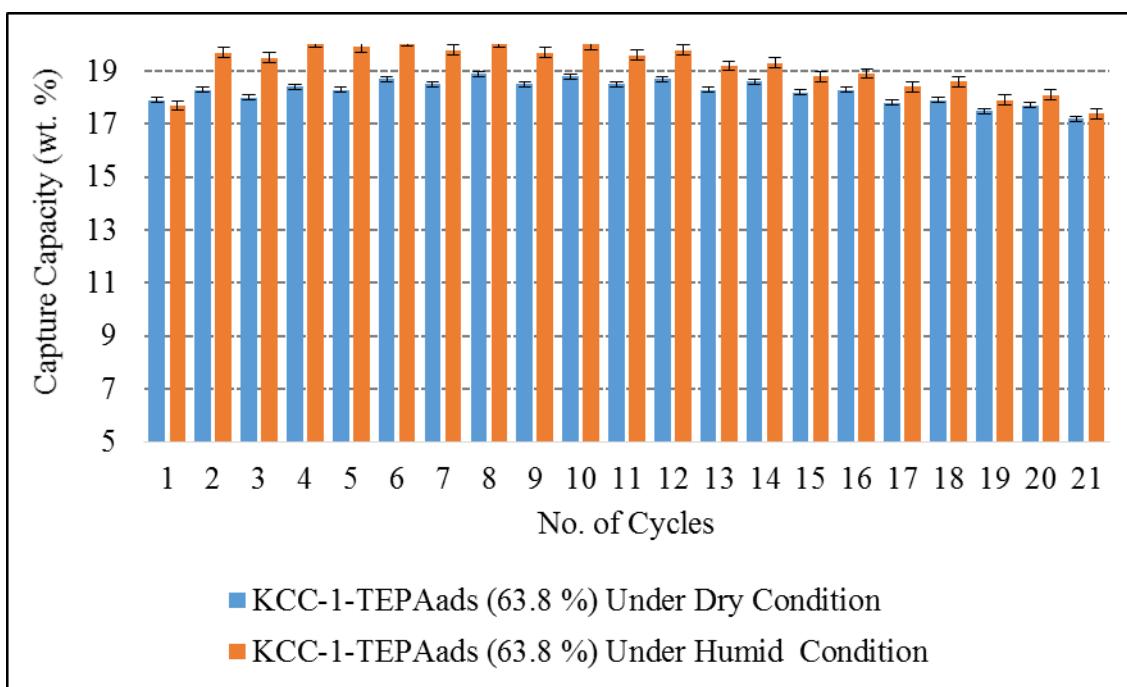


Figure S30. CO₂ adsorption recyclability study under dry and humid condition of KCC-1-TEPA_{ads} (63.8 wt. %) at 75 °C using 15 % CO₂.

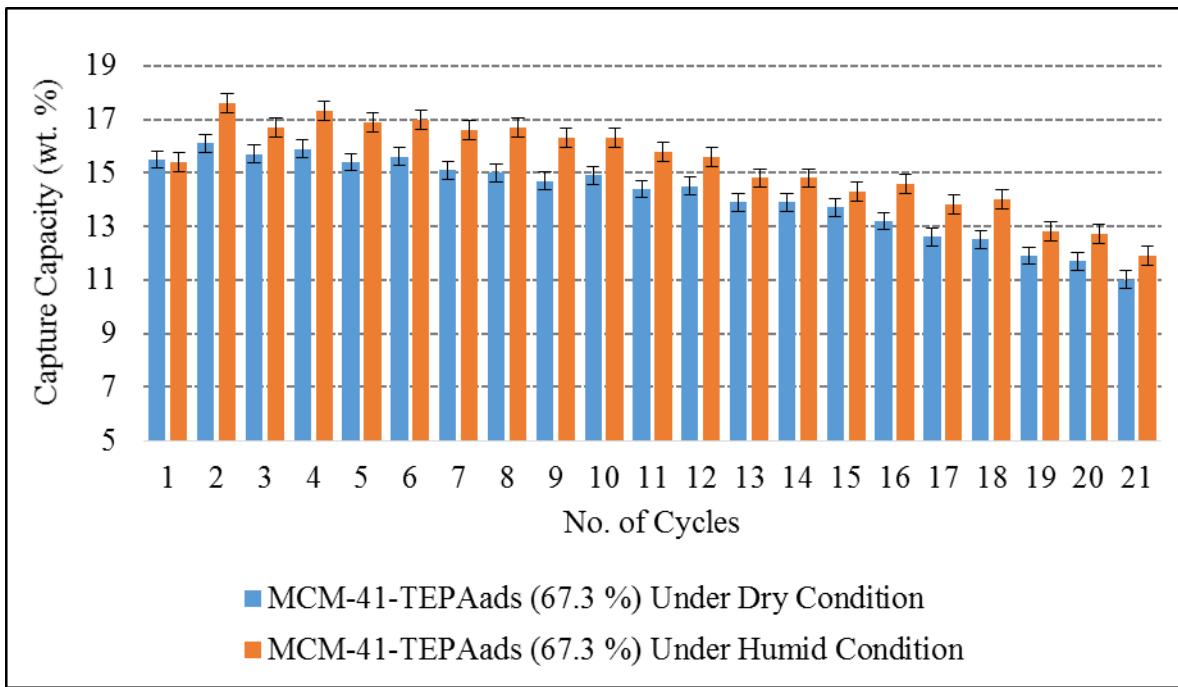


Figure S31. CO₂ adsorption recyclability study under dry and humid condition of MCM-41-TEPA_{ads} (67.3 wt. %) at 75 °C using 15 % CO₂.

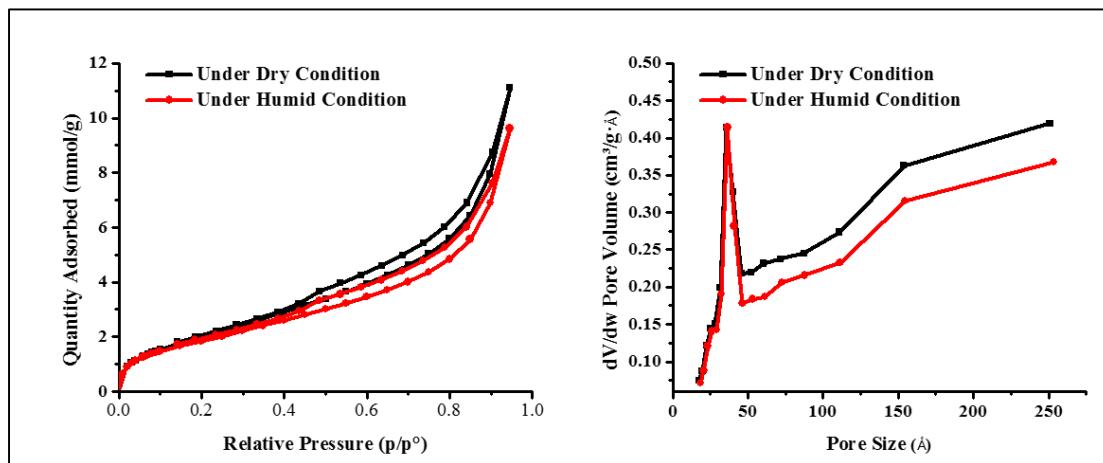


Figure S32. N₂ sorption isotherm and pore size distribution of recycled KCC-1-TEPA_{ads} (63.8 wt. %) after 21 cycles under dry and humid conditions.

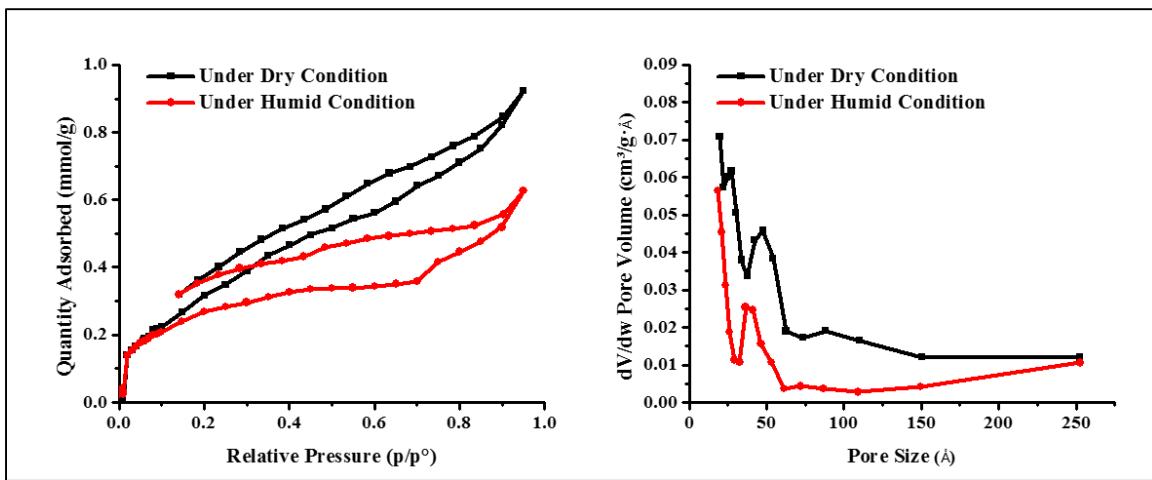


Figure S33. N₂ sorption isotherm and pore size distribution of recycled MCM-41-TEPA_{ads} (67.3 wt. %) after 21 cycles under dry and humid conditions.

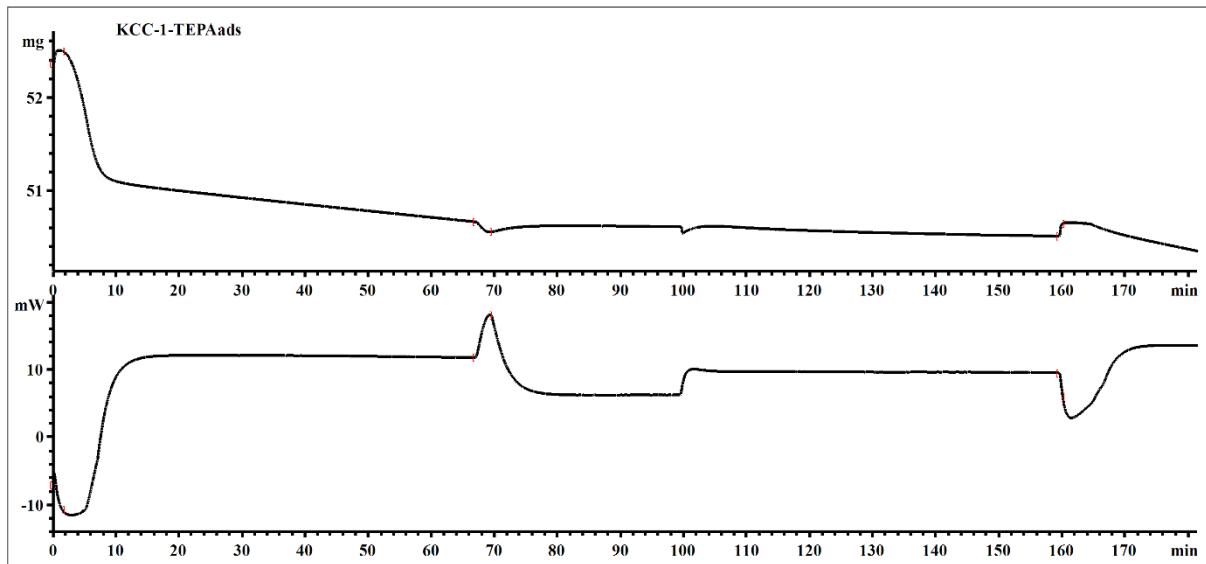


Figure S34. N₂ adsorption of KCC-1-TEPA_{ads} (63.8 wt. %) at 75 °C.

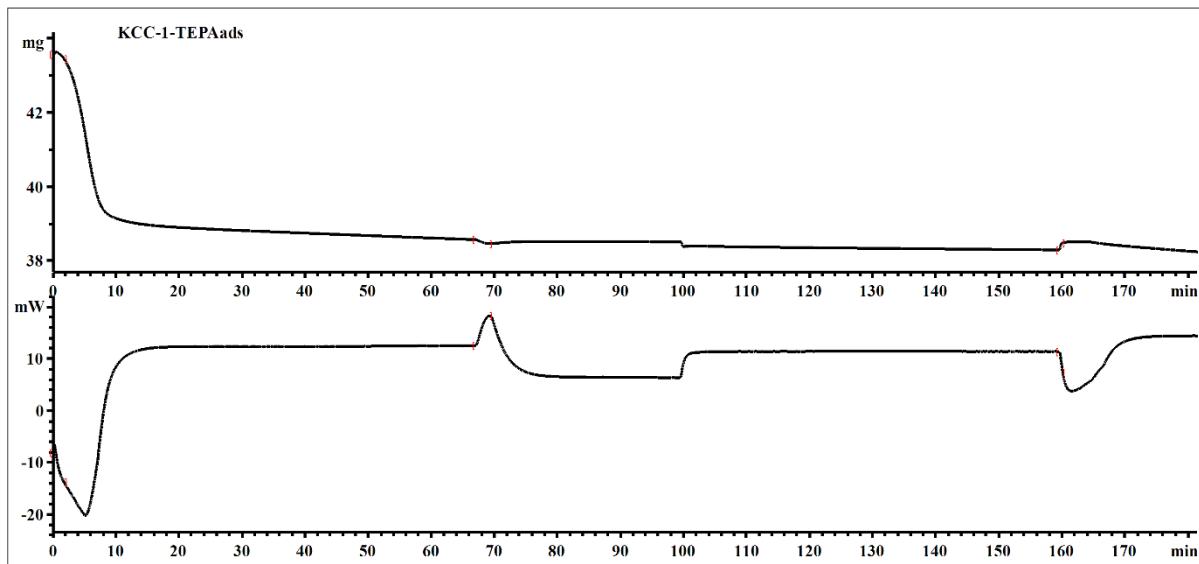


Figure S35. O₂ adsorption of KCC-1-TEPA_{ads} (63.8 wt. %) at 75 °C.

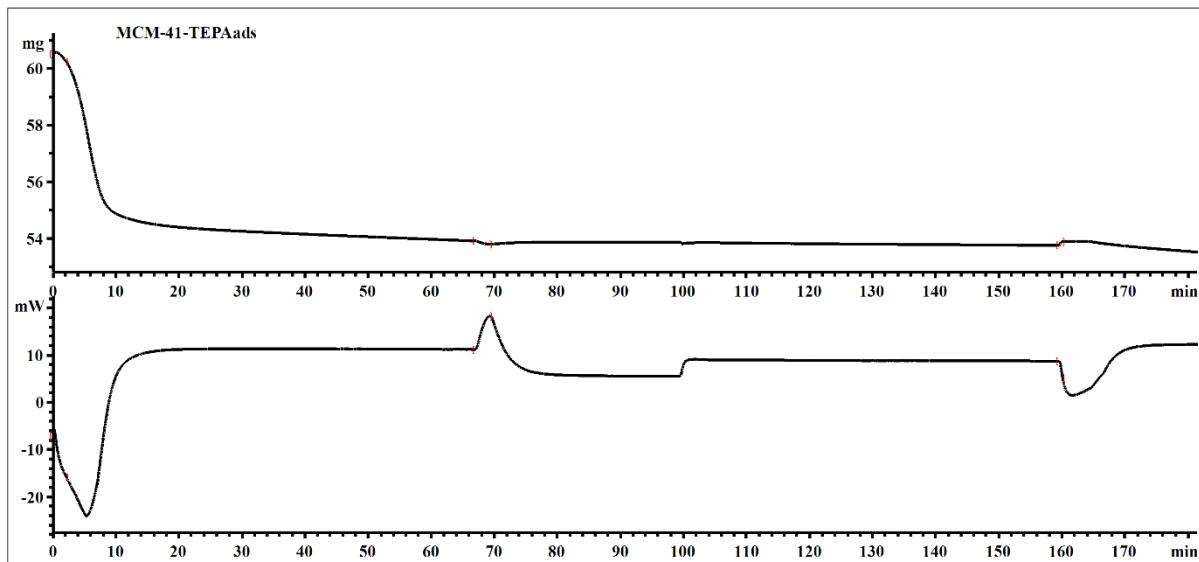


Figure S36. N₂ adsorption of MCM-41-TEPA_{ads} (67.3 wt. %) at 75 °C.

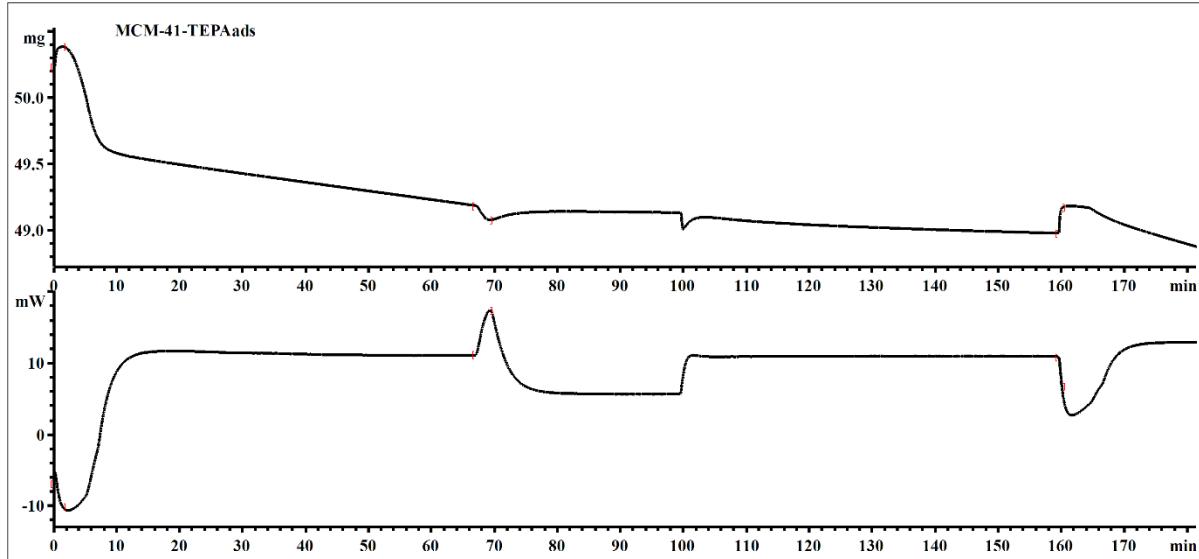


Figure S37. O₂ adsorption of MCM-41-TEPAads (67.3 wt. %) at 75 °C.

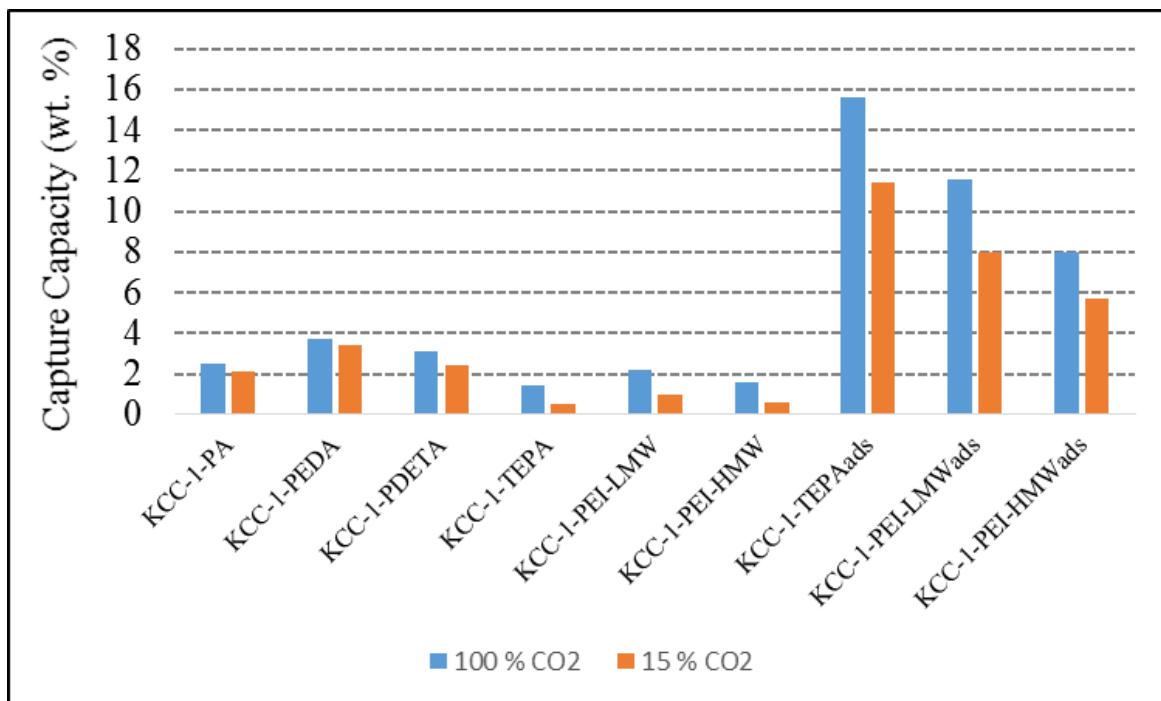


Figure S38. CO₂ adsorption comparison of different KCC-1 sorbent using 15 % CO₂ and 100 % CO₂ at 50 °C