Supporting Information for

Electrocatalytic CO₂ reduction by a cobalt bis(pyridylmonoimine) complex: effect of acid concentration on catalyst activity and stability

Weixuan Nie and Charles C. L. McCrory*

Contents:

Experimental Information	S 3
Figure S1. ¹ H -NMR spectrum of L-L	S 8
Figure S2. ¹ H-NMR Spectrum of [Co(L-L)Br ₂]Br	S 8
Table S1. Crystal data and structure refinement for [Co(L-L)Br2]Br	S 9
Table S2. Related bond lengths and bond angles of [Co(L-L)Br2]Br	S10
Figure S3. IR Spectrum of [Co(L-L)Br ₂] and [Co(L-L)Br ₂]Br	S11
Figure S4. UV-vis spectrum of 0.1 mM [Co(L-L)Br2] and [Co(L-L)Br2]Br	S 11
in MeCN in air	
Figure S5. UV-vis spectrum of 0.1 mM [Co(L-L)Br ₂] in MeCN in air and	S12
under CO ₂	
Figure S6. UV-vis spectrum of 0.1 mM [Co(L-L)Br2] in MeCN in air and	S12
with 11 M H ₂ O in air	
Figure S7. UV-vis spectrum of 0.1 mM (black curve) and 0.3 mM (red curve)	S13
[Co(L-L)Br ₂] in MeCN in air.	
Paramagnetic Susceptibility Measurements (Evans Method)	S13
Figure S9. CVs of 0.3 mM [Co(L-L)Br ₂] with increasing H ₂ O concentration	S16
Figure S10. CVs of 0.3 mM [Co(L-L)Br ₂] with increasing TFE concentration	S17
Figure S11. CVs of 0.3 mM [Co(L)Br2] under N2 and CO2 with TFE.	S18
Figure S12. CVs of 0.3 mM [Co(L-L)Br ₂] under N ₂ and CO ₂ with different	S18
H ₂ O concentrations	
Figure S13. CVs of 0.3 mM [$Co(L-L)Br_2$ under N_2 and CO_2 with different	S19
TFE concentrations	
Figure S14. The Controlled-Potential Electrolysis cell setup	S19
Table S5. Conditions and Product Analysis of the Controlled Potential	S20
Electrolysis for CO ₂ reduction with 0.3 mM Co(L-L)Br ₂	
Table S6. Conditions and Product Analysis of the CPE control groups for CO2	S20
reduction	
Table S7. Conditions and Product Analysis of the CPE control groups for CO2	S21
reduction at different potentials.	

ICP-MS tests	S22
Figure S15-S22 SEM-EDS analysis of a representative working electrode	S24
surface in a series of electrolysis	
Turnover Frequency (TOF) calculations	S28
Long-time CPE experiments	S 33
Table S11. Summary of Co-complex catalysts for electrochemical CO ₂ RR	S38
References	S43

Experimental Information

Materials

Ultrapure water (18.2 M Ω cm resistivity) was purified with a Thermo Scientific Barnstead Nanopure water purification system. Nitrogen (N₂) was boil-off gas from a liquid nitrogen source. Carbon dioxide (CO₂, medical grade, >99.0%) was purchased from Cryogenic gases. Tetrabutylammonium hexaflurophosphate (*n*Bu₄NPF₆, >98.0%) was purchased from TCI America and recrystallized from Methonal/H₂O (v/v = 8/1). 2,2,2-trifluoroethanol (TFE, ReagentPlus grade, ≥99.0%) was purchased from Sigma Aldrich. Acetonitrile (MeCN, HPLC plus, ≥99.9%) was purchased from Sigma Aldrich and used without additional purification. The typical water concentration in MeCN as received has been previously measured to be [H₂O] ≈ 0.040 M.^[S1] Nitric acid (HNO₃, 67-70% w/w, TraceMetal Grade with <1 ppb metal concentration) was purchased from Fisher Scientific. All other chemicals were purchased from commercial sources, and all chemicals were used as received unless otherwise noted.

General Methods

NMR spectra were recorded on Varian MR400 (400 MHz) spectrometers, and chemical shifts are reported in ppm relative to TMS standards. Elemental analyses were performed by Midwest Microlab, Inc. Gas chromatography measurements were conducted on a custom-designed 2-channel Thermo Scientific Trace 1310 gas chromatograph with dual TCD detectors. HPLC measurements were collected using a Thermo Scientific Dionex Ultimate 3000 series HPLC. Electrochemical experiments were conducted using a Bio-Logic/Science Instruments SP-200 potentiostat using the EC-Lab V10.44 software package. UV-Vis spectra were collected with Perkin Elmer PDA UV-Vis Lambda 265 equipment. IR spectra were collected with Thermo Scientific NICOLET iS50 FT-IR. ICP-MS data were collected using PerkinElmer NexION 2000. X-ray diffraction data was collected on a CrystalClear-SM Expert 2.0 r16 (Rigaku, 2014) with a Rigaku Saturn944+ CCD detector using Cu Kα (wavelength

is 1.54 Å). The structure was solved by direct methods and refined on F2 full-matrix least-squares using SHELXL-2013 (Sheldrick, 2013).^[S2]

Synthesis

Preparation of Ligand L-L. The Ligand L-L was synthesized according to literature methods.^[S3] A solution of 2-acetylpyridine (1.00 g, 8.04 mmol) in 20 mL *i*-PrOH was added into a solution of ethylenediamine (0.24 g, 4.00 mmol) in 20 mL *i*-PrOH. The mixture was stirred at room temperature for 24 hours. After removing the solvent, the yellow oil residue was put into a -4 °C refrigerator to get a semi-solid crude product. The crude ligand was re-crystallized from 5 mL hexane to give white needles which were dried in vacuum overnight (0.70 g, 65% yield). ¹H NMR (CD₃Cl-*d*₃, 400 MHz, Fig S1): δ 8.59 (2H, d, *Ar*-H), δ 8.07 (2H, d, *Ar*-H), δ 7.69 (2H, m, *Ar*-H), δ 7.28 (2H, m, *Ar*-H), δ 3.98 (4H, s, CH₂), δ 2.44 (6H, s, CH₃).

Preparation of [*Co*(*L*-*L*)*Br*₂]. A 5 mL THF solution of CoBr₂ (87.50 mg, 0.40 mmol) was added into a 3 mL THF solution of ligand L-L (106.50 mg, 0.40 mmol) with a 1:1 metal salt : ligand molar ratio. The mixture was stirred at room temperature for 24 hours. The dark purple precipitate was collected by filtration and then washed with THF and ether three times. The product was obtained after drying in vacuum overnight (183.40 mg, 95% yield). Anal. Calcd (found) for [Co(L-L)Br₂], (C₁₆H₁₈N₄CoBr₂): %C 39.62, (38.92); %H 3.74, (3.80); %N 11.55, (11.22).

Preparation of [Co(L-L)Br₂]Br. Aerobic oxidation of in situ prepared [Co(L-L)Br₂] in the presence of 1 equiv HBr(aq) in ethanol overnight (18 hours) resulted a green solid (179.78 mg, 80% yield). Recrystallization was accomplished by diffusion of Et₂O into a MeOH solution of the green solid. Dark green crystals were obtained after a few days and kept in dark to avoid photochemical degradation. ¹H NMR (Trifluoroacetic acid d_1 , 400 MHz): δ 9.44 (2H, d, *Ar*-H), δ 8.28 (2H, t, *Ar*-H), δ 8.14 (2H, d, *Ar*-H), δ 7.94 (2H, t, *Ar*-H), δ 4.81 (4H, s, CH₂), δ 2.92 (6H, s, CH₃). Anal. Calcd (found) for [Co(L-L)Br₂]Br (C16H18N4CoBr3): %C 34.01, (34.07); %H 3.21, (3.30); %N 9.92, (9.89).

Electrochemical Methods and Product Analysis

Cyclic Voltammetry. The working electrode was a 0.071 cm^2 glassy carbon disk electrode (CH instruments), and the counter electrode was carbon rod (99.999% Strem). The reference electrode was a Ag/AgNO₃ (1.0 mM)/MeCN nonaqueous reference electrode (also containing 0.1 M nBu₄NPF₆), separated from the solution by a Vycor frit (Bioanalytical Systems, Inc.) and externally referenced to ferrocene. The scan rate was 50 mV/s. Prior to each set of measurements, the uncompensated solution resistance (R_u) in the cell was measured using a single-point impedance measurement at 100 kH_z with a 20 mV amplitude about the open-circuit potential. Cyclic voltammograms were automatically corrected for IR drop at 85% through positive feedback using the Bio-Logic ECLab software.

Controlled-Potential The *Electrolysis.* controlled-potential electrolysis experiments were conducted in a two-chamber H-cell shown in Fig S8. The left chamber held the working and reference electrodes and was filled with 20 mL of 0.3 mM catalyst solution in MeCN with 0.1 M nBu₄NPF₆. The right chamber held the counter electrode in 15 mL of a 5 mM ferrocene solution in MeCN. These two chambers were separated by a fine-porosity glass frit. The working electrode was a $3.2 \text{ cm} \times 1.6$ $cm \times 0.1$ cm glassy carbon plate (HTW Hochtemperatur-Werkstoff GmbH) which was half immersed in the solution. Prior to each experiment, the working electrode was first polished on 600-grit SiC polishing paper (Buehler, Ltd) and sonicated for 5 min in i-PrOH. The reference electrode was a Ag/AgNO₃ (1.0 mM)/MeCN nonaqueous reference electrode (also containing $0.1 \text{ M} n \text{Bu}_4 \text{NPF}_6$) separated from the solution by a Vycor frit (Bioanalytical Systems, Inc.). The counter electrode was nichrome wire (ARCOR). Prior to each electrolysis experiment, the cell was purged with CO2 or N2 for 30 minutes and then sealed under an atmosphere of CO or N₂. The CPE experiments were conducted with no IR compensation for solution resistance (~60 Ω), and the reported electrolysis potentials are the actual applied potentials. After each electrolysis, the headspace was sampled using a Thermo Scientific 10 mL Syringe, and the CO and H₂ concentration were measured by gas chromatography. The post-electrolysis solution was analyzed using HPLC to determine HCOOH concentration. The Faradaic

efficiency of every product was calculated by dividing the measured product concentrations by the amount expected on the basis of charge passed during the CPE measurement.

Product Analysis. Gaseous products (*i.e.* CO and H₂) in the headspace were measured using a Thermo Scientific Trace 1310 with two analyzer systems. Using a valve system, column configuration, and method developed by Thermo Scientific and Custom Solutions Group LLC., gases were separated so that H₂ was detected on one channel using an Ar carrier, and all other gases were detected on a second channel using a He carrier gas. 5.0 mL aliquots of the working-electrode headspace were collected using a Thermo Scientific 10 mL Syringe. The headspace sample was injected directly into the 5 mL sample loop. Gases were detected on both channels using thermal conductivity detectors (TCDs), and chromatographs were analyzed using Thermo Scientific Dionex ChromeleonTM 7.2.2.6686 Chromatography Data System software.

Liquid products (*i.e.* HCOOH) were analyzed using high-performance liquid chromatography (HPLC). HPLC measurements were collected using a Thermo Scientific Dionex Ultimate 3000 series HPLC equipped with a UV-Vis detector and refractive index detector (RID). Liquid aliquots were collected from the working-electrode chamber post-electrolysis and placed in an autosampler from which 10 μ L aliquots of each liquid sample was injected into a HyperREZ XP Carbohydrate H+ column. The eluent was 0.05 M H₂SO₄ aqueous solution at a flow rate of 0.6 mL min⁻¹. The temperature of the column was maintained at 50 °C Products were detected using the RID detector and chromatographs were analyzed using Thermo Scientific Dionex ChromeleonTM 7.2.2.6686 Chromatography Data System software.

Faradaic efficiencies were calculated by dividing the total number of moles of each product by the moles of electrons calculated from the amount of charge passed during the electrolyses normalized for the number of electrons required to produce each product.

SEM-EDS tests. All electrodes tested by SEM-EDS (JEOL-7800FLV FE) were not rinsed post electrolysis. The SEM images showing the morphology of the electrode surface were recorded with a field emission gun scanning electron microscope at 18 kV,

equipped with an energy dispersive X-ray (EDS) detector. The EDS analyses were conducted using an SEM acceleration voltage of 18 kV.



Figure S1. ¹H-NMR Spectrum of Ligand **L-L** in CD₃Cl- d_3 (δ 7.69 solvent residual peak)



Figure S2. ¹H-NMR Spectrum of [Co(L-L)Br₂]Br in Trifluoroacetic acid- d_1 (δ =11.5 solvent residual peak)

Formula	[Co(L-L]Br ₂]Br
гопциа	$(C_{16}H_{18}Br_{3}CoN_{4})$
FW	565.00
Crystal system	triclinic
Space group	P -1
a (Å)	8.2736(4)
b (Å)	10.7007(5)
c (Å)	11.1674(4)
a (deg)	85.313(4)
β (deg)	71.078(4)
γ (deg)	86.856(4)
Z	2
Volume (Å ³)	931.71(7)
Temperature (K)	293(2)
Density (g/mL)	2.014
Reflections collected / unique	13611 / 3345 [R(int) = 0.0293]
Final R indices [I>2sigma(I)]	R1 = 0.0252, wR2 = 0.0637
R indices (all data)	R1 = 0.0254, wR2 = 0.0638
Goodness-of-fit on F ²	1.005

Table S1. Crystal data and structure refinement for the cobalt complex catalyst

Bonds	/ Å
Co(1)-N(3)	1.865(2)
Co(1)-N(2)	1.868(2)
Co(1)-N(4)	1.961(2)
Co(1)-N(1)	1.971(2)
Co(1)-Br(2)	2.3906(4)
Co(1)-Br(1)	2.4047(4)
Bond angles	/ deg
N(3)-Co(1)-N(2)	85.81(9)
N(3)-Co(1)-N(4)	82.78(9)
N(2)-Co(1)-N(4)	167.50(9)
N(3)-Co(1)-N(1)	167.50(9)
N(2)-Co(1)-N(1)	82.52(9)
N(4)-Co(1)-N(1)	109.22(9)
N(3)-Co(1)-Br(2)	91.40(6)
N(2)-Co(1)-Br(2)	88.44(6)
N(4)-Co(1)-Br(2)	86.76(6)
N(1)-Co(1)-Br(2)	92.75(6)
N(3)-Co(1)-Br(1)	87.00(6)
N(2)-Co(1)-Br(1)	92.69(6)
N(4)-Co(1)-Br(1)	91.79(6)
N(1)-Co(1)-Br(1)	89.08(6)
Br(2)-Co(1)-Br(1)	177.965(19)

Table S2. Related bond lengths and bond angles of the cobalt complex catalyst



Figure S3. IR Spectrum of [Co(L-L)Br2] and [Co(L-L)Br2]Br



Figure S4. UV-vis spectrum of 0.1 mM [Co(L-L)Br₂] and [Co(L-L)Br₂]Br in MeCN in air. Based on UV-vis spectra of Co complexes adopting similar structures reported in literatures^[S3, S18, S19], the intense peaks at 221 nm and 270 nm (for [Co(L-L)Br₂]), 221 nm and 313 nm (for [Co(L-L)Br₂]Br) were assigned to ligand $\pi \rightarrow \pi^*$ transition. The peak at 528 nm in [Co(L-L)Br₂] spectrum was assigned to Co²⁺ *d-d* transition (⁴T_{1g}(F) \rightarrow ⁴T_{1g}(P)), which is not observed in [Co(L-L)Br₂]Br spectrum.



Figure S5. UV-vis spectrum of 0.1 mM [**Co**(**L**-**L**)**Br**₂] in MeCN in air and under CO₂. CO₂ has little influence on UV-vis spectrum of 0.1mM [**Co**(**L**-**L**)**Br**₂] in MeCN.



Figure S6. UV-vis spectrum of 0.1 mM [**Co(L-L)Br**₂] in MeCN in air and with 11 M H₂O in air. Proton source H₂O has little influence on UV-vis spectrum of 0.1 mM [**Co(L-L)Br**₂] in MeCN.



Figure S7. UV-vis spectrum of 0.1 mM (black curve) and 0.3 mM (red curve) [**Co**(**L**-**L**)**Br**₂] in MeCN in air. The concentration of [**Co**(**L**-**L**)**Br**₂] affects absorption features of ligand $\pi \rightarrow \pi^*$ transition but has little influence on Co²⁺ *d*-*d* transition. The concentration 0.3 mM was used consistently in the following electrolysis experiments.

Paramagnetic Susceptibility Measurements (Evans Method)

The measurement of paramagnetic susceptibility

The paramagnetic susceptibility of $[Co(L-L)]Br_2$ was studied by Evans method which was established in 1959 for paramagnetic susceptibility measurement by using NMR^[S20]. The most commonly used equation is

$$\chi_{mass} = \frac{3\Delta f}{4\pi fc} + \chi_0 + \frac{\chi_0(d_0 - d_s)}{c}$$

$$\chi_{mol} = M \chi_{mass}$$

Where χ_{mass} is mass susceptibility $(cm^3 \cdot g^{-1})$, χ_{mol} is molar susceptibility $(cm^3 \cdot mol^{-1})$, Δf is observed frequency difference (Hz), f is spectrometer frequency $(400 \times 10^6 Hz)$, c is concentration of the sample solution $(g \cdot cm^{-3})$, χ_0 is mass susceptibility of solvent DMSO $(-0.68 \times 10^{-6} cm^3 \cdot g^{-1})$, d_0 is density of solvent $(g \cdot cm^{-3})$, d_s is density of solution $(g \cdot cm^{-3})$, M is molecular weight of [Co(L-L)]Br₂ (485.08 $g \cdot mol^{-1}$). In the most cases, the density of the solution is almost the

same as the density of the solvent. So the equation is usually



Figure S8. The shifted DMSO peaks in ¹H-NMR Spectrum of 2.0 mg [Co(L-L)Br₂] in 0.55 mL d_6 -DMSO

Table S3. The paramagnetic susceptibility of [Co(L-L)]Br2 calculated based on Evans Method

m(sample)/g	$V(d_6 DMSO)/cm^3$	$[sample]/g \cdot ml^{-1}$	$\chi_{mass}/cm^3 \cdot g$	$\chi_{mol}/cm^3 \cdot mol$
0.0028	0.55	0.0051	8.7×10^{-6}	4.2×10^{-3}
0.0022	0.55	0.0040	7.5×10^{-6}	3.6×10^{-3}
0.0020	0.55	0.0036	9.6×10^{-6}	4.7×10^{-3}
	Ave	rage		4.2×10^{-3}

The number of unpaired electrons

Based on Curie's Law,

$$\chi_{mol}T = constant for a simple paramagnet$$
$$\chi_{mol}T = \frac{1}{2}[S(S+1)] = 8n(n+2)$$
$$\mu_{eff} = \sqrt{8(\chi_{mol}T)} = 2\sqrt{S(S+1)} = \sqrt{n(n+2)}$$

Where *T* is temperature (*K*), *S* is total spin quantum number, *n* is the number of unpaired electrons, μ_{eff} is effective magnetic moment (*Bohr magneton*, μ_B), which is independent of temperature.

$\chi_{mol}/cm^3 \cdot mol$	$\chi_{mol}T$	μ_{eff}	n	μ_{eff} in literature^{[S3]}	n in literature ^[S3]
4.2×10^{-3}	1.22	3.12	2.28	2.85	2.02

Table S4. the calculated μ_{eff} and n in [Co(L-L)]Br₂ at 293K based on χ_{mol}

The effective magnetic moment μ_{eff} 3.12 matches the value 2.85 reported in the literature.^[S3] Based on the calculation [Co(L-L)]Br₂ shows μ_{eff} between the value ca. 1.73 for a pure octahedral low spin state and 3.87 for a pure octahedral high spin state. This could be explained by the occurrence of a thermal equilibrium between these two spin states at the room temperature.^[S3]



Figure S9. CVs of 0.3 mM [Co(L-L)Br₂] in acetonitrile with 0.1 M nBu_4NPF_6 with increasing H₂O concentration



Figure S10. CVs of 0.3 mM [Co(L-L)Br₂] in acetonitrile with 0.1 M nBu_4NPF_6 with increasing TFE concentration



Figure S11. CVs of 0.3 mM [Co(L)Br₂] in acetonitrile with 0.1 M nBu_4NPF_6 under N₂ and CO₂ with TFE.



Figure S12. CVs of 0.3 mM [Co(L-L)Br₂] in acetonitrile with 0.1 M nBu_4NPF_6 under N₂ and CO₂ with different H₂O concentrations to show that the inverted peak shape is attributed to the overlap of the catalytic current response for CO₂ reduction with the more negative, reversible Co^{1+/0} redox feature.



Figure S13. CVs of 0.3 mM [Co(L-L)Br₂] in acetonitrile with 0.1 M nBu_4NPF_6 under N₂ and CO₂ with different TFE concentrations to show that the inverted peak shape is attributed to the overlap of the catalytic current response for CO₂ reduction with the more negative, reversible Co^{1+/0} redox feature.



Figure S14. The Controlled-Potential Electrolysis cell setup

E. A.	E / V vs. [Proton		Charge /	Charge / Farada		uc Efficiency / %		
Entry	FeCp ₂	source] / M	С	СО	H_2	нсоон	wt% ^a	
0	-1.95	-	2.2 ± 0.3	2.8 ± 2.7	0	6.3 ± 2.6	0.52	
1-a	-1.95	[H ₂ O] 0.55 M	2.2 ± 0.5	7.0 ± 2.9	0	7.5 ± 3.8	_b	
1-b	-1.95	[H ₂ O] 1.10 M	3.4 ± 0.4	16.3 ± 5.1	0	4.5 ± 1.1	_b	
1-c	-1.95	[H ₂ O] 2.75 M	5.2 ± 0.3	56.5 ± 11.5	0	3.4 ± 0.8	_b	
1-d	-1.95	[H ₂ O] 5.50 M	7.1 ± 0.7	67.4 ± 11.0	0.3 ± 0.1	1.9 ± 0.5	_b	
1	-1.95	[H ₂ O] 11.00 M	8.3 ± 0.9	80.5 ± 4.7	1.1 ± 0.5	0.7 ± 0.3	0.3	
2-a	-1.85	[TFE] 0.275 M	3.4 ± 0.6	13.6 ± 1.7	0	5.6 ± 2.4	_b	
2-b	-1.85	[TFE] 0.55 M	4.0 ± 0.4	34.7 ± 1.4	0	4.0 ± 0.3	_b	
2-c	-1.85	[TFE] 1.10 M	6.2 ± 1.1	65.8 ± 5.2	0	2.2 ± 1.1	0.13	
2-d	-1.85	[TFE] 2.75 M	11.2 ± 3.0	75.4 ± 1.0	1.3 ± 1.2	0.7 ± 0.6	0.01	
2	-1.85	[TFE] 5.50 M	10.1 ± 2.3	87.7 ± 8.2	1.7 ± 0.7	0	0.01	

Table S5. Conditions and Product Analysis of the Controlled Potential Electrolysis for CO_2 reduction with 0.3 mM Co(L-L)Br₂

^{*a*}Weight percent of Co deposited onto the electrode post-electrolysis as measured by SEM-EDS. b Not measured.

Table S6. Conditions and Product Analysis of the CPE control groups for CO₂ reduction

_	Catalyst /	E/V	[Proton	[Proton		Faradaic Efficiency / % ^a		
Entry	0.3 mM	vs. FeCp ₂	source] / M	Charge / C	СО	H_2	wt% ^b	
1-A	CoBr ₂	-1.95	[H ₂ O] 11.00 M	2.0 ± 0.1	0	24.5 ± 13.6	7.2	
2-A	CoBr ₂	-1.85	[TFE] 5.5 M	6.2 ± 1.3	0	21.5 ± 13.0	0.45	
1-B	Glassy Carbon	-1.95	[H ₂ O] 11.00 M	2.0 ± 0.1	0	20.2 ± 4.1	_ ^c	
2-B	Glassy Carbon	-1.85	[TFE] 5.5 M	3.8 ± 1.2	0	20.1 ± 12.0	_ ^c	
1-C	Ligand	-1.95	[H ₂ O] 11.00 M	2.9 ± 0.3	3.5 ± 3.2	6.6 ± 3.4	_c	

^{*a*}No HCOOH was detected after electrolysis with control groups. ^{*b*}Weight percent of Co deposited onto the electrode post-electrolysis as measured by SEM-EDS. ^{*c*}Not measured.

E / V vs.	[Proton source] /		Farad	aic Efficiency	/ %	Co /		
FeCp ₂	Μ	Charge / C	СО	H2	нсоон	wt% ^a		
No proton source								
-1.95	0	2.2 ± 0.3	2.8 ± 2.7	0	6.3 ± 2.6	0.52%		
-2.15	0	4.3 ± 1.4	4.2 ± 1.7	0	2.7 ± 0.9	0.52%		
	Water							
-1.75	11.00 M	3.1 ± 0.3	30.3 ± 10.8	6.4 ± 1.8	0	0.97%		
-1.95	11.00 M	8.3 ± 0.9	80.5 ± 4.7	1.1 ± 0.5	0.7 ± 0.3	0.35%		
-2.15	11.00 M	16.2 ± 2.5	104.3 ± 5.5	0.7 ± 0.4	0	0.18%		
-2.35	11.00 M	17.0 ± 0.6	44.3 ± 12.2	45.5 ± 2.5	0	0.54%		
TFE								
-1.85	5.5 M	10.1 ± 2.3	87.7 ± 8.2	1.7 ± 0.7	0	0.01%		
-2.05	5.5 M	16.8 ± 2.5	102.7 ± 3.1	1.0 ± 0.4	0	0.007%		

Table S7. Conditions and Product Analysis of the CPE control groups for CO₂ reduction at different potentials.

^aWeight percent of Co deposited onto the electrode post-electrolysis as measured by SEM-EDS.

ICP-MS tests

Deposits on the surface of unrinsed glassy carbon (GC) electrode after electrolysis were digested in 3.0 mL TraceMetal Grade HNO₃. The resulting acidic solution was first diluted to a 10.0 mL stock solution with 18 M Ω water, and then a final test solution for ICP-MS measurements was made by diluting 10 uL stock solution into 10.0 mL with 18 M Ω water. All ICP-MS measurements were corrected for an HNO₃ background at the same concentration as the test solutions.

The fraction of the catalyst $[Co(L-L)]Br_2$ decomposed on the electrode surface could be calculated based on the following equations:

$$n(Co)_{on \ electrode \ surface} = \frac{[Co]_{ICP-MS} \times 10^{-6} \left(\frac{g}{L}\right) \times 1000 \times 0.01(L)}{58.93 \left(\frac{g}{mol}\right)}$$

 $Fraction = \frac{n(Co)_{on \ electrode \ surface}}{([Cat] \times V_{solution})}$

Where $[Co]_{ICP-MS}$ is Co concentration in ICP-MS test solution after correction, [*Cat*] is $[Co(L-L)]Br_2$ concentration in the electrolysis solution, $V_{solution}$ is the volume of the electrolysis solution.

Electrode, [proton source], potential vs. Fc ^{+/0}	[Co] in ICP-MS test solution / ppb (as measured)	<i>n</i> (Co) on electrode surface / mol	Calculated fraction of [Co(L-L)Br2] decomposed on the electrode surface
GC1, no H2O, -1.95 V	2.98	5.06×10^{-7}	8.43 %
GC2, no H2O, -1.95 V	2.95	$5.01 imes 10^{-7}$	8.34 %
GC3, no H2O, -1.95 V	3.14	5.31×10^{-7}	8.86 %
Average		${\bf 5.13 \pm 0.17 \times 10^{\text{-7}}}$	8.54 ± 0.28 %
GC4, 11 M H ₂ O, - 1.95 V	2.801	$4.75 imes 10^{-7}$	7.91 %
GC5, 11 M H ₂ O, - 1.95 V	2.424	4.11×10^{-7}	6.85 %
GC6, 11 M H ₂ O, - 1.95 V	1.933	$3.28 imes 10^{-7}$	5.46 %
GC7, 11 M H ₂ O, -1.95 V	2.46	4.16×10^{-7}	6.94 %
GC8, 11 M H ₂ O, -1.95 V	2.67	4.54×10^{-7}	7.56 %
Average		${\bf 4.17 \pm 0.56 \times 10^{\text{-7}}}$	$6.94 \pm 0.94 \%$
GC9 (5.5M TFE, -1.85V)	1.034	1.75×10^{-7}	2.92 %
GC10 (5.5M TFE, - 1.85V)	1.750	2.97×10^{-7}	4.94 %
GC11 (5.5M TFE, - 1.85V)	1.069	$1.81 imes 10^{-7}$	3.02 %
GC12 (5.5M TFE, - 1.85V)	1.491	2.53×10^{-7}	4.21 %
GC13 (5.5M TFE, - 1.85V)	1.405	2.38×10^{-7}	3.97 %
Average		$2.29 \pm 0.51 \times 10^{-7}$	3.81 ± 1.14 %

Table.S8. ICP-MS results of Co content on the surface of GC electrode after electrolysis

a[Co] in ICP-MS test solution (after correction) = [Co] in ICP-MS test solution - [Co] background

Note that a [Co] concentration of 0.927 ppb, $n(\text{Co}) = 1.57 \times 10^{-7}$ mol, was measured from the ICP-MS test solution of a bare GC electrode without electrolysis, suggesting some residual Co exists on the electrodes after polishing and before electrolysis.



Figure S15. SEM-EDS analysis of a representative working electrode surface after a 30minute CO₂RR electrolysis using 0.3 mM [Co(L-L)Br₂] with 0.1 M nBu_4PF_6 in acetonitrile at -1.95 V vs. Fc/Fc⁺



Figure S16. SEM-EDS analysis of a representative working electrode surface after a 30minute CO₂RR electrolysis using 0.3 mM Ligand L-L in acetonitrile with 11.00 M H₂O and 0.1 M nBu_4PF_6 in acetonitrile at -1.95 V vs. Fc/Fc⁺



Figure S17. SEM-EDS analysis of a representative working electrode surface after a 30minute CO₂RR electrolysis using 0.3 mM [Co(L-L)Br₂] with 11.00 M H₂O and 0.1 M nBu_4PF_6 in acetonitrile at -1.95 V vs. Fc/Fc⁺



Figure S18. SEM-EDS analysis of a representative working electrode surface after a 30minute CO₂RR electrolysis using 0.3 mM [Co(L-L)Br₂] with 5.50 M TFE and 0.1 M nBu_4PF_6 in acetonitrile at -1.85 V vs. Fc/Fc⁺



Figure S19. SEM-EDS analysis of a representative working electrode surface after a 30minute CO₂RR electrolysis using 0.3 mM CoBr₂ with 11.00 M H₂O and 0.1 M nBu_4PF_6 in acetonitrile at -1.95 V vs. Fc/Fc⁺



Figure S20. SEM-EDS analysis of a representative working electrode surface after a 30minute CO_2RR electrolysis using 0.3 mM $CoBr_2$ with 5.50 M TFE and 0.1 M nBu_4PF_6 in acetonitrile at -1.85 V vs. Fc/Fc⁺



Figure S21. SEM-EDS analysis of a representative working electrode surface after a 30minute CO_2RR electrolysis using bare glassy carbon electrode with 11.00 M H₂O and 0.1 M nBu_4PF_6 in acetonitrile at -1.95 V vs. Fc/Fc⁺.



Figure S22. SEM-EDS analysis of a representative working electrode surface after a 30minute CO₂RR electrolysis using bare glassy carbon electrode with 5.50 M TFE and 0.1 M nBu_4PF_6 in acetonitrile at -1.85 V vs. Fc/Fc⁺

Turnover Frequency (TOF) calculations

Method 1:

*TOF*s for CO are calculated based on the total amount of CO generated divided by the total amount of the catalyst in the electrolysis solution and the time of the electrolysis.

$$TOF = \frac{\frac{n(CO)}{n(Cat)}}{t}$$

n(CO) is the total number of moles of CO produced, n(Cat) is the number of moles of the catalyst in the solution, and t is the electrolysis time in seconds.

n(CO) is calculated based on the amount of electrons used specifically for CO generation divided by a factor 2F (it is a two-electron reduction reaction from CO₂ to CO):

$$n(CO) = \frac{Q \times FE(CO)}{2F}$$

Q is the charge passed in Coulombs (C); FE(CO) is the Faradaic Efficiency of CO in percentage (%); F is Faraday constant (C/mol)

n(Cat) is calculated based on the following equation:

$$n(Cat) = [Cat] \times V_{sol}$$

[*Cat*] is the concentration of the catalyst (mol/L); V_{sol} is the volume of the solution (L)

Method 2:

TOF values for CO are calculated from CPE data with the equations described by Savéant et al. ^{[S4],[S5]}

A) Calculation of diffusion constants D from cyclic voltammograms

For the homogenous system, the relation between the peak current and scan rate in CV is given by the Randles-Sevcik equation:

$$i_p = 0.4463 \left(\frac{F}{RT}\right)^{\frac{1}{2}} n_p^{\frac{3}{2}} FAD^{\frac{1}{2}} [Cat] v^{\frac{1}{2}}$$

 i_p is peak current (A), F is Faraday constant (96500 C/mol), R is the universal gas constant (8.31 $J \cdot K^{-1} \cdot mol^{-1}$), T is temperature (298 K), n_p is the number of electrons transferred (1 for each Co-complex redox process), A is the active surface area of the electrode ($A = 0.071 \ cm^2$), D is the diffusion coefficient for the complex (cm^2/s), [Cat] is the concentration of the catalyst (mol/cm^3), and v is the scan rate (V/s).

The diffusion coefficients (D) were calculated from the slopes of $i_p - v^{\frac{1}{2}}$ plots



Figure S23. Cyclic voltammograms of the 1.2 mM Cat in MeCN (with 0.1 M nBu_4NPF_6) recorded at different scan rates. The couples of redox peaks P1, P2 and P3 are corresponded to $Co^{3+/2+}$, $Co^{2+/1+}$ and L-L/L-L⁻ process.

The diffusion coefficient D of the catalyst $[Co(L-L)Br_2]$ could be calculated based on the slopes of the fitted linear curves in Figure S18 and S19, concentration of $[Co(L-L)Br_2]$ and the working electrode surface, using the Randles-Sevcik equation mentioned above. The result is shown in Table S6.



Figure S24. $i_p - v^{1/2}$ plots of P1 (Co^{3+/2+} redox process)



Figure S25. $i_p - v^{1/2}$ plots of P2 (Co^{2+/1+} redox process)

Peak	slope / (mV/s) ^{1/2}	[Cat] / mM	A /cm ²	D /cm ² /s	D(average)/ cm ² /s
P1cathodic	0.00149	1.2	0.071	4.24×10^{-6}	
P1anodic	0.00142	1.2	0.071	3.85× 10 ⁻⁶	4.05. 10-6
P2cathodic	0.00137	1.2	0.071	3.58× 10 ⁻⁶	4.05×10°
P2anodic	0.00154	1.2	0.071	4.53× 10 ⁻⁶	

Table S9. The calculation of the diffusion coefficient D for the catalyst

B) Calculation of TOF for CO generation derived from CPE data using the equations described by Savéant et al. ^{[3],[4]}

$$TOF = \frac{\frac{n(CO)}{n(Cat)}}{t}$$

TOF values for CO generation were calculated from the CPE data as reported by Saveant and co-workers.^{[3],[4],[15]} In the homogeneous case, n(Cat) is obtained by space integration of catalyst amount in the reaction-diffusion layer near the surface of the working electrode. n(CO) is calculated based on the charge specially used for CO generation.

$$n(Cat) = A \sqrt{\frac{D}{k_{cat}}} [Cat] = A \sqrt{\frac{D}{TOF_{max}}} [Cat]$$
$$n(CO) = \frac{Q_{el} \times FE}{F}$$

A is the active surface area of the working electrode (2.56 cm^2), D is the diffusion coefficient for the complex ($4.05 \times 10^{-6} cm^2/s$), k_{Cat} is the reaction rate of catalysis process, TOF_{mas} is the maximum turnover frequency obtained from CVs. It is used to replace k_{Cat} in the calculation, [Cat] is the concentration of the catalyst ($0.3 \times 10^{-6} cm^2/s$), F is Faraday constant (96500 C/mol).

So the expression of *TOF* is:

$$TOF = \frac{\frac{n(CO)}{n(Cat)}}{t} = \frac{\frac{Q_{el} \times FE}{F}}{A\sqrt{\frac{D}{TOF_{max}}}[Cat]}}$$
$$i_{el} = \frac{Q_{el} \times FE}{t}$$
$$TOF = \frac{i_{el}}{FA}\frac{\sqrt{TOF_{max}}}{\sqrt{D}[Cat]}}$$

 i_{el} is average current of CPE for CO generation (A), Q_{el} is the charge passed in 30min CPE (C), FE is the faradaic efficiency of CO (%), t is the time of CPE (s).

The equations below were used for the calculation under the assumption that the electron transfer process to the catalyst is fast and the Nernst equation is obeyed.

$$TOF = \frac{TOF_{max}}{1 + exp\left[\frac{F}{RT}(E_{app} - E_{1/2})\right]}$$

R is the universal gas constant (8.31 $J \cdot K^{-1} \cdot mol^{-1}$), *T* is temperature (298 *K*), E_{app} is the applied potential during electrolysis (*V*), $E_{1/2}$ is the redox potential of the ligand (1.65*V*).

Combination of the equations above gives:

$$TOF = \frac{i_{el}^2 \left(1 + exp \left[\frac{F}{RT} \left(E_{app} - E_{1/2} \right) \right] \right)}{F^2 A^2 D [Cat]^2}$$

Long-time CPE experiments

Teduci	reduction of 0.5 million CO(L-L)B12								
T/min	E /V vs. FeCp2	E /V vs.	[Proton source]	Charge /C	TOF ^a /s ⁻¹	TOF ^b /s ⁻¹	Fara Efficie	adaic ncy /%	Co / wt% ^c
						CO	H_2		
60	-1.95	[H ₂ O] 11.00 M	14.4	3.0× 10 ⁻³	560	88.2	1.6	0.83 %	
90	-1.95	[H ₂ O] 11.00 M	21.6	2.7× 10 ⁻³	448	78.9	3.5	1.53 %	
120	-1.95	[H ₂ O] 11.00 M	28.5	1.0× 10 ⁻³	61.3	29.5	18.7	7.20 %	
120	-1.85	[TFE] 5.5 M	31.4	0.8×10 ⁻³	34.9	20.2	7.9	4.43 %	

Table S10. Conditions and Product Analysis of the long-time CPE control groups for CO_2 reduction of 0.3 mM Co(L-L)Br₂

^{*a*}TOF is the turnover frequency for CO calculated based on total concentration of catalyst in solution, and therefore is a significant underestimate of catalytic activity. ^{*b*}TOF is the turnover frequency for CO generation, derived from CPE data using the equations described by Savéant et al. ^{*c*}Weight percent of Co deposited onto the electrode post-electrolysis as measured by SEM-EDS



Figure S26. SEM-EDS analysis of the working electrode surface after a 60-minute CO_2RR electrolysis using 0.3 mM [Co(L-L)Br₂] with 11.00 M H₂O in acetonitrile at -1.95 V vs. Fc/Fc⁺



Figure S27. SEM-EDS analysis of the working electrode surface after a 90-minute CO_2RR electrolysis using 0.3 mM [Co(L-L)Br₂] with 11.00 M H₂O in acetonitrile at -1.95 V vs. Fc/Fc⁺



Figure S28. SEM-EDS analysis of the working electrode surface after a 120-minute CO₂RR electrolysis using 0.3 mM [Co(L-L)Br₂] with 11.00 M H₂O in acetonitrile at -1.95 V vs. Fc/Fc⁺



Figure S29. SEM-EDS analysis of the working electrode surface after a 120-minute CO_2RR electrolysis using 0.3 mM [Co(L-L)Br₂] with 5.50 M TFE in acetonitrile at -1.85 V vs. Fc/Fc⁺



Figure S30. The UV-vis spectra of the acetonitrile solution of 0.3 mM $[Co(L-L)Br_2]$ with 11.00 M H₂O at -1.95 V vs. Fc/Fc⁺ before and after 30-minute CPE for CO₂RR



Figure S31. The UV-vis spectra of the acetonitrile solution of 0.3 mM $[Co(L-L)Br_2]$ with 11.00 M H₂O at -1.95 V vs. Fc/Fc⁺ before and after 1 hour CPE for CO₂RR



Figure S32. The UV-vis spectra of the acetonitrile solution of 0.3 mM $[Co(L-L)Br_2]$ with 11.00 M H₂O at -1.95 V vs. Fc/Fc⁺ before and after 1.5 hour CPE for CO₂RR



Figure S33. The UV-vis spectra of the acetonitrile solution of 0.3 mM $[Co(L-L)Br_2]$ with 11.00 M H₂O at -1.95 V vs. Fc/Fc⁺ before and after 2 hour CPE for CO₂RR

Catalyst	CO ₂ RR E _{onset} /V vs. Fc ⁺ /Fc	CPE condition	CO ₂ RR E _{applied} /V vs. Fc ⁺ /Fc	TOF /s ^{-1 a}	TOF /s ^{-1 b}	TOF /s ^{-1 c}	Product selectivity	Ref.
Br		0.3 mM Cat in MeCN(0.1 M <i>n</i> Bu ₄ NPF ₆)	-1.95	$(3.2 \pm 0.4) \times 10^{-3}$	620	_d	$\begin{array}{c} \text{CO} (80.5\%): \\ \text{H}_2(1.1\%): \\ \text{HCOOH} (0.7\%) \end{array}$	
	-1.65	CO ₂ with 11M H ₂ O	-2.15	$(8.1 \pm 1.3) \times 10^{-3}$	3961	-	CO (104.3%) : H ₂ (0.6%)	This work
		0.3 mM Cat in MeCN(0.1	-1.85	$(4.2 \pm 0.5) \times 10^{-3}$	1089	-	CO (87.7%) : H ₂ (1.7%)	
Br		$M nBu_{4}NPF_{6}$) CO ₂ with 5.5M TFE	-2.05	$(8.2 \pm 0.9) \times 10^{-3}$	4131	-	CO (102.7%) : H ₂ (1.0%)	
Other Cobalt Complexes								
	-	1.2 mM Cat 0.1 M KNO, in H ₂ O/CH,CN 2: 1 (v/v) or H ₂ O only	-2.00	2.2×10^{-3}	-	-	CO (46.5%) : H ₂ (46.5%)	[0,2]
	-		-1.90	2.5×10^{-3}	-	-	CO (45.0%) : H ₂ (45.0%)	[36]
$ \begin{array}{c} $	~-1.8 0.18-0.21 mM Cat mercury electrode DMF/H ₂ O (95/5 v/v) 0.1 M Et ₄ NCl. H ₂ O	-1.70	-	-	-	CO (7.9%) : H ₂ (13.1%)	[\$7]	
		$0.1 \text{ M Et}_4 \text{NCl. H}_2 \text{O}$	-2.0		-	-	CO (56.2%) : H ₂ (25.0%)	

Table S11. Summary of Co-complex catalysts for electrochemical CO₂RR

H,N,N Co H,N,N H,N	~-1.8	0.18-0.21 mM Cat	-2.0	-	-	-	CO (13.3%) : H ₂ (58.8%)	
2+ N	1.0	DMF/H ₂ O (95/5 v/v) 0.1 M Et ₄ NCl. H ₂ O	-1.7	-	-	-	CO (66.4%) : H ₂ (5.3%)	[S7]
	~-1.0		-2.0	-	-	-	CO (41.5%) : H ₂ (10.9%)	
$[Co(tpy)_2]^{2+}$ $tpy: \qquad \qquad$	~-2.03	2 mM Cat CO2-saturated DMF/ H2O (95 : 5, v : v) with 0.1 M TBAP	-1.93	-	-	-	CO (20.0%) : H ₂ (1.0%)	[\$8]
			-2.03	-	-	-	CO (12.0%) : H ₂ (5.0%)	
2+ N C C - N H	~-1.55	0.3 mM Cat MeCN(0.1 M <i>n</i> Bu ₄ NPF ₆) CO ₂ with 10M H ₂ O	-2.13	1.7× 10 ⁻³	_	-	CO (45.0%) : H ₂ (30.0%)	[89]
$\begin{bmatrix} tBu_2 \\ F^{-P} NCCH_3 \\ N^{-Co''-NCCH_3} \\ F^{-P} tBu_2 \end{bmatrix} BF_{4]_2}$ $E = CH_2$	~-2.1	1.0 mM Cat in CH ₃ CN with 0.20 M Bu ₄ NBF ₄	-	-	-	-	-	[S10]
$\begin{bmatrix} \begin{matrix} tBu_2 \\ E^{-P} & NCCH_3 \\ N^{-C^{(l)}} - NCCH_3 \\ E^{-P} \\ tBu_2 \\ \end{bmatrix} \begin{bmatrix} BF_{4]_2} \\ BF_{4]_2} \\ E = \mathbf{NH} \end{bmatrix}$	~-2.5		-	-	-	-	-	

$\begin{bmatrix} tBu_2 \\ E \xrightarrow{P} NCCH_3 \\ N \xrightarrow{Co^{II} - NCCH_3} \\ E \xrightarrow{P} tBu_2 \end{bmatrix} [BF_4]_2$ $E = O$	~-2.2	1.0 mM Cat in CH ₃ CN with 0.20 M Bu ₄ NBF ₄	-	-	_	-	-	[S10]
[Co ^{II} (TPA)CI][CI]	~-1.94	MeCN(0.1 M <i>n</i> Bu ₄ NPF ₆)	-	-	-	-	-	[S11]
	~-1.7	1.0 mM Cat in DMF, 0.1M <i>n</i> Bu ₄ NPF ₆	-1.9	-	-	-	CO (82.0%)	[S12]
[Co ^{II} (L-R)(solv1)(solv2)] RN NR $NRL-R:R = H; solv1 = solv 2 = acetone$	-2.36	0.5 mM Cat in DMF, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂ with 1.2M TFE	-2.8	0.86× 10 ⁻³	170	360	CO (98.0%)	[\$13]
[CoII(L-R)(solv1)(solv2)] R = Me; solv1 = MeCN solv 2 = none	-2.58	0.5 mM Cat in DMF, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂ with 1.2M TFE	-2.8	0.04× 10 ⁻³	0.5	78	CO (23.0%)	

	-1.95	1 mM Cat in MeCN, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂	-2.1	-	-	-	30min: CO (96.0%) 4 hours: CO (85.0%)	
	-1.93	1 mM Cat in MeCN, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂	-2.1	low	low	-	-	[S14]
	-1.97	1 mM Cat in MeCN, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂	-2.1	low	low	-	-	
	-1.87	1 mM Cat in MeCN, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂	-2.1	low	low	-	-	
$[Co(TPA)X]^+$ $TPA: \qquad \qquad$	-1.96	in MeCN, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂	-	-	-	-	-	[S15]
$[Co(TPA)X]^+$ $X = Br$	-1.83		-	-	-	-	-]
$[Co(TPA)X]^+$ $X = I$	-1.72	in MeCN, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂	-	-	-	-	-	

$[Co(TPA)X]^+$ $X = NCS$	-1.76		-	-	-	-	-	
R = R' = Co - 1 - 2.0 $R' = Co - 1 - 2.0$		0.5 mM Cat in DMF, 0.1M nBu_4NPF_6 CO ₂ with 1.1M H ₂ O	-2.10	2.2×10 ⁻³	70	-	HCOOH(92%): CO (<1%) : H ₂ (5%)	
	-2.08		-2.25	7.2× 10 ⁻³	650	-	HCOOH(98%): CO (<1%) : H ₂ (5%)	
2(R'= Cy; R=Ph)	-2.0	0.5 mM Cat in DMF, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂ with 1.1M H ₂ O	-2.05	1.4× 10 ⁻³	60	-	HCOOH(94%): CO (1%) : H ₂ (3%)	[S16]
			-2.20	2.5× 10 ⁻³	180	-	HCOOH(98%): CO (<1%) : H ₂ (4%)	
		0.5 mM Cat in DMF, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂ with 1.1M H ₂ O	-2.00	0.5×10 ⁻³	20	-	HCOOH(88%): CO (<1%) : H ₂ (8%)	
3(R'= Ph; R=Bn)	-1.93		-2.05	1.0× 10 ⁻³	40	-	HCOOH(86%): CO (<1%) : H ₂ (6%)	
	-2.20	1 mm CoTPP in DMF, 0.1M <i>n</i> Bu ₄ NPF ₆ CO ₂ with	-2.35	2.6× 10 ⁻⁴	-	-	CO (50.0%) : H ₂ (2.0%): HCOOH(4%): Acetate(2%): Oxlate(0.2%)	[S17]

^{*a*}TOF is the turnover frequency for CO calculated based on total concentration of catalyst in solution, and therefore is a significant underestimate of catalytic activity (See TOF method 1 in page 18). Included for comparison purposes only. ^{*b*}TOF is the turnover frequency for CO generation, derived from CPE data using the equations described by Savéant et al. (See TOF method 2 in page 18).^{[S4],[S5]} ^{*c*}TOF is the turnover frequency derived from CV experiments. ^{*d*}Not measured

Reference

[S1] C. C. L. McCrory, N. K. Szymczak, and J. C. Peters, *Electrocatalysis*, 2016, 7, 87-96.

[S2] SHELXTL (version 5.0), Reference Manual, Siemens Industrial Automation, Analytical Instruments, Madison, WI, 1995.

[S3] S. Gourbatsis, S. P. Perlepes, N. Hadjiliadis, Transition Met. Chem., 1990, 15, 300.

[S4] C. Costentin, M. Robert, J.-M. Saveant, Chem. Soc. Rev., 2013, 42, 2423.

[S5] C. Costentin, S. Drouet, M. Robert, J.-M. Savéant, Science, 2012, 338, 90

[S6] B. J. Fisher, R. Eisenberg, J. Am. Chem. Soc., 1980, 102, 7361

[S7] A. H. A. Tinnemans, T. P. M. Koster, D. H. M. W. Thewissen, A. Mackor, *Rec. Trav. Chim. Pays Bas*, 1984, **103**, 288.

[S8] N. Elgrishi, M. B. Chambers, V. Artero, M. Fontecave, *Phys. Chem. Chem. Phys.* 2014, 16, 13635

[S9] D. C. Lacy, C. C. L. McCrory, J. C. Peters, Inorg. Chem 2014, 53, 4980

[S10] D. W. Shaffer, S. I. Johnson, A. L. Rheingold, J. W. Ziller, W. A. Goddard, R. J. Nielsen, J. Y. Yang, *Inorg. Chem* 2014, 53, 13031.

[S11] S. L.-F. Chan, T. L. Lam, C. Yang, S.-C. Yan, N. M. Cheng, *Chem. Commun.* 2015, **51**, 7799

[S12] L. Chen, Z. Guo, X.-G. Wei, C. Gallenkamp, J. Bonin, E. Anxolabéhère-Mallart, K.-C. Lau, T.-C. Lau, M. Robert, *J. Am. Chem. Soc.*, 2015, **137**, 10918.

[S13] A. Chapovetsky, T. H. Do, R. Haiges, M. K. Takase, S. C. Marinescu, J. Am. Chem. Soc., 2016, **138**, 5765.

[S14] F. Wang, B. Cao, W.-P. To, C.-W. Tse, K. Li, X.-Y. Chang, C. Zang, S. L.-F. Chan, C.-M. *Che, Catal. Sci. Technol.*, 2016, **6**, 7408

[S15] S. L.-F. Chan, T. L. Lam, C. Yang, J. Lai, B. Cao, Z. Zhou, Q. Zhu, *Polyhedron* 2017, **125**, 156.

[S16] S. Roy, B. Sharma, J. Pécaut, P. Simon, M. Fontecave, P. D. Tran, E. Derat, V. Artero, *J. Am. Chem. Soc.*, 2017, **139**, 3685.

[S17] X-M. Hu, M. H. Rønne, S. U. Pedersen, T. Skrydstrup, K. Daasbjerg. Angew. Chem. Int. Ed. 2017, 56, 6468.

[S18] M. Popescu, P. Rotaru, M-V. Bubulica, A. Kriza, J. Therm. Anal. Calorim., 2015, 120, 641.

[S19] B. D. Stubbert, J. C. Peters, H. B. Gray, J. Am. Chem. Soc. 2011, 133, 18070.

[S20] D.F. Evans, J. Chem. Soc., 1959, 0, 2003.