## **Supporting Information**

Photocatalytic Decomposition of Benzene Enhanced by the Heating Effect of Light: Improving Solar Energy Utilization with Photothermocatalytic Synergy

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**Figure S1.** The spectra of irradiance for 500 W Xe-arc lamp as simulated solar light source for the experiment of catalytic activity, inserting the magnified graph within

250<λ<800 nm.



**Figure S2.** The spectra of irradiation of 500 W Xe-arc lamp equipped with a  $300 < \lambda < 800$  nm filter as the UV-VIS light source for the photocatalytic experiment of

ESR.



Figure S3. The spectra of irradiation of 500 W Xe-arc lampe quipped with a  $\lambda$ >300 nm filter as simulated solar light source for the photothermocatalytic experiment of

ESR, inserting the magnified graph within  $250 < \lambda < 800$  nm.



Figure S4. The spectra of irradiation of 500 W Xe-arc lamp equipped with a  $\lambda$ >800 nm filter as the NIR light source for the thermocatalytic experiment of ESR.



Figure S5 Raman spectra of BVT-Origin, de-BVT, BVT-PCR, BVT-TCR and BVT-

PTCR samples



**Figure S6** The photocatalytic conversion of benzene versus time over  $TiO_2$ -Origin, de-  $TiO_2$ ,  $TiO_2$ -PCR,  $TiO_2$ -TCR and  $TiO_2$ -PTCR at 30 °C, inserting their color after reaction.

## The calculation of apparent rate constant of reaction $(k_{app})$

The catalyst bed we used can be depicted as follows:



When the steady state is obtained, the mass balance can be depicted as:

$$F_0[C_i - (C_i + dC_i)] = r_i dV \qquad (1)$$

 $F_0$ : flow rate.  $C_i$ : concentration of composition i.  $r_i$ : the reaction rate of composition i.

The concentration can be connected with conversion as:

$$x_i = (C_{i,0} - C_i)/C_i$$
 (2)

*x<sub>i</sub>: conversion of composition i.* 

According to (1) and (2), the reaction rate  $r_i$  can be depicted as:

$$r_i = C_{i,0} dx_i / d(V/F_0)$$
 (3)

Order  $F = F_0 C_{i,0}$  and t = V/F which refers to contact time, then (3) can be depicted as:

$$r_i = dx_i/dt$$
 (4)

The reaction of oxidation of benzene corresponds to first-order kinetics, so

$$r_i = kC_i \qquad (5)$$

k:reaction rate constant.

Combining (4) and (5) and considering the weight of catalyst, the apparent rate constant  $k_{app}$  can be depicted as:

$$k_{app} = \frac{v}{w} \ln \frac{1}{1 - x}$$

v is the flow rate of benzene (20 mL·min<sup>-1</sup>); w is the weight of catalyst; x is the

conversion of benzene.

The Arrhenius equation here:

$$\ln k = -\frac{E_a}{RT} + \ln A = -B\frac{1}{T} + \ln A$$

*k herein* is calculated according to the  $k_{app}$  above;  $E_a$  is the Arrhenius activation energy; R is the gas constant; T is the reaction temperature; A is the pre-exponential factor.



**Figure S7** The ln  $k_{app}$  versus 1000T<sup>-1</sup> Arrhenius plot for BVT.

\*The higher the value of Adj. R-Square, the better linearity.



**Figure S8** The ln  $k_{app}$  versus 1000T<sup>-1</sup> Arrhenius plot for TiO<sub>2</sub>.



**Figure S9** The ln  $k_{app}$  versus 1000T<sup>-1</sup> Arrhenius plot for P25.



Figure S10 XPS spectra for Pt 4f for 0.2PBVT, 0.5PBVT, 1PBVT and 2PBVT; XPS

spectra of Ti 2p (b), O 1s (c), Bi 4f (d) and V 2p (d) for 1PBVT



Figure S11 The amount of CO<sub>2</sub> under PTC and TC condition at different

temperatures for 0.2PBVT, 0.5PBVT, 1PBVT and 2PBVT.



**Figure S12** The ln  $k_{app}$  versus 1000T<sup>-1</sup> Arrhenius plot for PBVT.

\*The higher the value of Adj. R-Square, the better linearity.



**Figure S13** ESR signals of DMPO-·OH and  $O_2$ ·· of BVT, 02PBVT, 05PBVT and 2PBVT under under PC (photocatalytic, see the irradiation graph in Figure S2) and PTC (photothermocatalytic, see the irradiation graph in Figure S3) condition.



Figure S14 O<sub>2</sub>-TPD profile of BVT with the process of oxygen adsorption under (A)
80 °C, (B) UV-vis irradiation (irradiation spectra in Figure S2) at ambient temperature,
(C) simulated solar irradiation (irradiation spectra in Figure S3) at 80 °C and the

merge image of (A), (B) and (C).