## Electronic supplementary information

## CoMn<sub>x</sub>O<sub>y</sub> nanosheets with molecular scaled homogeneity: An excellent catalyst for toluene combustion

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## Experimental

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## **Catalyst Characterization**

X-ray powder diffraction (XRD) analysis was conducted using an x`pert3 powder equipment (PANalytical B.V., Netherlands) with Cu Ka radiation. The loading amount of the catalysts was determined by inductively coupled plasma-atomic emission spectroscopy (ICP-AES, Optima 2000DV, USA). The N<sub>2</sub> sorption measurements were performed using physisorption (ASAP 2020, Micromeritics, USA) at -196 °C. The mesopore specific surface area and the pore size distribution were calculated using the Brunauer-Emmett-Teller (BET) and Barrett-Joyner-Halenda (BJH) methods, respectively. The micropore specific surface area and volume from the micropore were calculated by the t-plot method. The pore volume was calculated according to the adsorption amount of N<sub>2</sub> at  $P/P_0$  (the relative pressure) = 0.995. TEM images were obtained on a JEOL-2010F electron microscope operated at 200 kV. XPS analysis was performed on an AXIS-ULTRA DLD-600W spectrometer (Shimadzu, Japan) using Al K $\alpha$  radiation as the excitation source. The binding energies were calculated with respect to the C (C,H) component of the C 1s peak fixed at 284.8 eV. H<sub>2</sub> temperature programmed reduction (H<sub>2</sub>-TPR) and O<sub>2</sub>-TPD experiments were carried out on a chemical adsorption analyzer (Autochem II 2920, Micromeritics). Before TPR measurement, ca. 30 mg of catalyst (40-60 mesh) was loaded to a quartz fixed-bed U-shaped microreactor (i.d. = 4 mm) and pretreated in an O2 flow of 50 mL/min at 360 °C for 1 h. After being cooled at the same atmosphere to room temperature (RT) and then purged with a N<sub>2</sub> flow of 50 mL/min for 15 min, the pretreated sample was finally exposed to a flow (50 mL/min) of 5% H<sub>2</sub>/Ar mixture and heated from RT to 550 °C at a ramp of 10 °C/min. O<sub>2</sub>-TPD analysis: 50 mg catalyst was heated to 110 °C and purged with He for 1 h to remove surface H<sub>2</sub>O. After being cooled at the same atmosphere to room temperature (RT) and then purged with a  $O_2$  flow of 50 mL/min for 1 h, followed just by the flow of He for 1 h to remove physical absorption oxygen. Then the catalyst was heated from 100 to 600 °C at a rate of 10 °C min.

**Table S1**. Preparation conditions, BET surface areas, pore volumes, average pore sizes, and  $H_2$  consumption of the Co<sub>3</sub>O<sub>4</sub> and MnO<sub>2</sub> catalysts.

Catalyst	Preparation method	$S_{\rm BET} a (m^2/g)$	$\frac{P_{\rm v} b}{(\rm cm^3/g)}$	APD <sup>c</sup> (nm)	H <sub>2</sub> consumption <sup>d</sup> (mmol/g)
Co <sub>3</sub> O <sub>4</sub>	prec.	20	0.035	36.1	15.7
MnO <sub>2</sub>	prec.	14	0.031	40.6	6.8

<sup>*a*</sup> BET specific surface areas determined from the linear part of the BET equation ( $P/P_0 = 0.05-0.25$ ). <sup>*b*</sup> The total adsorption pore volume at  $P/P_0 = 0.995$ . <sup>*c*</sup> Average pore diameter (APD). <sup>*d*</sup> The data were estimated by quantitatively analyzing the H<sub>2</sub>-TPR profiles.

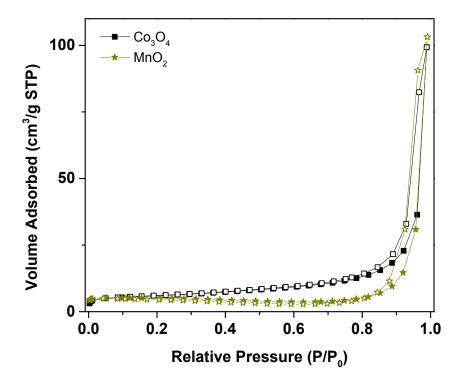


Fig. S1.  $N_2$  adsorption-desorption isotherms curves of the as-synthesized  $Co_3O_4$  and  $MnO_2$  catalysts.

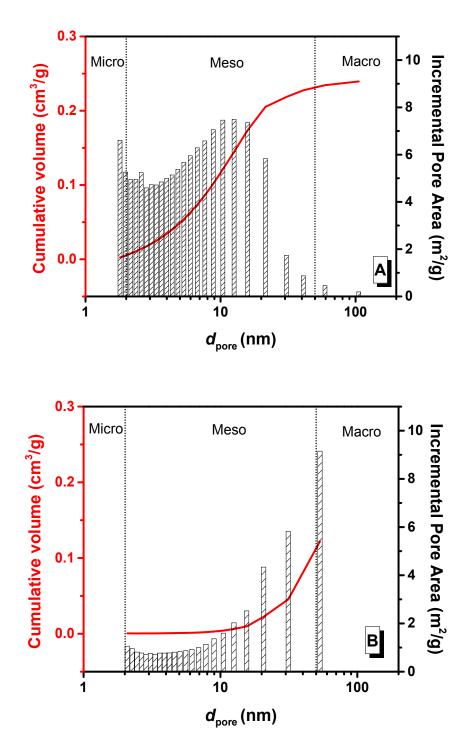


Fig. S2. Pore size distribution (PSD) of the (A) C3M1-R and (B) C3M1-C catalysts.

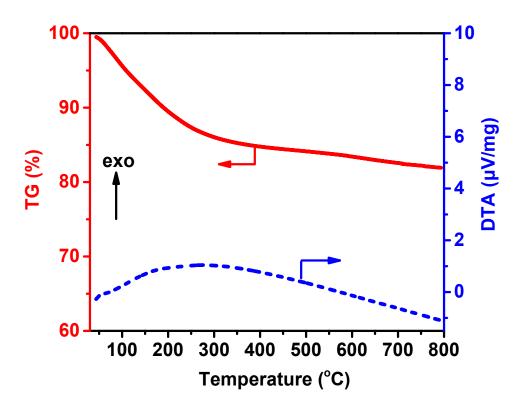
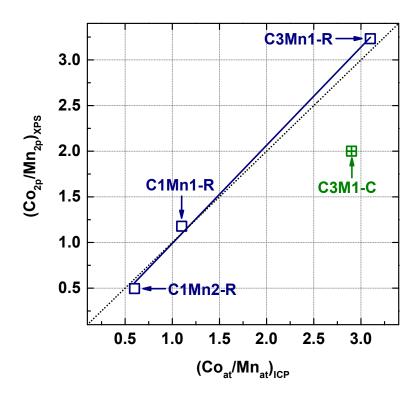


Fig. S3. TG-DTA data for the decomposition of the C3M1-R in air.



**Fig. S4.** Surface Co/Mn atomic ratio from Co 2p/Mn 2p signals (XPS) ratio vs the bulk (ICP) atomic composition of the CoMn<sub>x</sub>O<sub>y</sub> catalysts.

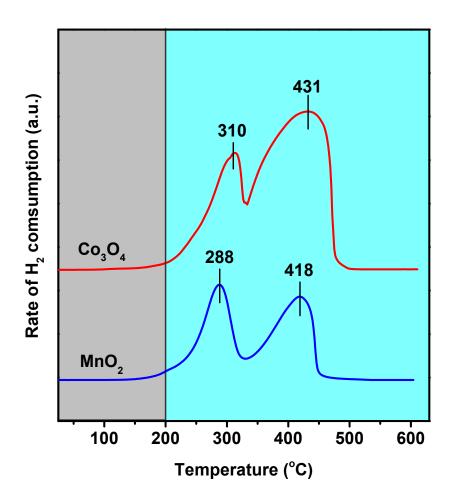


Fig. S5.  $H_2$ -TPR profiles of the  $Co_3O_4$  and  $MnO_2$  catalysts.

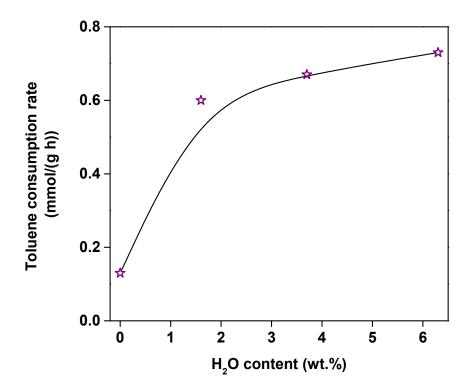
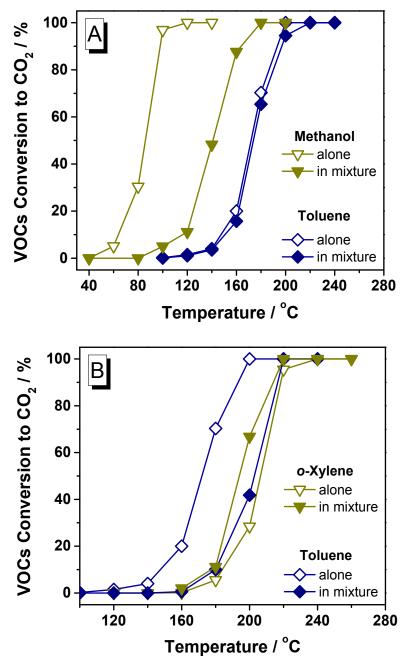


Fig. S6. Toluene consumption rates versus  $H_2O$  content of the C3M1-R catalyst.



**Fig. S7.** (A) Comparison of toluene and methanol conversion alone or in mixture over the C3M1-R catalyst (Toluene alone: 500 ppm toluene/1.6 wt.% H<sub>2</sub>O/10 vol.% O<sub>2</sub>/N<sub>2</sub>; methanol alone: 1000 ppm methanol/1.6 wt.% H<sub>2</sub>O/10 vol.% O<sub>2</sub>/N<sub>2</sub>; mixture of the two VOCs: 500 ppm toluene + 1000 ppm methanol/1.6 wt.% H<sub>2</sub>O/10 vol.% O<sub>2</sub>/N<sub>2</sub>, GHSV = 67,500 h<sup>-1</sup>); (B) Comparison of toluene and *o*-xylene conversion alone or in mixture over the C3M1-R catalyst (Toluene alone: 500 ppm toluene/1.6 wt.% H<sub>2</sub>O/10 vol.% O<sub>2</sub>/N<sub>2</sub>; *o*-xylene alone: 500 ppm *o*-xylene/1.6 wt.% H<sub>2</sub>O/10 vol.% O<sub>2</sub>/N<sub>2</sub>; mixture of the two VOCs: 500 ppm *o*-xylene/1.6 wt.% H<sub>2</sub>O/10 vol.% O<sub>2</sub>/N<sub>2</sub>; mixture of the two VOCs: 500 ppm toluene + 500 ppm *o*-xylene/1.6 wt.% H<sub>2</sub>O/10 vol.% O<sub>2</sub>/N<sub>2</sub>; GHSV = 67,500 h<sup>-1</sup>).