

Supporting Information for:

**Prototype reactor for highly selective solar-driven CO<sub>2</sub> reduction to synthesis gas using nanosized earth-abundant catalysts and silicon photovoltaics**

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## Experimental Details

### 1. Chemicals and Materials

Zinc sulfate pentahydrate ( $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ , 99.995% trace metals basis) was purchased from Merck Millipore; copper and nickel foams (2.5 mm and 1.6 mm thick, respectively) were purchased from Recemat BV; potassium hydrogen carbonate ( $\text{KHCO}_3$ , ACS purity >99.7%) was purchased from Merck Millipore. The laminating acrylic tape (0.075 mm thick) was purchased from Thorlabs, Inc. Electrolyte solutions were prepared with deionized water (DI- $\text{H}_2\text{O}$ , Ricca Chemical, ASTM Type I).

A bipolar membrane (fumasep FBM-type) was purchased from FuMA-Tech GmbH and kept in 1 M NaCl. The Nafion (N-117 membrane, 0.18 mm thick) was purchased from Alfa Aesar and kept in 0.5 M NaOH solution. A leak-free reference electrode (Ag/AgCl 3.4 M KCl) was purchased from Warner Instruments.

### Solar-to-Syngas Conversion Efficiency Calculation

Considering an active electrode area of  $10 \text{ cm}^2$  for  $\text{CO}_2\text{RR}$  and OER, respectively, the bias-free operation  $\text{CO}_2\text{RR}$  current of  $5 \text{ mA/cm}^2$ , which we measured (Fig. 5), corresponds to an electric charge of 50 mC, i.e.  $31.2 \cdot 10^{16}$  electrons (assuming 1 s of interval duration). These charges are used produced  $\text{H}_2$  and CO which both need 2 electrons to be formed. Over the course of the bias-free measurement, a faradaic efficiency of 76 % for the  $\text{H}_2$  production and 16 % for the CO production was measured. Consequently, for the number of molecules we can derive that:

$$0.76 * 31.2 * 10^{16} / 2 = 11.86 * 10^{16} \text{ molecules of } \text{H}_2 \text{ and}$$

$$0.16 * 31.2 * 10^{16} / 2 = 2.49 * 10^{16} \text{ molecules of CO were produced, which correspond to } 1.97 * 10^{-7} \text{ moles of } \text{H}_2 \text{ and } 4.15 * 10^{-8} \text{ moles of CO.}$$

Considering the respective molar masses, we obtain  $0.394 \mu\text{g}$  of  $\text{H}_2$  and  $1.16 \mu\text{g}$  of CO.

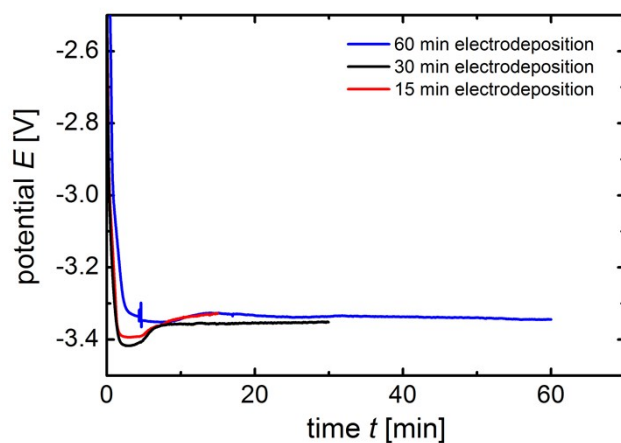
Taking into account the higher heat value (HHV) and lower heat value (LHV) for  $\text{H}_2$  and CO of  $286 \text{ kJ/mol}$  and  $283.5 \text{ kJ/mol}$ , respectively, the specific power of the produced products can be obtained as  $143330 \text{ kW/kg}$  for  $\text{H}_2$  and  $10125 \text{ kW/kg}$  for CO.

Using these values allows to calculate the total bias-free power output of the device.  $\eta_{\text{STS}}$  is given by

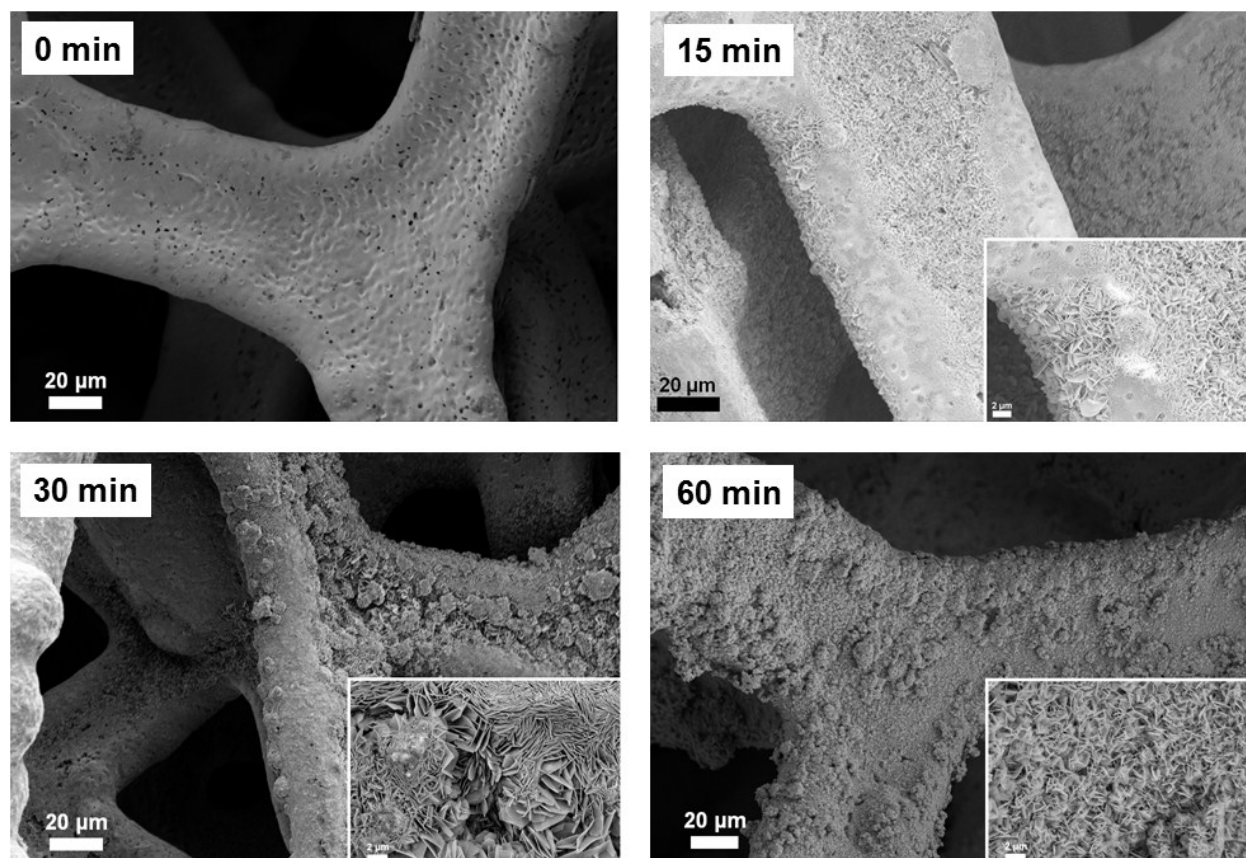
$$\eta_{\text{STS}} = \frac{0.394 \mu\text{g } \text{H}_2 \times 143330 \text{ kW/kg} + 1.16 \mu\text{g } \text{CO} \times 10125 \text{ kW/kg}}{\text{total integrated power input}}$$

where the input power (for  $16 \text{ cm}^2$  illuminated solar cell area) is the incident light intensity ( $1600 \text{ mW}$ ). Thus, the solar-to-syngas efficiency of our device was 4.26 %.

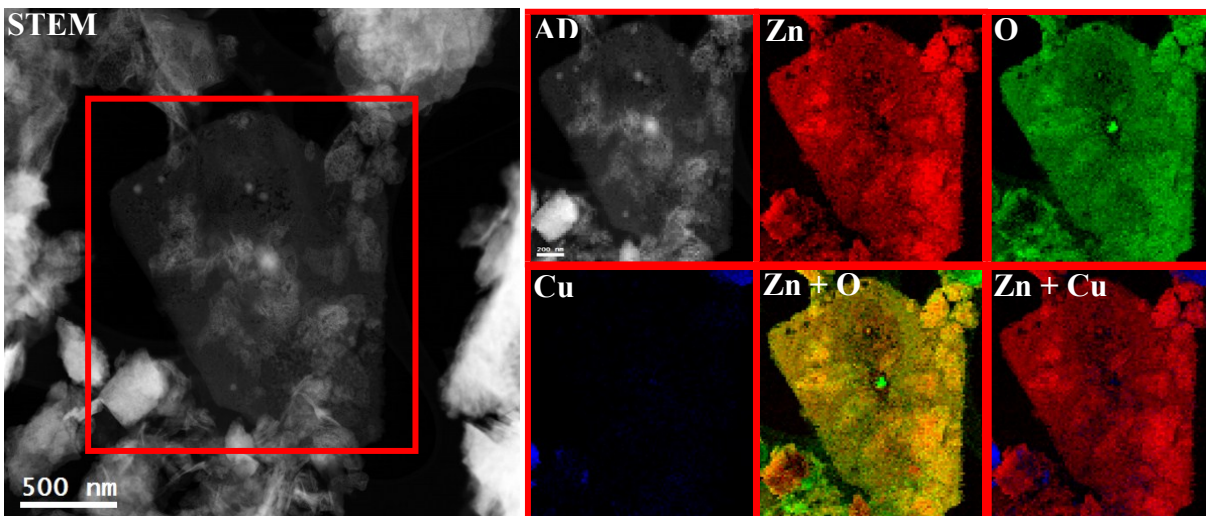
## Figures



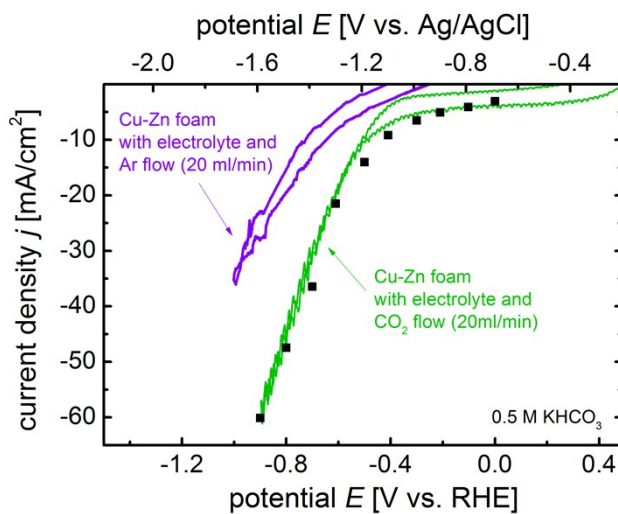
**Fig. S1** Potential-time curves during electrodeposition of Zn on Cu-foams at  $-40$  mA.



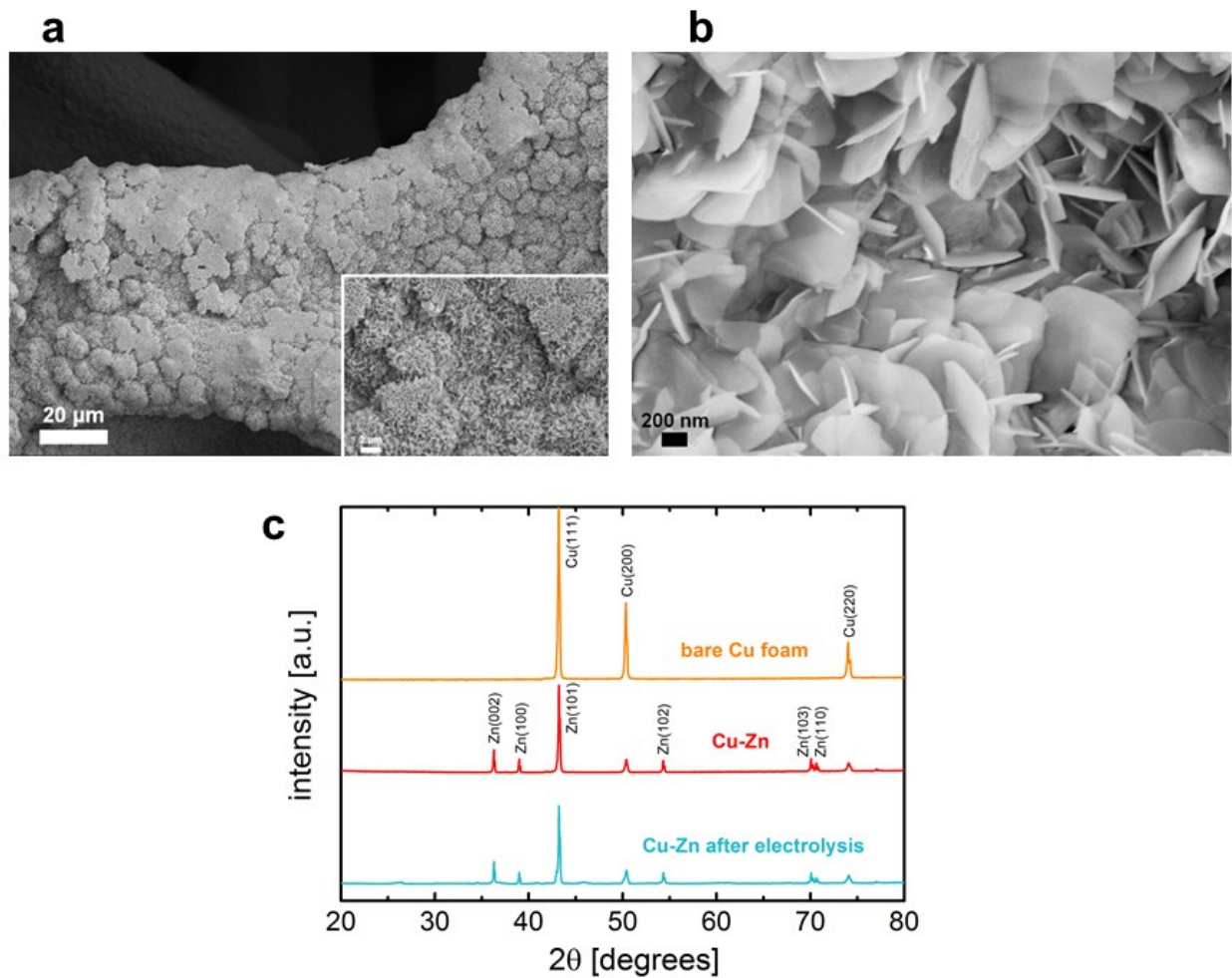
**Fig. S2** SEM images of a bare Cu foam (low magnification) and of the Zn catalyst coated Cu-foam after electrodeposition for 15, 30, and 60 minutes, respectively (low and high magnification).



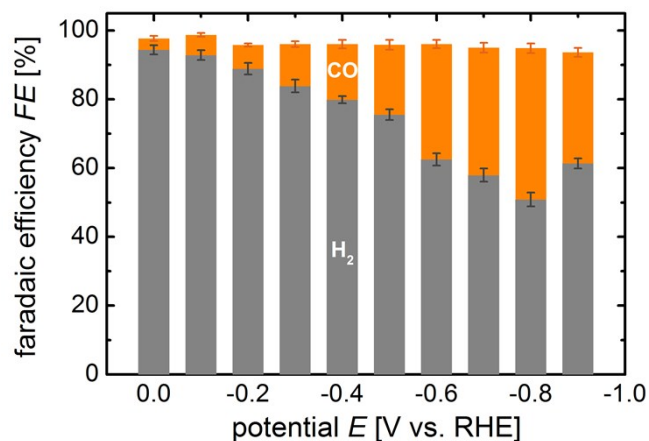
**Fig. S3** Low magnification EELS chemical composition maps obtained from the red rectangular area on the ADF-STEM micrograph. Individual Zn (red), O (green), Cu (blue) maps and their composite.



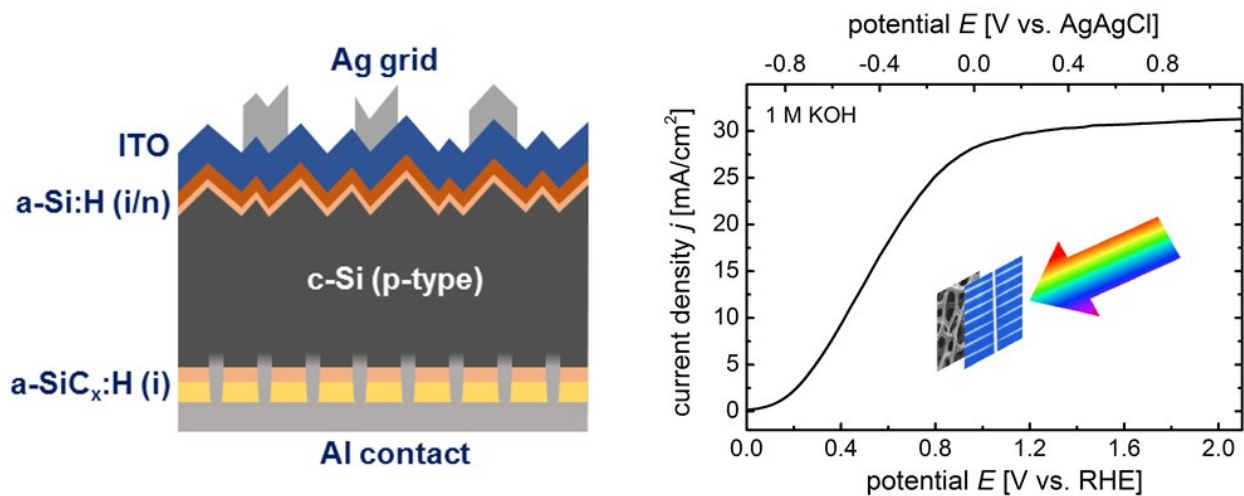
**Fig. S4** Cyclic voltammetry (CV) curves of Cu-foam decorated cathodes measured in the filter-press cell with electrolyte flow (20 ml/min) and CO<sub>2</sub> (green curve) or Ar (purple curve) flow (20 ml/min). The electrolyte was 0.5 M KHCO<sub>3</sub> in both measurements, which were conducted at a scan rate of 10 mV/s. The black squares represent the average current density values from hour-long potentiostatic experiments carried out at different applied potentials (see Fig. 4(a)).



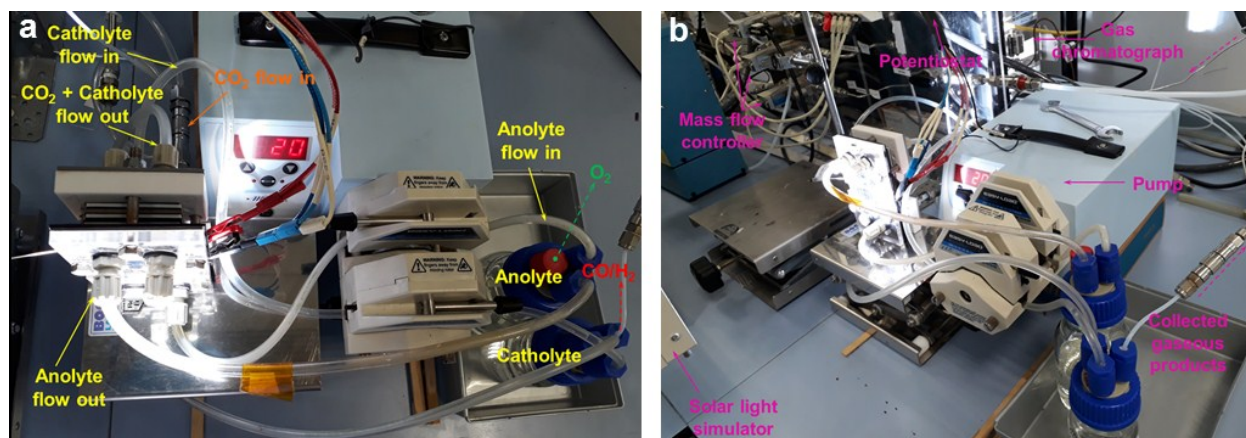
**Fig. S5** (a) SEM image of the Cu-Zn cathode after CO<sub>2</sub>RR at -0.8 V<sub>RHE</sub> for one hour. (b) With high magnification. (c) XRD pattern of the bare Cu-foam, of the as-prepared Cu-Zn cathode, and of the Cu-Zn cathode after one hour electrolysis.



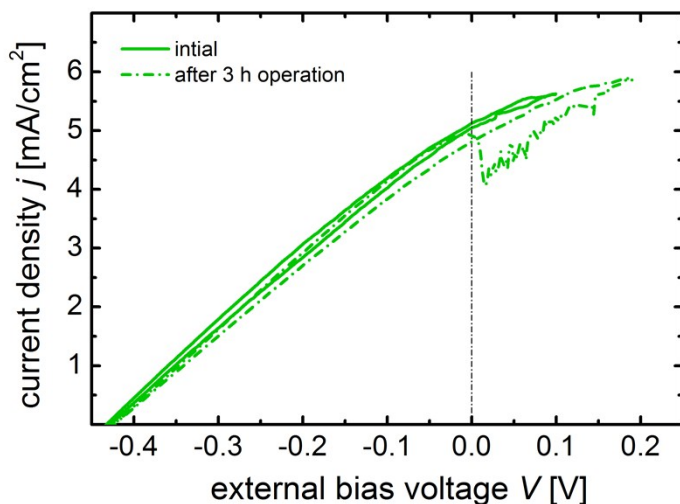
**Fig. S6** Faradaic efficiencies of CO and H<sub>2</sub> production from CO<sub>2</sub>RR at different potentials for a flat Zn foil cathode measured in 0.5 M KHCO<sub>3</sub>. The error bars are standard deviations obtained from 3 experimental repeats. All measurements were conducted at a CO<sub>2</sub> and electrolyte flow rate of 20 ml/min.



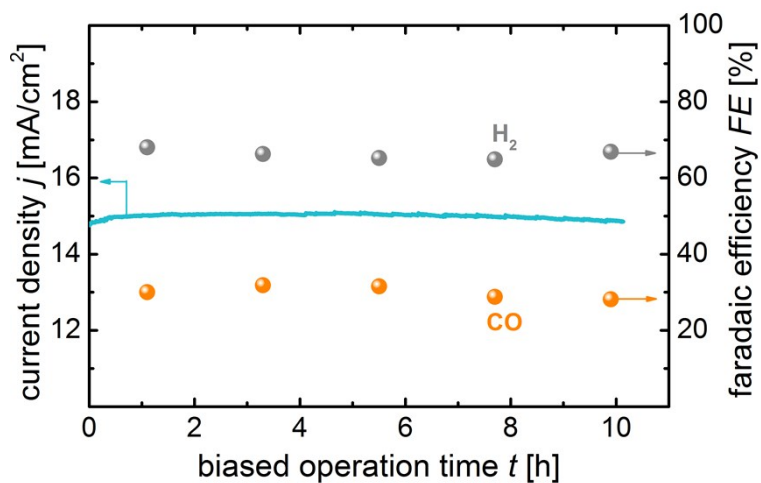
**Fig. S7** Left: Schematic drawing of the layer stack used for the deposition of Si heterojunction solar cells. Right: Linear sweep measurement of the Si/Ni foam photoanode in 1 M KOH solution under 100 mW/cm<sup>2</sup> of simulated AM1.5 illumination. The inset illustrates the Si/Ni foam photoanode structure under illumination. Details on the fabrication of the Si heterojunction solar cells can be found in Supplementary Ref. 1.



**Fig. S8** Photographs of the prototype reactor device under operation. (a) Prototype reactor device under continuous flow and illumination. Catholyte and anolyte flows are highlighted. (b) Complete set-up for the solar CO<sub>2</sub> conversion experiments comprising mass flow controller, solar light simulator, potentiostat, gas chromatograph, and the reactor device, shown in more detail in Fig.1 and Fig. S8(a).



**Fig. S9** Two-electrode current density-voltage characteristics with a Si heterojunction solar cell/Ni foam photoanode and a Zn catalyst coated Cu foam cathode in a bipolar membrane configuration using 1 M KOH as anolyte and 0.5 M KHCO<sub>3</sub> as catholyte solution. The measurements were conducted under simulated AM1.5 illumination at a scan rate of 10 mV/s before and after the bias-free stability testing. The illuminated area of the PV cells was 16 cm<sup>2</sup>, while the active electrode/liquid areas of the cathode and anode were 10 cm<sup>2</sup>.



**Fig. S10** Operation of the prototype solar CO<sub>2</sub> conversion reactor (see Fig. 1) as a function of the operation time under an applied bias potential of 1.7 V. Left y-axis: Solar-driven CO<sub>2</sub>RR current density (normalized to the area of the electrodes in contact with the electrolyte; 10 cm<sup>2</sup>) as a function of the operational time using a photoanode based on two Si HIT cells and Ni foam catalyst and a Cu-Zn cathode in a biased two-electrode 0.5 M KHCO<sub>3</sub>/BPM/1 M KOH configuration under simulated AM1.5G illumination. Right y-axis: Faradaic efficiencies of H<sub>2</sub> and CO production as a function of the operation time.

**Supplementary Reference:**

[1] M. Colina, A. Belén Morales-Vilches, C. Voz, I. Martín, P. R. Ortega, and R. Alcubilla, IEEE J. Photovolt., 2015, **5**, 805-811.