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1	Supporting Information
2	Direct use of humic acid mixtures to construct efficient Zr-
3	containing catalysts for Meerwein-Ponndorf-Verley reactions
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	Catalysts	H donor	<b>Reaction conditions</b>	C./%	Y./%	S./%	Refs.
1	Zr-HAs	IPA	70 °C,9 h, IPA	97.3	80.4	82.6	This work
2	Zr-HAs	IPA	50 °C, 15 h, IPA	97.2	97.2	>99	This work
3	Zr-PhyA	IPA	100 °C, 2 h, IPA	99.3	99.3	100.0	1
4	Zr-SBA-15	IPA	90 °C, 6 h, IPA	65.0	45.0	69.2	2
5	ZrPN	IPA	100 °C, 15h, IPA	93.0	90.0	96.8	3
6	γ-Fe <sub>2</sub> O <sub>3</sub> @HAP	IPA	180°C, 3 h, IPA	96.2	91.7	95.3	4
7	Ni-Cu/Al <sub>2</sub> O <sub>3</sub>	IPA	200 °C, 4h, IPA	95.4	95.4	100	5
8	MgO	IPA	170 °C, 5 h, IPA	100.0	74.0	74.0	6
9	Fe/NC	IPA	160 °C, 15h, IPA	91.6	76.0	83.0	7
10	Ru/Uio-66	$H_2$	20 °C, H <sub>2</sub> 0.5 MPa, 4h, H <sub>2</sub> O	94.9	94.9	100	8
11	Ru(II) complex	$H_2$	85 °C, H <sub>2</sub> 1 MPa, 2h, Ethanol	100.0	93.0	93.0	9
12	Pt(5 wt%)/Al2O3	$H_2$	25 °C, H <sub>2</sub> 2 MPa, 8 h, in IPA	95.5	90.7	95.0	10
13	$Pt/\gamma$ - $Al_2O_3$	$H_2$	50 °C, 1 atm, 7h, in methanol	80.0	79.2	99.0	11
14	5%Pt/TECN	$H_2$	100 °C, H <sub>2</sub> 1 MPa, 5 h, H <sub>2</sub> O	100.0	99.0	99.0	12
15	Au/TiO <sub>2</sub>	CO/H <sub>2</sub> O	90 °C, 4 MPa CO	100.0	100.0	100.0	13
16	Fe(NiFe)O <sub>4</sub> -SiO <sub>2</sub>	$H_2$	90 °C, H <sub>2</sub> 2MPa, 4h, Heptane	94.3	94.3	100.0	14
17	Co/SBA-15	$H_2$	150 °C, 2MPa H <sub>2</sub> ,1.5h,	95.0	91.2	96.0	15
18	Capped Ni	$H_2$	110 °C, H <sub>2</sub> , 3 MPa, 3 h, IPA	96.6	91.8	95.0	16
19	Ni-Sn/AlOH	$H_2$	180 °C, H <sub>2</sub> 3 MPa, 1 h, IPA	98.0	94.0	95.9	17
20	5 wt%Ni/NDC	$H_2$	200 °C, H <sub>2</sub> 1MPa,5h, IPA	96.0	91.2	95.0	18
21	CuNi/MgAlO	$H_2$	100 °C, H <sub>2</sub> 4MPa, 4 h, IPA	99.0	98.0	99.0	19
22	CuO-Cr <sub>2</sub> O <sub>3</sub>	$H_2$	200 °C, $H_2$ 6 Mpa, 3 h, Octane	75.0	64.5	86.0	20

**Table S1.** Comparison of Zr-HAs<sup>C</sup> catalyst with different catalysts in typical literatures.<sup>*a*</sup>

2 <sup>a</sup>C., conversion of furfural; Y., Yield of FA; S., Selectivity of FA.



Figure S1. TG analysis of the Zr-HAs<sup>C</sup> catalyst



Figure S2. Comparison of the freshly prepared and recycled Zr-HAs<sup>C</sup> catalysts after nine reuses.
 SEM of the fresh (a) and recycled Zr-HAs<sup>C</sup> (b), XRD spectra (c), and FTIR patterns (d).



2 Figure S3. Characterization of the extracted HAs and corresponding Zr-HAs<sup>E</sup> catalyst. SEM-EDS
3 of the extracted HAs (a, b) and Zr-HAs<sup>E</sup> catalyst (c, d), FTIR spectra (e) and XRD patterns (f).

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In the IR spectra of Zr-HAs<sup>E</sup>, the peak at 1708 cm<sup>-1</sup> assigned to the C=O bond 4 vibration in the carboxylic acid groups became much weaker compared to that of 5 HAs<sup>E</sup>, indicating that the carboxylic acid groups were converted into their metal salt 6 form after interaction with Zr<sup>4+, 21, 22</sup> HAs<sup>E</sup> and Zr-HAs<sup>E</sup> also displayed the 7 characteristic asymmetric (HAs<sup>E</sup>, 1603 cm<sup>-1</sup>; Zr-HAs<sup>E</sup>, 1579 cm<sup>-1</sup>) and symmetric 8 vibrations (HAs<sup>E</sup>,1370 cm<sup>-1</sup>; Zr-HAs<sup>E</sup>, 1413 cm<sup>-1</sup>) of carboxylate groups. Compared 9 with the IR spectrum of HAs<sup>E</sup>, the wavenumber difference of asymmetric and 10 symmetric vibrations of carboxylate anions in Zr-HAs<sup>E</sup> was narrowed from 233 cm<sup>-1</sup> 11 12 to 16 cm<sup>-1</sup>, which indicated that carboxylate groups were coordinated to  $Zr^{4+}$  ions.<sup>23, 24</sup>

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