

Supporting Information

Adsorptive Removal of Ciprofloxacin by Ethylene Diaminetetraacetic Acid/ β -cyclodextrin Composite from Aqueous Solution

Yu Fei^{a, c§}, Chen Dexian^{a§}, Ma Jie^{b, d*}

^a *School of Chemical and Environmental Engineering, Shanghai Institute of
Technology, 100 Hai Quan Road, Shanghai 201418, P.R. China*

^b *Shanghai Institute of Pollution Control and Ecological Security, Shanghai, 200092,
P.R. China*

^c *College of Ecology and Environment, Shanghai Ocean University, Shanghai 201306,
P.R. China*

^d *Key Laboratory of Yangtze River Water Environment, College of
Environmental Science and Engineering, Tongji University, 1239 Siping Road,
Shanghai 200092, P.R. China*

1. Adsorption kinetic models

The pseudo-first-order model is as follows:

$$\log(q_e - q_t) = \log q_e - k_1 t$$

where q_t and q_e (mg/g) are the amount of CPX adsorbed per unit mass of adsorbent at any time t (min) and equilibrium, respectively. k_1 (min^{-1}) is the rate constant of pseudo-first-order model.

The pseudo-second-order kinetic model is as follows:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t$$

where k_2 (g/mg min) is the rate constant of pseudo-second-order model.

2. Adsorption isotherm models

The nonlinear forms of Langmuir and Freundlich models were expressed as follows:

$$q_e = \frac{q_m k_l c_e}{1 + k_l c_e}$$
$$q_e = K_f + C_e^{\frac{1}{n}}$$

where C_e and q_e are the concentrations of adsorbate in water and the amount of adsorbate adsorbed to adsorbent when the adsorption equilibrium is reached, respectively. q_m is the maximum adsorption capacity, and K_l is Langmuir constant (L/mg) related to the energy of adsorption and the affinity of the binding sites. Moreover, K_f are Freundlich constant, also known as capacity factor related to adsorption capacity $((\text{mg g}^{-1})(\text{L mg}^{-1})^{1/n})$. $1/n$ related to adsorption intensity, which is a dimensionless empirical parameter.

In order to adequately study the adsorption mechanisms, the linear Dubinin Radushkevich (D-R) isotherm model was chosen and exhibited as follows:

$$\ln q_e = \ln q_m - B \varepsilon^2$$

where B is a constant related to the mean free energy of adsorption ($\text{mol}^2 \text{kJ}^{-2}$), q_m is the theoretical saturation capacity (mg g^{-1}), and ε is the Polanyi value, which can be calculated from eq 7:

$$\varepsilon = RT \ln\left(1 + \frac{1}{c_e}\right)$$

where R (J mol⁻¹ K⁻¹) is thermal equilibrium constant and T(K) is the absolute temperature.