# Colloidal Nanoparticle Size Control: Experimental and Kinetic Modeling Investigation of the Ligand-Metal Binding Role in Controlling the Nucleation and Growth Kinetics

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**Palladium (II)** Acetate Recrystallization. 0.75 g palladium acetate  $(Pd(OAc)_2)$  was dissolved in 40 mL anhydrous acetic acid under stirring in a flask. After palladium acetate could not dissolve further, the solution temperature was increased to 100 °C until all the palladium acetate was dissolved. Then the solution was quickly filtered. The filtrate was transferred into glass vials, and cooled down slowly to room temperature overnight in a water bath. After the palladium acetate crystal formed, we separated the solution from the crystal. Washed the crystal with small amount of hexane to remove the acid residual, and dried the crystal through nitrogen flow overnight. The crystal product was stored in the nitrogen glovebox for further use.

**Trioctylphosphine (TOP) Distillation.** The trioctylphosphine was distilled under nitrogen atmosphere under low vacuum. The distillate above 192 °C was collected, and stored in the glovebox.

**Ex-situ Small-angle X-ray Scattering (SAXS) Experiments.** Ex-situ SAXS measurements were performed on Bruker N8 Horizon equipped with Cu (K $\alpha$  radiation,  $\lambda = 1.54$  Å) source, 2D VÅNTEC-500<sup>TM</sup> detector and SCATEX<sup>TM</sup> scatter-free pinholes. The colloidal nanoparticle solution samples were loaded in sealed quartz capillaries (d = 1.5 mm or 2.0 mm). For absolute scale calibration, water was used as the standard liquid. All the measurements were taken in vacuum (2 mbar) at room temperature. Data processing and analysis were performed using Bruker SAXS software. The spectra were fitted using Schultz size distribution model.

# **TEM Results.**



**Figure S1.** TEM images of Pd nanoparticles in (a) toluene and (b) pyridine. The average particle sizes in toluene and pyridine were  $1.8\pm0.4$  and  $4.3\pm0.5$  nm, respectively. Reaction conditions:  $10 \text{ mM Pd}(OAc)_2$  in 50:50 solvent:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.

SAXS Spectra.



**Figure S2.** a) Original SAXS data after absolute scaling and Schultz polydisperse spherical model fitting at different reaction times; b) The temporal evolution of the number of particles and their average size in pyridine. Reaction conditions: 10 mM Pd(OAc)<sub>2</sub> in 50:50 pyridine:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.



**Figure S3**. Polydispersity as a function of time. Reaction conditions: 10 mM  $Pd(OAc)_2$  in 50:50 solvent:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.

**Damköhler Number (Da).** The ratio of reaction rate to the diffusion rate, Da, can be estimated as  $Da \approx (\frac{k_{growth} \times [A]}{D_{AB}}) \times r^2$ .<sup>1</sup>  $D_{AB}$  is the diffusion coefficient of Pd(II) complex in toluene or pyridine solutions that can

be calculated using Stokes-Einstein equation<sup>2</sup> ( $D_{AB} = \frac{k_B T}{6\pi\mu R_{eff}}$ , where  $k_B$ , T,  $R_{eff}$  and  $\mu$  are the Boltzmann constant,

the absolute temperature, the effective radius of the diffusing molecule (in our case Pd(II) complex binding with TOP), and the solvent viscosity, respectively), [A] is the concentration of Pd(II) that will be reduced on the nanoparticle surface,  $k_{growth}$  is the growth rate constant, and r is the radius of the growing particle. The Da for the nanoparticles having a radius of 1 nm was ~10<sup>-8</sup> which indicates that the growth is not diffusion limited.

**Extracting nucleation and growth rates from the model and in-situ experimental data.** From the kinetic model, the nucleation and Growth/Nucleation rates can be calculated as follows

Nucleation rate = 
$$\frac{k_{1-nuc} \lfloor A \rfloor}{m} \times N_A$$
 (#nuclei/lit.s) (1A)

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Nucleation rate = 
$$k_{1-nuc} [A]$$
 (mol/lit.s) (1P)

Growth rate = 
$$k_{2-growth} [A] [B]$$
 (mol/lit.s) (2P)

$$\left(\frac{\text{Growth}}{\text{Nucleation}}\right)_{\text{model}} = \frac{k_{2-growth} \left[A\right] \left[B\right]}{k_{1-nuc} \left[A\right]} = \frac{k_{2-growth} \left[B\right]}{k_{1-nuc}} \quad \text{(unitless)}$$
(2A)

Specifically, the nucleation rate calculated in equation (1A) is the number of nuclei per unit volume per unit time (#nuclei/lit.s). However, to compare the rates of growth and nucleation, it is required that both have the same units (i.e. mol/lit.s). Therefore, the nucleation rate used in equation (1P) does not include m or avogadro's number so the units become mol/lit.s.

Using the experimentally measured number of particles ( $N_{P-\exp}$ ), the nucleation rate at a short time interval ( $\Delta t$ ) can be estimated through:

Nucleation rate (exp)=
$$\frac{\Delta N_{P-exp}}{\Delta t}$$
 (3A)

By estimating the rate of nucleation, the growth rate can be extracted from the slope of total number of atoms in all formed nanoparticles ( $Y_{exp}$ ).  $Y_{exp}$  includes the total number of Pd atoms that contribute to form nuclei and assist with the particle growth (both nucleation and growth events). Therefore,

Growth rate (exp) = 
$$\frac{\Delta Y_{exp}}{\Delta t} - (\frac{\Delta N_{P-exp}}{\Delta t} \times \frac{m}{N_A})$$
 (4A)

The dimensionless Growth/Nucleation rate can be written as follows:

$$\left(\frac{\text{Growth}}{\text{Nucleation}}\right)_{\exp} = \frac{\frac{\Delta Y_{\exp}}{\Delta t} - \left(\frac{\Delta N_{P-\exp}}{\Delta t} \times \frac{m}{N_A}\right)}{\left(\frac{\Delta N_{P-\exp}}{\Delta t} \times \frac{m}{N_A}\right)} = \frac{\frac{\Delta Y_{\exp}}{\Delta t} - 1}{\left(\frac{\Delta N_{P-\exp}}{\Delta t} \times \frac{m}{N_A}\right)}$$
(5A)

The number of particles per liter of solution  $N_p$  can be determined through the integration of the nucleation rate (equation 1A) and considering the number of atoms per nucleus (*m*) as shown below:

$$N_p = \int_0^{t_f} \frac{k_{1-nuc} \left[A\right] N_A}{m} dt$$
(6A)

The smallest measured nanoparticle size using SAXS at the early stage of the reaction was about  $0.6\pm0.3$  nm. Therefore, in the absence of other information on the size of the nucleus, we assumed that the nucleus consists of 4 atoms. There have been a wide range of reported values for atoms/nucleus for different metals including 4 (Pt)<sup>3</sup>, 6 (Ir)<sup>4</sup>, 9 (Au)<sup>5</sup>, 10 (Au)<sup>6</sup>.

For Pt, Pd and other fcc metals, to form the 1<sup>st</sup> shell it needs 13 atoms in total<sup>7</sup>, which is 0.8 nm. For a nucleus, it is possible that the nucleus consists of fewer atoms than a full first shell.

**Estimation of nucleation and growth rate constants from the in-situ experimental data.** As discussed above the nucleation and growth rates can be estimated from the experiment. Therefore, the nucleation rate at the early stage is used to estimate the nucleation rate constant as shown below:

Nucleation rate (exp) =  $\frac{k_{1-nuc} [A] N_A}{m}$  where [A] is the precursor concentration. In the case of 10 mM Pd(OAc)<sub>2</sub>

in toluene:

$$\begin{cases} \left[A\right] = \left[A\right]_{0} = 10^{-2} \text{ M}, & k_{1-nuc} \text{ (lower limit)} \approx 10^{-5} \text{ s}^{-1} \\ \\ \left[A\right] = 0.001 \left[A\right]_{0} = 10^{-5} \text{ M}, & k_{1-nuc} \text{ (upper limit)} \approx 10^{-2} \text{ s}^{-1} \end{cases}$$

when

Growth rate (exp) =  $k_{2-growth} [A] [B]$ , where [B] is the uncapped Pd surface atom.

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$$B] = 0.001 [A]_0 \quad (assuming [BL]=0)$$

## Ligand-based model:

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**Reactions:** 

$$A \xrightarrow{k_{1-nuc}} B \tag{9}$$

$$A + B \xrightarrow{k_{2-growth}} 2B \tag{10}$$

$$A + L \xleftarrow{k_{3-f}, K_{5-eq}} AL \tag{11}$$

$$B + L \xleftarrow{k_{4-f}, K_{6-eq}}{BL}$$
(12)

#### **Differential Equations:**

$$\frac{d[A]}{dt} = -k_{1-nuc} [A] - k_{2-growth} [A] [B] - k_{3-f} [A] [L] + \frac{k_{3-f}}{K_{5-eq}} [AL]$$

$$\frac{d[B]}{dt} = k_{1-nuc} [A] + k_{2-growth} [A] [B] - k_{4-f} [B] [L] + \frac{k_{4-f}}{K_{6-eq}} [BL]$$

$$\frac{d[L]}{dt} = -k_{3-f} [A] [L] + \frac{k_{3-f}}{K_{5-eq}} [AL] - k_{4-f} [B] [L] + \frac{k_{4-f}}{K_{6-eq}} [BL]$$

$$\frac{d[AL]}{dt} = k_{3-f} [A] [L] - \frac{k_{3-f}}{K_{5-eq}} [AL]$$

$$\frac{d[BL]}{dt} = k_{4-f} [B] [L] - \frac{k_{4-f}}{K_{6-eq}} [BL]$$

**Initial Conditions:** 

	$[A]_0$	$[L]_0$	$[B]_0$	$[AL]_0$	$[BL]_0$
Initial conditions	10 mM	20 mM	0	0	0

**Model Assumptions:** As stated in the manuscript, the model assumes that all the atoms added to the nanoparticles during growth (or during nucleation) to be surface atoms, which introduces errors in the rate constants for equations 9 and 10. To account for the size increase, the autocatalytic reaction,  $A+B \rightarrow 2B$  should be more accurately written as  $A+B \rightarrow (1+X_{growth})B$ , where  $X_{growth}$  is the ratio of increase in surface sites divided by the increase in total number of atoms in the nanoparticle. While assuming  $(1+X_{growth})=2$  is not accurate, it is not expected to significantly affect the results since the effect of incorporation in the core during growth does not become important until larger sizes. For example, for increase in number of atoms in the cluster from 1 atom to 13 atoms (0.3 to 0.8 nm) vs. from 923 to 1415 atoms (3.5 to 4.1 nm), X<sub>growth</sub> changes from 0.92 to 0.28. Therefore, instead of  $A+B \rightarrow 2B$  as assumed in equation 10,  $(1+X_{growth})$ , should be between ~1.3-1.9 which is not that large of an error compared to the value of 2 used in the model. Accounting for  $X_{growth}$  as a variable during growth, requires a different type of modeling approach (it is a cumulative error that propagates as the size increases). Therefore, while the simplification is not very accurate, it is needed; otherwise, the number of model parameters becomes intractable.

In our system the effect of this simplification should be more pronounced in the case of pyridine (where the nanoparticles are larger) than toluene which is likely why the model deviation and calculated errors are more pronounced for pyridine. In addition, we need to state that in pyridine the nanoparticles grow very fast and at ~120 seconds the size is already larger than 2.5 nm (see Figure S2). Therefore, the estimated value of  $k_{growth}$  (which is the average over the entire reaction time) to a great extent is weighted toward larger particle size (lower percentage of

surface sites) where  $(1 + X_{growth})$  is between 1.3 and 1.5. Therefore, this assumption cannot have a significant effect on our modeling results but will affect the absolute value of  $k_{growth}$ , which should be larger to account for the lower  $X_{growth}$ .

**Extended ligand-based model**. We considered other possible reactions that can occur during the formation of Pd nanoparticles. We expanded the ligand-based model by adding the following reactions: nucleation through ligand-precursor complex (AL), reversible reaction of ligand with the AL (i.e.  $AL_2$ ), and autocatalytic surface growth through reduction of AL on the particle surface. The reactions in model system are shown below:

## **Extended ligand-based model:**

#### **Reactions:**

$$A \xrightarrow{k_{1-nuc}} B \tag{a}$$

$$AL \xrightarrow{k_{2-nuc+cap}} BL$$
 (b)

$$A + L \xleftarrow{k_{3-f}, K_{8-eq}} AL \tag{c}$$

$$AL + L \xleftarrow{k_{4-f}, K_{9-eq}} AL_2 \tag{d}$$

$$B + L \xleftarrow{k_{5-f}, K_{10-eq}} BL \tag{e}$$

$$A + B \xrightarrow{k_{6-growth}} 2B \tag{f}$$

$$AL + B \xrightarrow{k_{7-growth+cap}} B + BL$$
 (g)

#### **Differential Equations:**

$$\begin{aligned} \frac{d[A]}{dt} &= -k_{1-nuc} \left[ A \right] - k_{6-growth} \left[ A \right] \left[ B \right] - k_{3-f} \left[ A \right] \left[ L \right] + \frac{k_{3-f}}{K_{8-eq}} \left[ AL \right] \\ \frac{d[B]}{dt} &= k_{1-nuc} \left[ A \right] + k_{6-growth} \left[ A \right] \left[ B \right] - k_{5-f} \left[ B \right] \left[ L \right] + \frac{k_{5-f}}{K_{10-eq}} \left[ BL \right] \\ \frac{d[L]}{dt} &= -k_{3-f} \left[ A \right] \left[ L \right] + \frac{k_{3-f}}{K_{8-eq}} \left[ AL \right] - k_{4-f} \left[ AL \right] \left[ L \right] + \frac{k_{4-f}}{K_{9-eq}} \left[ AL_2 \right] - k_{5-f} \left[ B \right] \left[ L \right] + \frac{k_{5-f}}{K_{10-eq}} \left[ BL \right] \\ \frac{d[AL]}{dt} &= -k_{2-nuc+cap} \left[ AL \right] + k_{3-f} \left[ A \right] \left[ L \right] - \frac{k_{3-f}}{K_{8-eq}} \left[ AL \right] - k_{4-f} \left[ AL \right] \left[ L \right] + \frac{k_{4-f}}{K_{9-eq}} \left[ AL_2 \right] - k_{7-growth+cap} \left[ AL \right] \left[ B \right] \\ \frac{d[AL]}{dt} &= k_{4-f} \left[ AL \right] \left[ L \right] - \frac{k_{4-f}}{K_{9-eq}} \left[ AL_2 \right] \\ \frac{d[BL]}{dt} &= k_{2-nuc+cap} \left[ AL \right] + k_{5-f} \left[ B \right] \left[ L \right] - \frac{k_{5-f}}{K_{10-eq}} \left[ BL \right] + k_{7-growth+cap} \left[ AL \right] \left[ B \right] \end{aligned}$$

**Initial Conditions:** 

	$[A]_0$	$[L]_0$	$[B]_0$	$[AL]_0$	$\left[AL_2\right]_0$	$\begin{bmatrix} BL \end{bmatrix}_0$
Initial conditions	10 mM	20 mM	0	0	0	0

We should note that more than one TOP can bind to the Pd(OAc)<sub>2</sub> precursor which is considered in the extended ligand-based model. However, thermodynamic studies conducted for PdCl<sub>2</sub> (and likely other Pd complexes such as Pd(OAc)<sub>2</sub>) demonstrated that the equilibrium binding constant for the second TOP binding ( $AL + L \xleftarrow{K_{eq-2}} AL_2$ ) is around two orders of magnitude lower than for the first binding ( $A + L \xleftarrow{K_{eq-1}} AL$ ).<sup>8</sup> This experimental report<sup>8</sup> was also in good agreement with our modeling result. Therefore, it is reasonable to account only for the first TOP binding in the kinetic model.

Estimation of Model Parameters. The forward reaction rate constants  $(k_f)$  and equilibrium constants  $(K_{eq}$ , reverse rate constants were constrained by thermodynamics, i.e.  $k_r = \frac{k_f}{K_{eq}}$  were estimated by simultaneously minimizing

the sum of normalized squared errors between the model and experiments for  $N_p$  (number of particles) and Y (total number of atoms in all formed nanoparticles) in Matlab (using *fminsearch*). The sum of normalized squared errors, J, is expressed as:

$$J = \min\left(\sum_{i=1}^{\lambda} \left(\frac{Y_{\exp} - Y_{\text{model}}}{Y_{\exp}}\right)^2 + \sum_{i=1}^{\lambda} \left(\frac{N_{P-\exp} - N_{P-\text{model}}}{N_{P-\exp}}\right)^2\right)$$
(7A)

where  $\lambda$  is the number of data points. To calculate *J* without bias based on the number of points collected at early versus later reaction times, the data points were selected to yield an even distribution along both the x-axis (time) and y-axis ( $N_p$  or *Y*). Also, due to the non-linearity of kinetic models, there might not be a unique set of parameters.<sup>9</sup> Therefore, we implemented a parameter space search to find multiple parameter sets that can reasonably capture the in-situ data. To discriminate between different kinetic models (for models having different number of parameters), the normalized posterior probability<sup>10</sup> was calculated for each individual model. The kinetic model with the highest probability value is statistically the most likely model.<sup>9, 10</sup>

**Model Discrimination.** The posterior probability of each model candidate based on Bayesian analysis can be written as follows:<sup>10</sup>

$$P(N_j | \mathbf{Z}, \sigma) \alpha 2^{\frac{-P_j}{2}} P(N_j) \exp(\frac{-S'_j}{2\sigma^2})$$
(1B)

where  $P(N_j | Z, \sigma)$  is the posterior probability of model  $N_j$  for data Z with variance of  $\sigma$ ,  $P_j$  the number of parameters estimated in the model  $N_j$ ,  $P(N_j)$  the prior probability, and  $S'_j$  the sum of residual squares. Normalization of the posterior probability over model candidates gives

$$\pi \left(N_{j} \middle| \mathbf{Z}, \sigma\right) = \frac{P\left(N_{j} \middle| \mathbf{Z}, \sigma\right)}{\sum_{\lambda} P\left(N_{\lambda} \middle| \mathbf{Z}, \sigma\right)}$$
(2B)

The model with the highest probability,  $\pi (N_i | \mathbf{Z}, \sigma)$ , is statistically the most likely model.

Model	$\pi \left( N_{j} \right  \mathbf{Z}, \sigma)$
Finke-Watzky (2 parameters)	0.31
Ligand-based model (6 parameters)	0.54
Extended ligand-based model (10 parameters)	0.15



**Figure S4.** Finke-Watzky model- considering only the total number of atoms (*Y*). The rate constants are  $k_{1-nuc} = 1.77 \times 10^{-4} \text{ s}^{-1}$  and  $k_{2-growth} = -6 \times 10^{-2} \text{ L.mol}^{-1} \text{ .s}^{-1}$ . Reaction conditions: 10 mM Pd(OAc)<sub>2</sub> in 50:50 toluene:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.



**Figure S5**. Finke-Watzky model- considering both the total number of atoms (*Y*) and number of particles (*N<sub>P</sub>*). The rate constants are  $k_{1-nuc} = 1.74 \times 10^{-5} \text{ s}^{-1}$  and  $k_{2-growth} = 2.5 \times 10^{-1} \text{ L.mol}^{-1} \text{ s}^{-1}$ . Reaction conditions: 10 mM Pd(OAc)<sub>2</sub> in 50:50 toluene:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.

## Ligand-based model (considering ligand interactions with both precursor and particle surface).

**Table S1.** The estimated rate constants extracted for three different sets of in-situ data in toluene. Reaction conditions:  $Pd(OAc)_2$  in 50:50 toluene:hexanol, T = 100 °C.

	k <sub>1-nuc</sub>	k <sub>2-growth</sub>	$k_{3-f}$ (A+L)	<i>k</i> <sub>4-<i>f</i></sub> ( <i>B</i> + <i>L</i> )	$K_{5-eq}$ (A+L)	$K_{6\text{-}eq}\ (B+L)$
Units	s <sup>-1</sup>	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup>	L.mol <sup>-1</sup>
10 mM Pd TOP:Pd=2	$2.45 \times 10^{-5}$	8.49×10 <sup>-1</sup>	7.9×10 <sup>-3</sup>	$2.1 \times 10^{-1}$	$2.18 \times 10^{1}$	$1.27 \times 10^{3}$
10 mM Pd TOP:Pd=1	$2.9 \times 10^{-5}$	8.39×10 <sup>-1</sup>	$4.2 \times 10^{-3}$	3×10 <sup>-1</sup>	$1.84 \times 10^{1}$	$1.2 \times 10^{3}$
25 mM Pd TOP:Pd=2	$1.8 \times 10^{-5}$	$10 \times 10^{-1}$	$4.7 \times 10^{-3}$	3×10 <sup>-1</sup>	$1.5 \times 10^{1}$	$1 \times 10^{3}$

Ligand-based Model (considering ligand interaction only with particle surface).



**Figure S6**. Ligand-based model (considering ligand interaction only with the particle surface). The rate constants are  $k_{1-nuc} = 1.7 \times 10^{-5} \text{ s}^{-1}$ ,  $k_{2-growth} = 2.5 \times 10^{-1} \text{ L.mol}^{-1} \text{.s}^{-1}$ ,  $k_{f-B+L} = 1.92 \times 10^{-2} \text{ L.mol}^{-1} \text{.s}^{-1}$ , and  $K_{eq-B+L} = 7.05 \text{ L.mol}^{-1}$ . Reaction conditions: 10 mM Pd(OAc)<sub>2</sub> in 50:50 toluene:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.

Growth/Nucleation ratio prediction in toluene using Finke-Watzky and ligand-based models.



**Figure S7**. Growth/Nucleation ratio using Finke-Watzky<sup>11</sup> and ligand-based models. Growth/Nucleation always increased with time in the case of Finke-Watzky two-step model. Reaction conditions:  $10 \text{ mM Pd}(OAc)_2$  in 50:50 toluene:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.

**Bound ligand to metal ratio in toluene.** Other important information that can be extracted from the model is bound ligand (this includes the ligand binding with both the precursor and Pd surface atoms) to metal ratio with respect to the reaction time. The bound-ligand/metal can be defined as:

$$\frac{\text{Bound ligand}}{\text{Metal}} = \frac{L_0 - L_{free}}{A_0}$$
(1C)

where  $L_0$  is the initial concentration of ligand (TOP),  $A_0$  the initial concentration of metal precursor, and  $L_{free}$  the concentration of free TOP. As shown in Figure S8, the bound-ligand/metal ratio increases with time.



**Figure S8.** Bound-ligand/metal ratio. Reaction conditions: 10 mM  $Pd(OAc)_2$  in 50:50 toluene:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.

Growth rates comparison in toluene and pyridine using ligand-based model.



**Figure S9**. Growth rates comparison in toluene and pyridine. Reaction conditions: 10 mM  $Pd(OAc)_2$  in 50:50 solvent:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.

**Predictive Synthesis.** To use the model for predicting the size under different conditions, we first extracted the size from the model assuming that the nanoparticles are monodisperse using the following equation:

$$D_{\text{model}} = \left(\frac{6 M_w N_{\text{avg}}}{\pi \rho N_A}\right)^{\frac{1}{3}} = \left(\frac{6 M_w}{\pi \rho}\right)^{\frac{1}{3}} \left(\frac{Y_{\text{model}}}{N_{p-\text{model}}}\right)^{\frac{1}{3}}$$
(1D)

where *Y* and  $N_p$  are the total number of atoms in all formed nanoparticles (mol/L) and the number of particles (per liter of solution), respectively. The mean number of atoms per particle  $N_{avg}$  in model is calculated by dividing the total number of atoms in all formed nanoparticles by the number of particles at any given time.



**Figure S10**. Prediction of size (left) and number of particles (right) as a function of time in toluene and pyridine using ligand-based. Reaction conditions:  $Pd(OAc)_2$  in 50:50 solvent:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.



**Figure S11**. Prediction of final particle size a function of TOP concentration in toluene and pyridine using ligandbased model. Reaction conditions: 10 mM Pd(OAc)<sub>2</sub> in 50:50 solvent:hexanol, T = 100 °C.

**Generality of the Ligand-Based Model.** In the case of Pd (Teranishi et al.<sup>12</sup>), we lowered the binding constant of ligand to the surface by 1-2 orders of magnitude as it is known that PVP is a much weaker capping ligand than TOP<sup>13</sup>, see Tables S1 and S2. With respects to thiol-Au system (Hostetler et al.<sup>14</sup>), thiol strongly binds to the surface of Au nanoparticles, which can affect the particle growth rate.<sup>15, 16, 17</sup> Additionally, thiols interact with the gold precursor and reduce Au(III) to Au(I).<sup>18, 19</sup> The Au(III)/Au(I) ratio in solution depends on the amount of thiol added to the system.<sup>6, 18, 19</sup> Therefore, we expect that the thiol binding to the nanoparticle surface and to the Au precursor will both be important in determining the final size.

**Table S2.** The rate constants used for prediction of final Pd particle size as a function of PVP:Pd ratio (experimental data was reported by Teranishi et al.<sup>12</sup>).

	k <sub>1-nuc</sub>	k <sub>2-growth</sub>	k <sub>3-f</sub>	<i>k</i> <sub>4-f</sub>	$K_{5-eq}$	K <sub>6-eq</sub>
			(A+L)	(B+L)	(A+L)	(B+L)
Units	s <sup>-1</sup>	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup>	L.mol <sup>-1</sup>
PVP-Pd	1.22×10 <sup>-6</sup>	8.49×10 <sup>-1</sup>	1.8×10 <sup>-2</sup>	2×10 <sup>-2</sup>	1.2	$4.2 \times 10^{1}$

**Table S3.** The rate constants used for prediction of final Au particle size as a function of thiol:Au ratio (experimental data was reported by Hostetler et al.<sup>14</sup>).

	$k_{1-nuc}$	$k_{2\text{-}growth}$	<i>k</i> <sub>3-f</sub>	$k_{4-f}$	$K_{5-eq}$	$K_{6-eq}$
			(A+L)	(B+L)	(A+L)	(B+L)
Units	$s^{-1}$	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup> .s <sup>-1</sup>	L.mol <sup>-1</sup>	L.mol <sup>-1</sup>
Thiol-Au	$0.82 \times 10^{-6}$	8.49×10 <sup>-1</sup>	7.93×10 <sup>-3</sup>	2.1	$2.18 \times 10^{1}$	$1.27 \times 10^{4}$



**Figure S12.** Calculated final particle sizes as a function thiol:Au<sup>14</sup> ratios ([HAuCl<sub>4</sub>]=10 mM). We considered thiol to interact irreversibly with gold nanoparticle (i.e.  $B + L \rightarrow BL$ ) similar to the work done by Perala et al<sup>6</sup>.



**Figure S13.** Growth/Nucleation rate ratios under different concentrations of ligand and precursor in toluene (left) and pyridine (right).

Kinetic Descriptor for Final Nanoparticle Size. The correlation for the final size  $(D_f)$  in Figure 9 as a function of

Growth/Nucleation can be written as follows:

Final Size (D<sub>f</sub>) = 
$$\alpha \times (\frac{\text{Growth}}{\text{Nucleation}})^{\frac{1}{3}} + \beta$$
 (1E)

The values of  $\alpha$  (slope) and  $\beta$  (intercept) were determined to be 0.48 and 0.4, respectively.

From equation (1E) we can see that when nucleation is much higher than the growth rate  $\left(\frac{\text{Growth}}{\text{Nucleation}} \approx 0\right)$ , the

intercept represents the nucleus size of  $\sim 0.4$  nm.

Equilibrium approach analysis in toluene using ligand-based model. With respect to the reactions 11  $(A + L \xleftarrow{k_{3-f}, K_{5-eq}} AL)$  and 12  $(B + L \xleftarrow{k_{4-f}, K_{6-eq}} BL)$ , we can examine how far these two reversible reactions

are from the equilibrium:

$$\left(\text{Approach to equilibrium for reaction } (A + L \xleftarrow{k_{3-f}, K_{5-eq}} AL) = \frac{\begin{bmatrix} AL \\ \hline [A] \begin{bmatrix} L \\ \hline \end{bmatrix}}{K_{5-eq}} = \frac{\begin{bmatrix} Pd(II) \text{-TOP} \end{bmatrix}}{K_{5-eq}} \right)$$

$$(1F)$$

$$(Approach to equilibrium for reaction  $(B + L \xleftarrow{k_{4-f}, K_{6-eq}} BL) = \frac{\begin{bmatrix} BL \\ \hline B \end{bmatrix} \begin{bmatrix} L \\ K_{6-eq} \end{bmatrix}}{K_{6-eq}} = \frac{\begin{bmatrix} Pd^0 \text{-TOP} \end{bmatrix}}{K_{6-eq}}$$$

 $K_{5-eq}$  and  $K_{6-eq}$  are the equilibrium constants for ligand binding with the precursor and Pd surface atom, respectively. As mentioned in the manuscript, at t = 0,  $A + L \xleftarrow{k_{3-f}, K_{5-eq}} AL$  is considered at equilibrium. Since the concentration of the metal precursor, A, is dropping fast due to the fast autocatalytic surface growth, less A is present in the solution as time proceeds (also concentration of free ligands decreases with time due to association with the surface atoms B to form BL). As a result, reaction  $A + L \xleftarrow{k_{3-f}, K_{5-eq}} AL$  gets far from the equilibrium and more AL starts to decompose. On the other hand, with time, the particle capping reaction,  $B + L \xleftarrow{k_{4-f}, K_{6-eq}} BL$ ,

gets closer to equilibrium (see Figure S14c).



**Figure S14**. Equilibrium approach analysis for reactions of ligand with precursor (*AL*) and particle surface (*BL*). Reaction conditions: 10 mM Pd(OAc)<sub>2</sub> in 50:50 toluene:hexanol, trioctylphosphine:Pd = 2:1, T = 100 °C.

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