

MOFs-derived Co@CN Bi-functional Catalysts for Selective Transfer Hydrogenation of α,β -unsaturated Aldehyde without Using the Base Additives

Xiaomei Liu,^a Shujuan Cheng,^a Jilan Long,^{a*} Wei Zhang,^{b*} Xiaohong Liu^c and Dapeng Wei^b

^aChemical Synthesis and Pollution Control Key Laboratory of Sichuan Province, College of Chemistry and Chemical Engineering, China West Normal University, Nanchong 637000, P.R. China

^bChongqing Institute of Green and Intelligent Technology, Chinese Academy of Sciences, Chongqing 400714, P.R. China

^cDepartment of Laboratory Medicine, Southwest Hospital, Third Military Medical University, Chongqing 400038, P. R. China

* Corresponding authors, e-mails: xlong612@126.com (Jilan Long),

andyzhangwei@163.com (Wei Zhang).

Contents

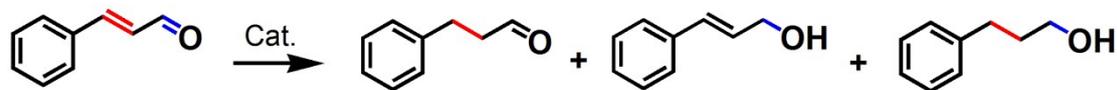
1. Characterizations
2. Results of experiments
3. References

1. Characterizations

Powder X-ray diffraction patterns of the Co-MOF ([Co(TPA)(ted)_{0.5}]) and Co@CN catalysts were measured on a Rigaku diffractometer (D/MAX-III A) equipped with a Cu K α radiation (40kV, 30mA, 0.1543nm). The surface appearances of Co@CN samples were investigated by Scanning Electron Microscope (ZEISS, MERLIN) and Transmission Electron Microscope (JEOL, JEM-2010HR) assembled with energy-dispersive X-ray spectroscopy (EDS) analysis. X-ray Photoelectron Spectroscopy (XPS) tests were conducted on a Kratos Axis Ultra DLD system with a base pressure of 10⁻⁹Torr. BET surface areas and pore sizes were obtained from N₂ physisorption at 77K (Micromeritics ASAP 2020M). The mass of Co in the Co@CN samples were measured by atomic absorption spectroscopy (AAS, Hitachi, Z-2000). CO₂-TPD measured on a Micromeritics AutoChem II 2920 instrument. Typically, 200mg of activated sample was heated at 900°C for 2h under a He flow (50mL.min⁻¹) to remove the adsorption gases from the catalyst, and then cooling down to 50°C. After adsorption of CO₂ at 50°C for 1h, the catalyst was purged with the He flow for 1h to remove the weakly adsorbed species. The TPD data were collected from 100°C to 900°C at a heating rate of 20°C min⁻¹ in a flow of He.

2. Results of experiments

Table S1. Representative literature results for the hydrogenation of cinnamaldehyde over some catalysts.



Entry	Cat.	Sol.	Additives	T (°C)	P (MPa)	t (h)	Con. (%)	Sel. (%)			Ref.
								HCAL	COL	HCOL	
1	Au/PZnO	<i>i</i> -PrOH	-	110	2	0.5	88.1	3.7	74.3	22	1
2	Au/Fe ₂ O ₃	<i>i</i> -PrOH	-	110	2	1.5	94.6	0.9	89.1	10	1
3	Au/MA	EtOH	-	120	1	6	96	42	40	15	2
4	Pt/C	<i>i</i> -PrOH	-	25	0.1	3	3.5	70.5	10.8	18.7	3
6	Pt/MIL-101	THF	-	25	0.1	3	48.6	87.6	8.2	4.2	3
5	Pt NCs	MeOH	-	25	4	44	98.7	2.5	91.7	4	4
7	0.5%Pt/GRA	EtOH	-	70	2	1.5	83.6	39.7	28	7.2	5,6
8	37%Co/Al ₂ O ₃	EtOH	-	50	0.98	2	55	0	99.3	0	7
9	Ni-Co/MWCNT	EtOH	-	150	0.5	8.0	62.6	37.9	62.1	0	8
10	Ni-Co/AC	EtOH	-	150	0.5	9.5	63.2	50.5	46.9	2.6	8
11	Ni-Co/GRA	EtOH	-	150	0.5	5.0	29.8	44.7	55.3	0	8
12	Au/SiC	<i>i</i> -PrOH	KOH	20	-	2	100	-	100	-	9
13	Cobalt complex	<i>i</i> -PrOH	P-ligands	80	-	24	96	-	-	98	10
14	Fe complex	<i>i</i> -PrOH	P-ligands KO ^t Bu	24	-	2	70	-	68	-	11
15	MgAl doxide	<i>i</i> -PrOH	Hydrotalcites	80	-	5	75	-	92	-	12

Table S2. The contents of Co, C and N of some samples.

Entry	Samples	Co contents (%) ^a	C contents (%) ^b	N contents (%) ^b
1	Co-MOF	21.0	46.9	9.6
2	Co@CN-600	37.1	58.5	2.6
3	Co@CN-700	37.7	57.3	2.2
4	Co@CN-800	37.6	57.9	2.1
5	Co@CN-900	38.7	57.8	1.9

^a Measured by AAS.

^b Measured by elemental analysis.



Figure S1. The illustration for the magnetic separation of catalysts after reaction.

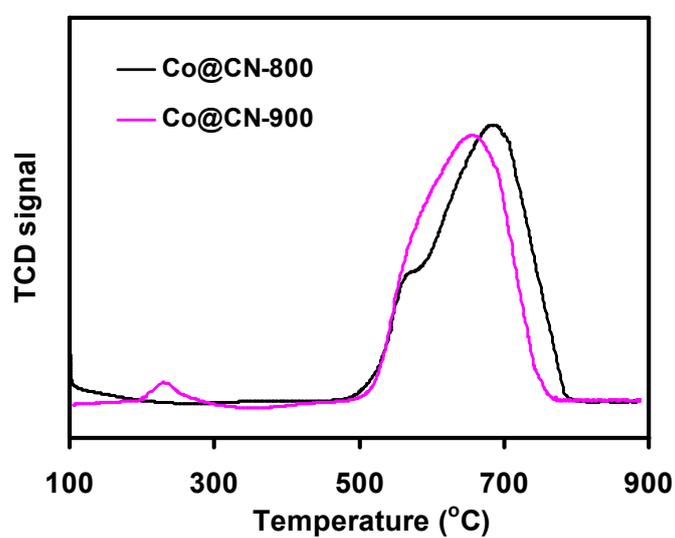


Figure S2. CO₂-TPD curves of Co@CN catalysts.

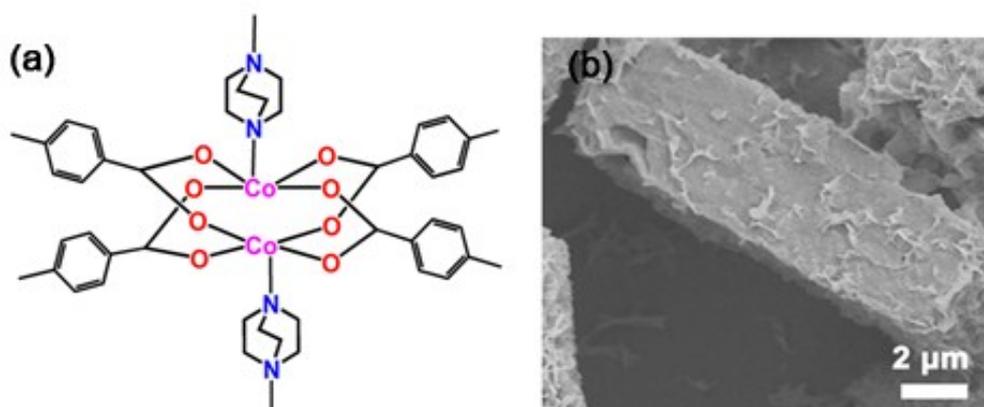


Figure S3. (a) The chemical structure of Co-MOF, (b) the typical SEM image of Co-MOF.

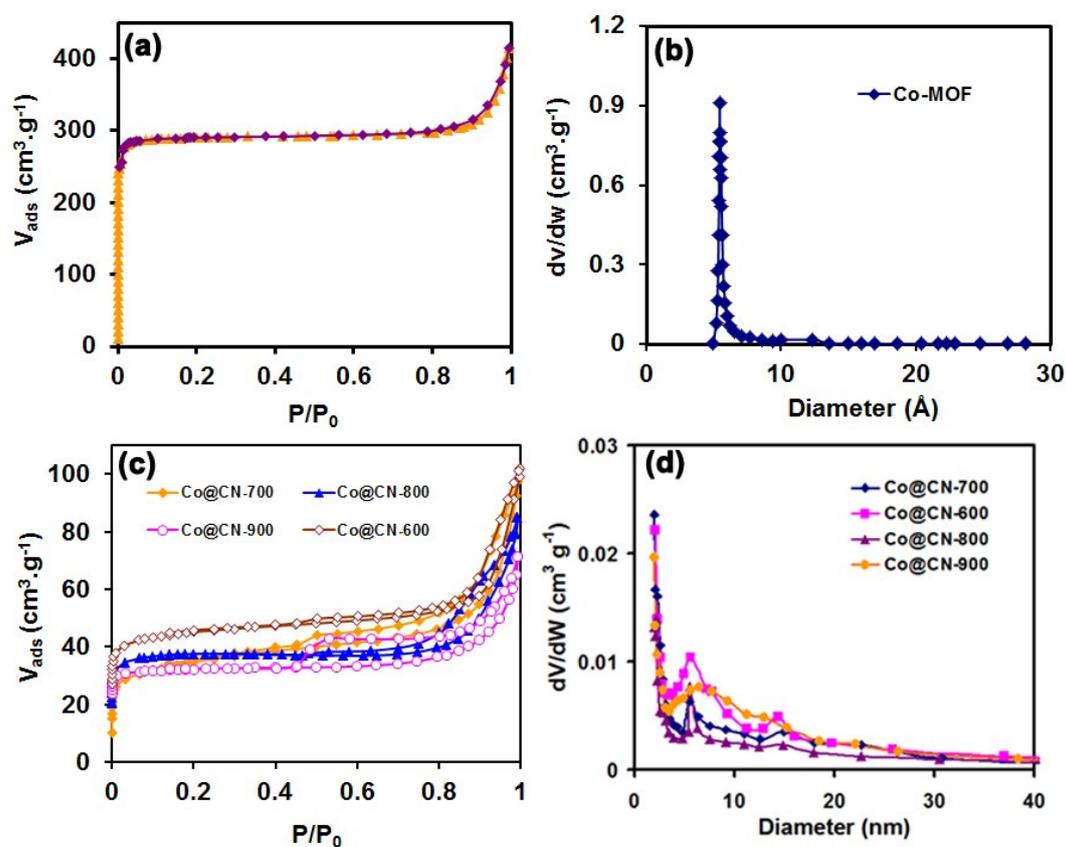


Figure S4. N₂ adsorption/desorption isotherms of Co-MOF (a) and the corresponding pore size distribution (b); the N₂ adsorption/desorption isotherms of Co@CN with different thermolysis temperatures (c), and the corresponding pore-distribution (d).

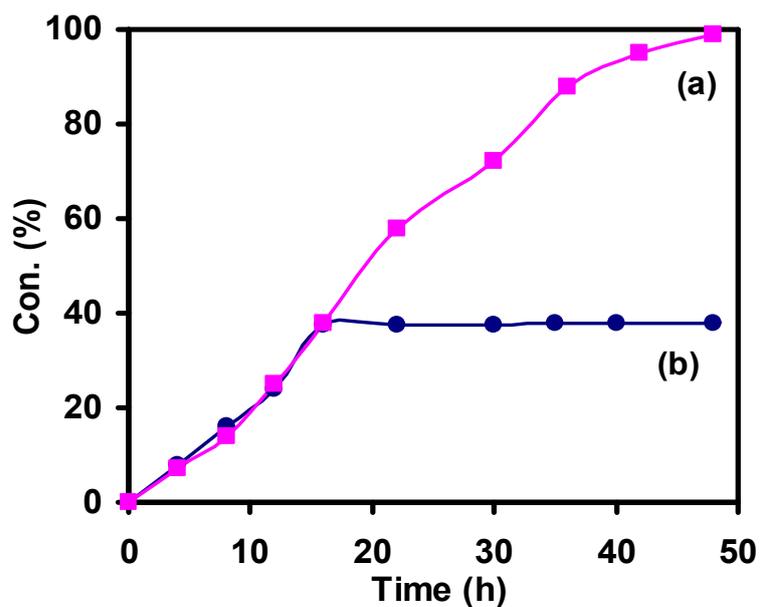


Figure S5. Cinnamaldehyde conversion as a function of time: 1mmol cinnamaldehyde, Co@CN-900 15mmol% catalyst, 2mL *n*-hexanol, 80°C. (a)

Conversion of cinnamaldehyde, (b) cinnamaldehyde conversion after removal of catalyst at 16h.

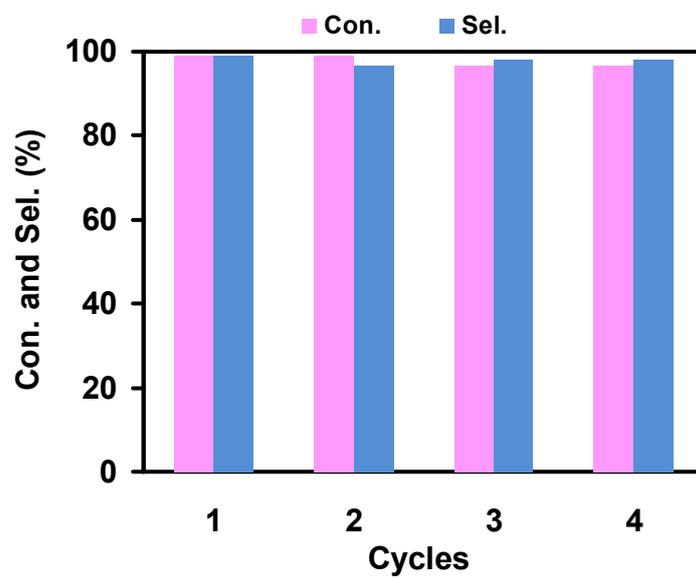


Figure S6. Reuses of Co@CN-900 catalyst in selective transfer hydrogenation of CAL to COL at the optimal conditions.

References

- 1 H. N. Chen, A. C. Davidn and J. Z. Larese, *J. Phys. Chem. C.*, 2015, **119**, 28885.
- 2 Z. M. Tian, X. Xu, L. S. Xie and L. J. Feng, *Ind. Eng. Chem. Res.*, 2013, **52**, 288.
- 3 H. L. Zhong and Y. W. Li, *Ind. Eng. Chem. Res.*, 2015, **54**, 1487.
- 4 Z. Y. Guo, C. X. Xiao, M. G. Raghu V, L. Zhou, T. W. Goh , X. L. Li, D. Tesfagaber, A. Thiel and W. Y. Huang, *ACS Catal.*, 2014, **4**, 1340.
- 5 Y. Li, P. F. Zhu and R. X. Zhou, *Appl. Surf. Sci.*, 2008, **254**, 2609.
- 6 Y. Li, G. H. Lai and R. X. Zhou, *Appl. Surf. Sci.*, 2007, **253**, 4978.
- 7 C. Ando, H. Kurokawa and H. Miura, *Appl. Catal.*, 1999, **185**, 181.
- 8 J. M. Lankitsi, H. Josef, G. A. Willem and M. Cele. Leskey, *Ind. Eng. Chem. Res.*, 2014, **53**, 13910.
- 9 C. H. Hao, X. N. Guo, Y. T. Pan, S. Chen, Z. F. Jiao, H. Yang and X. Y. Guo, *J. Am. Chem. Soc.*, 2016, **138**, 9361.
- 10 G. Q. Zhang and S. K. Hanson, *Chem. Commun.*, 2013, **49**, 10151.
- 11 N. Meyer, A. J. Lough and H. M. Robert, *Chem. Eur. J.*, 2009, **15**, 5605.
- 12 J. Lopez, J. Sanchez Valente, J. M. Clacens and F. Figueras, *J. Catal.*, 2002, **208**, 30.