

## High efficient degradation of high-loaded phenol over Ru-Cu/Al<sub>2</sub>O<sub>3</sub> catalyst at mild conditions

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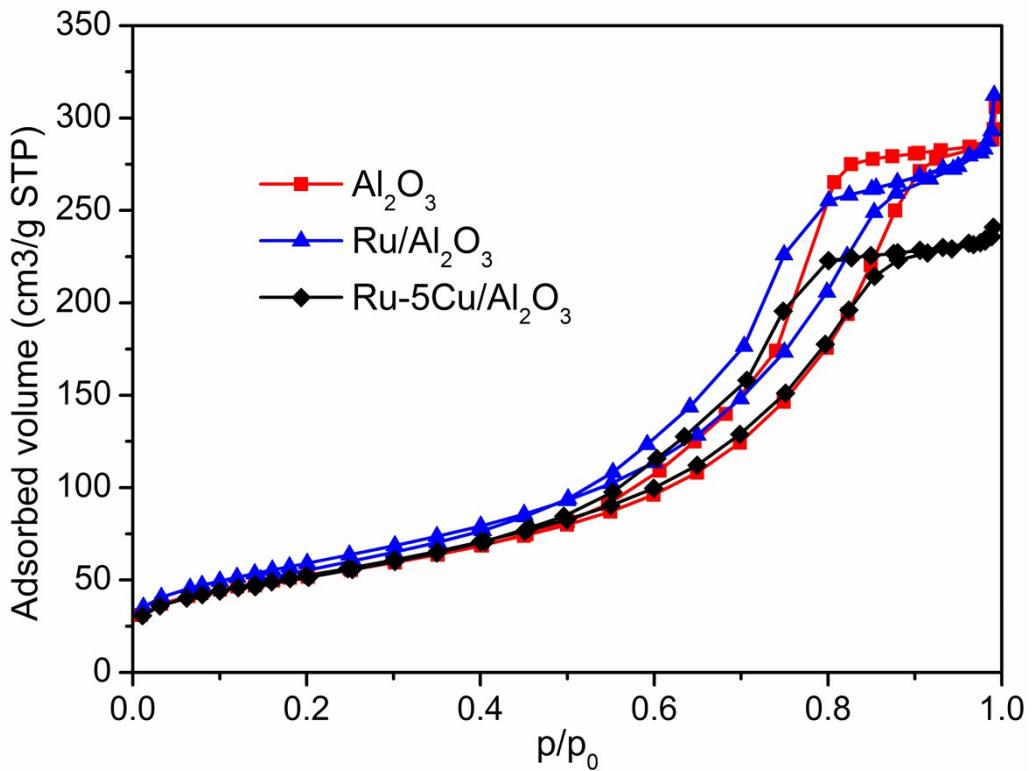
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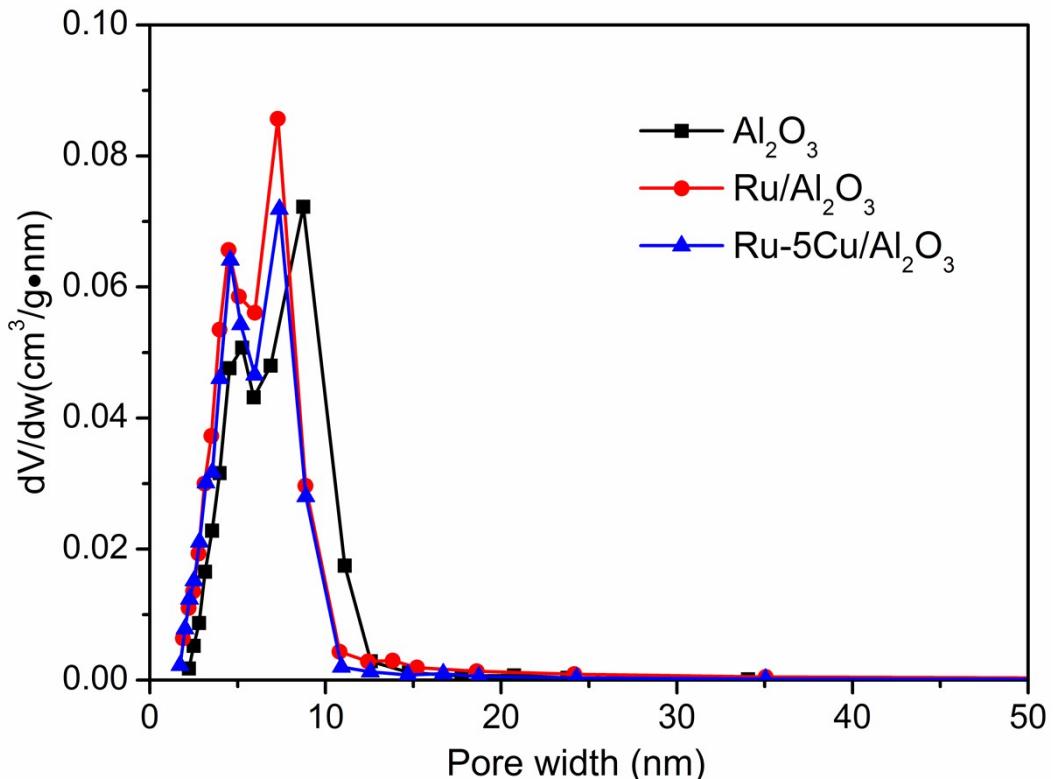
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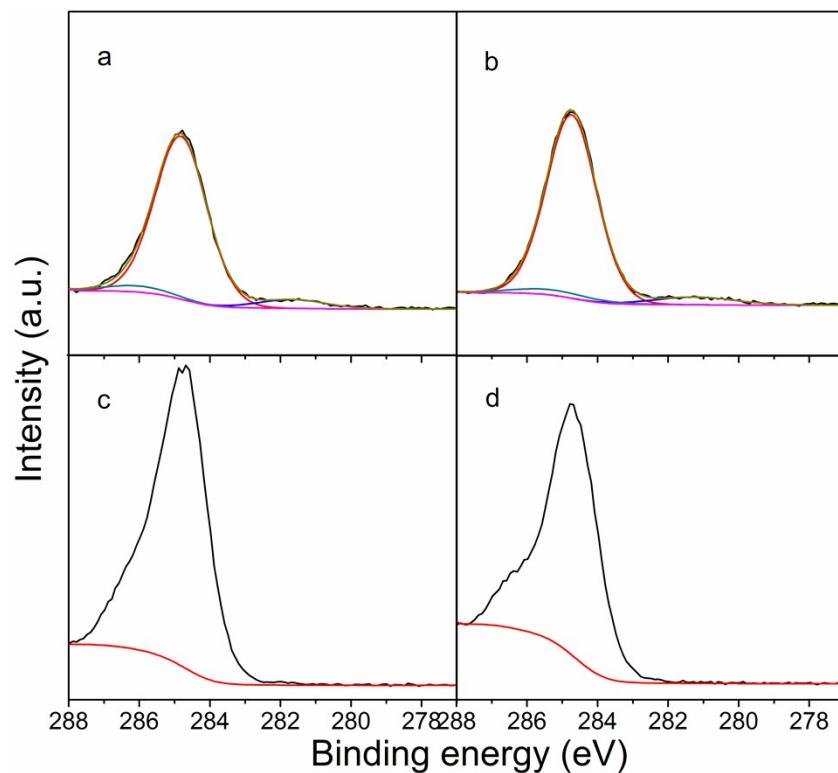
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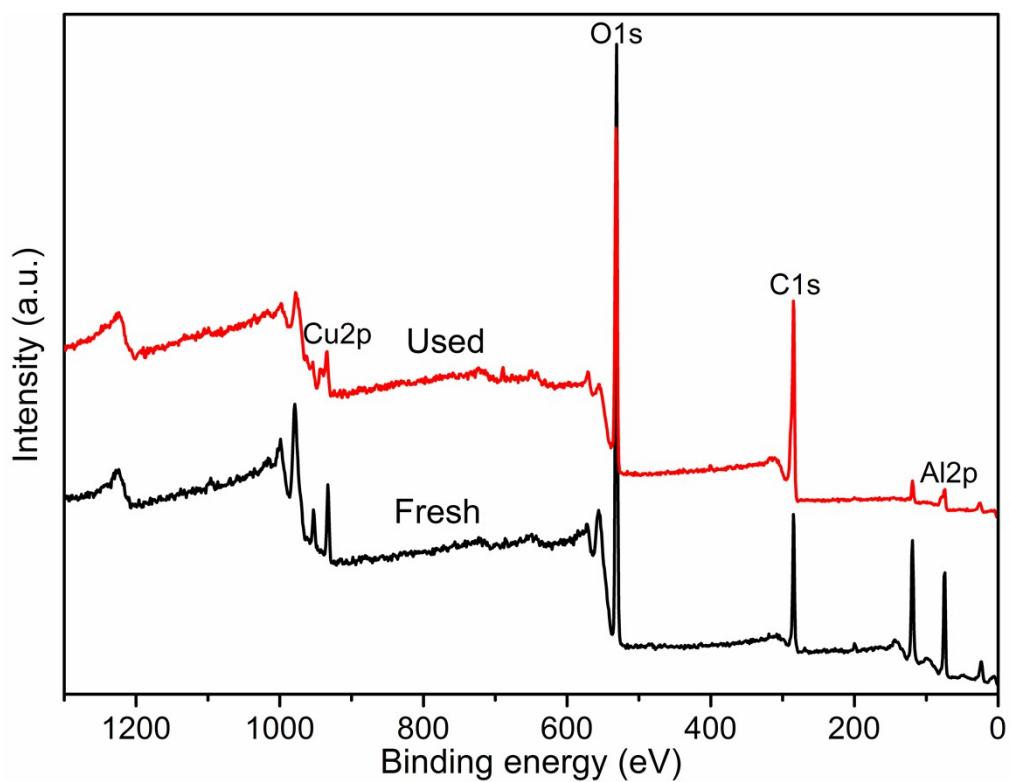
**Fig. S1.**  $N_2$  adsorption-desorption isotherms for support and catalysts.



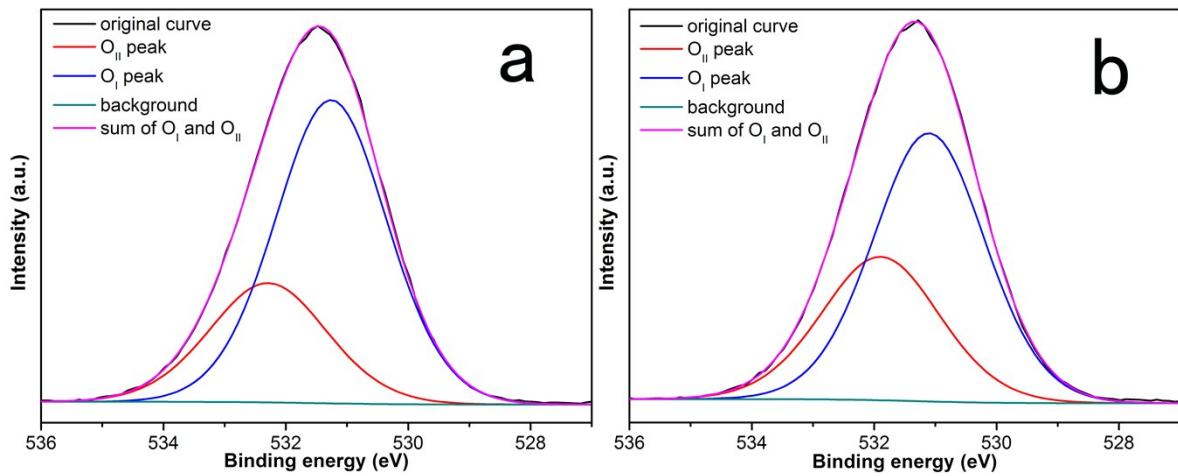
**Fig. S2.** Pore size distribution of support and catalysts derived from the desorption branch of the isotherm.



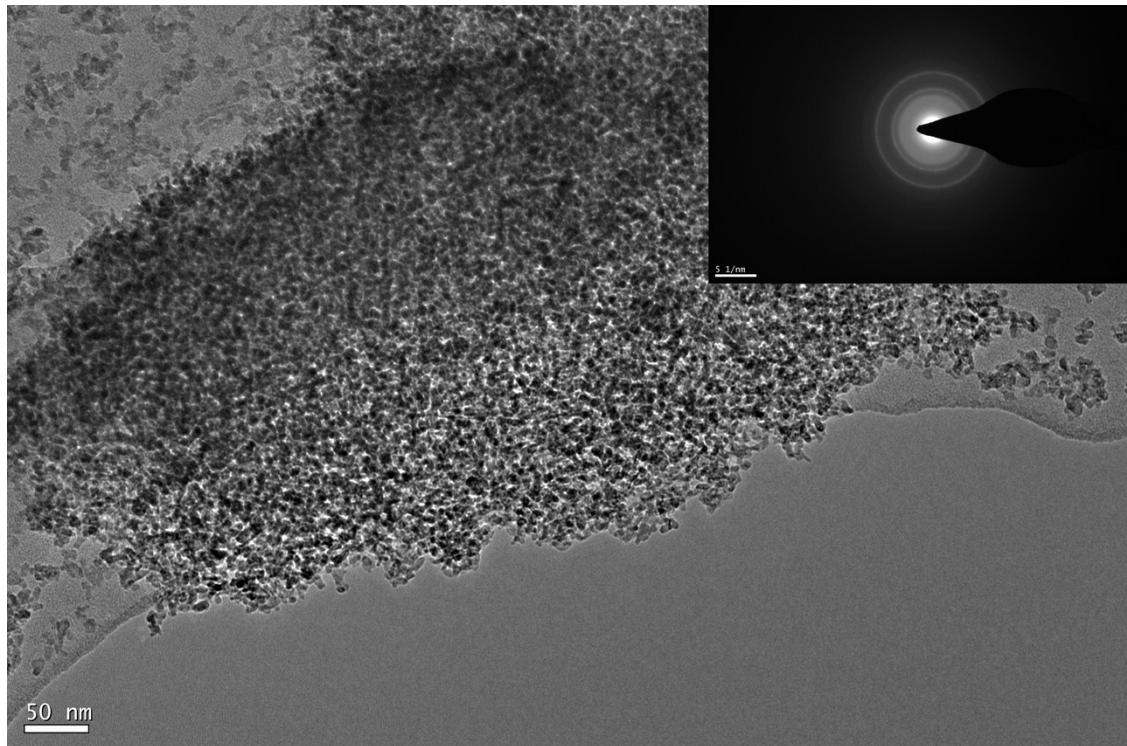
**Fig. S3.** Ru 3d spectra of different catalysts: (a) Ru/Al<sub>2</sub>O<sub>3</sub>; (b) Ru-5Cu/Al<sub>2</sub>O<sub>3</sub>; (c) used Ru/Al<sub>2</sub>O<sub>3</sub>; (d) used Ru-5Cu/Al<sub>2</sub>O<sub>3</sub>.



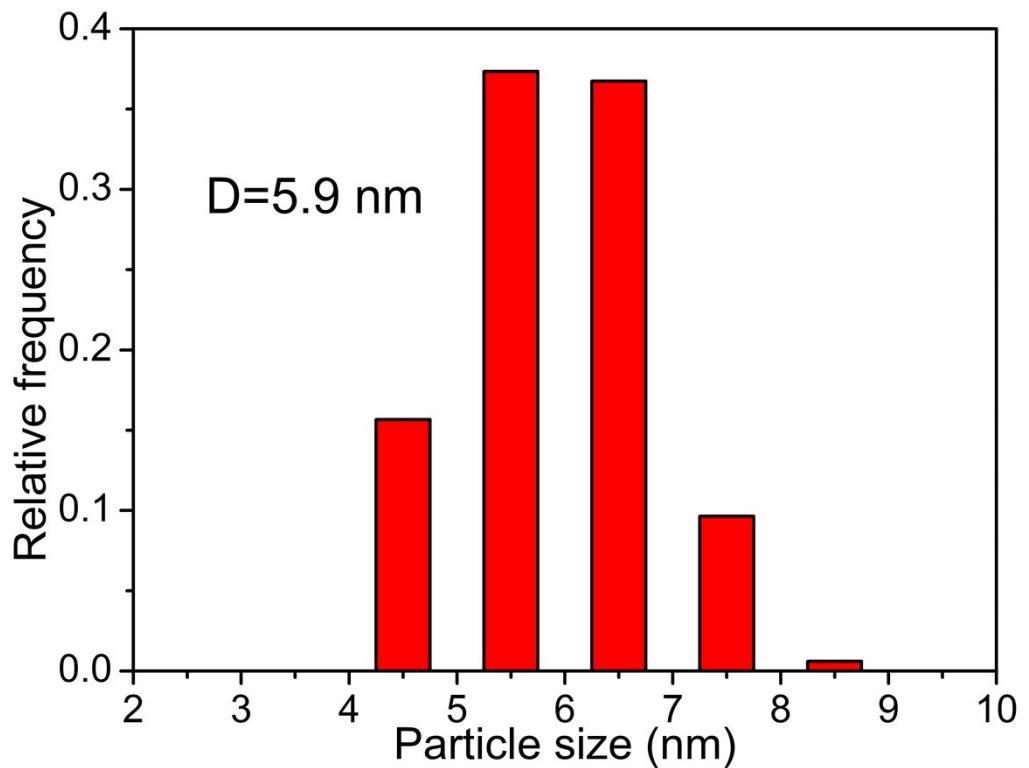
**Fig. S4.** XPS survey spectra of fresh and used catalyst.



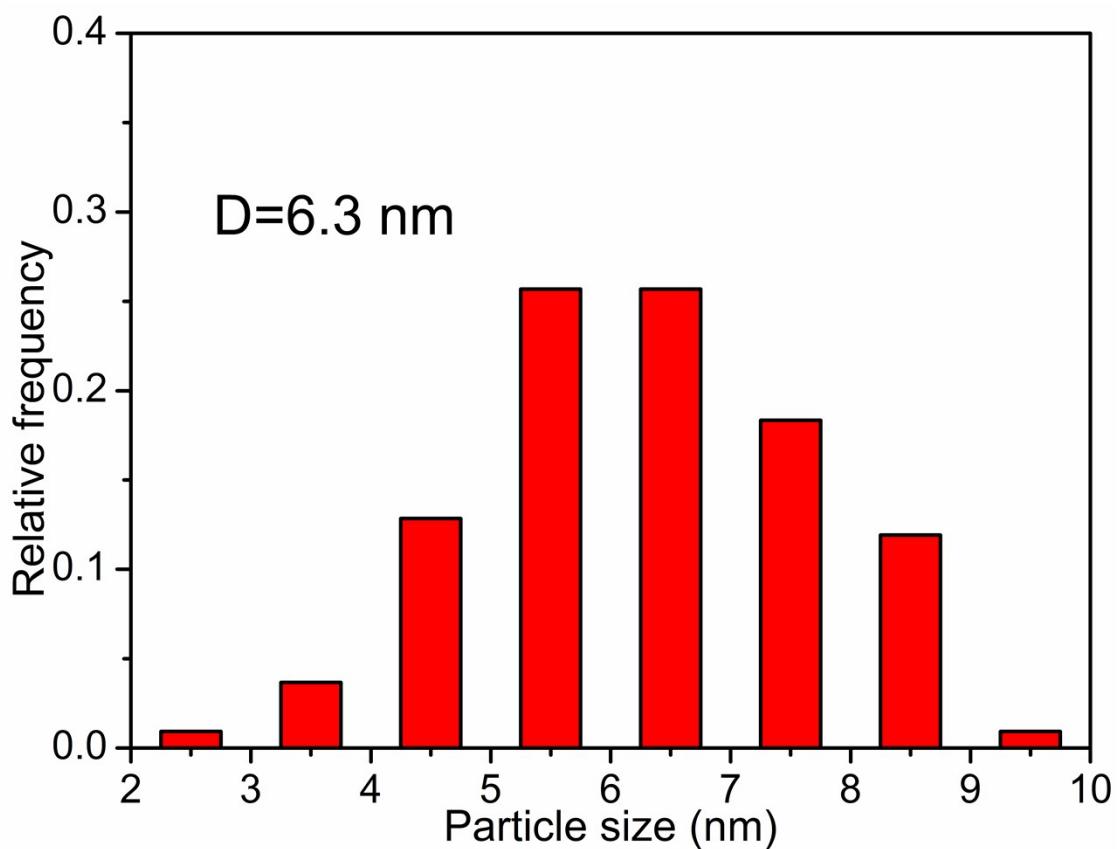
**Fig. S5.** XPS O1s spectra of (a) Ru/Al<sub>2</sub>O<sub>3</sub> and (b) Ru-5Cu/Al<sub>2</sub>O<sub>3</sub>.



**Fig. S6.** TEM images of Ru-5Cu/Al<sub>2</sub>O<sub>3</sub>.



**Fig. S7.** Particle size distribution of Ru-5Cu/Al<sub>2</sub>O<sub>3</sub>.



**Fig. S8.** Particle size distribution of Ru/Al<sub>2</sub>O<sub>3</sub>.

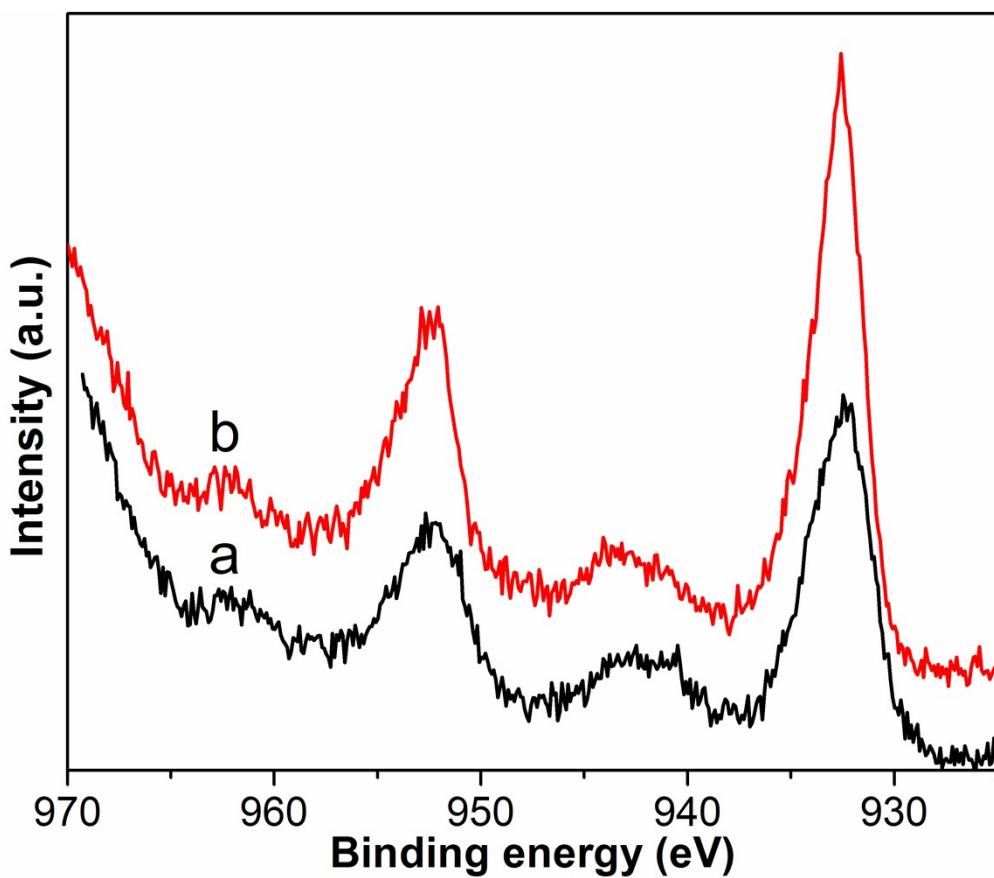


Fig. S9. Cu 2p XPS spectra of (a) used Ru-5Cu/Al<sub>2</sub>O<sub>3</sub> after calcination under 500 °C and (b) used Ru-5Cu/Al<sub>2</sub>O<sub>3</sub> after calcination under 500 °C and H<sub>2</sub> treatment (H<sub>2</sub> treatment conditions was the same as catalyst preparation).