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Supplementary Information

## Promotional Effect of Lanthana on High Temperature Thermal Stability of Pt/TiO<sub>2</sub> Sulfur

## **Resistance Diesel Oxidation Catalyst**

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Fig. 1 The CO (a) and C<sub>3</sub>H<sub>6</sub> (b) oxidation conversion over as-prepared Pt/TiO<sub>2</sub>, Pt/TiO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub> and commercial Pt/Al<sub>2</sub>O<sub>3</sub>, Pt-Pd/CeO<sub>2</sub>-ZrO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> catalysts

Reaction conditions:  $C_3H_6$ : 330 ppm, CO: 1000 ppm, NO: 200 ppm, O<sub>2</sub>: 10%, CO<sub>2</sub>: 8%, vapor: 7%, SO<sub>2</sub>: 50 ppm, N<sub>2</sub>: balance, GHSV = 60,000 h<sup>-1</sup>. Commercial Pt/Al<sub>2</sub>O<sub>3</sub>, Pt-Pd/CeO<sub>2</sub>-ZrO<sub>2</sub>-Al<sub>2</sub>O<sub>3</sub> DOC catalysts were supplied by Sichuan provincial vehicular exhaust gases abatement engineering technology center. All catalysts were pre-treated at 500 °C for 3h under the reaction atmosphere before running the performance test.



Fig. 2 The CO and C<sub>3</sub>H<sub>6</sub> oxidation conversion over Pt/TiO<sub>2</sub>(850) and Pt/TiO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub> (850) catalysts

Reaction conditions:  $C_3H_6$ : 330 ppm, CO: 1000 ppm, NO: 200 ppm, O<sub>2</sub>: 10%, CO<sub>2</sub>: 8%, vapor: 7%, SO<sub>2</sub>: 50 ppm, N<sub>2</sub>: balance, GHSV = 60,000 h<sup>-1</sup>. The Pt/TiO<sub>2</sub>(850) and Pt/TiO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub>(850) catalysts were obtained by baking the fresh monolithic catalysts at 850 °C for 3h under the air. All catalysts were pre-treated at 500 °C for 3h under the reaction atmosphere before running the performance test.



Fig. 3 The CO and C<sub>3</sub>H<sub>6</sub> oxidation conversion over Pt/TiO<sub>2</sub>(A) and Pt/TiO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub> (A) catalysts

Reaction conditions:  $C_3H_6$ : 330 ppm, CO: 1000 ppm, NO: 200 ppm,  $O_2$ : 10%, CO<sub>2</sub>: 8%, vapor: 7%, SO<sub>2</sub>: 50 ppm, N<sub>2</sub>: balance, GHSV = 60,000 h<sup>-1</sup>. The simulative 160 000 km vehicle aged catalysts, Pt/TiO<sub>2</sub>(A) and Pt/TiO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub>(A), obtained by following the reference [J. Andersson et. al., Appl. Catal. B: Environ., 72 (2007) 71-81]. The fresh monolithic catalysts were placed in the reactor and aged at 670 °C for 15 h and then at 250 °C for 15 h in the aging gases: 600 ppm C<sub>3</sub>H<sub>6</sub>, 1500 ppm CO, 200 ppm NO, 50 ppm SO<sub>2</sub>, 5% O<sub>2</sub>, 4% CO<sub>2</sub>, 8% vapor, and N<sub>2</sub> balance at 800 mL/min flow rate. All catalysts were pre-treated at 500 °C for 3h under the reaction atmosphere before running the performance test.



Fig. 4 The CO and  $C_3H_6$  oxidation conversion over fresh and high temperature treated Pt/TiO<sub>2</sub>-YO<sub>x</sub>, Pt/TiO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub> catalysts

Reaction conditions: C<sub>3</sub>H<sub>6</sub>: 330 ppm, CO: 1000 ppm, NO: 200 ppm, O<sub>2</sub>: 10%, CO<sub>2</sub>: 8%, vapor: 7%, SO<sub>2</sub>: 50 ppm, N<sub>2</sub>: balance, GHSV = 60,000 h<sup>-1</sup>. The Pt/TiO<sub>2</sub>-YO<sub>x</sub>(750) and Pt/TiO<sub>2</sub>-YO<sub>x</sub>(850) catalysts were obtained by baking the fresh Pt/TiO<sub>2</sub>-YO<sub>x</sub> monolithic catalysts at 750 °C and 850 °C for 3h under the air, respectively. All catalysts were pre-treated at 500 °C for 3h under the reaction atmosphere before running the performance test.



Fig. 5 TEM micrographs of the fresh  $Pt/TiO_2$  (a)(b) and  $Pt/TiO_2$ -La<sub>2</sub>O<sub>3</sub> (c)(d) catalysts



Fig. 6 XPS (Pt 4f) spectra of the Pt/TiO<sub>2</sub>, Pt/TiO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub>, Pt/TiO<sub>2</sub>(A) and Pt/TiO<sub>2</sub>-La<sub>2</sub>O<sub>3</sub>(A) catalysts