

## Supplementary Information:

### A Comparative Study of Microbial Dynamics and Phosphorus Removal for two Side-Stream Wastewater Treatment Processes

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**MiSeq.** The forward primer was constructed with the Illumina i5 adapter (5'-3') (AATGATACGGCGACCACCGAGATCTACAC), an 8–10 bp barcode, a primer pad (Forward: TATGGTAATT), and the 28F-GAGTTTGATCNTGGCTCAG primer. The reverse fusion primer was constructed with (5'-3') the Illumina i7 adapter (CAAGCAGAAGACGGCATAACGAGAT), an 8–10 bp barcode, a primer pad (Reverse: AGTCAGTCAG), and the reverse primer (388R-TGCTGCCTCCCGTAGGAGT). Reactions were performed on ABI Veriti thermocyclers (Applied Biosystems, Carlsbad, California, USA) under the following thermal profile: 95 °C for 5 min, then 35 cycles of 94 °C for 30 sec, 54 °C for 40 sec, 72 °C for 1 min, followed by one cycle of 72 °C for 10 min and 4°C hold. Amplification products were then pooled equimolar and each pool was size selected in two rounds using AgencourtAMPure XP (Beckman Coulter, Indianapolis, Indiana, USA) in a 0.7 ratio for both rounds. Size selected pools were then quantified using the Qubit 2.0 Fluorometer (Life Technologies) and loaded on an Illumina MiSeq (Illumina, Inc. San Diego, California, USA) 2 × 300 flow cell at 10 pM. After denoising (USEARCH application) and chimera removal (UCHIIME in de novo mode), the sequences were clustered into operational taxonomic units (OTU) clusters with 100% identity (0% divergence) using USEARCH for taxonomic identification.

**Table S1.** Characteristics of influent wastewaters at different stages of operation

Major parameters (mg/L)	Stage 1‡		Stage 2†	Stage 3†
	Phase I	Phase II		
COD (dissolved)	100-120	124-130	360-410	360-420
Total P	6.9-7.8	7.5-7.8	3.9-4.9	20.6-22.2
Reactive P	5.9-6.5	6.9-7.2	3.6-4.6	19.6-20.9
NH <sub>3</sub> -N	45.4-50.1	31.2-35.4	22.1-26.4	22.2-23.6
NO <sub>2</sub> -N	<0.01	<0.01	<0.03	<0.4
NO <sub>3</sub> -N	0.5-1.0	0.5-1.0	1.0-2.0	<1.0
Alkalinity	420	458	436	497
pH (unitless)	6.85	6.71	6.86	4.97

‡Stage 1: The raw municipal wastewater in Goldbar wastewater treatment plant was used for the operation of two systems in Stage 1.

Phase I: The wastewater was collected before primary clarifier on March 08, 2015.

Phase II: The wastewater was collected before primary clarifier on May 12, 2015.

†Stage 1 & 2: Mixed wastewater was prepared after mixing of treated wastewater and raw wastewater collected from Goldbar plant. Sodium acetate was added to increase the COD of simulated wastewater.

**Table S2.** Volumetric flow rate in each reactor for Modified and Denitrifying EBPR processes

	Modified		Denitrifying	
	Flow rate, mL/min	Recycle%	Flow rate, mL/min	Recycle%
Feed/influent	4	-	4	-
Internal return to anoxic	-	-	12	300
Sludge to anaerobic tank	2.1	-	2.1	-
Return anaerobic sludge	1.4	35	1.4	35
Effluent	3.4	-	3.4	-
Conc. P effluent	0.6	-	0.6	-

**Table S3.** Target genes and primers for qPCR analyses of total bacteria and the different clades from *Accumulibacter ppk1* gene <sup>1</sup>

<b>Primer</b>	<b>Sequence (5'-3')</b>	<b>Target</b>	<b>Annealing temperature (°C)</b>
341f 534r	CCTACGGGAGGCAGCAG ATTACCGCGGCTGCTGG	Bacterial 16S rRNA genes	60
Acc-ppk1-763f Acc-ppk1-1170r	GACGAAGAAGCGGTCAAG AACGGTCATCTTGATGGC	Acc-I ppk 1	61
Acc-ppk1-893f Acc-ppk1-997r	AGTTCAATCTCACCGAGAGC GGAACTTCAGGTCGTTGC	Acc-IIA ppk 1	61
Acc-ppk1-870f Acc-ppk1-1002r	GATGACCCAGTTCCTGCTCG CGGCACGAACTTCAGATCG	Acc-IIB ppk1	61
Acc-ppk1-254f Acc-ppk1-460r	TCACCACCGACGGCAAGAC CCGGCATGACTTCGCGGAA G	Acc-IIC ppk1	66
Acc-ppk1-375f Acc-ppk1-522r	GGGTATCCGTTTCCTCAAGC G GAGGCTCTTGTTGAGTACAC GC	Acc-IID ppk1	63
Acc-ppk1-355f Acc-ppk1-600r	CGAACTCGGCGAAAGCGAG TA ATCGCCTCCGAGCAACTGTT C	Acc-IIF ppk1	70

**Table S4.** Target genes and primers for qPCR analyses of nitrifiers and denitrifiers

Function	Target gene	Primer	Sequence	Reference
Nitrification	AOB	amoA-1F	GGGGTTTCTACTGGTGGT	2
	<i>amoA</i>	amoA-2R	CCCCTCKGSAAAGCCTTCTTC	
	<i>Nitrospira</i> spp. 16S rDNA	NSR 1113f	CCTGCTTTCAGTTGCTACCG	
		NSR 1264r	GTTTGCAGCGCTTTGTACCG	
	<i>Nitrobacter</i> spp. 16S rDNA	Nitro 1198f	ACCCCTAGCAAATCTCAAAA AACCG	
Denitrification	<i>narG</i> gene	narG 1960	TAYGTSGGGCAGGARAAACT	3
		m2f	G	
		narG 2050	CGTAGAAGAAGCTGGTGCTG	
	m2r	TT		
	<i>nirS</i> gene	nirS 1f	TACCACCCSGARCCGCGCGT	
		nirS 3r	GCCGCCGTCRTGVAGGAA	
	<i>nirK</i> gene	nirK 876	ATYGGCGGVCA YGGCGA	
		nirK 1040	GCCTCGATCAGRTRRTGGTT	
	<i>nosZ</i> gene	nosZ 2f	CGCRACGGCAASAAGGTSMS GT	
nosZ 2r		CAKRTGCAKSGCRTGGCAGA A		

**Table S5.** qPCR amplification programs for total, nitrifying and denitrifying bacteria

Target gene	Initial denaturation	Cycles				Final extension (72 °C)
		Cycles	Denaturation	Annealing	Extension (72 °C)	
<i>AOB amoA</i>	95 °C, 15 min	45	95 °C, 1 min	54 °C, 1 min	1 min	10 min
<i>Nitrospira</i> spp. 16S rDNA	50 °C, 2 min; 95 °C, 10 min	50	95 °C, 30 s	60 °C, 60 s	-	-
<i>Nitrobacter</i> spp. 16S rDNA	50 °C, 2 min; 95 °C, 10 min	50	94 °C, 20 s	58 °C, 60 s	40 s	-
<i>narG</i> gene	95 °C, 30 s	35	95 °C, 15 s	58 °C, 30 s	31 s	-
<i>nirS</i> gene	95 °C, 30 s	30	95 °C, 15 s	60 °C, 20 s	31 s	-
<i>nirK</i> gene	95 °C, 30 s	30	95 °C, 15 s	58 °C, 30 s	31 s	-
<i>nosZ</i> gene	95 °C, 30 s	30	95 °C, 15 s	60 °C, 30 s	31 s	-

**Table S6.** Steady-state nutrient concentrations (mg/L) in influent and effluent streams for the conventional and denitrifying EBPRs.

Stages	Time	COD			NH <sub>4</sub> <sup>+</sup> -N			Total P (phosphorus)			
	d	influent	effluent	% removal	influent	effluent	% removal	influent	effluent	% removal	
<b>Modified</b>	<b>1, I</b>	0-56	113.4 ± 5.2	67.6 ± 9.6	86.9 ± 1.9	46.3 ± 2.4	23.4 ± 7.3	47.4 ± 7.8	7.3 ± 0.2	4.8 ± 0.5	35.2 ± 3.4
	<b>1, II</b>	57-80	129.2 ± 2.9	56.9 ± 6.6	89.7 ± 2.2	33.6 ± 0.8	5.8 ± 1.2	83.4 ± 3.2	7.2 ± 1.6	3.0 ± 0.0	57.4 ± 3.6
	<b>2</b>	81-100	377.2 ± 17.7	62.7 ± 4.6	91.9 ± 0.5	24.9 ± 1.7	0.1 ± 0.1	99.5 ± 0.4	4.2 ± 0.3	1.3 ± 0.1	68.4 ± 0.9
	<b>3</b>	100-120	396.2 ± 10.3	61.3 ± 9.3	92.3 ± 1.1	22.2 ± 0.7	0.2 ± 0.3	99.0 ± 1.1	20.7 ± 0.3	9.0 ± 0.8	56.7 ± 4.4
<b>Denitrifying</b>	<b>1, I</b>	0-56	113.4 ± 5.2	62.8 ± 7.3	88.2 ± 1.4	46.3 ± 2.4	1.3 ± 2.1	96.1 ± 4.9	7.3 ± 0.2	2.4 ± 0.3	69.2 ± 2.8
	<b>1, II</b>	57-80	129.2 ± 2.9	51.2 ± 5.8	90.2 ± 1.1	33.6 ± 0.8	0.3 ± 0.2	99.1 ± 0.7	7.2 ± 1.6	1.8 ± 0.2	75.0 ± 1.2
	<b>2</b>	81-100	377.2 ± 17.7	58.3 ± 5.1	92.6 ± 0.9	24.9 ± 1.7	0.1 ± 0.1	99.7 ± 0.3	4.2 ± 0.3	1.0 ± 0.3	78.6 ± 3.3
	<b>3</b>	100-120	396.2 ± 10.3	49.3 ± 7.9	93.9 ± 0.9	22.2 ± 0.7	0.1 ± 0.3	99.3 ± 0.9	20.7 ± 0.3	6.7 ± 0.9	67.9 ± 2.1

Note: The COD removal was calculated based on the following equation:

$$\text{Removal} = 1 - (\text{effluent COD}) / (\text{influent COD} + \text{NaOAc COD entering anaerobic reactor})$$



**Table S7.** Abundance (%) of nitrifiers and denitrifiers in terms of OTUs in the modified and denitrifying EBPRs

	Stage	AOB		NOB		Denitrifiers			
		<i>amoA</i>	<i>Nitrospira</i>	<i>Nitrobacter</i>	<i>nirK</i>	<i>nirS</i>	<i>narG</i>	<i>nosZ</i>	
<b>Modified</b>	<b>Contact</b>	1	0.11	0.02	1.69	6.42	4.16	0.31	13.45
		2	0.06	0.01	1.55	5.19	1.56	0.64	20.36
		3	0.13	0.02	1.94	6.89	2.18	1.24	35.53
	<b>Stabilization</b>	1	0.20	0.02	1.90	7.18	4.52	0.31	13.79
		2	0.07	0.01	1.95	5.92	2.69	0.84	31.18
		3	0.13	0.02	1.94	6.39	2.20	1.12	33.34
	<b>Anaerobic</b>	1	0.09	0.01	1.14	4.71	2.65	0.18	9.05
		2	0.09	0.02	2.10	6.75	3.01	0.72	23.09
		3	0.12	0.02	1.96	6.88	2.33	1.03	30.23
<b>Denitrifying</b>	<b>Aerobic</b>	1	0.09	0.01	2.14	8.18	3.65	0.49	17.40
		2	0.14	0.01	2.05	9.17	3.98	0.73	27.03
		3	0.15	0.02	2.39	7.72	2.65	0.89	33.15
	<b>Anoxic</b>	1	0.08	0.01	1.86	5.78	2.52	0.36	12.41
		2	0.12	0.01	1.85	6.88	2.81	0.51	22.63
		3	0.18	0.02	2.60	8.83	2.95	1.11	36.29
	<b>Anaerobic</b>	1	0.14	0.01	3.16	11.85	4.41	0.58	18.33
		2	0.09	0.01	1.51	6.01	2.72	0.42	20.70
		3	0.15	0.01	2.35	7.47	2.97	0.97	27.19

**Table S8.** Abundance (%) of *Dechloromonas* related PAOs in terms of OTUs in different reactors of the modified and denitrifying EBPRs

	Stage	Modified			Denitrifying		
		Contact	Stabilization	Anaerobic	Anoxic	Aerobic	Anaerobic
<i>Dechloromonas denitrificans</i>	1	0.495	0.361	0.425	0.433	0.424	0.593
	2	0.028	0.118	0.000	0.045	0.259	0.231
	3	0.006	0.090	0.129	0.341	0.472	0.326
<i>Dechloromonas sp.</i>	1	6.254	4.684	6.406	6.594	5.797	7.509
	2	0.634	2.304	2.199	2.728	4.395	5.429
	3	1.677	2.668	3.591	1.349	3.331	1.611

## References

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