Supporting Information for:

Ultra-deep oxidative desulfurization of fuel with H₂O₂ catalyzed by molybdenum

oxide supported on alumina modified by Ca²⁺

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Fig. 1 shows the FT-IR spectra of MoO_3 (a), Al_2O_3 (b), and $Ca/MoO_3/Al_2O_3$ (c). The characteristic peaks observed in the FT-IR spectrum of MoO_3 at 988, 878 and 634 cm⁻¹ were attributed to the fundamental vibrational modes of $Mo=O.^1$ The dominion band at 821 cm⁻¹ is associated with the vibration of Mo-O-Mo bridging bonds.¹ For the Ca/MoO₃/Al₂O₃ (c), owing to the overlap of the characteristic peaks of MoO₃ with that of the Al₂O₃ appeared at 740 and 640 cm⁻¹ (Al-O bands),² the bands of MoO₃ were not observed after the immobilization of MoO₃ on the support. It suggested that MoO₃ was highly dispersed on the Al₂O₃ support.



Fig.1. FT-IR spectra of MoO_3 (a), Al_2O_3 (b) and $Ca/MoO_3/Al_2O_3$ (c).

Fig. 2 shows the powder X-ray diffractions of ammonium molybdate(a), $Al_2O_3(b)$, and $Ca/MoO_3/Al_2O_3(c)$. As shown in Fig. 2, The characteristic peaks of ammonium molybdate at 2θ = 13.0°, 23.2°, 25.6°, 27.2°, 34.3°, 39.1°, 46.5°, 50.1°, 53.7° and 60.4° emerged, which belonged to the characteristic peaks of the MoO₃ unit.³ For Ca/MoO₃/Al₂O₃, no crystal diffraction peaks of MoO₃ were found, which indicates that MoO₃ clusters are highly dispersed on the surface of Al₂O₃. XRD analysis confirms that the catalyst Ca/MoO₃/Al₂O₃ structure is an amorphous phase because of no characteristic diffraction peaks.



Fig.2. X-ray diffractions of ammonium molybdate (a), Al₂O₃ (b) and Ca/MoO₃/Al₂O₃ (c).

The N₂ adsorption desorption isotherm (a) and pore size distribution (b) of Ca/MoO₃/Al₂O₃ are showed in Fig.3. Based on the taxonomy, the adsorption isotherm of Ca/MoO₃/Al₂O₃ exhibit type IV isotherms using IUPAC, revealing that the catalysts are characteristic of mesoporous materials.⁴ The adsorption isotherm data were processed by the BET and BJH theoretical models. The pore size distribution of Ca/MoO₃/Al₂O₃ was concentrated at the average pore diameter of 8.00 nm, the specific surface area was 151.09 m²/g, and the total pore volume was 0.302 cm³/g. The abundant pores and high pore volume would be favorable to the oxidation reaction because it would assist the adsorption of 4,6-DMDBT, DBT and BT on the catalyst surface.



Fig.3. Pore structure parameters of $Ca/MoO_3/Al_2O_3$. (a) Adsorption desorption isotherm; (b) Pore size distribution.

Fig.4 shows the XPS spectra of Ca/MoO₃/Al₂O₃ and MoO₃/Al₂O₃. From Fig. 4 (a), the comparison showed that the XPS spectra of Ca/MoO₃/Al₂O₃ had gained a new Ca 2p characteristic peak than MoO₃/Al₂O₃. It indicated that the presence of Ca in the catalyst Ca/MoO₃/Al₂O₃. Fig. 4(b) and (d) present the Mo 3*d* spectrum of Ca/MoO₃/Al₂O₃ and MoO₃/Al₂O₃. The appearance of two signals at 233.7 eV(233.0 eV) and 236.9 eV (236.2 eV) for Mo 3*d*_{5/2} and Mo 3*d*_{3/2} respectively. Based on the researches of García-Gutiérrez,⁵ the absorption peak at 232.7 eV corresponded to Mo

⁶⁺, so it shall serve to illustrate the valence of molybdenum element in the catalysts are +6. The comparison of Fig. 4(b) and (d) showed the binding energy (233.7 eV) of the Mo $3d_{5/2}$ on the Ca/MoO₃/Al₂O₃ catalyst was increased by 0.7 eV with MoO₃/Al₂O₃ (233.0 eV). The result indicated that the electron cloud density of Mo atoms in the Mo=O bands was increased by Ca-doping, which was beneficial to the good association of H₂O₂, and thereby increase the activity of desulfurization. Fig. 4 (c) presents the Ca 2*p* spectrum of Ca/MoO₃/Al₂O₃. The appearance of two signals at 347.8 eV and 350.9 eV for Ca $2p_{3/2}$ and Ca $2p_{1/2}$ respectively, and these binding energy values corresponded to Ca^{2+.6}





Fig.4. XPS spectra of Ca/MoO₃/Al₂O₃:(a) Survey, (b) Mo 3*d*, (c) Ca 2*p* and MoO_3/Al_2O_3 :(a) Survey, (d) Mo 3*d*.

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