

Effect of relative humidity on the gas transport properties of Zeolite A/PTMSP mixed matrix membranes

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Electronic Supplementary Information

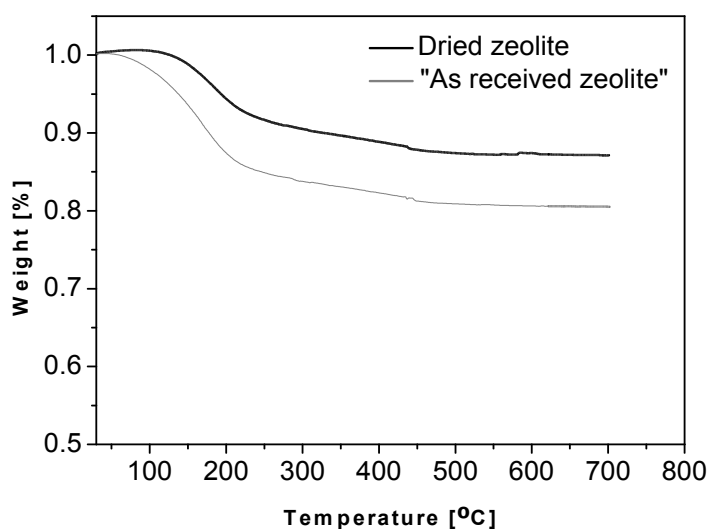
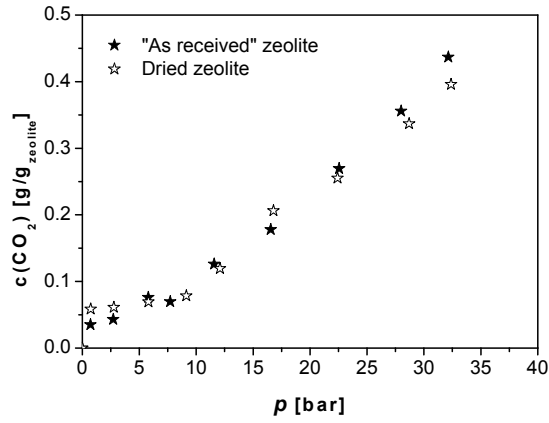
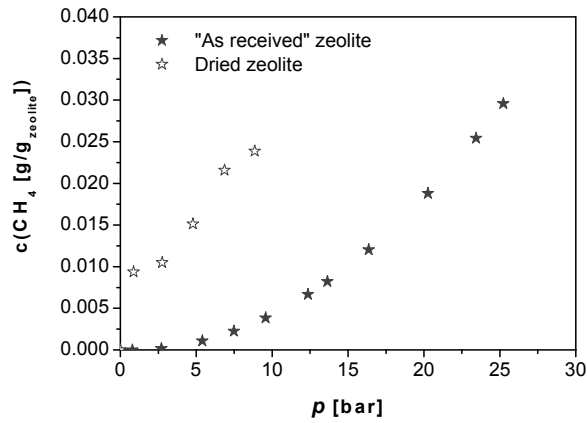


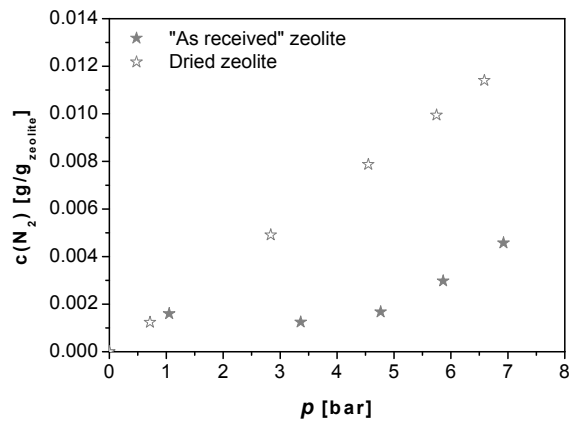
Figure S1. TGA of undried “as received” and dried zeolite.



(a)

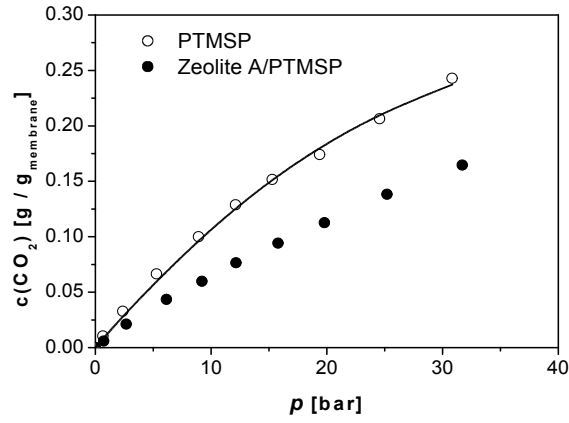


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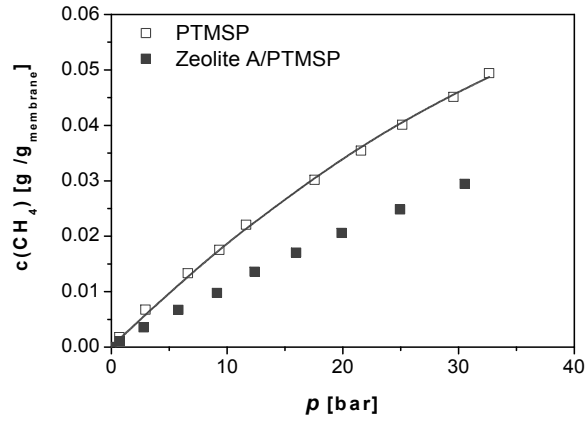


(c)

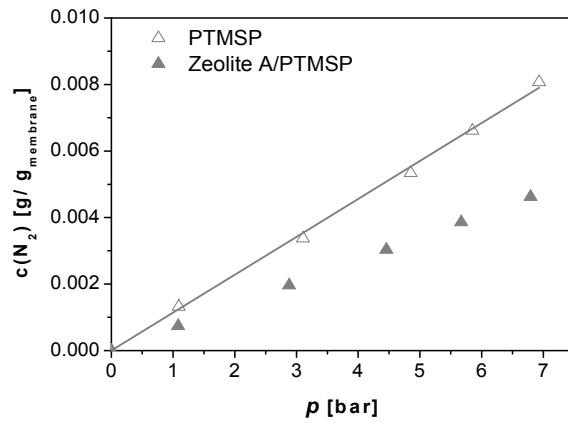
Figure S2. Gas sorption isotherms of (a) CO₂ (a), (b) CH₄ and (c) N₂ onto the Zeolite A particles “as received” (full symbols) and dried at 100 °C for 24h under vacuum (void symbols).



(a)



(b)



(c)

Figure S3. Experimental gas sorption isotherms at 35 °C of (a) CO₂, (b) CH₄ and (c) N₂ for the pristine PTMSP membrane and the Zeolite A/PTMSP MMM. The solid line represents the adjustment with the NELF model.

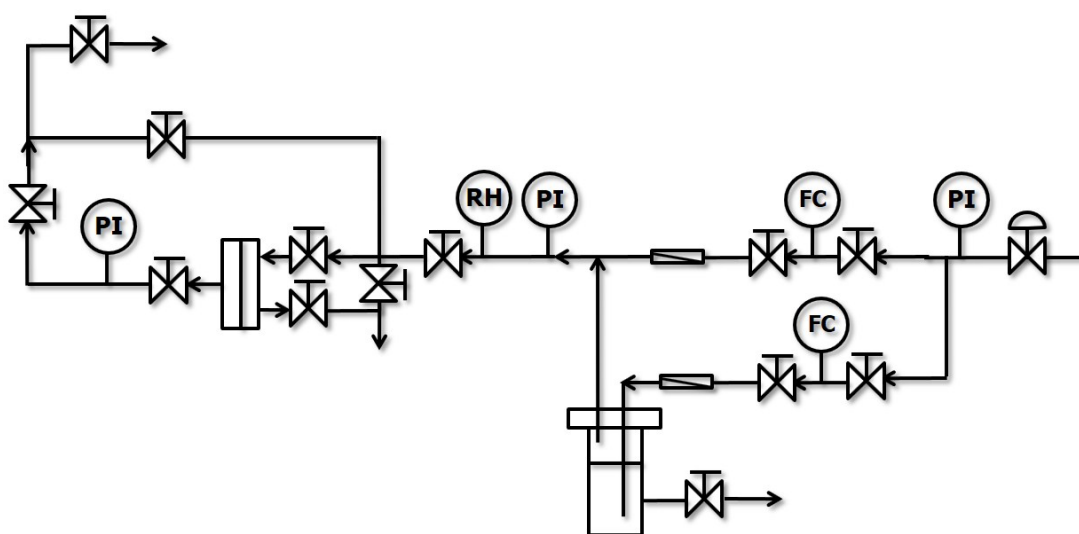


Figure S4. Humid permeometer setup. Redrawn from ^{1,2}.

- 1 M. Minelli, M. G. Baschetti, F. Doghieri, M. Ankerfors, T. Lindström, I. Siró and D. Plackett, *J. Memb. Sci.*, 2010, **358**, 67–75.
- 2 J. Catalano, T. Myezwa, M. G. De Angelis, M. G. Baschetti and G. C. Sarti, *Int. J. Hydrogen Energy*, 2012, **37**, 6308–6316.

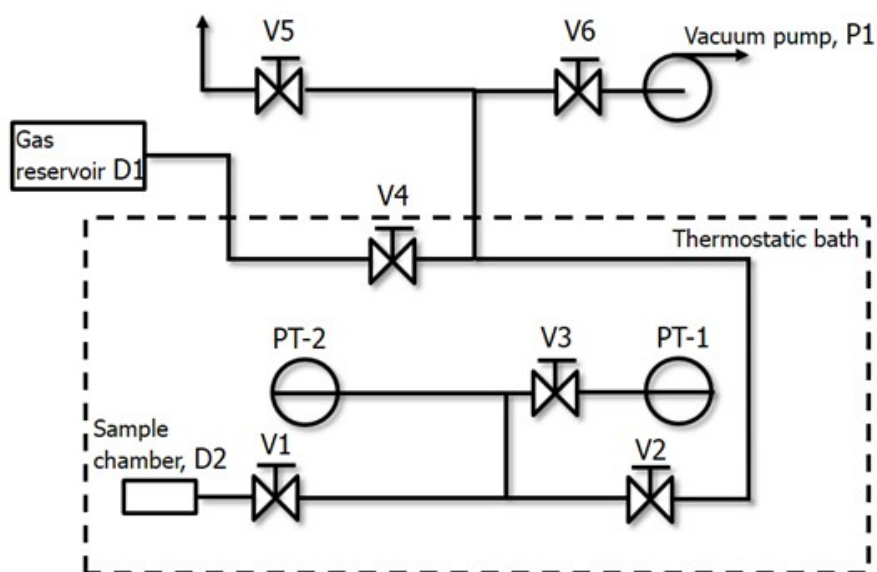


Figure S5. Pressure decay experimental equipment. D1: Gas reservoir, D2: Membrane sample chamber, PT-1: low pressure transducer, PT-2: High pressure transducer, V1: sample chamber valve, V1-V2 with V3 opened: pre-chamber PT-1, V1-V2-V3: pre-chamber PT-2, V4: feed valve, V5: vent valve, V6: vacuum valve.