

## Supplemental information

### **Bifunctional CO oxidation over Mn-mullite anchored Pt sub-nanoclusters via atomic layer deposition**

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## Experimental details

*Catalysts preparation.* The coprecipitation method was chosen to prepare the  $\text{SmMn}_2\text{O}_5$  (SMO) mullite oxide as reported in previous studies.[1,2] Briefly,  $\text{Sm}(\text{NO}_3)_3 \cdot 6\text{H}_2\text{O}$ ,  $\text{Mn}(\text{NO}_3)_2$  and Pluronic F127 (surfactant) with the appropriate amounts were dissolved by deionized water, which were purchased from Aladdin. Then, tetramethylammonium hydroxide was used to tune the pH of solution to 9 ~ 10 and  $\text{H}_2\text{O}_2$  was added to the solution to reduce the Mn ions in the following step. The mixture was stirred for two hours at room temperature and filtered to get the SMO precursors. At last, the SMO products were prepared by performing the over-night drying at 100 °C and calcination treatments on the precursors. The dried SMO precursors were firstly calcined at 500 °C for 8 h, and then the calcination treatment at 800 °C is followed for 8 h. The ramp rates for both calcination treatments are 5 °C/min.

The Pt/SMO composite catalyst was prepared by atomic layer deposition (ALD) method with the precursors of trimethyl(methylcyclopentadienyl)platinum (98%, Sigma-Aldrich) and 11 vol. %  $\text{O}_3$  balanced by  $\text{O}_2$ . The home-made ALD chamber based on the principle of fluidized bed was kept at 200 °C, which was used in our previous study.[3] About 200 mg of SMO supports were held into the powder holder during Pt ALD. The stainless steel bottle containing Pt precursor was kept at 65 °C to increase its vapor pressure. The pretreatment process of 30 min with 500 mL/min of  $\text{O}_3$  has been performed to fluidize the SMO supports sufficiently. One cycle Pt ALD was performed to prepare the Pt/SMO catalyst with the long pulse and purge time of 200 s and 200 s, respectively. The same ALD recipe of Pt/SMO was also used for the preparation of Pt/ $\text{Al}_2\text{O}_3$  reference.

The incipient wet-impregnation method was used to prepare  $\text{Pt}_{\text{tWI}}/\text{SMO}$  catalyst. Firstly, 1.00 g of SMO supports was immersed in 1 mL  $\text{Pt}(\text{NO}_3)_2$  solution that contained 0.02 g Pt. The mixture was continuously stirred about 15 min, and dried at 60 °C for 6 hours after  $\text{Pt}(\text{NO}_3)_2$  solution was totally adsorbed by SMO supports. Then, the dried precursors were calcined at 450 °C for 4 hours to get the  $\text{Pt}_{\text{tWI}}/\text{SMO}$  catalyst.

*Characterizations.* The X-ray diffraction (XRD) patterns were recorded by the PANalytical X'Pert Pro with a Cu K $\alpha$ 1 radiation source. The Pt mass loading of catalysts were measured by inductively coupled plasma atomic emission spectrometer (ICP-OES, Optima 4300 DV). Transmission electron microscopy (TEM) and high-resolution TEM observations were performed by Tecnai G2 F30 electron microscope (FEI) to characterize the morphology of catalysts and interfacial structure. The valence states of deposited Pt clusters were characterized by X-ray photoelectron spectrometer (XPS, AXIS-ULTRA DLD-600W), the binding energies of which were calibrated according to the C1s at 284.8 eV. The X-ray absorption fine structure (XAFS) measurements were carried out at the 1W1B beamline of Beijing synchrotron radiation facility. The signals at the Pt L<sub>III</sub>-edge (11368-12463 eV) of Pt/SMO were collected. The Pt L<sub>III</sub>-edge of Pt foil and PtO<sub>2</sub> were tested as references. The Pt  $k^2$ -weighted Fourier transformed extended X-ray absorption fine structure (EXAFS) spectrum of Pt/SMO was analyzed with the Pt foil and PtO<sub>2</sub> modes by using Demeter program.[4] The parameters such as coordinated number (N), bond length (R, Å), Debye-Waller factor ( $\sigma^2$ , Å<sup>2</sup>) and shift in the edge energy ( $\Delta E_0$ , eV) were fitted.

The *in situ* diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) spectra of CO adsorption at different temperature were collected by wide band mercury cadmium telluride (MCT-B) detector deployed on Nicolet iS50 FTIR spectrometer (ThermoFisher Scientific). The DRIFTS cell with a KBr window was connected to a reaction gas system with ultrahigh purity N<sub>2</sub>, 1% vol. CO balanced by N<sub>2</sub>, and 2% vol. O<sub>2</sub> balanced by N<sub>2</sub>. The samples were firstly pretreated at 200 °C by 30 ml/min of N<sub>2</sub> for 30 min, and then the background spectra were collected after the samples cooling to room temperature. Note that, the samples were heated to a specified temperature (25 °C, 40 °C, 60 °C, 80 °C, 100 °C for Pt/SMO and 25 °C, 100 °C, 120 °C, 140 °C, 160 °C for Pt/Al<sub>2</sub>O<sub>3</sub>) by 30 ml/min of N<sub>2</sub>. For the CO adsorption at the specified temperature, continuous 15 ml/min of 1% vol. CO and 15 ml/min N<sub>2</sub> were introduced to the DRIFTS cell for 30 min, and then the spectra were collected. Similarly, the collection of spectra for CO oxidation were carried out after introducing continuous 15 ml/min of 1% vol. CO and 15 ml/min of 2% vol. O<sub>2</sub> to the DRIFTS cell

for 30 min. Then, 30 ml/min of N<sub>2</sub> was introduced for 30 min to purge the reaction gas before the next heating process.

The isotope-labelling experiments were carried out by VDSorb-91x chemisorption analyzer. For temperature programmed isotope exchange (TPIE) experiment, 25 mg of Pt/SMO loaded into the U-type quartz tube reactor was pretreated by 50 ml/min of 1% <sup>18</sup>O<sub>2</sub> (balanced by He) at 400 °C for 60 min. Then the signals of m/e = 34 and 36 (<sup>16</sup>O<sup>18</sup>O and <sup>18</sup>O<sub>2</sub>) were monitored by the AMETEK® quadrupole mass spectrometer (QMS) from room temperature to 600 °C with the continuous 50 ml/min of 1% <sup>16</sup>O<sub>2</sub> (balanced by He). For the isothermal CO oxidation, 25 mg of Pt/SMO was firstly pretreated by 50 ml/min of 1% <sup>16</sup>O<sub>2</sub>, and then the sample was cooled to 80 °C with He. Subsequently, 50 ml/min of 1% <sup>18</sup>O<sub>2</sub> and 0.5% C<sup>16</sup>O (balanced by He) were introduced to the reactor and the signals of m/e = 28, 44, 46 and 48 (C<sup>16</sup>O, C<sup>16</sup>O<sub>2</sub>, C<sup>16</sup>O<sup>18</sup>O and C<sup>18</sup>O<sub>2</sub>) were monitored by QMS.

*Activity evaluation.* The catalytic activity of catalysts for CO oxidation was also evaluated by VDSorb-91x chemisorption analyzer. 50 mg of catalysts were loaded into the U-type quartz tube reactor. 100 mL/min of feed gas consisted by 1% vol. CO, 10% vol. O<sub>2</sub> and N<sub>2</sub> flowed through the reactor for catalytic reaction tests, which was corresponding to the space velocity of 120000 mL (g<sup>-1</sup> h<sup>-1</sup>). The reactor was heated from room temperature to 200 °C with the rate of 2 °C/min. The partial pressures of CO and CO<sub>2</sub> in the tail gas were monitored by the *in situ* HPR-20 mass spectrometer. The CO conversion (X<sub>CO</sub>) was calculated by:

$$X_{\text{CO}} = \frac{p_{\text{CO}_2}^{\text{T}} - p_{\text{CO}_2}^{\text{start}}}{p_{\text{CO}_2}^{\text{end}} - p_{\text{CO}_2}^{\text{start}}} \times 100\% \quad (1)$$

where  $p_{\text{CO}_2}^{\text{start}}$ ,  $p_{\text{CO}_2}^{\text{end}}$  and  $p_{\text{CO}_2}^{\text{T}}$  are the partial pressure of CO<sub>2</sub> in the tail gas before CO oxidation, after the total conversion of CO and at a reaction temperature (T), respectively, which had been calibrated by the portable emission analyzer (MEXA-584L, Horiba). The turn-over frequency (TOF) of the catalysts at a reaction temperature was calculated by:

$$\text{TOF} = \frac{\frac{P \times V}{R \times T} \times w_{\text{CO}} \times X_{\text{CO}}}{n_{\text{Pt}} \times w_{\text{surf}}} \quad (2)$$

where P, V and R were the pressure of feed gas, the flow rate of feed gas and universal gas constant, which were equal to 101325 Pa, 1.67\*10<sup>-6</sup> m<sup>3</sup>/s and 8.134 J mol<sup>-1</sup> s<sup>-1</sup>, respectively.  $w_{\text{CO}}$  and  $X_{\text{CO}}$  were the vol. percentage (1%) of CO and the CO conversion at the temperature (T).  $n_{\text{Pt}}$  was the mass of Pt nanoparticles in mole, which was calculated by the mass loading of Pt.  $w_{\text{surf}}$  was the percentage of surface Pt atoms compared with the total Pt atoms, which was estimated by the average size of Pt clusters.[5] The detailed data had been summarized in Table S1. In order to eliminate the thermal and diffusion effects, the kinetics tests were performed with CO conversion less than 15 % at the reaction temperature by decreasing the mass of catalysts. The activation energies ( $E_a$ ) of catalysts were calculated according to the slope of the Arrhenius plots. During the reaction orders tests, the feed gas was changed to 0.25~1.0% vol. CO and 2.5~10% vol. O<sub>2</sub> balanced by N<sub>2</sub> with a fixed space velocity of 120000 mL (g<sup>-1</sup> h<sup>-1</sup>).

*Density functional theory calculations.* All spin-polarized density functional theory (DFT) calculations were carried out by using the Vienna Ab initio Simulation Package (VASP).[6,7,8] The antiferromagnetic state was chosen as the ground state of SMO with the optimized lattice constants of  $2a = 1.464$  nm,  $b = 0.859$  nm,  $c = 0.568$  nm, which were consistent with previous experimental and theoretical studies.[9,10] The exchange and correlation energy was described by Perdew-Burke-Ernzerhof (PBE)[11] functional and the ionic cores were treated by projector augmented wave (PAW)[12] method. The energy cutoff of plane wave basis was set to 400 eV. The atomic structural optimization was not converged until the Hellmann-Feynman force on each atom is smaller than 0.05 eV/Å. The Monkhorst-Pack[13]  $k$ -mesh was set to  $3 \times 5 \times 7$  for the structure optimization of a  $2 \times 1 \times 1$  SMO supercell. The SMO (010) slab with the thickness of about 10 Å was used to simulated the SMO oxide supports. The thickness of vacuum layer was set to 15 Å to avoid the interactions between two periodic slabs. The  $k$ -mesh was set to  $2 \times 2 \times 1$  and the energy

difference for total energy was smaller than 5 meV for a finer k-mesh. The minimum energy paths of O<sub>2</sub> dissociation and CO<sub>2</sub> formation steps were calculated by using the climbing image nudged elastic band (CI-NEB)[14] method. During the CI-NEB calculations, six intermediate images were used to make sure the accuracy of results.

Figures S1-S17

Fig. S1

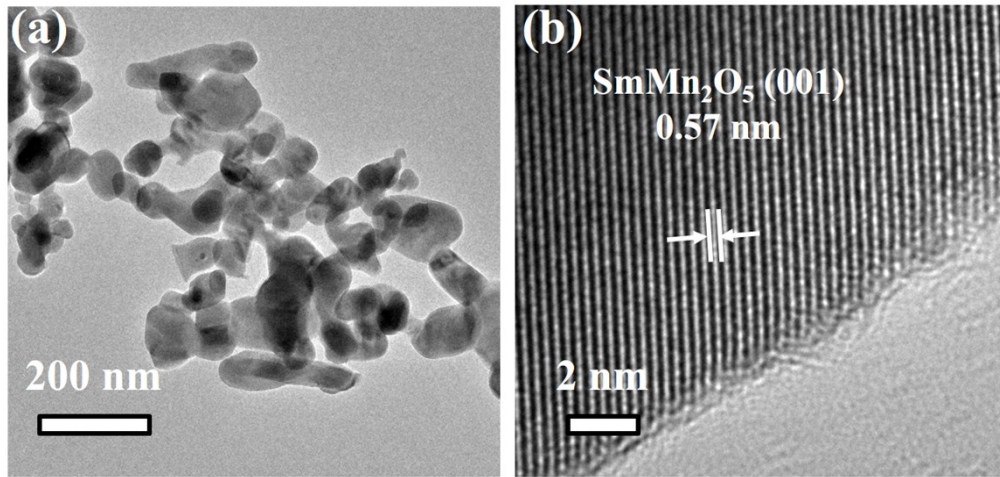
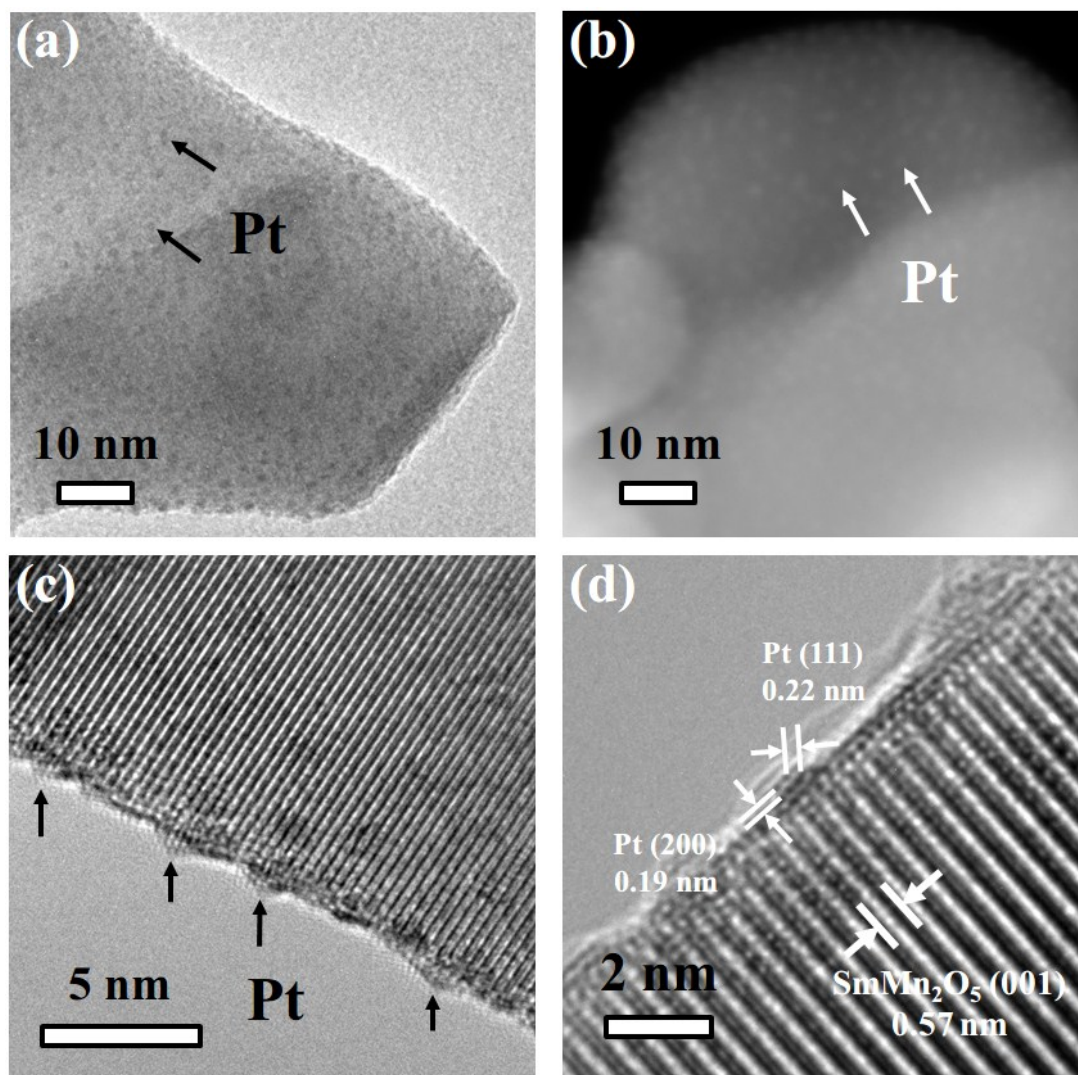


Fig. S1 The TEM images of SMO oxide supports prepared by coprecipitation method.

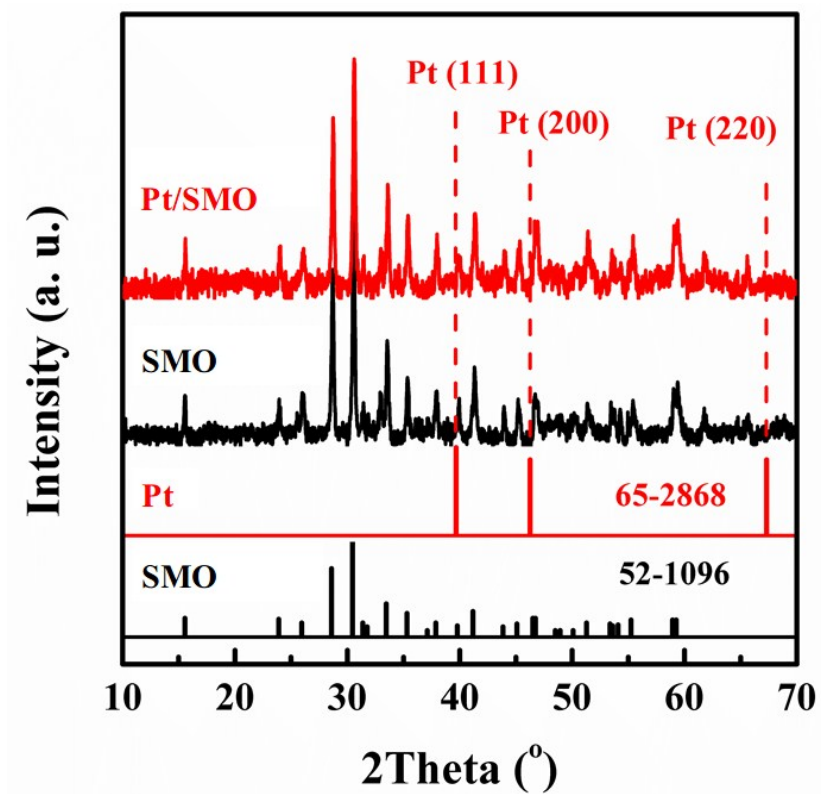
**Fig. S2**



**Fig. S2** (a) TEM and (b) high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) images of Pt/SMO. (c) and (d) are the high resolution TEM images of Pt/SMO, which focus on the Pt clusters at the edge of SMO oxide supports.

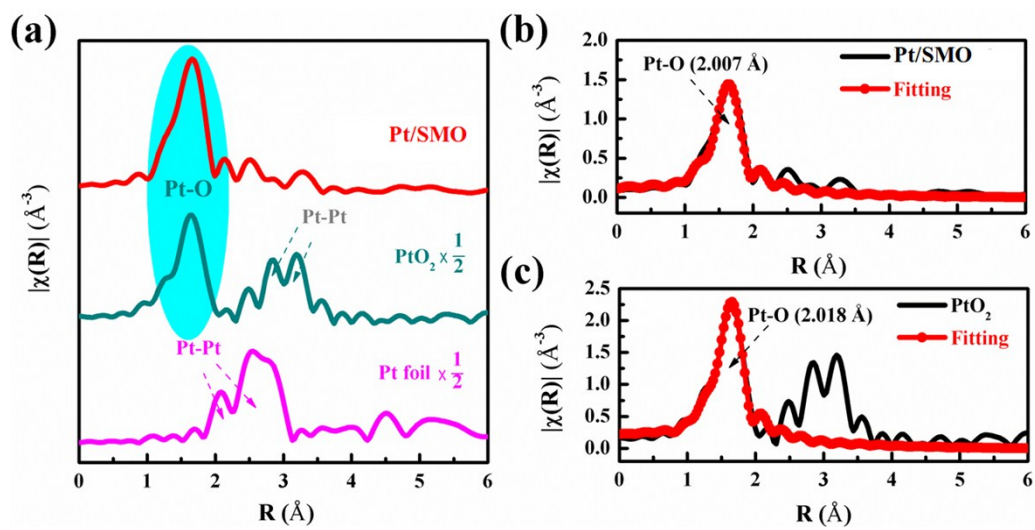


Fig. S3



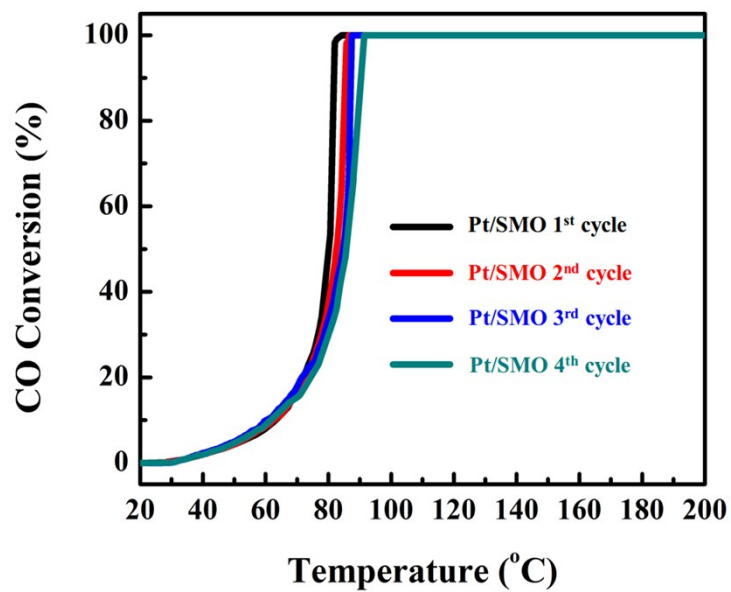
**Fig. S3** The XRD patterns of SMO and Pt/SMO. It is difficult to observe Pt's diffraction peaks for Pt/SMO catalyst, which may be due to the high dispersion and small size of Pt clusters.

**Fig. S4**



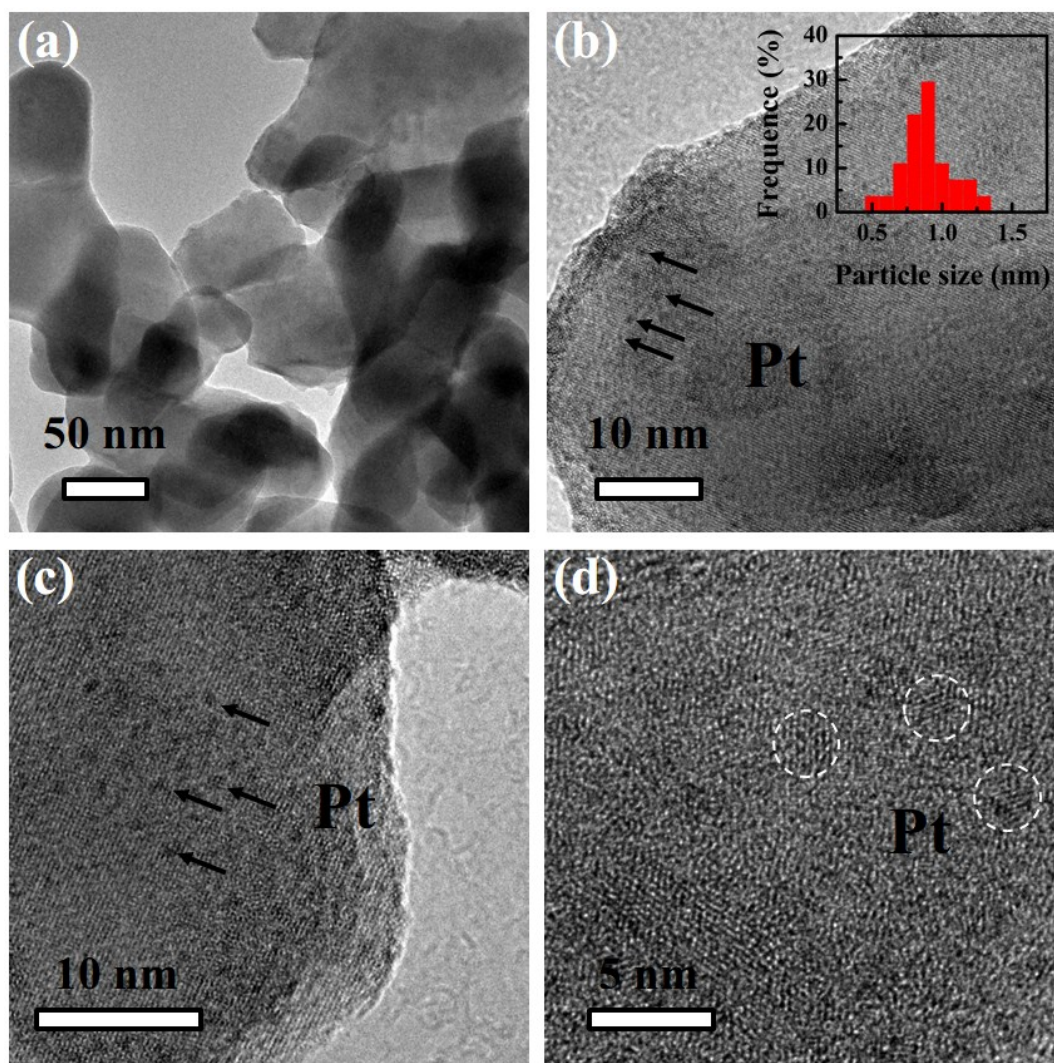
**Fig. S4** (a) The Fourier transformed EXAFS spectra of Pt/SMO, PtO<sub>2</sub> and Pt foil. The fitting with Pt-O bond of Fourier transformed EXAFS spectra of (b) Pt/SMO and (c) PtO<sub>2</sub>. The detailed fitting parameters have been listed in Table S2.

**Fig. S5**



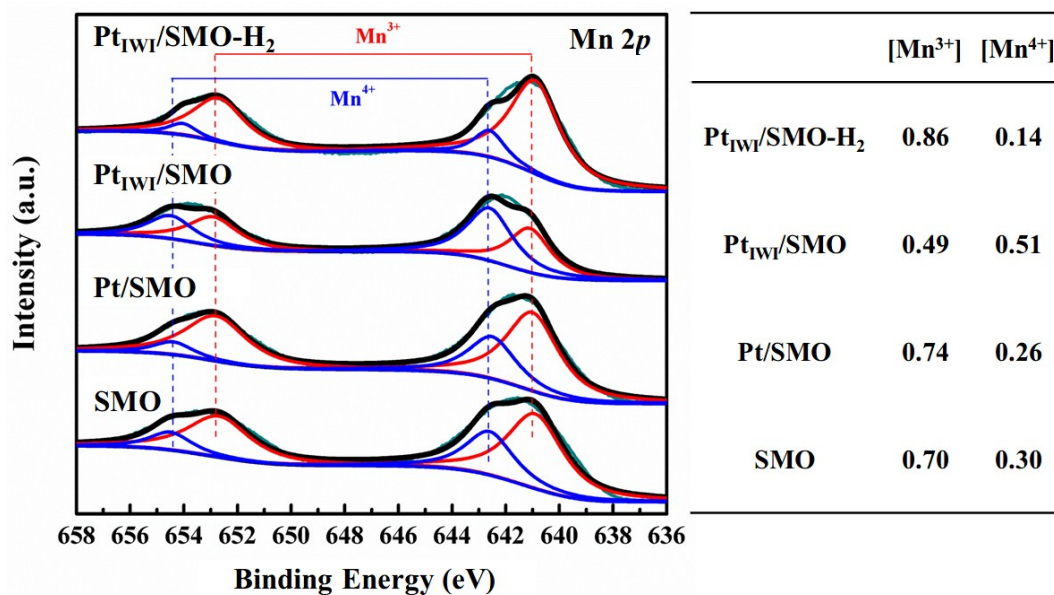
**Fig. S5** CO conversion curves of Pt/SMO catalyst for four cycles. The changes of  $T_{50s}$  for the four curves are less than 5 °C, which can indicate the structural stability of Pt/SMO during the activity test.

**Fig. S6**



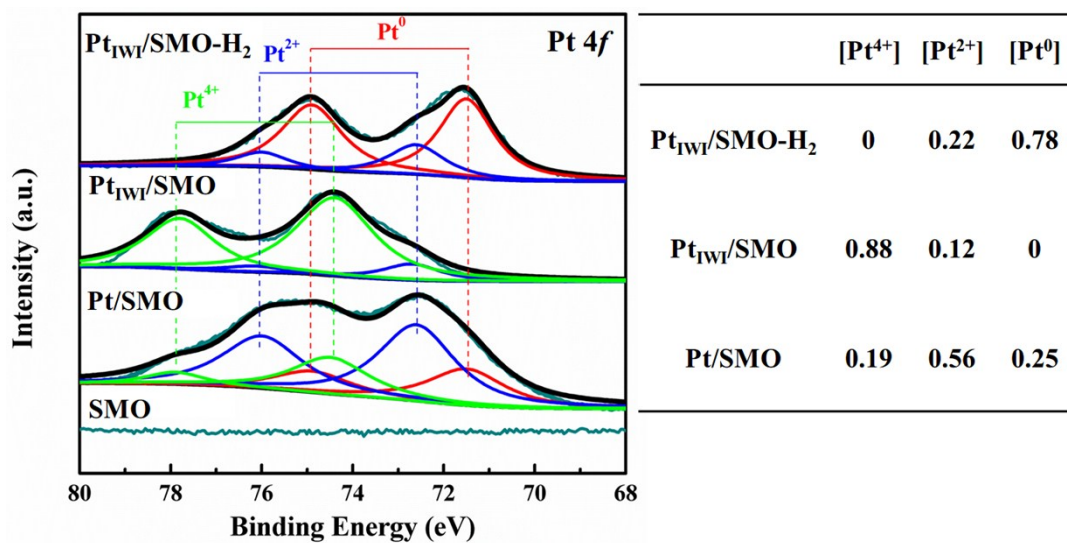
**Fig. S6** The TEM images of Pt<sub>TWI</sub>/SMO prepared by incipient wetness impregnation method. It is difficult to observe the Pt clusters at the edge of SMO supports and the interface structure between Pt clusters and SMO supports cannot be well controlled. The undulating edge of SMO supports may imply the change of surface structures in the preparation process of supported Pt clusters, which can be further demonstrated by the XPS results in Fig. S7.

Fig. S7



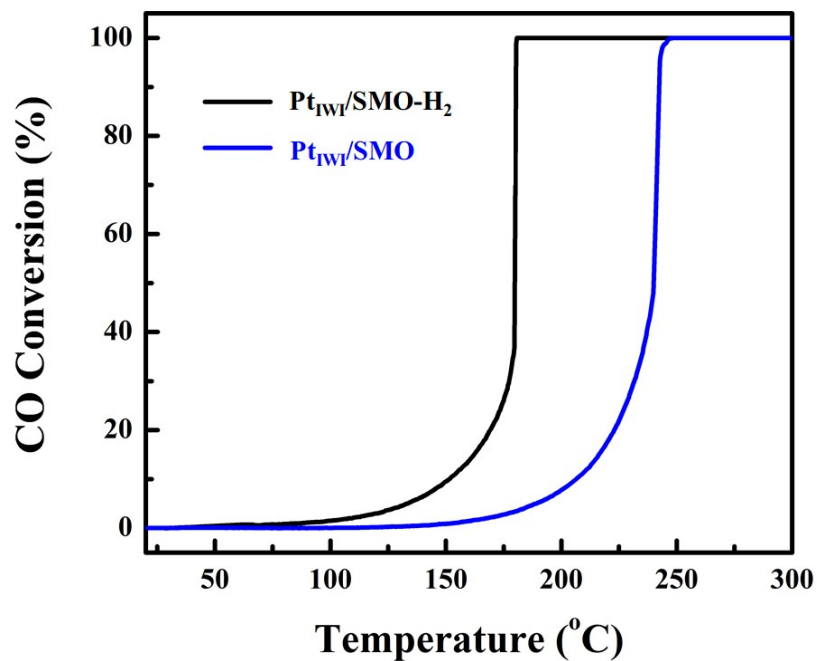
**Fig. S7** Mn 2p XPS spectra of SMO, Pt/SMO, Pt<sub>IWI</sub>/SMO and Pt<sub>IWI</sub>/SMO after H<sub>2</sub> reduction (Pt<sub>IWI</sub>/SMO-H<sub>2</sub>). The H<sub>2</sub> reduction treatment is performed at 300 °C for 1 h using 10 vol. % H<sub>2</sub> balanced by Ar. The concentrations of Mn<sup>3+</sup> and Mn<sup>4+</sup> are calculated by the integrated areas of their corresponding peaks. After Pt clusters are deposited on SMO by ALD method, there is only slight change of the concentrations of Mn<sup>3+</sup> and Mn<sup>4+</sup> ([Mn<sup>3+</sup>] and [Mn<sup>4+</sup>]). However, the incipient wet-impregnation method can cause significant changes of [Mn<sup>3+</sup>] and [Mn<sup>4+</sup>], which can indicate the surface structure's change of SMO supports.

**Fig. S8**



**Fig. S8** Pt 4f XPS spectra of SMO, Pt/SMO, Pt<sub>IWI</sub>/SMO and Pt<sub>IWI</sub>/SMO-H<sub>2</sub>. The concentrations of Pt<sup>4+</sup>, Pt<sup>2+</sup> and Pt<sup>0</sup> have been listed in the right table. It is obviously that H<sub>2</sub> reduction treatment can yield more Pt<sup>2+</sup> and Pt<sup>0</sup> states for Pt<sub>IWI</sub>/SMO catalyst.

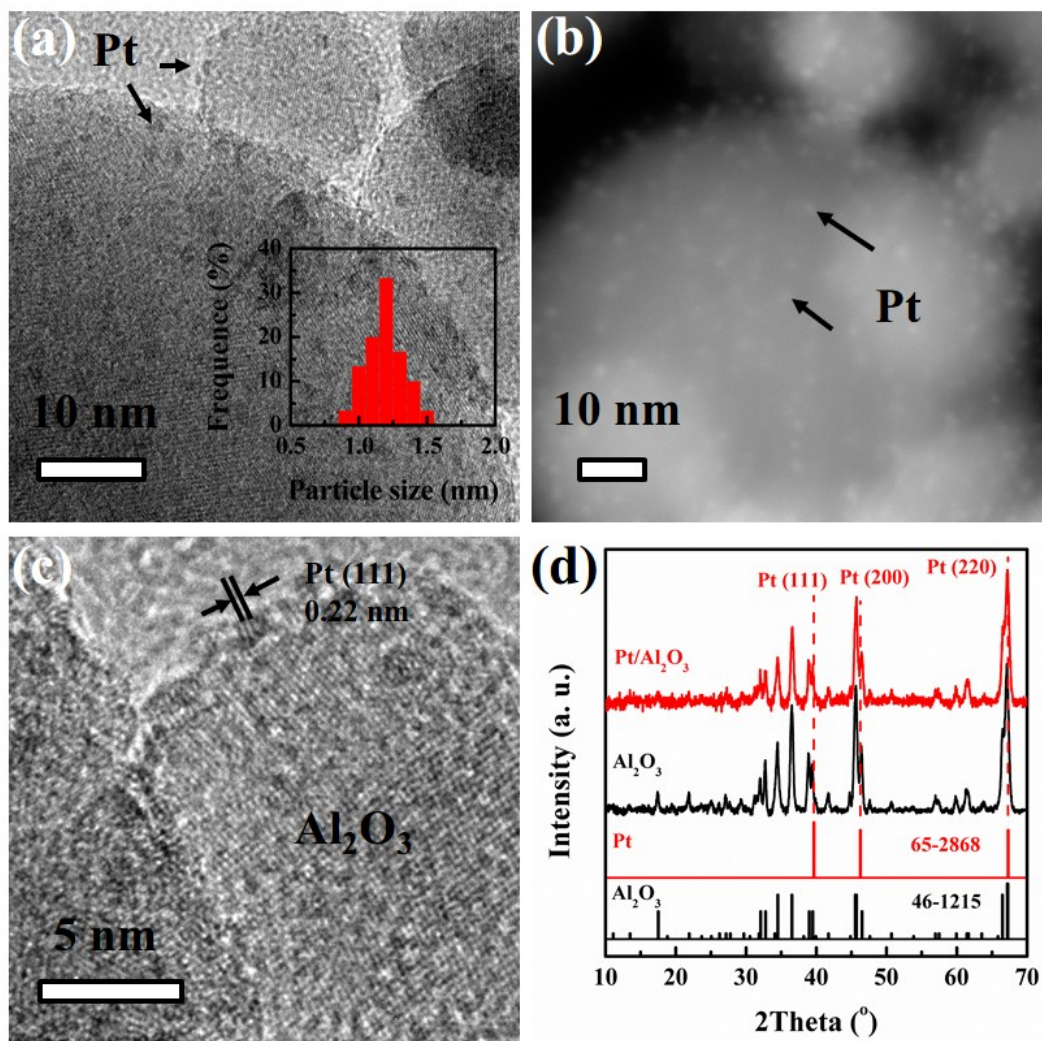
**Fig. S9**



**Fig. S9** The CO conversion curves of Pt<sub>1W1</sub>/SMO-H<sub>2</sub> and Pt<sub>1W1</sub>/SMO. The results show that the activity of Pt<sub>1W1</sub>/SMO can be enhanced after H<sub>2</sub> reduction treatment, which may due to the change of Pt clusters' chemical states. However, the T<sub>50</sub> of Pt<sub>1W1</sub>/SMO-H<sub>2</sub> is 180 °C, which is still much higher than that of Pt/SMO.



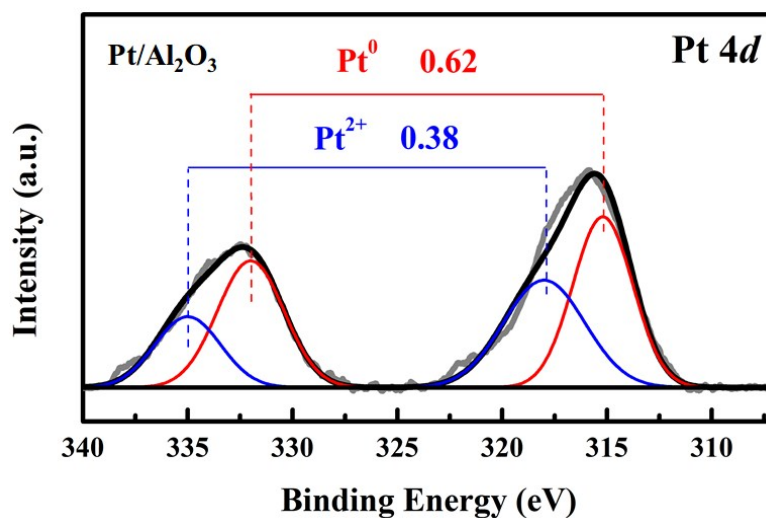
Fig. S10



**Fig. S10** (a) TEM, (b) HAADF-STEM and (c) high resolution TEM images of Pt/Al<sub>2</sub>O<sub>3</sub>. The inserted figure in (a) shows the size distribution of Pt clusters on Al<sub>2</sub>O<sub>3</sub> supports. (d) The XRD patterns of Al<sub>2</sub>O<sub>3</sub> supports and Pt/Al<sub>2</sub>O<sub>3</sub>.

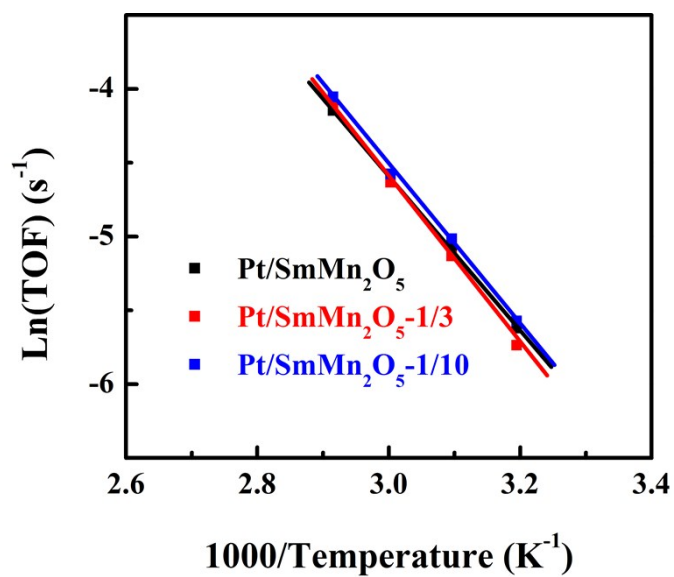


Fig. S11



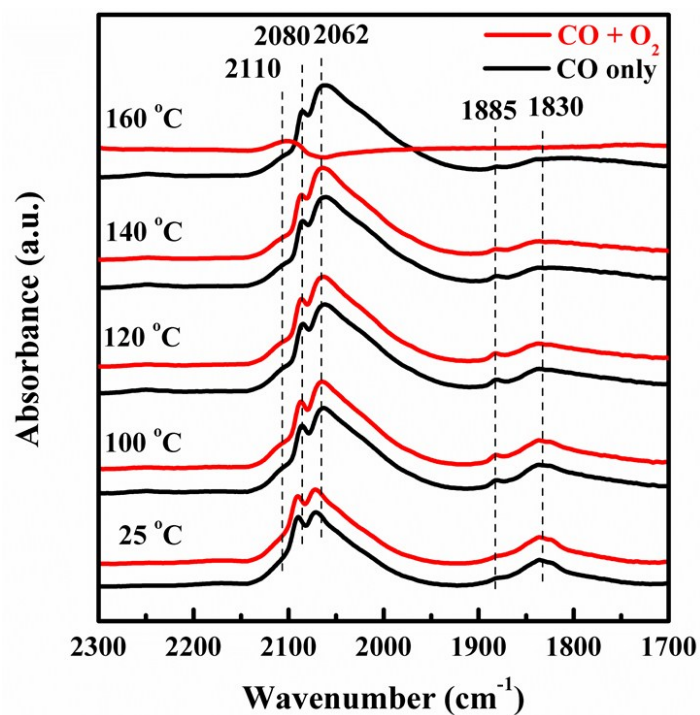
**Fig. S11** The Pt 4d XPS spectrum of Pt/Al<sub>2</sub>O<sub>3</sub> are tested due to the mutual interference between Pt 4f and Al 2p spectra. The labelled concentrations of Pt<sup>0</sup> (0.62) and Pt<sup>2+</sup> (0.38) indicate that Al<sub>2</sub>O<sub>3</sub> supported Pt clusters are mainly in metallic Pt state, which can imply the weak metal-support interaction.

**Fig. S12**



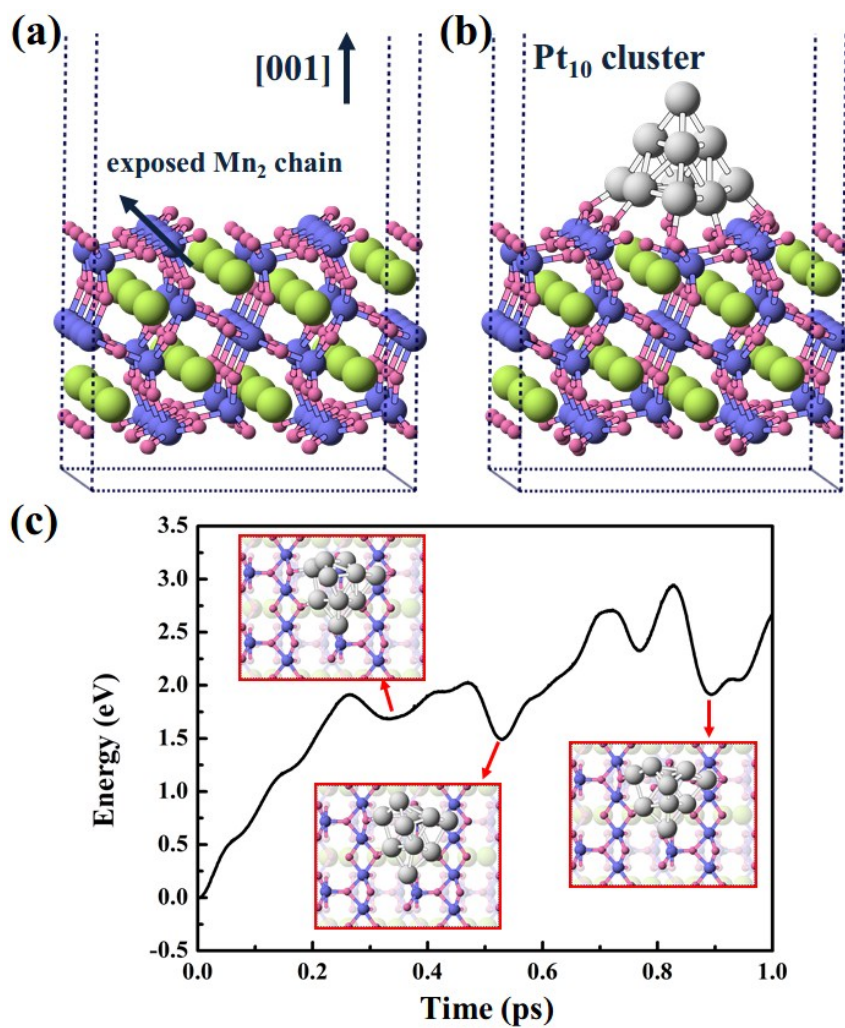
**Fig. S12** The CO oxidation rates of catalysts. The pure catalyst (Pt/SmMn<sub>2</sub>O<sub>5</sub>) or diluted with inert quartz sand have been tested. Two different mass ratios between catalyst and quartz sand have been used, which are 1:3 and 1:10 (labeled as Pt/SmMn<sub>2</sub>O<sub>5</sub>-1/3 and Pt/SmMn<sub>2</sub>O<sub>5</sub>-1/10).

Fig. S13



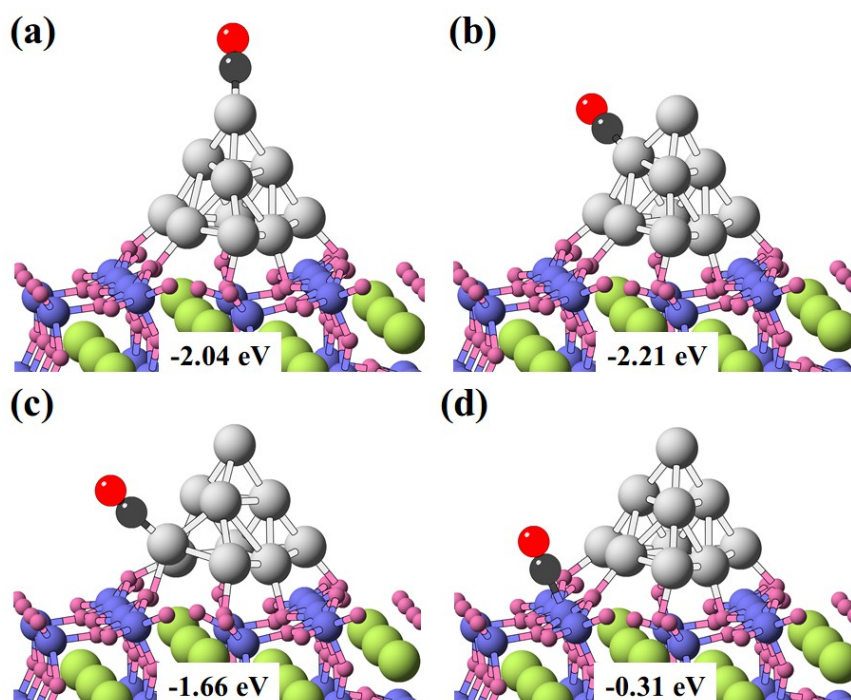
**Fig. S13** The *in situ* DRIFTS spectra of CO adsorption (black lines) on Pt/Al<sub>2</sub>O<sub>3</sub> catalyst at different reaction temperature. The red lines are recorded after the reaction feed gas (1% vol. CO and 2% vol. O<sub>2</sub>) introduced into the DRIFTS cell. The peaks at 1830 cm<sup>-1</sup> (1885 cm<sup>-1</sup>), 2062 cm<sup>-1</sup> (2080 cm<sup>-1</sup>) and 2110 cm<sup>-1</sup> are assigned to the CO molecules adsorbed at the bridge sites, the a-top sites, and the Pt ions or single atoms, respectively.

Fig. S14



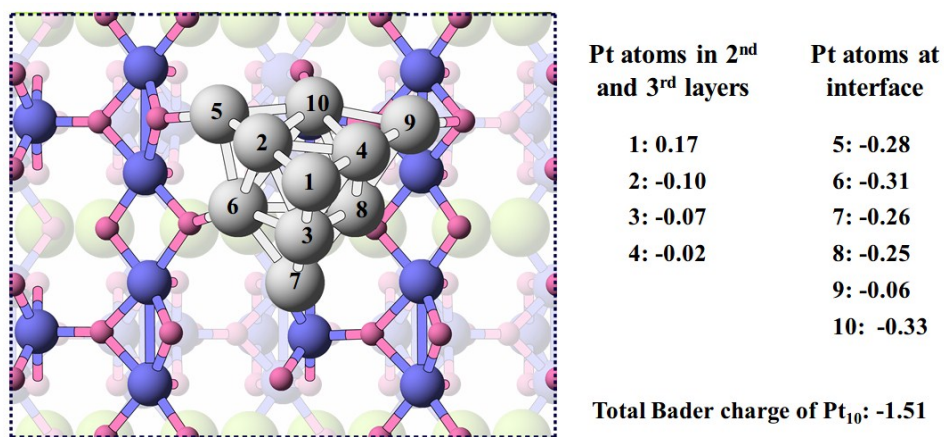
**Fig. S14** The atomic structures of (a) SMO (010) slab and (b) Pt<sub>10</sub>/SMO. The green, blue, pink and grey spheres represent Sm, Mn, O and Pt atoms, respectively. (c) is the total energy of Pt<sub>10</sub>/SMO as a function of simulation time during the first-principle molecular dynamic simulations at 973 K. The inserted figures are the snapshots of Pt<sub>10</sub>/SMO with the local minimum total energies, which indicate the structural stability of supported Pt<sub>10</sub> cluster.

**Fig. S15**



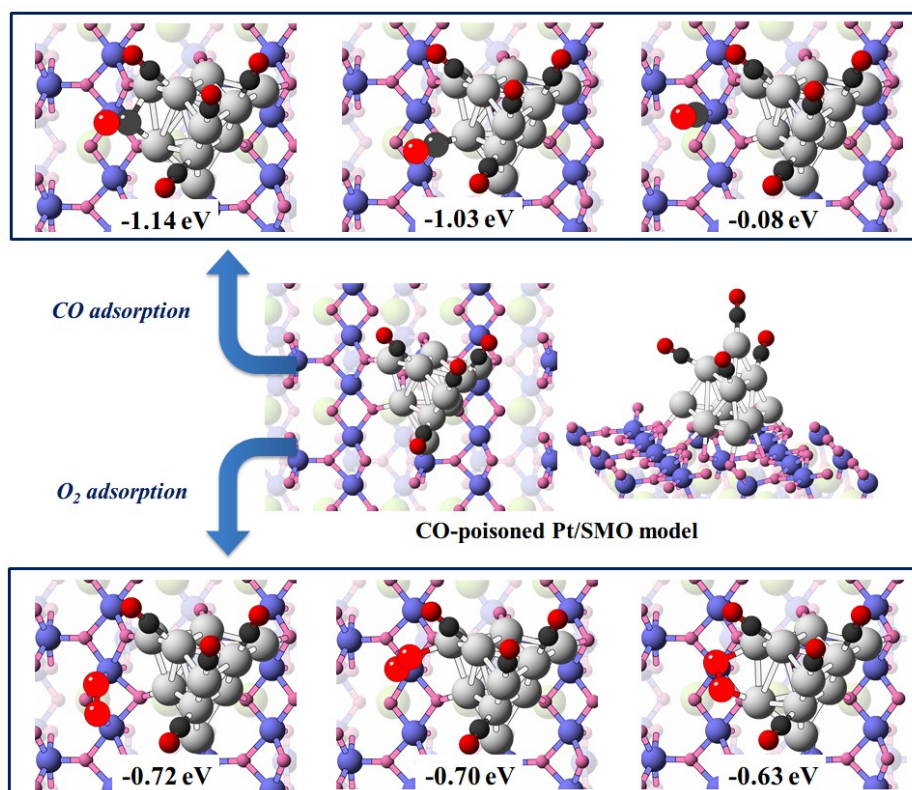
**Fig. S15** The atomic structures of CO adsorption on Pt<sub>10</sub>/SMO. The corresponding CO adsorption energies ( $E_{\text{CO}}^{\text{ads}}$ ) are labelled.  $E_{\text{CO}}^{\text{ads}}$  is calculated by  $E_{\text{CO}}^{\text{ads}} = E_{\text{slab+CO}} - E_{\text{slab}} - E_{\text{CO}}$ , where  $E_{\text{slab+CO}}$ ,  $E_{\text{slab}}$  and  $E_{\text{CO}}$  are the total energies of Pt<sub>10</sub>/SMO with adsorbed CO, pure Pt<sub>10</sub>/SMO and isolated CO molecule, respectively. The results indicate that CO molecules tend to poison the Pt atoms far away from the interface with  $E_{\text{CO}}^{\text{ads}}$  smaller than -2 eV.

**Fig. S16**



**Fig. S16** The Bader charge[15] analysis of Pt<sub>10</sub>/SMO. The result shows that the supported Pt<sub>10</sub> cluster quantitatively donates in total 1.51e to the SMO slab, which are mostly from the Pt atoms at the interface.

**Fig. S17**



**Fig. S17** Top view and side view of CO-poisoned Pt/SMO model. The atomic structures of CO and O<sub>2</sub> adsorption at the interface are presented, which are labelled by the corresponding adsorption energies. The results indicate that CO molecule prefers to bridged adsorb on Pt atoms at the interface (-1.14 eV), while O<sub>2</sub> molecule tends to adsorb on the Mn<sub>2</sub> dimer with the adsorption energy ( $E_{\text{O}_2}^{\text{ads}}$ ) of -0.72 eV.  $E_{\text{O}_2}^{\text{ads}}$  is calculated by  $E_{\text{O}_2}^{\text{ads}} = E_{\text{slab+O}_2} - E_{\text{slab}} - E_{\text{O}_2}$ , where  $E_{\text{slab+O}_2}$ ,  $E_{\text{slab}}$  and  $E_{\text{O}_2}$  are the total energies of slab with adsorbed O<sub>2</sub>, pure slab and isolated O<sub>2</sub> molecule, respectively.

**Table S1**

**Table S1.** Lists of the reaction temperature (T, K), CO conversion ( $X_{CO}$ ), contents of Pt in mole ( $n_{Pt}$ ,  $10^{-6}$  mol), average size of Pt clusters ( $d_{Pt}$ , nm), surface Pt atoms percentage ( $w_{surf}$ ), turn over frequency (TOF,  $10^{-2}$  s $^{-1}$ ) and activation energy ( $E_a$ , kJ/mol).

Catalysts	T (K)	$X_{CO}$ (%)	$n_{Pt}$ ( $10^{-6}$ mol)	$d_{Pt}$ (nm)	$w_{surf}$	TOF ( $10^{-2}$ s $^{-1}$ )	$E_a$ (kJ/mol)
Pt/SMO	313	2.38	4.74	0.75	0.92	0.36	43.87
	323	4.20				0.62	
	333	6.95				0.99	
	343	11.40				1.58	
Pt <sub>TWI</sub> /SMO	433	2.23	3.41	0.89	0.88	0.35	68.21
	453	3.42				0.52	
	463	5.21				0.78	
	473	7.71				1.13	
Pt/Al <sub>2</sub> O <sub>3</sub>	373	0.64	3.15	1.19	0.51	0.22	94.58
	383	1.60				0.37	
	393	3.50				1.15	
	403	6.70				2.15	



**Table S2**

**Table S2.** Structural information and fitting parameters obtained from Pt L<sub>III</sub>-edge EXAFS of Pt/SMO and PtO<sub>2</sub>. The fitting results of PtO<sub>2</sub> references agree well with the previous studies.[16,17]

sample	shell	N	R (Å)	$\sigma^2$ (Å <sup>2</sup> )	$\Delta E_0$ (eV)
Pt/SMO	Pt-O	3.51 ± 0.52	2.007 ±	0.0016 ±	11.98 ±
			0.014	0.0018	1.78
PtO <sub>2</sub>	Pt-O	6	2.018 ±	0.0023 ±	10.24 ±
			0.008	0.0009	1.02

**Table S3**

**Table S3.** Comparing the Pt mass loading (wt%), gas hourly space velocity (GHSV, mL g<sup>-1</sup> h<sup>-1</sup>), 50% CO conversion temperature (T<sub>50</sub>, °C), turn over frequency (TOF, s<sup>-1</sup>) and activation energy (E<sub>a</sub>, kJ/mol) of our reported catalysts to that in previous studies. Note that the listed TOF is tested under the temperature in parentheses.

catalysts	Loading (wt%)	GHSV (mL g <sup>-1</sup> h <sup>-1</sup> )	T <sub>50</sub> (°C)	TOF (s <sup>-1</sup> )	E <sub>a</sub> (kJ/mol)	Ref.
Pt/SMO	1.85	120000	86	0.033 (90)	43.87	This work
Pt/Al <sub>2</sub> O <sub>3</sub>	1.23	120000	157	<0.001 (90)	94.58	This work
Pt <sub>1W1</sub> /SMO	1.33	120000	240	0.011 (200)	68.21	This work
Pt/Al <sub>2</sub> O <sub>3</sub>	1.0	18837	176	0.014 (200)	/	[17]
Pt/Al <sub>2</sub> O <sub>3</sub>	10	60000	177	/	/	[18]
Pt/Al <sub>2</sub> O <sub>3</sub>	1.5	15000	/	0.034 (130)	115.5	[19]
Pt/TiO <sub>2</sub>	1.0	20400	61	0.002 (27)	49	[20]
Pt/CeO <sub>2</sub>	/	/	/	0.18 (200)	145.2	[21]
Pt/CeO <sub>2</sub>	0.5	/	182	0.60 (200)	63.7	[22]
Pt/Co <sub>3</sub> O <sub>4</sub>	0.38	/	130	443 (200)	52.5	[22]
Pt/MnO <sub>2</sub>	0.5	/	227	0.53 (200)	58.7	[22]
Pt/NiO	0.5	/	187	1.12 (200)	80.3	[22]
Pt/Fe <sub>2</sub> O <sub>3</sub>	0.5	/	207	0.15 (200)	59.6	[22]
Pt/FeOx	1.5	15000	/	0.151(27)	30.4	[19]

**Table S4**

**Table S4.** Comparing the adsorption energies of CO ( $E_{\text{CO}}^{\text{ads}}$ , eV) and O<sub>2</sub> ( $E_{\text{O}_2}^{\text{ads}}$ , eV), as well as the barrier energies of O<sub>2</sub> dissociation ( $E_{\text{O}_2}^{\text{dis}}$ , eV) and CO<sub>2</sub> formation ( $E_{\text{CO}_2}^{\text{form}}$ , eV) of our proposed reaction route at the interface of CO-poisoned Pt<sub>10</sub>/SMO to references.

	$E_{\text{CO}}^{\text{ads}}$ (eV)	$E_{\text{O}_2}^{\text{ads}}$ (eV)	$E_{\text{O}_2}^{\text{dis}}$ (eV)	$E_{\text{CO}_2}^{\text{form}}$ (eV)	Ref.
Pt <sub>10</sub> /SMO	-1.14	-0.46	0.41	0.22	This work
Pt <sub>11</sub> /TiO <sub>2</sub>	-1.39	-1.68	0.52	0.98	Ref. 23
Pt <sub>14</sub> /TiO <sub>2</sub>	-1.80	-1.49	0.64	0.62	Ref. 24
Pt <sub>4</sub> /CeO <sub>2</sub>	-2.02	/	/	/	Ref. 25
Pt <sub>4</sub> /CeO <sub>2</sub>	/	-1.39	1.93	/	Ref. 26
Pt <sub>4</sub> /La <sub>0.625</sub> Sr <sub>0.375</sub> Co <sub>0.25</sub> Fe <sub>0.75</sub> O <sub>3-δ</sub>	/	-1.89	0.53	/	Ref. 27
Pt <sub>10</sub> /Al <sub>2</sub> O <sub>3</sub>	-2.13	-1.60	0.60	0.30	Ref. 28
Isolated Pt <sub>10</sub>	-2.07	-0.81	0.60	0.30	Ref. 28

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