

**Supporting Information for**  
**Recycling Biowaste Shells to Produce 0D/2D Mn-Ca Nanostructure**  
**for Efficient Trace-level Metal Extraction: Confined Growth of**  
**Nanosheets and Well Dispersion of Quantum Dots**

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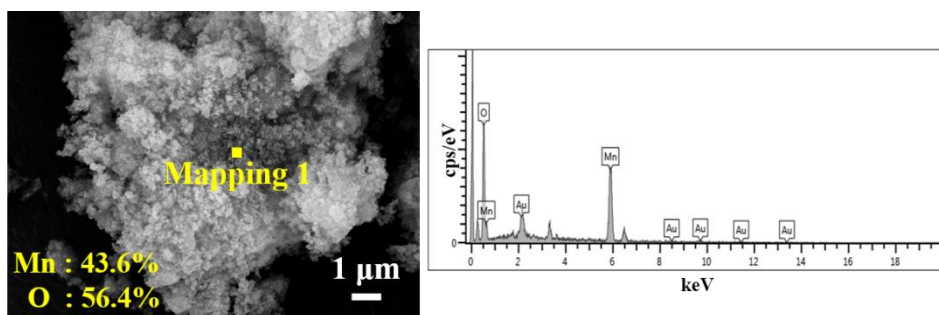
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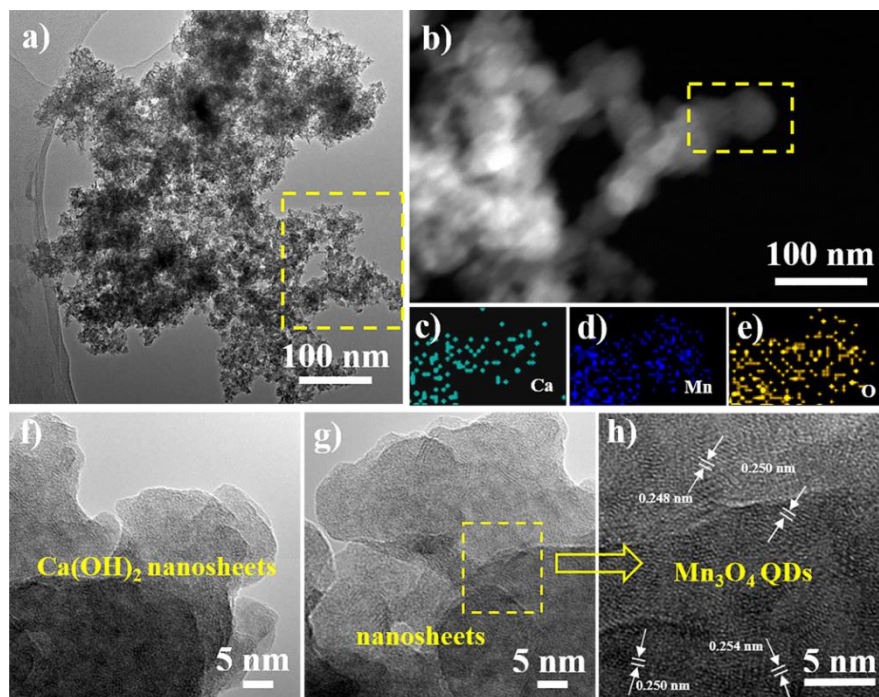
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**Table S1.** Parameters of porous structure of the Mn-Ca composite, CaO in ethanol, CaO in water and Pure  $\text{Mn}_3\text{O}_4$ , respectively.

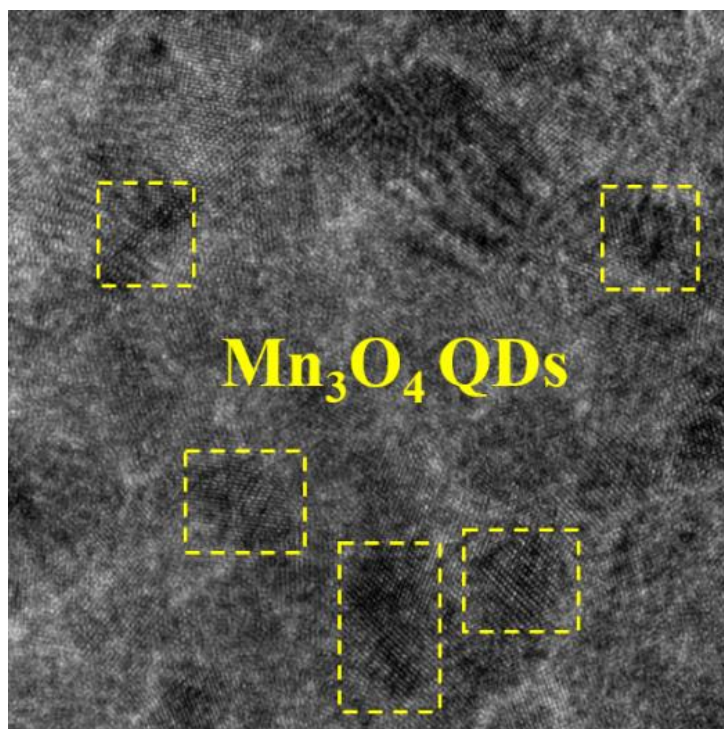
Samples	Specific surface area ( $\text{m}^2\cdot\text{g}^{-1}$ )	Volume of pores ( $\text{cm}^3\cdot\text{g}^{-1}$ )	Average pore size (nm)
Mn-Ca composite	155	0.26	3.21
CaO in ethanol	4.57	0.01	4.82
CaO in water	7.20	0.05	30.6
Pure $\text{Mn}_3\text{O}_4$	92.7	0.48	11.7



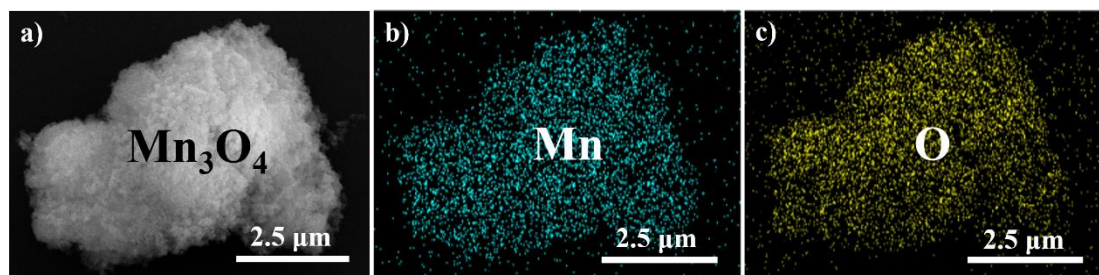
**Figure S1.** Elemental mapping image of  $\text{Mn}_3\text{O}_4$  obtained from acid etching of Mn-Ca composite.



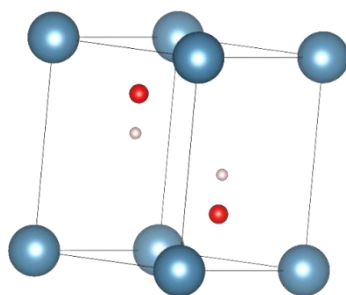
**Figure S2.** (a) TEM image and (f-h) HRTEM images of the Mn-Ca composite. (b-e) HAADF-STEM image and (c-e) elemental mapping images of the Mn-Ca composite.



**Figure S3.** HRTEM image of  $\text{Mn}_3\text{O}_4$  QDs on the Mn-Ca composite.



**Figure S4.** (a) SEM image of pure  $\text{Mn}_3\text{O}_4$  directly synthesized from the redox reaction of  $\text{KMnO}_4$  and  $\text{C}_2\text{H}_5\text{OH}$  without adding  $\text{CaO}$ . (b,c) The corresponding elemental mapping images of Mn and O.



**Figure S5.** The lattice structure of  $\text{Ca}(\text{OH})_2$ .

## I) Adsorption isotherm

Briefly, the Langmuir adsorption equation is expressed as follows<sup>[1]</sup>:

$$Q_e = Q_m \frac{bC_e}{1+bC_e} \quad (S1)$$

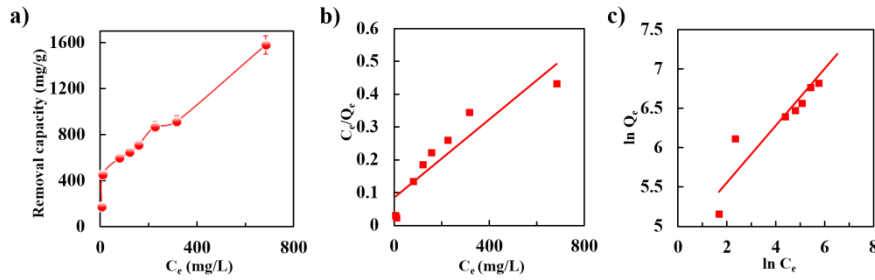
where  $Q_e$  is the amount adsorbed at equilibrium (mg/g) and  $C_e$  is the equilibrium concentration (mg/L).  $Q_m$  is the maximum amount or the saturated adsorption amount (mg/g). The  $b$  is a constant related to the binding strength (L/mg).

The Freundlich adsorption equation is shown as follows<sup>[1]</sup>:

$$Q_e = k C_e^{1/n} \quad (S2)$$

where  $k$  and  $n$  are the Freundlich constants,  $k$  is roughly an indicator of the adsorption capacity (mg/g), and  $1/n$  is an empirical parameter related to the adsorption intensity.

Figure S6 shows the adsorption isotherms of Pb(II) on Mn-Ca, where Langmuir and Freundlich isotherm models have been employed. The parameters of adsorption fitting are given in Table S2.



**Figure S6.** (a) Adsorption isotherm of Mn-Ca for Pb(II) ions (dose: 0.2 g/L, standing, initial concentration: 40-1000 mg/L, initial pH:  $4.5 \pm 0.1$ , temperature: 25 °C); (b) Linear fitting curves with the Langmuir model for Pb(II) ions; (c) Linear fitting curves with the Freundlich model for Pb(II) ions.

**Table S2.** Parameters of two kinetic models for the removal of Pb(II) ions over Mn-Ca.

Fitting model	Adsorption constants	Value
Langmuir	$Q_m$ (mg/g)	1675
	$b$ (L/mg)	0.007
	$R^2$	0.830
Freundlich	$k$ (mg/g)	126.0
	$n$	2.773
	$R^2$	0.869

## II) Adsorption kinetics

Figure S7 shows adsorption kinetic curves of Pb(II) ions over Mn-Ca composite (dose: 0.2 g/L, standing, initial concentration: 40 mg/L, initial pH: 4.5± 0.1, temperature: 25 °C). Two common kinetic models (pseudo first order equation and pseudo second order equation) were used to fit the experimental data.

Briefly, The pseudo first order equation model is shown as follows<sup>[2]</sup>:

$$-\ln(1 - Q_t/Q_e) = k_1 t + C \quad (S3)$$

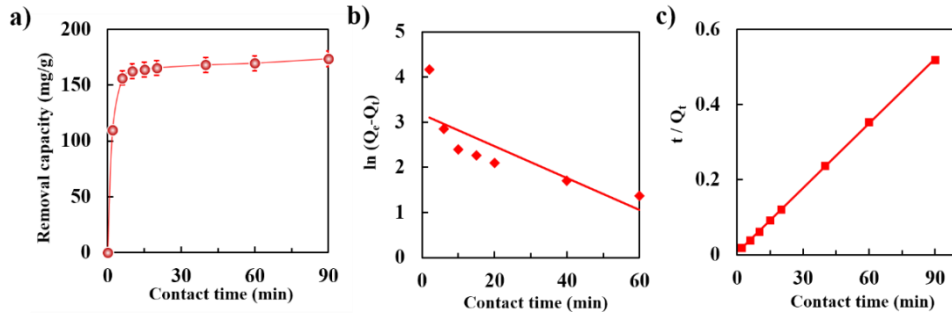
where  $Q_t$  and  $Q_e$  are the amounts of the metal ions adsorbed(mg/g) at equilibrium and  $t$  time (min), and  $k_1$  ( $\text{g mg}^{-1} \text{min}^{-1}$ ) is the adsorption rate constant.

The pseudo second order kinetic model is expressed as<sup>[3]</sup>:

$$\frac{t}{Q_t} = \frac{1}{k_2 Q_e^2} + \left(\frac{1}{Q_e}\right) t \quad (S4)$$

where  $k_2$  ( $\text{g mg}^{-1} \text{min}^{-1}$ ) is the rate constant of the pseudo second order adsorption reaction.

The kinetic parameters were summarized in Table S3, and the fitting curves were shown in Figure S7b-c.



**Figure S7.** (a) Removal of Pb(II) by the Mn-Ca composite (dose: 0.2 g/L, standing, initial concentration: 40 mg/L, initial pH:4.5 ± 0.1, temperature: 25 °C).(b) the pseudo-first-order kinetics and (c) the pseudo-second-order kinetics.

**Table S3.** Parameters of two kinetic models for the removal of Pb(II) ions over Mn-Ca

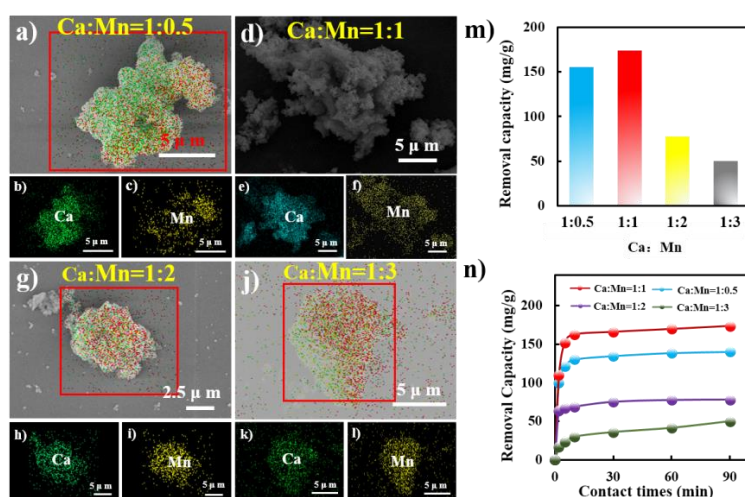
kinetic model	Kinetic constants	Value
pseudo-first-order	$k_1$ ( $\text{min}^{-1}$ )	0.0353
	$Q_e$ (mg/g)	23.9
	$R^2$	0.5905
pseudo-second-order	$k_2$ ( $\text{g mg}^{-1} \text{min}^{-1}$ )	0.005
	$Q_e$ (mg/g)	200.0
	$R^2$	0.9998

### III) Supplemental information on the effect of pH value on Pb(II) adsorption

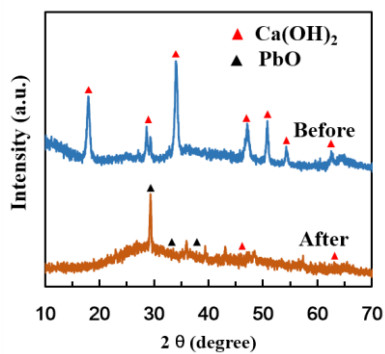
At  $\text{pH} > 7$ , the  $\text{Pb(II)}$  will be partially precipitated. Despite the difficulty in evaluating the concentration of  $\text{Pb(II)}$  extracted by adsorbent (i.e., the value of adsorption capacity), the concentration of residual  $\text{Pb(II)}$  can decrease to a low level (0.36 mg/L) when adding Mn-Ca composite in wastewater. No doubt, the Mn-Ca can efficiently extract the  $\text{Pb(II)}$  from solutions of a broad pH region ( $\text{pH} > 2$ ). In contrast, at  $\text{pH} < 2$ , a reduced adsorption capacity of  $\text{Pb(II)}$  was found. The reason may lie in that, abundant of  $\text{Ca(OH)}_2$  nanosheets will be dissolved and become inactive at acid condition.

### IV) Discussion on the effect of content of $\text{Mn}_3\text{O}_4$ and $\text{Ca(OH)}_2$ on $\text{Pb(II)}$ adsorption

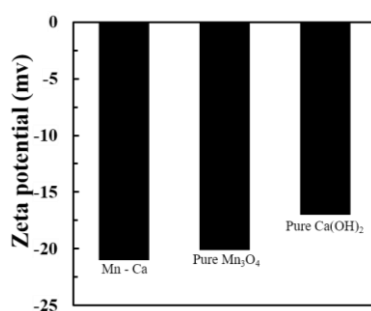
The content of  $\text{Mn}_3\text{O}_4$  and  $\text{Ca(OH)}_2$  in 0D/2D Mn-Ca nanostructure can be tuned, by adjusting the dose of starting precursors (i.e.,  $\text{CaO}$  and  $\text{KMnO}_4$ ). As shown in Figure S8, the sample of  $\text{Mn:Ca}=1:1$  has the highest efficiency. The reasons may lie in that: 1) With higher amount of  $\text{KMnO}_4$ , the  $\text{Mn}_3\text{O}_4$  was the dominant phase in 0D/2D Mn-Ca nanostructure. These  $\text{Mn}_3\text{O}_4$  QDs will be highly aggregated owing to the absence of  $\text{Ca(OH)}_2$ -nanosheets substrate, which results in fast decrease of capacity; 2) With less amount of  $\text{KMnO}_4$ , the hydrolysis and exfoliation of  $\text{CaO}$  could be prohibited due to limited amount of  $\text{H}_2\text{O}$ , which was released from reaction between  $\text{KMnO}_4$  and  $\text{C}_2\text{H}_5\text{OH}$ . Subsequently, it produced few  $\text{Ca(OH)}_2$  nanosheets and showed reduced adsorption capacity.



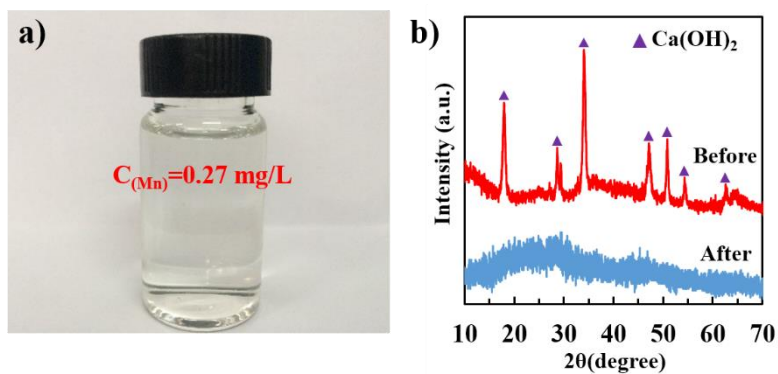
**Figure S8.** SEM images and elemental mapping of samples prepared from different precursors, with  $\text{CaO}$  and  $\text{KMnO}_4$  (denoted as  $\text{Ca:Mn}$ ) ranging from 1:0.5(a-c), 1:1(d-f), 1:2(g-i) to 1:3(j-l), respectively. (m, k) Removal of  $\text{Pb(II)}$  by the  $\text{Ca:Mn}$  ranging from 1:0.5, 1:1, 1:2 to 1:3 (dose: 0.2 g/L, standing, initial concentration: 40 mg/L, initial pH:  $4.5 \pm 0.1$ , temperature:  $25^\circ\text{C}$ ).



**Figure S9.** XRD pattern of the Mn-Ca composite before and after extraction of Pb(II).



**Figure S10.** Zeta potential of pure  $\text{Mn}_3\text{O}_4$ , pure  $\text{Ca}(\text{OH})_2$ , and the Mn-Ca composite.



**Figure S11.** (a) Photograph of the purified solution after removal of Eu(III) by Mn-Ca. (b) XRD pattern of the Mn-Ca composite before and after extraction of Eu(III).

## References:

1. V. Gbb, O. A. Oyetade, S. Rana, B. S. Martincigh, S. B. Jonnalagadda and V. O. Nyamori, *Acs Applied Materials & Interfaces*, 2017, **9**, 17290.
2. X. Li, C. Bian, X. Meng and F. S. Xiao, *Journal of Materials Chemistry A*, 2016, **4**, 5999-6005.
3. D. Chen, W. Shen, S. Wu, C. Chen, X. Luo and L. Guo, *Nanoscale*, 2016, **8**, 7172.